

# Biofilm kinetics IV

# Today's lecture

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- Estimating parameter values
  - Diffusion coefficients,  $D$  and  $D_f$
  - Effective diffusion layer thickness,  $L$
  - Biofilm loss coefficient,  $b'$
- Analyzing performance of an attached growth bioreactor

# Parameters for biofilm analysis

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- Eight variables:  $\hat{q}, K, Y, b', D_f, D, L, S$
- $S$  is given
- $\hat{q}, K, Y, and b$  are obtained from batch experiments

→ Still need to determine  $b_{det}, D_f, D, and L$

# Parameters for biofilm analysis

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You do not have to memorize any equations here. Just understand the concepts and logics and get ready for future uses!!!

# Parameters for biofilm analysis

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## 1. Aqueous diffusion coefficient, $D$

- Depends on size of a molecule
- Molecule size  $\uparrow \rightarrow D \downarrow$
- Look up chemical engineering handbooks
- Some online resources can be useful (ex: SPARC online calculator)

## 2. Diffusion coefficient in the biofilm, $D_f$

- Linear correlation with  $D$
- Smaller than  $D$ : restriction in diffusion (biofilm consists of bacterial cells and slime)
- For small solutes that do not adsorb to the biofilm matrix,  $D_f/D = 0.5-0.8$  (using 0.8 may be appropriate for general cases)
- Adsorption may result in significantly smaller  $D_f$

# Parameters for biofilm analysis

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## 3. Thickness of effective diffusion layer, $L$

- Depends on  $D$  and flow velocity of the bulk liquid,  $u$
- Look up the literature for correlation equations appropriate for your own system
- ex) For biofilm on spherical porous media, following equation may be used:

$$L = \frac{D(Re_m)^{0.75} Sc^{0.67}}{0.57u}$$

$Sc = \mu/\rho D$ , Schmidt number

$Re_m = 2\rho d_p u / (1 - \varepsilon)\mu$ , modified Reynolds number

$\mu$  = absolute viscosity [g/cm/d]

$\varepsilon$  = porosity of medium bed

$\rho$  = water density [g/cm<sup>3</sup>]

$Q$  = volumetric flow rate [cm<sup>3</sup>/d]

$u = Q/A_c$  = superficial flow velocity [cm/d]

$A_c$  = cross-sectional area of the flow stream [cm<sup>2</sup>]

$d_p$  = diameter of solid medium [cm]

# Parameters for biofilm analysis

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## 4. Overall biofilm-loss coefficient, $b'$

- Recall that  $b' = b + b_{det}$
- $b_{det}$  and  $b$  are comparable (both terms should be considered)
- $b_{det}$  depends on the shear stress acting on the biofilm surface
- ex) Rittmann (1982) suggested following equations:

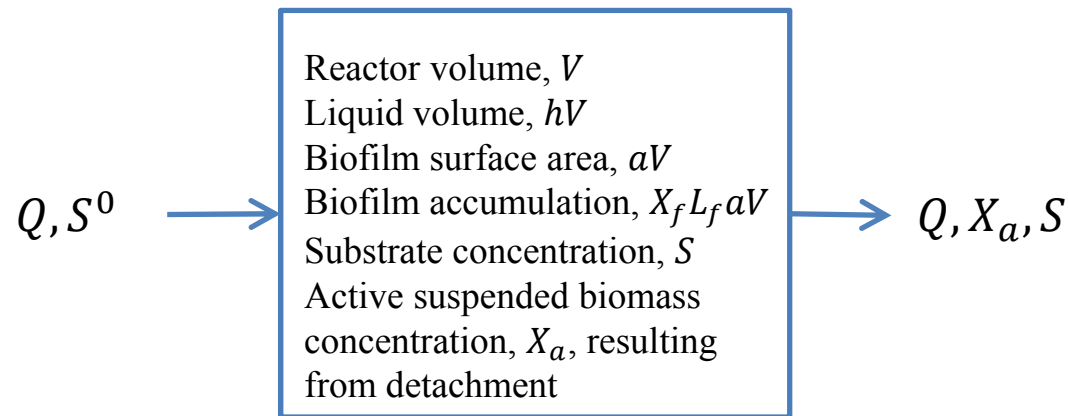
$$b_{det} = 8.42 \times 10^{-2} \cdot \sigma^{0.58} \quad (L_f < 0.003 \text{ cm})$$

$$b_{det} = 8.42 \times 10^{-2} \cdot \left( \frac{\sigma}{1 + 433.2(L_f - 0.003)} \right) \sigma^{0.58}$$
$$(L_f > 0.003 \text{ cm})$$

# Analyzing an attached growth bioreactor

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For simplicity, let's deal with the simplest attached growth bioreactor, a completely mixed biofilm reactor:



$h$  = fraction of water in the reactor

$a = A_{T,biofilm}/V$  = biofilm specific surface area [ $L^{-1}$ ]

$A_{T,biofilm}$  = total biofilm surface area in the reactor [ $L^2$ ]



# Analyzing an attached growth bioreactor

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Steady-state mass balance for substrate

$$0 = QS^0 - QS - J \cdot aV$$

Steady-state mass balance for biofilm's active biomass

$$0 = YJ \cdot aV - b'X_fL_f \cdot aV$$



Calculate  $J$  and  $X_fL_f$ , and get  $S$  (Final target I)

Get biomass production =  $b_{det}X_fL_f \cdot aV$  (Final target II)

# Analyzing an attached growth bioreactor

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## Suspended active biomass in an attached growth bioreactor

- For an attached growth bioreactor, suspended active biomass may not significantly contribute to the degradation of the substrate
- Still, we are interested in suspended active biomass (originates from detachment from the biofilm) because this affects the effluent quality (particulate BOD/COD)

## Steady-state mass balance for suspended active biomass

$$0 = -X_a Q + b_{det} X_f L_f \cdot aV$$



$$X_a = b_{det} X_f L_f \cdot aV / Q$$

# Analyzing an attached growth bioreactor

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**Q:** Calculate the effluent dissolved substrate concentration, biomass production, and total effluent COD in a completely mixed biofilm reactor with an initial substrate concentration of 100 mg/L and reactor configuration parameters as follows:

$$V = 1000 \text{ m}^3, a = 100 \text{ m}^{-1}, Q = 100 \text{ m}^3/\text{d}$$

Apply the parameters given in the last question for the biofilm, plus  $b_{det} = 0.05/\text{d}$ . Assume that substrate and suspended active biomass are the two main contributors of the effluent COD.