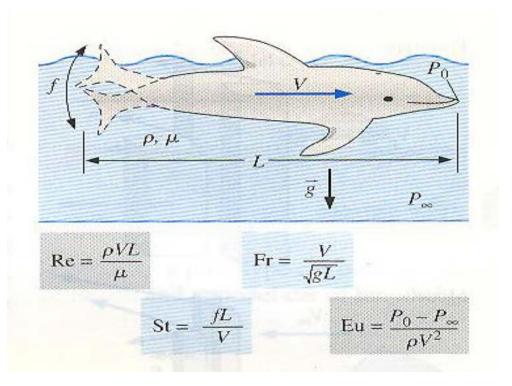


Similitude and Dimensional Analysis



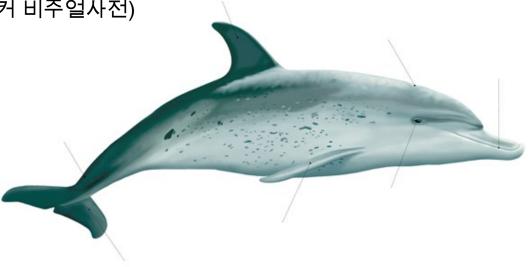




Chapter 8 Similitude and Dimensional Analysis

- ・ 가슴지느러미 (pectoral fin): 헤엄치는 데 사용하는 골질 부속지. 안정감, 방향 감각, 정지, 체 온 조절에 이용된다.
- ・ 등지느러미 (dorsal fin): 헤엄치는 데 사용하는 등 중간의 부속지. 매우 촘촘한 섬유질 조직이 며 안정감과 체온 조절을 담당한다.
- ・ 꼬리지느러미 / 미기 (caudal fin): 힘차게 헤엄치는 데 사용되는 부속지. 단단한 연골로 이루 어진 2개의 엽으로 갈라져 몸체의 뒤쪽 말단부에 수직으로 자리잡고 있으며, 추진 기능이 있다.
 ・ 꼬리 (tail): 돌고래 몸의 말단 부분. 이 꼬리에 의해 수직 동작으로 전진할 수 있다. 척추에 붙 은 강력한 근육으로 꼬리를 움직인다.

[Morphology of a dolphin] (브리태니커 비주얼사전)







Contents

- 8.0 Introduction
- 8.1 Similitude and Physical Models
- 8.2 Dimensional Analysis
- 8.3 Normalization of Equations





Objectives

- Learn how to begin to interpret fluid flows
- Introduce concept of model study for the analysis of the flow phenomena that could not be solved by analytical (theoretical) methods
- Study laws of similitude which provide a basis for interpretation of model results
- Study dimensional analysis to derive equations expressing a physical relationship between quantities

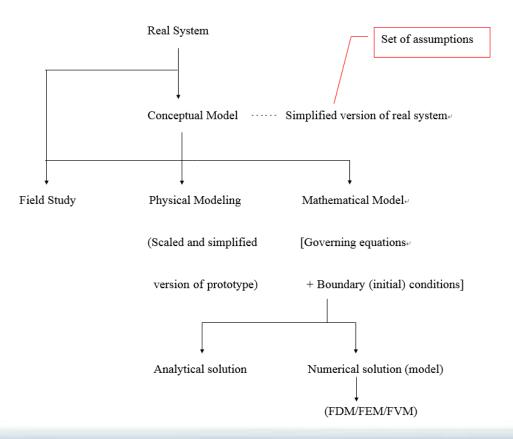




<u>A/79</u>

Why we need to model the real system?

Most real fluid flows are complex and can be solved only approximately.







- Three dilemmas in planning a set of physical or numerical experiments
- Number of possible and relevant <u>variables or physical parameters in</u> real system is huge and so the potential number of experiments is beyond our resources.
- 2) Many real flow situations are either too large or far too small for convenient experiment at their true size. → When testing the real thing (prototype) is not feasible, a physical model (scaled version of the prototype) can be constructed and the performance of the prototype simulated in the physical model.
- 3) The numerical models must be <u>calibrated and verified by use of</u> <u>physical models or measurements</u> in the prototype.





Model study

Physical models have been used for over a hundred years.

Models began to be used to study flow phenomena that could not be solved by analytical (theoretical) methods.

- Laws of similitude
- provide a basis for interpretation of physical and numerical model results and crafting both physical and numerical experiments
- Dimensional analysis
- derive equations expressing a physical relationship between quantities





[Example]

- Civil and environmental engineering: models of hydraulic structures,
- river sections, estuaries and coastal bays and seas
- Mechanical engineering: models of pumps and turbine, automobiles
- Naval architect: ship models
- Aeronautical engineering: model test in wind tunnels
- Justification for models
- 1) Economics: A model, being small compared to the prototype, <u>costs</u> <u>little</u>.
- 2) Practicability: In a model, environmental and flow conditions can be rigorously <u>controlled</u>.





8.0 Introduction



한강(미사리~잠실수중보) 수리모형 (서일원 , 1995)







8.0 Introduction







Similitude of flow phenomena not only occurs between a prototype and its model but also may exist between various natural phenomena.

There are three basic types of similitude; all three must be obtained if complete similarity is to exist between fluid phenomena.

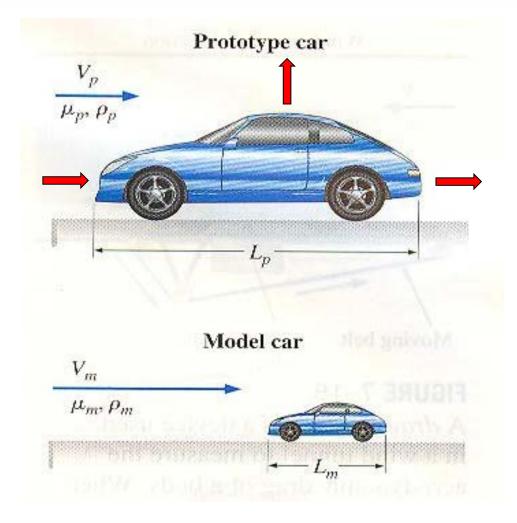
์ Geometrical similarity (기하학적 상사성)

Kinematic similarity (운동학적 상사성)

Dynamic similarity (동력학적 상사성)







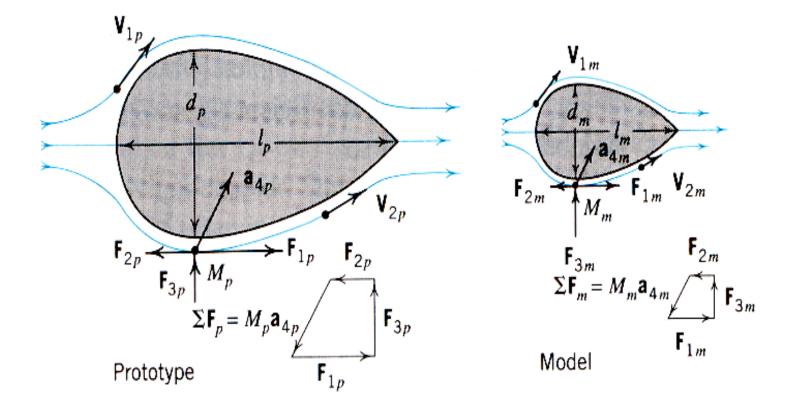




- 1) Geometrical similarity
- ~ Flow field and boundary geometry of model and of the prototype have <u>the same shape</u>.
- \rightarrow The ratios between corresponding lengths in model and prototype are the same.
- [Cf] Distorted model
- ~ not geometrically similar $(l_r > d_r)$
- ~ The flows are not similar and the models have to be calibrated and adjusted to make them perform properly.
- ~ used models of rivers, harbor, estuary
- ~ Numerical models are usually used in their place.











For the characteristic lengths we have

$$d_r = \frac{d_p}{d_m} = \frac{l_p}{l_m} = l_r$$

• Area

$$\frac{A_p}{A_m} = \left(\frac{d_p}{d_m}\right)^2 = \left(\frac{l_p}{l_m}\right)^2$$

Volume

$$\frac{Vol_p}{Vol_m} = \left(\frac{d_p}{d_m}\right)^3 = \left(\frac{l_p}{l_m}\right)^3$$



$$d_r = 50; l_r = 50$$

 $A_r = 50^2; Vol_r = 50^3$

2) Kinematic similarity

In addition to the flowfields having the same shape, the ratios of

corresponding velocities and accelerations must be the same through the flow.

 \rightarrow Flows with geometrically similar streamlines are kinematically similar.

$$V_{r} = \frac{\vec{V}_{1p}}{\vec{V}_{1m}} = \frac{\vec{V}_{2p}}{\vec{V}_{2m}}$$

$$a_r = \frac{\vec{a}_{3p}}{\vec{a}_{3m}} = \frac{\vec{a}_{4p}}{\vec{a}_{4m}}$$

(8.1)





3) Dynamic similarity

In order to maintain the geometric and kinematic similarity between

flowfields, the forces acting on corresponding fluid masses must be related by ratios similar to those for kinematic similarity.

Consider gravity, viscous and pressure forces, and apply Newton's 2nd law

$$F_{r} = \frac{\vec{F}_{1p}}{\vec{F}_{1m}} = \frac{\vec{F}_{2p}}{\vec{F}_{2m}} = \frac{\vec{F}_{3p}}{\vec{F}_{3m}} = \frac{M_{p}\vec{a}_{4p}}{M_{m}\vec{a}_{4m}}$$
(8.2)

Define inertia force as the product of the mass and the acceleration

$$\vec{F}_I = M \vec{a}$$





4) Complete similarity

~ requires simultaneous satisfaction of geometric, kinematic, and dynamic similarity.

 \rightarrow Kinematically similar flows must be geometrically similar.

 \rightarrow If the <u>mass distributions</u> in flows are similar, then kinematic similarity (density ratio for the corresponding fluid mass are the same) guarantees complete similarity from Eq. (8.2).

From Fig. 8.1, it is apparent that

$$\vec{F}_{1p} + \vec{F}_{2p} + \vec{F}_{3p} = M_p \,\vec{a}_{4p} \tag{a}$$
$$\vec{F}_{1m} + \vec{F}_{2m} + \vec{F}_{3m} = M_m \,\vec{a}_{4m} \tag{b}$$





If the ratios between three of the four corresponding terms in Eq.(a) and Eq.(b) are the same, the ratio between the corresponding fourth terms be the same as that the other three. Thus, one of the ratio of Eq.(8.2) is redundant. If the first force ratio is eliminated,

$$\frac{M_{p}\vec{a}_{4p}}{\vec{F}_{2p}} = \frac{M_{m}\vec{a}_{4m}}{\vec{F}_{2m}} \Longrightarrow \left(\frac{F_{I}}{F_{2}}\right)_{p} = \left(\frac{F_{I}}{F_{2}}\right)_{m}$$

$$\frac{M_{p}\vec{a}_{4p}}{\vec{F}_{3p}} = \frac{M_{m}\vec{a}_{4m}}{\vec{F}_{3m}} \Longrightarrow \left(\frac{F_{I}}{F_{3}}\right)_{p} = \left(\frac{F_{I}}{F_{3}}\right)_{m}$$

$$(8.3)$$





Forces affecting a flow field

 $F_I = M a = \rho l^3 \left(\frac{V^2}{l}\right) = \rho V^2 l^2$ Inertia force: $F_{p} = (\Delta p)A = \Delta p l^{2}$ Pressure force (\rightarrow Euler No.): $F_{c} = M g = \rho l^{3} g$ Gravity force (\rightarrow Froude No.): Viscosity force (\rightarrow Reynolds No.): $F_V = \mu \left(\frac{dv}{dv}\right) A = \mu \left(\frac{V}{l}\right) l^2 = \mu V l$ $F_{E} = EA = El^{2}$ Elasticity force (\rightarrow Cauchy No.): Surface tension (\rightarrow Weber No.): $F_{\tau} = \sigma l$

Here *l* and *V* are characteristic length and velocity for the system.



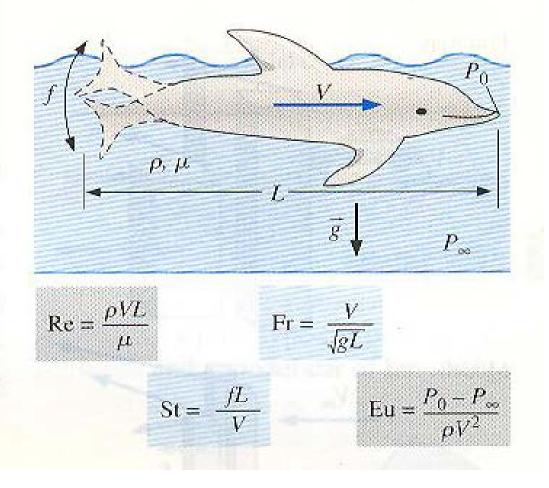


[Re] Other forces

- Coriolis force of rotating system \rightarrow Rossby number
- Buoyant forces in stratified flow \rightarrow Richardson number
- Forces in an oscillating flow \rightarrow Strouhal number











Dynamic similarity

To obtain dynamic similarity between two flowfields when all these forces act, <u>all corresponding force ratios must be the same in model and</u> prototype.

(i)
$$\left(\frac{F_I}{F_p}\right)_p = \left(\frac{F_I}{F_p}\right)_m = \left(\frac{\rho V^2}{\Delta p}\right)_p = \left(\frac{\rho V^2}{\Delta p}\right)_m$$

(8.5)

Define Euler number, $Eu = V \sqrt{\frac{\rho}{2\Delta p}}$

$$Eu_p = Eu_m$$





(ii)
$$\left(\frac{F_I}{F_V}\right)_p = \left(\frac{F_I}{F_V}\right)_m = \left(\frac{\rho V l}{\mu}\right)_p = \left(\frac{\rho V l}{\mu}\right)_m$$

Define Reynolds number, $Re = \frac{V l}{V}$

 $Re_p = Re_m \rightarrow \text{Reynolds law}$

(iii)
$$\left(\frac{F_I}{F_G}\right)_p = \left(\frac{F_I}{F_G}\right)_m = \left(\frac{V^2}{gl}\right)_p = \left(\frac{V^2}{gl}\right)_m$$

Define Froude number, $Fr = \frac{V}{\sqrt{g l}}$

 $Fr_p = Fr_m \rightarrow Froude law$

(8.6)







(iv)
$$\left(\frac{F_I}{F_E}\right)_p = \left(\frac{F_I}{F_E}\right)_m = \left(\frac{\rho V^2}{E}\right)_p = \left(\frac{\rho V^2}{E}\right)_m$$

Define Cauchy number, $Ca = \frac{\rho V^2}{E}$

$$Ca_p = Ca_m$$

[Cf] Define Mach number, $Ma = \sqrt{Ca} = \frac{V}{\sqrt{E/\rho}}$ $Ma_p = Ma_m$

(v)
$$\left(\frac{F_I}{F_T}\right)_p = \left(\frac{F_I}{F_T}\right)_m = \left(\frac{\rho l V^2}{\sigma}\right)_p = \left(\frac{\rho l V^2}{\sigma}\right)_m$$

Define Weber number, $We = \frac{\rho l V^2}{\sigma}$

$$We_p = We_m$$





(8.8)

(8.9)

Only four of these equations are independent. \rightarrow One equation is redundant according to the argument leading to Eq. (8.3) & (8.4). \rightarrow If four equations are simultaneously satisfied, then dynamic similarity will be ensured and fifth equation will also be satisfied.

In most engineering problems (real world), some of the forces above (1) may <u>not act</u>, (2) may be of <u>negligible</u> magnitude, or (3) may oppose other forces in such a way that the effect of both is reduced.

 \rightarrow In the problem of similitude a good understanding of fluid phenomena is necessary to determine how the problem may be <u>simplified by the elimination</u> of the irrelevant, negligible, or compensating forces.





1. Reynolds similarity

~ used for flows in pipe, viscosity-dominant flow

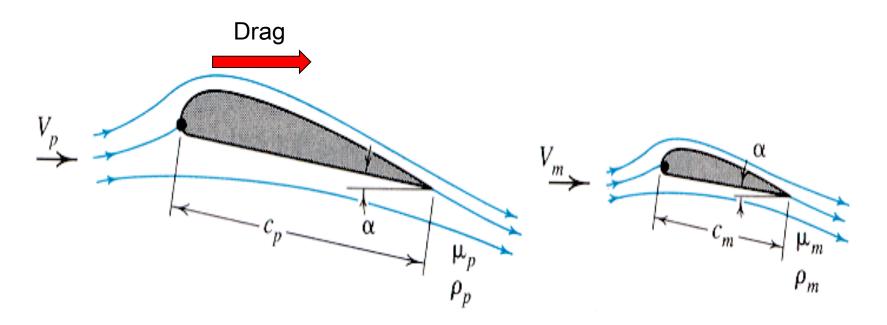
For low-speed submerged body problem, there are no surface tension phenomena, negligible compressibility effects, and gravity does not affect the flowfield.

- \rightarrow Three of four equations are not relevant to the problem.
- \rightarrow Dynamic similarity is obtained between model and prototype when the <u>Reynolds numbers (ratio of inertia to viscous forces) are the same</u>.





(i) low-speed submerged body







Reynolds similarity

$$\left(\frac{Vl}{v}\right)_p = Re_p = Re_m = \left(\frac{Vl}{v}\right)_m$$

Ratio of any corresponding forces will also be the same.

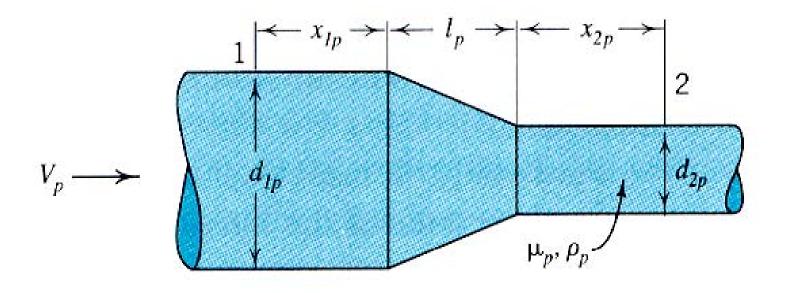
Consider drag force, $D = C \rho V^2 l^2$

$$\left(\frac{D}{F_I}\right)_p = \left(\frac{D}{F_I}\right)_m$$
$$\left(\frac{D}{\rho V^2 l^2}\right)_p = \left(\frac{D}{\rho V^2 l^2}\right)_m$$





(ii) Flow of incompressible fluids in pipes







Geometric similarity:

$$\left(\frac{d_2}{d_1}\right)_p = \left(\frac{d_2}{d_1}\right)_m$$
$$\left(\frac{l}{d_1}\right)_p = \left(\frac{l}{d_1}\right)_m$$

Assume <u>roughness pattern is similar</u>, surface tension and elastic effect are nonexistent.

Gravity does not affect the flow fields

Accordingly dynamic similarity results when Reynolds similarity, Eq. (8.10) is satisfied.

$$Re_p = Re_m$$





Eq. (8.11) is satisfied automatically.

$$Eu = \left(\frac{F_I}{F_P}\right)_p = \left(\frac{F_I}{F_P}\right)_m \quad \rightarrow \quad \left(\frac{p_1 - p_2}{\rho V^2}\right)_p = \left(\frac{p_1 - p_2}{\rho V^2}\right)_m \quad (8.11)$$

- Reynolds law
- ① Velocity:

$$Re_{p} = Re_{m} \qquad \left(\frac{Re_{p}}{Re_{m}} = 1, Re_{r} = 1\right)$$

$$\left(\frac{Vd}{v}\right)_{p} = \left(\frac{Vd}{v}\right)_{m} \rightarrow \frac{V_{m}}{V_{p}} = \frac{v_{m}}{v_{p}}\frac{1}{\frac{d_{m}}{d_{p}}} = \frac{v_{m}}{v_{p}}\frac{d_{p}}{d_{m}}$$
If $v_{m} = v_{p} \rightarrow \frac{V_{m}}{V_{p}} = \left(\frac{d_{m}}{d_{p}}\right)^{-1}$

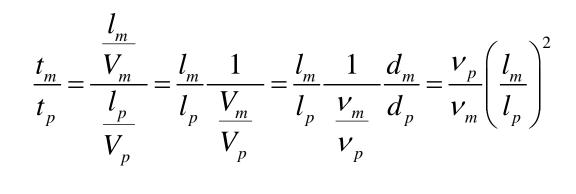




② Discharge: Q = VA

$$\frac{Q_m}{Q_p} = \left(\frac{d_m}{d_p}\right)^2 \frac{V_m}{V_p} = \left(\frac{d_m}{d_p}\right)^2 \frac{v_m}{v_p} \frac{1}{\frac{d_m}{d_p}} = \frac{v_m}{v_p} \frac{d_m}{d_p}$$

③ Time:







④ Force:

$$\frac{F_m}{F_p} = \frac{\left(M_m l_m / t_m^2\right)}{\left(M_p l_p / t_p^2\right)} = \frac{\left(\rho_m l_m^3 l_m / t_m^2\right)}{\left(\rho_p l_p^3 l_p / t_p^2\right)} = \left(\frac{\mu_m}{\mu_p}\right)^2 \left(\frac{\rho_p}{\rho_m}\right)$$

⑤ Pressure:

$$\frac{P_m}{P_p} = \left(\frac{\mu_m}{\mu_p}\right)^2 \left(\frac{\rho_p}{\rho_m}\right) \left(\frac{l_p}{l_m}\right)^2$$





[IP 8.1] p. 298 Water flow in a horizontal pipeline

Water flows in a 75 mm horizontal pipeline at a mean velocity of 3 m/s.

Prototype: Water $0^{\circ}C$

Prototype: Water 0°C
$$\mu_p = 1.781 \times 10^{-3} \text{ Pa} \cdot \text{s}$$

 $\rho_p = 99.8 \text{ kg/m}^3$
 $v_p = \frac{1.781 \times 10^{-3}}{998.8} = 1.78 \times 10^{-6} \text{ m}^2/\text{s}$
 $d_p = 75 \text{ mm}, \ V_p = 3 \text{ m/s}, \ \Delta p = 14 \text{ kPa}, \ l_p = 10 \text{ m}$
Model: Gasoline 20°C $\mu_m = 2.9 \times 10^{-4} \text{ Pa} \cdot \text{s}$ (Table A 2.1)
 $\rho_m = 0.68 \times 998.8 = 679.2 \text{ kg/m}^3$
 $v_m = 4.27 \times 10^{-7} \text{ m}^2/\text{s}$
 $d_m = 25 \text{ mm}$





[Sol] Use Reynolds similarity; $\operatorname{Re}_p = \operatorname{Re}_m$

$$\frac{V_m}{V_p} = \frac{v_m}{v_p} \left(\frac{d_m}{d_p}\right)^{-1} = \frac{4.27 \times 10^{-7}}{1.78 \times 10^{-6}} / \left(\frac{25}{75}\right) = 0.753$$

$$\therefore V_m = 0.753(3) = 2.26 \,\mathrm{m/s}$$

$$Eu_{p} = Eu_{m}$$

$$\left(\frac{\Delta p}{eV^{2}}\right)_{p} = \left(\frac{\Delta p}{eV^{2}}\right)_{m}$$

$$\frac{14}{[998.8 \times (3)^{2}]} = \frac{\Delta p_{m}}{[679.2 \times (2.26)^{2}]}$$

$$\therefore \Delta p_{m} = 5.4 \text{ kPa}$$



2. Froude similarity

~ open channel flow, free surface flow, gravity-dominant flow.

For flow field about an object moving on the surface of a liquid such as ship model (William Froude, 1870)

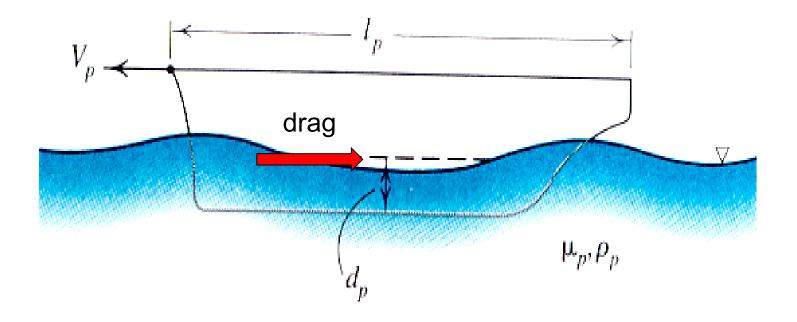
- ~ Compressibility and surface tension may be ignored.
- ~ Frictional effects are assumed to be ignored.

$$Fr_{p} = \left(\frac{V}{\sqrt{g l}}\right)_{p} = Fr_{m} = \left(\frac{V}{\sqrt{g l}}\right)_{m}$$
$$\frac{V_{m}}{V_{p}} = \sqrt{\frac{g_{m}}{g_{p}}\frac{l_{m}}{l_{p}}}$$





(i) ship model







Froude law

① Velocity

$$\frac{V_m}{V_p} = \sqrt{\frac{g_m}{g_p} \frac{l_m}{l_p}}$$

② Time
$$t = \frac{l}{V}$$

$$\frac{t_m}{t_p} = \frac{l_m}{l_p} \frac{V_p}{V_m} = \frac{l_m}{l_p} \sqrt{\frac{g_p}{g_m} \frac{l_p}{l_m}} = \sqrt{\frac{g_p}{g_m} \frac{l_m}{l_p}}$$

③ Discharge Q = VA

$$\frac{Q_m}{Q_p} = \frac{V_m}{V_p} \left(\frac{l_m}{l_p}\right)^2 = \sqrt{\frac{g_m}{g_p} \frac{l_m}{l_p}} \left(\frac{l_m}{l_p}\right)^2 = \left(\frac{g_m}{g_p}\right)^{0.5} \left(\frac{l_m}{l_p}\right)^{2.5}$$





④ Force

$$\frac{F_m}{F_p} = \left(\frac{\rho_m}{\rho_p}\right) \left(\frac{l_m}{l_p}\right)^3$$

⑤ Pressure

$$\frac{P_m}{P_p} = \left(\frac{\rho_m}{\rho_p}\right) \left(\frac{l_m}{l_p}\right)$$

[IP 8.2] p. 301 ship model (free surface flow)

 $l_p = 120 \text{ m}$ $l_m = 3 \text{ m}$ $V_p = 56 \text{ km/h} = 15.56 \text{ m/s}$ $D_m = 9 \text{ N}$

Find model velocity and prototype drag.





[Sol] Use Froude similarity

$$\left(\frac{V}{\sqrt{g\,l}}\right)_{p} = \left(\frac{V}{\sqrt{g\,l}}\right)_{m}$$

$$l_{r} = \frac{l_{m}}{l_{p}} = \frac{3}{120} = \frac{1}{40}$$

$$V_{m} = V_{p} \sqrt{\frac{(g\,l)_{m}}{(g\,l)_{p}}} = \frac{56 \times 10^{3}}{3600} \left(\frac{3}{120}\right)^{1/2} = 2.46 \text{ m/s}$$

• Drag force ratio

$$\left(\frac{D}{\rho V^2 l^2}\right)_p = \left(\frac{D}{\rho V^2 l^2}\right)_m$$
$$D_p = D_m \frac{\left(\rho V^2 l^2\right)_p}{\left(\rho V^2 l^2\right)_m} = 9 \times \left(\frac{56 \times 10^3 / 3600}{2.46}\right)^2 \times \left(\frac{120}{3}\right)^2 = 575.8 \text{ kN}$$





[Re] Combined action of gravity and viscosity

For ship hulls, the <u>contribution of wave pattern and frictional action</u> to the drag are the same order.

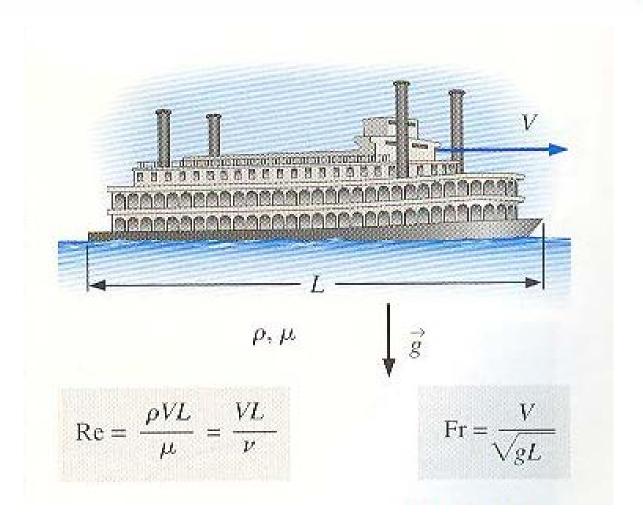
 \rightarrow Frictional effects cannot be ignored.

 \rightarrow This problem requires both Froude similarity and Reynolds similarity.

$$Fr_{p} = Fr_{m} = \left(\frac{v}{\sqrt{g l}}\right)_{p} = \left(\frac{v}{\sqrt{g l}}\right)_{m} \rightarrow \frac{V_{m}}{V_{p}} = \sqrt{\frac{g_{m}}{l_{p}}} \qquad (a)$$
$$Re_{p} = Re_{m} = \left(\frac{V l}{v}\right)_{p} = \left(\frac{V l}{v}\right)_{m} \rightarrow \frac{V_{m}}{V_{p}} = \frac{v_{m}}{v_{p}}\frac{l_{p}}{l_{m}} \qquad (b)$$











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Combine (a) and (b)

$$\sqrt{\frac{g_m}{g_p}\frac{l_m}{l_p}} = \frac{v_m}{v_p}\frac{l_p}{l_m} \rightarrow \frac{v_m}{v_p} = \left(\frac{g_m}{g_p}\right)^{0.5} \left(\frac{l_m}{l_p}\right)^{1.5}$$

This requires

(a) A liquid of appropriate viscosity must be found for the model test.

(b) If same liquid is used, then model is as large as prototype.





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For
$$g_m = g_p$$

$$\frac{v_m}{v_p} = \left(\frac{l_m}{l_p}\right)^{1.5} \rightarrow v_m = \frac{v_p}{\left(\frac{l_m}{l_p}\right)^{1.5}}$$
$$f \quad \frac{l_m}{l_p} = \frac{1}{10} \rightarrow v_m = \frac{v}{31.6}$$

Water: $\mu = 1.0 \times 10^{-3} \text{ Pa} \cdot \text{s} \rightarrow 0.32 \times 10^{-4} \text{ Pa} \cdot \text{s}$

Hydrogen: $\mu = 0.21 \times 10^{-4}$ Pa·s

~ choose only one equation \rightarrow Reynolds or Froude law

~ correction (correcting for scale effect) is necessary.





[I.P.8.3] p. 301 Model of hydraulic <u>overflow structure</u> → spillway model

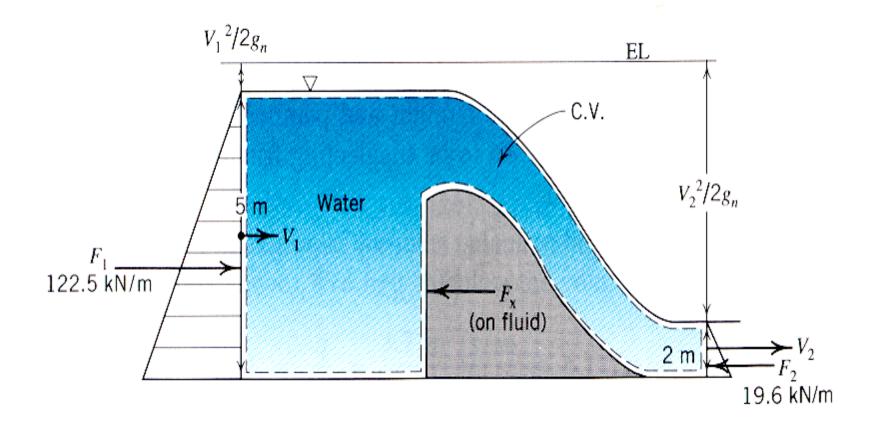
$$Q_p = 600 \text{ m}^3/\text{s}$$
$$l_r = \frac{l_m}{l_p} = \frac{1}{15}$$

[Sol] Since gravity is dominant, use Froude similarity.

$$\frac{Q_m}{Q_p} = \left(\frac{g_m}{g_p}\right)^{0.5} \left(\frac{l_m}{l_p}\right)^{2.5}$$
$$Q_m = Q_p \left(\frac{l_m}{l_p}\right)^{2.5} = 600 \left(\frac{1}{15}\right)^{2.5}$$
$$= 0.69 \text{ m}^3/\text{s} = 690 \text{ l/s}$$











3. Mach similarity

Similitude in compressible fluid flow

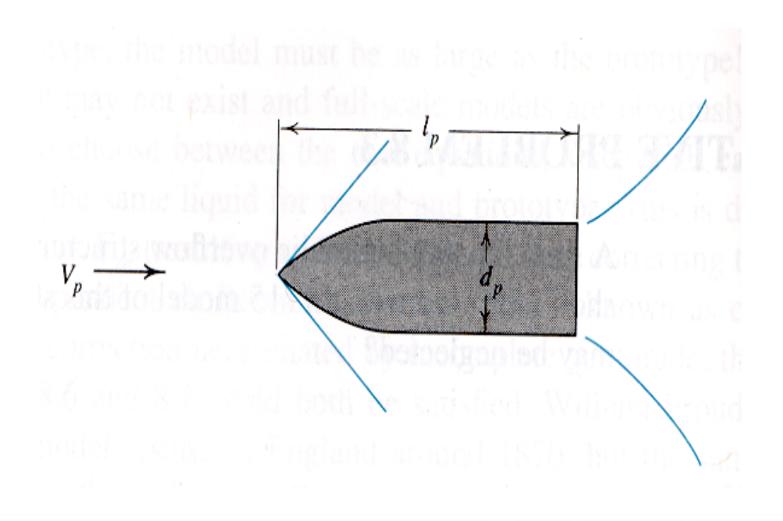
- ~ gas, air
- ~ Gravity and surface tension are ignored.
- ~ Combined action of resistance and elasticity (compressibility)

$$R e_{p} = R e_{m} \rightarrow \frac{V_{p}}{V_{m}} = \frac{V_{p}}{V_{m}} \frac{l_{m}}{l_{p}}$$
$$Ma_{p} = Ma_{m} = \left(\frac{V}{a}\right)_{p} = \left(\frac{V}{a}\right)_{m}$$





(a)







where
$$a = \text{sonic velocity} = \sqrt{\frac{E}{\rho}}$$

$$\frac{V_p}{V_m} = \frac{a_p}{a_m}$$

Combine (a) and (b)

$$\frac{l_p}{l_m} = \left(\frac{\nu_p}{\nu_m}\right) \left(\frac{a_m}{a_p}\right)$$

 \rightarrow gases of appropriate viscosity are available for the model test.





(b)

Velocity

$$\frac{V_m}{V_p} = \frac{a_m}{a_p} = \sqrt{\frac{E_m}{E_p}\frac{\rho_p}{\rho_m}}$$

• Time

$$\frac{T_m}{T_p} = \frac{l_m}{l_p} \frac{V_p}{V_m} = \sqrt{\frac{E_p}{E_m} \frac{\rho_m}{\rho_p}} \frac{l_m}{l_p}$$

• Discharge

$$\frac{Q_m}{Q_p} = \left(\frac{l_m}{l_p}\right)^2 \frac{V_p}{V_m} = \sqrt{\frac{E_p}{E_m} \frac{\rho_m}{\rho_p}} \left(\frac{l_m}{l_p}\right)^2$$





4. Euler Similarity

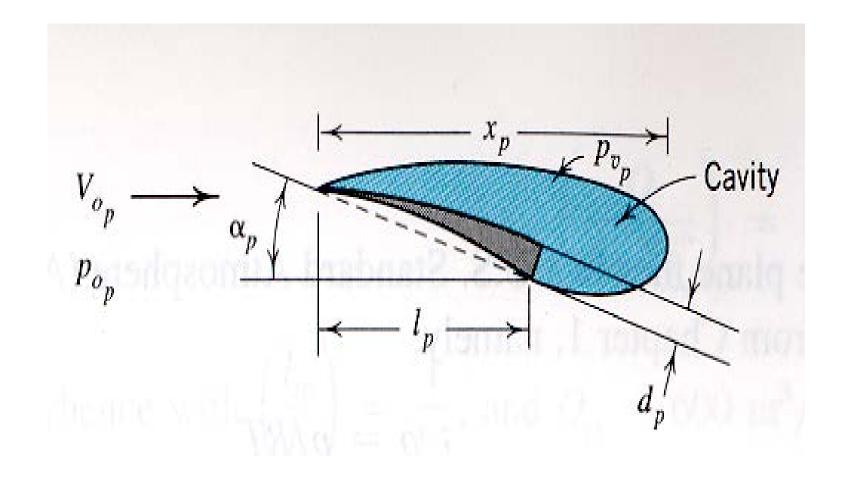
- ~ Modeling of prototype cavitation
- ~ For cavitation problem, <u>vapor pressure</u> must be included.

[Ex.1] cavitating hydrofoil model in a water tunnel

Here gravity, compressibility, and surface tension are neglected. Dynamic similitude needs <u>Reynolds similarity and Euler similarity</u>.











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$$Re_{p} = Re_{m} = \left(\frac{Vl}{v}\right)_{p} = \left(\frac{Vl}{v}\right)_{m}$$

$$\sigma_{p} = \sigma_{m} = \left(\frac{p_{0} - p_{v}}{\rho V_{0}^{2}}\right)_{p} = \left(\frac{p_{0} - p_{v}}{\rho V_{0}^{2}}\right)_{m}$$

$$\sigma_{p} = \frac{p_{0} - p_{v}}{\rho V^{2}} = \text{cavitation number}$$

$$p_0$$
 = absolute pressure

- p_v = vapor pressure
- ~ Virtually impossible to satisfy both equation.
- ~ Cavitation number must be the same in model and prototype.





Dimensional analysis

- ~ mathematics of the dimensions of quantities
- ~ is closely related to laws of similitude
- ~ based on Fourier's principle of dimensional homogeneity (1882)

 \rightarrow An equation expressing a physical relationship between quantities must be dimensionally homogeneous.

 \rightarrow The dimensions of each side of equation must be the same.





- ~ <u>cannot produce analytical solutions</u> to physical problems.
- ~ powerful tool in formulating problems which defy analytical solution and <u>must be solved experimentally</u>.
- ~ It points the way toward a maximum of information from a <u>minimum</u> of <u>experiment</u> by the formation of dimensionless groups, some of which are identical with the force ratios developed with the laws of similitude.
- Four basic dimension
- ~ directly relevant to fluid mechanics
- ~ independent fundamental dimensions





length, L

mass, M or force, F

time, t

thermodynamic temperature T

Newton's 2nd law

$$F = M a = \frac{M L}{t^2}$$

~ There are only three independent fundamental dimensions.





(1) Rayleigh method

Suppose that power, *P*, derived from <u>hydraulic turbine</u> is dependent on Q, γ, E_T

Suppose that the relation between these four variables is unknown but it is known that these are the only variables involved in the problem.

$$P = f\left(Q, \gamma, E_T\right) \tag{a}$$

Q =flow rate

- γ = specific weight of the fluid
- E_T = unit mechanical energy by unit weight of fluid (Fluid system \rightarrow turbine)





Principle of dimensional homogeneity

 \rightarrow Quantities involved cannot be added or subtracted since their dimensions are different.

Eq. (a) should be a combination of products of power of the quantities.

$$P = C \ Q^a \ \gamma^b \ E_T^c \tag{b}$$

where *C* = dimensionless constant ~ cannot be obtained by dimensional methods

a, b, c = unknown exponents





Eq. (b) can be written dimensionally as

(Dimensions of P) = (Dimensions of Q)^{*a*} (Dimensions of γ)^{*b*} (Dimensions of E_T)^{*c*}

$$\frac{ML^2}{t^3} = \left(\frac{L^3}{t}\right)^a \left(\frac{M}{L^2 t^2}\right)^b (L)^c$$
(C)

Using the principle of dimensional homogeneity, the exponent of each of the fundamental dimensions is the same on each side of the equation.

$$M: 1=b$$
$$L: 2=3a-2b+c$$
$$t: -3=-a-2b$$





Solving for *a*, *b*, and *c* yields

$$a = 1, b = 1, c = 1$$

Resubstituting these values Eq. (b) gives

$$P = C \ Q \ \gamma \ E_T \tag{d}$$

C = dimensionless constant that can be obtained from

① a physical analysis of the problem

② an experimental measurement of P, Q, γ, E_T

Rayleigh method ~ early development of a dimensional analysis





(2) Buckingham theorem

~ generalized method to find useful dimensionless groups of variables to describe process (E. Buckingham, 1915)

- Buckingham's Π theorem
- 1. n variables are functions of each other
- → Then *k* equations of their exponents (a, b, c, \cdots) can be written.

k = largest number of variables among n variables which cannot be combined into a dimensionless group

[Example]

Drag force on ship: $f(D,l,V,\rho,\mu,g) = 0 \rightarrow n = 6$





2. In most cases, k is equal to the number m of independent dimensions (M, L, t) $k \le m$

3. Application of dimensional analysis allows expression of the functional relationship in terms of (n-k) distinct dimensionless groups.

[Ex]
$$n = 6, k = m = 3 \rightarrow n - k = 3$$
 groups
 $\pi_1 = \frac{D}{\rho l^2 V^2}$
 $\pi_2 = R_e = \frac{\rho V l}{\mu}$
 $\pi_3 = F_r = \frac{V}{\sqrt{gl}}$





[Ex] Drag on a ship

$$f(D, l, \rho, \mu, V, g) = 0$$

Three basic variables = repeating variables

$$V, l, \rho$$

$$\vdots \quad \vdots \quad \vdots$$

$$t, L, M$$

Other variables D, μ , g appear only in the unique group describing the ratio of inertia force to force related to the variable.





• Procedure:

1. Find the largest number of variables which do not form a dimensionless

 Π - group.

For drag problem, No. of independent dimensions is m = 3 and $\underline{V, \rho}$ and \underline{l} cannot be formed into a Π -group, so k = m = 3

2. Determine the number of π - groups to be formed: n = 6, k = m = 3

 \therefore No. of Π - group = n - k = 3

3. Combine sequentially the variables that cannot be formed into a dimensionless group, with each of the remaining variables to form the requisite Π - groups.





$$\Pi_{1} = f_{1}(D, \rho, V, l)$$
$$\Pi_{2} = f_{2}(\mu, \rho, V, l)$$
$$\Pi_{3} = f_{3}(g, \rho, V, l)$$

4. Determine the detailed form of the dimensionless groups using principle of dimensional homogeneity.

i)
$$\Pi_1$$

 $\Pi_1 = D^a \rho^b V^c l^d$ (a)

Since Π_1 is dimensionless, writing Eq. (a) dimensionally

$$M^{0}L^{0}t^{0} = \left(\frac{ML}{t^{2}}\right)^{a} \left(\frac{M}{L^{3}}\right)^{b} \left(\frac{L}{t}\right)^{c} \left(L\right)^{d}$$
(b)





The following equations in the exponents of the dimensions are obtained

$$M: 0 = a + b$$
$$L: 0 = a - 3b + c + d$$
$$t: 0 = -2a - c$$

Solving these equations in terms of *a* gives

$$b = -a, c = -2a, d = -2a$$
$$\Pi_{1} = D^{a} \rho^{-a} V^{-2a} l^{-2a} = \left(\frac{D}{\rho l^{2} V^{2}}\right)^{a}$$





(C)

The exponent may be taken as any convenient number other than zero. If a = 1, then

$$\Pi_1 = \frac{D}{\rho l^2 V^2}$$

ii) Π_2

$$\Pi_{2} = \mu^{a} \rho^{b} V^{c} l^{d}$$
$$M^{0} L^{0} t^{0} = \left(\frac{M}{Lt}\right)^{a} \left(\frac{M}{L^{3}}\right)^{b} \left(\frac{L}{t}\right)^{c} \left(L\right)^{d}$$

$$M : 0 = a + b$$

$$L: 0 = -a - 3b + c + d$$

$$t: 0 = -a - c$$





Solving these equations in terms of *a* gives

$$b = -a, \ c = -a, \ d = -a$$

$$\Pi_2 = \mu^a \rho^{-a} V^{-a} l^{-a} = \left(\frac{\mu}{\rho \, lV}\right)^a$$

If a = -1, then

$$\Pi_2 = \frac{V \, l \rho}{\mu} = \operatorname{Re}$$

(d)





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8.2 Dimensional Analysis

$$\Pi_{3}$$

$$\Pi_{3} = g^{a}l^{b}\rho^{c}V^{d}$$

$$M^{0}L^{0}t^{0} = \left(\frac{L}{t^{2}}\right)^{a}L^{b}\left(\frac{M}{L^{3}}\right)^{c}\left(\frac{L}{t}\right)^{d}$$

$$M : 0 = c$$

$$L : 0 = a + b - 3c + d$$

$$t : 0 = -2a - d$$

Solving these equations in terms of *a* gives

$$b = a, c = 0, d = -2a$$

 $\Pi_3 = g^a l^a V^{-2a} = \left(\frac{g l}{V^2}\right)^a$





(e)

If a = -1/2, then

$$\Pi_3 = \frac{V}{\sqrt{g \, l}} = \mathrm{Fr}$$

Combining these three equations gives

$$f'\left(\frac{D}{\rho l^2 V^2}, \operatorname{Re}, \operatorname{Fr}\right) = 0$$
$$\frac{D}{\rho l^2 V^2} = f''(\operatorname{Re}, \operatorname{Fr})$$





Dimensional analysis

~ no clue to the functional relationship among $D/\rho l^2 V^2$, Re and Fr

~ arrange the numerous original variables into a relation between a smaller number of

dimensionless groups of variables.

~ indicate how test results should be processed for concise presentation

[Problem 8.48] p. 320 Head loss in a pipe flow

 $f(h_L, D, l, \rho, \mu, V, g) = 0$

Pipe diameter





Repeating variables: l, ρ, V

 $\begin{aligned} \Pi_1 &= f_1 \big(h_L, \, l, \, \rho, V \big) \\ \Pi_2 &= f_1 \big(D, \, l, \, \rho, V \big) \\ \Pi_3 &= f_3 \big(\mu, \, l, \, \rho, V \big) \\ \Pi_4 &= f_4 \big(g, \, l, \, \rho, V \big) \end{aligned}$

(i) $\Pi_{1} = h_{L}^{a} l^{b} \rho^{c} V^{d}$ $M^{0} L^{0} t^{0} = L^{a} L^{b} \left(\frac{M}{L^{3}}\right)^{c} \left(\frac{L}{t}\right)^{d}$ M : 0 = c





$$M : 0 = c$$

$$L : 0 = a + b - 3c + d$$

$$t : 0 = -d$$

$$b = -a$$

$$\therefore \quad \Pi_1 = \left(\frac{h_L}{l}\right)^a$$

$$If \quad a = 1: \quad \Pi_1 = \frac{h_L}{l}$$





d

(1)

2

3

(ii)
$$\Pi_{2} = D^{a}l^{b}\rho^{c}V^{d}$$
$$M^{0}L^{0}t^{0} = L^{a}L^{b}\left(\frac{M}{L^{3}}\right)^{c}\left(\frac{L}{t}\right)$$
$$M : 0 = c$$
$$L : 0 = a + b - 3c + d$$
$$t : 0 = -d$$
$$(2) : 0 = a + b \quad b = -a$$
$$(2) : 0 = a + b \quad b = -a$$
$$\therefore \quad \Pi_{2} = \left(\frac{D}{l}\right)^{a}$$
$$If \quad a = 1 : \Pi_{2} = \frac{D}{l}$$





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8.2 Dimensional Analysis

(iii) $\Pi_3 = \mu^a l^b \rho^c V^d$

$$M^{0}L^{0}t^{0} = \left(\frac{M}{LT}\right)^{a}L^{b}\left(\frac{M}{L^{3}}\right)^{c}\left(\frac{L}{t}\right)^{d}$$

$$M: 0 = a + c \qquad (1) \rightarrow c = d \rightarrow c = -a$$

$$L: 0 = -a + b - 3c + d \qquad (2)$$

$$t: 0 = -a - d \rightarrow d = -a \qquad (3)$$

$$(2) d + b - 3d + d = 0 \qquad b = d \rightarrow b = -a$$

$$\therefore \quad \Pi_{3} = \mu^{a}l^{-a}\rho^{-a}V^{-a}$$

$$If \quad a = -1 \qquad \therefore \quad \Pi_{3} = \frac{l\rho V}{\mu} = \operatorname{Re}$$





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8.2 Dimensional Analysis

(iv)
$$\Pi_{4} = g^{a}l^{b}\rho^{c}V^{d}$$
$$M^{0}L^{0}t^{0} = \left(\frac{L}{t^{2}}\right)^{a}L^{b}\left(\frac{M}{L^{3}}\right)^{c}\left(\frac{L}{t}\right)^{d}$$
$$M: 0 = c \qquad (1)$$
$$L: 0 = a + b - 3c + d \qquad (2)$$
$$t: 0 = -2a - d \qquad (3)$$
$$(3) d = -2a$$
$$(2) 0 = a + b - 0 - 2a \rightarrow b = a$$





$$\Pi_{4} = g^{a} l^{a} V^{-2a} = \left(\frac{g^{l}}{V^{2}}\right)^{a}$$

$$If \quad a = -\frac{1}{2}: \quad \Pi_{4} = \frac{V}{\sqrt{g l}} = Fr$$

$$f\left(\frac{h_{L}}{l}, \frac{l}{D}, \text{Re, Fr}\right) = 0$$

$$\frac{h_{L}}{l} = f'\left(\frac{l}{D}, \text{Re, Fr}\right)$$





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Homework Assignment #8

Due: 1 week from today

- Prob. 8.6
- Prob. 8.10
- Prob. 8.14
- Prob. 8.20
- Prob. 8.24
- Prob. 8.30
- Prob. 8.56
- Prob. 8.59



