

# RADIATIVE TRANSFER BETWEEN TWO OR MORE SURFACES

- View Factor
- Methods of View Factor Evaluation
- Blackbody Radiation Exchange
- Radiation Exchange between Diffuse, Gray Surfaces in an Enclosure
- Radiation in Participating Media

# View Factor

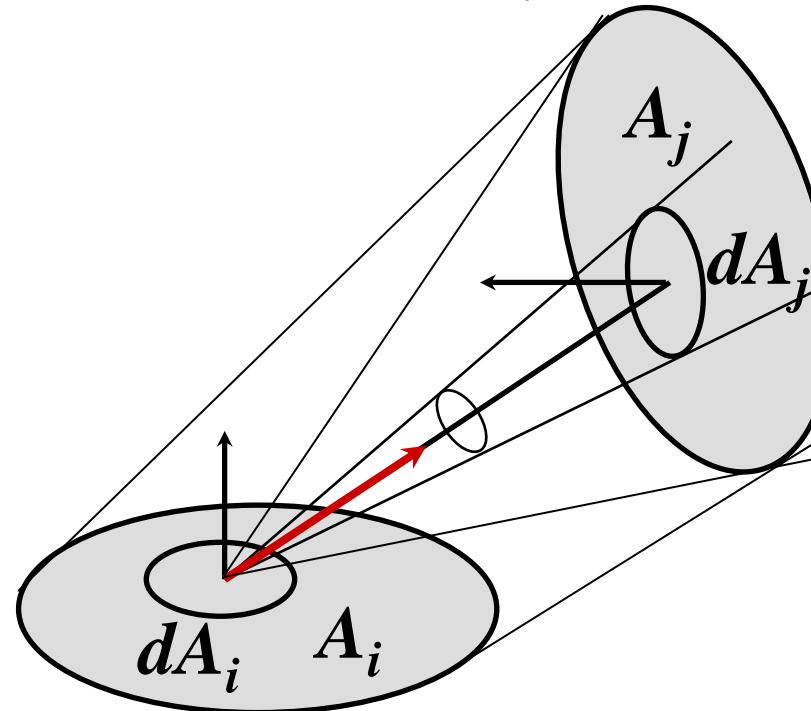
## The (Diffuse) View Factor

configuration factor, angle factor, shape factor

## View Factor Integral

$$F_{ij} = \frac{\text{radiation energy intercepted by } A_j}{\text{radiation energy leaving } A_i \text{ hemispherically}}$$

$$= \frac{q_{i \rightarrow j}}{q_i}$$



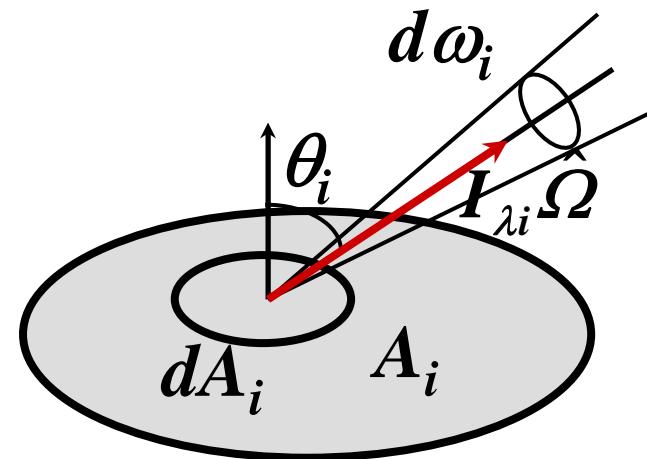
$$q_i = \int_{A_i} \int_{\cap} \int_0^{\infty} I_{\lambda i} \cos \theta_i dA_i d\omega_i d\lambda$$

$$= \int_{A_i} \left( \int_{\cap} I_i \cos \theta_i d\omega_i \right) dA_i$$

$$= \int_{A_i} J_i dA_i$$

When  $J_i$  is uniform over  $A_i$ ,

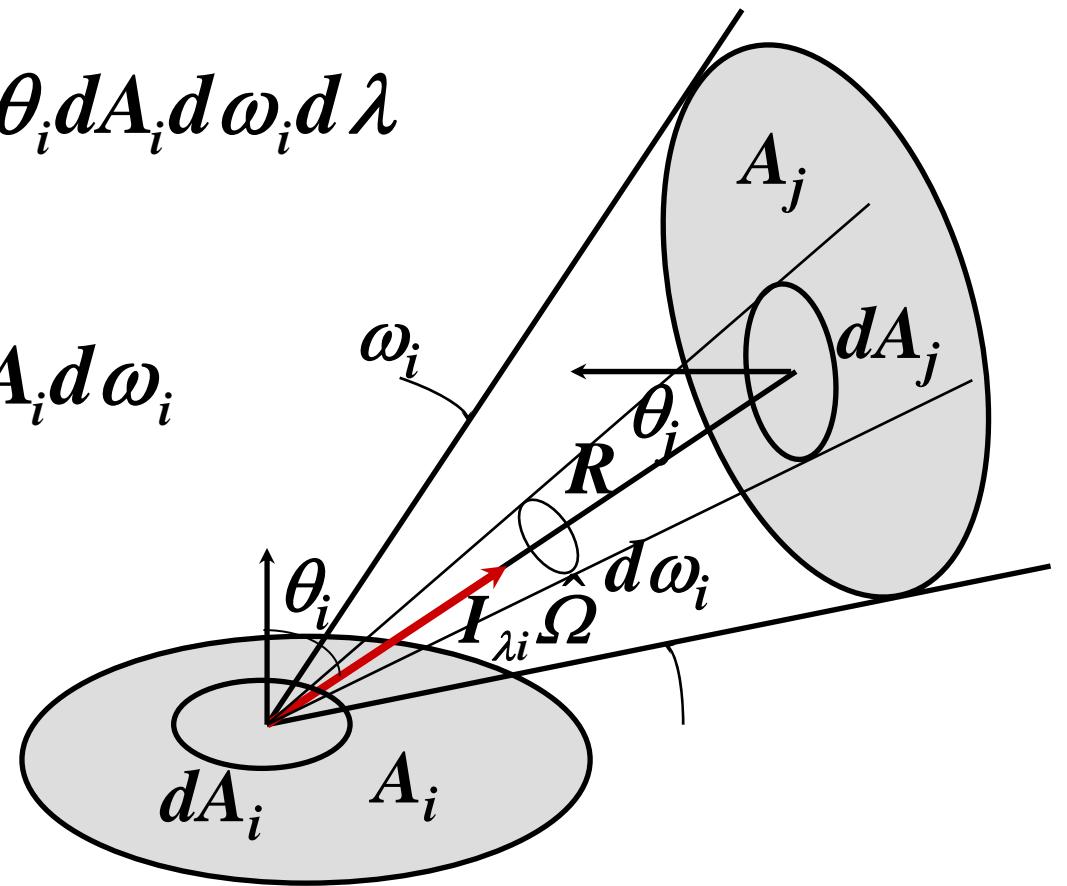
$$q_i = J_i A_i$$



$$q_{i \rightarrow j} = \int_{A_i} \int_{\omega_i} \int_0^\infty I_{\lambda i} \cos \theta_i dA_i d\omega_i d\lambda$$

$$= \int_{A_i} \int_{\omega_i} I_i \cos \theta_i dA_i d\omega_i$$

$$d\omega_i = \frac{dA_j \cos \theta_j}{R^2}$$



$$q_{i \rightarrow j} = \int_{A_j} \int_{A_i} I_i \frac{\cos \theta_i \cos \theta_j}{R^2} dA_i dA_j$$

$$F_{ij} = \frac{q_{i \rightarrow j}}{q_i} = \frac{\int_{A_j} \int_{A_i} I_i \frac{\cos \theta_i \cos \theta_j}{R^2} dA_i dA_j}{\int_{A_i} J_i dA_i}$$

When  $I_i$  is independent of propagation direction (diffuse radiation) and  $J_i$  is uniform over  $A_i$ ,

$$F_{ij} = \frac{\int_{A_j} \int_{A_i} \pi I_i \frac{\cos \theta_i \cos \theta_j}{\pi R^2} dA_i dA_j}{J_i A_i}$$

For diffuse radiation,

$$J = \int_{\cap} \int_0^{\infty} I_{\lambda} \cos \theta d\lambda d\omega = \int_{\cap} I \cos \theta d\omega = \pi I$$

$$F_{ij} = \frac{\int_{A_j} \int_{A_i} \pi I_i \frac{\cos \theta_i \cos \theta_j}{\pi R^2} dA_i dA_j}{J_i A_i}$$

$$= \frac{1}{A_i} \int_{A_j} \int_{A_i} \frac{\cos \theta_i \cos \theta_j}{\pi R^2} dA_i dA_j$$

Similarly,  $F_{ji} = \frac{1}{A_j} \int_{A_j} \int_{A_i} \frac{\cos \theta_i \cos \theta_j}{\pi R^2} dA_i dA_j$

# View Factor Relations

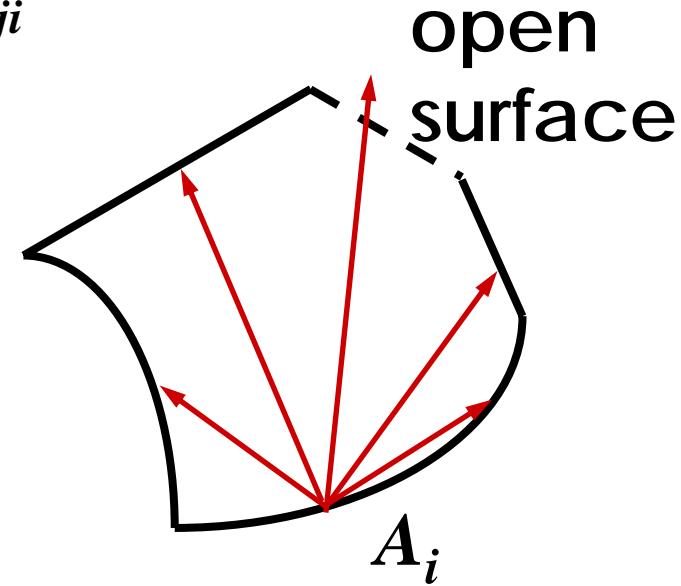
$$F_{ij} = \frac{1}{A_i} \int_{A_j} \int_{A_i} \frac{\cos \theta_i \cos \theta_j}{\pi R^2} dA_i dA_j$$

$$F_{ji} = \frac{1}{A_j} \int_{A_j} \int_{A_i} \frac{\cos \theta_i \cos \theta_j}{\pi R^2} dA_i dA_j$$

**Reciprocity:**  $A_i F_{ij} = A_j F_{ji}$

**Summation rule:**

$$\sum_{j=1}^N F_{ij} = 1$$

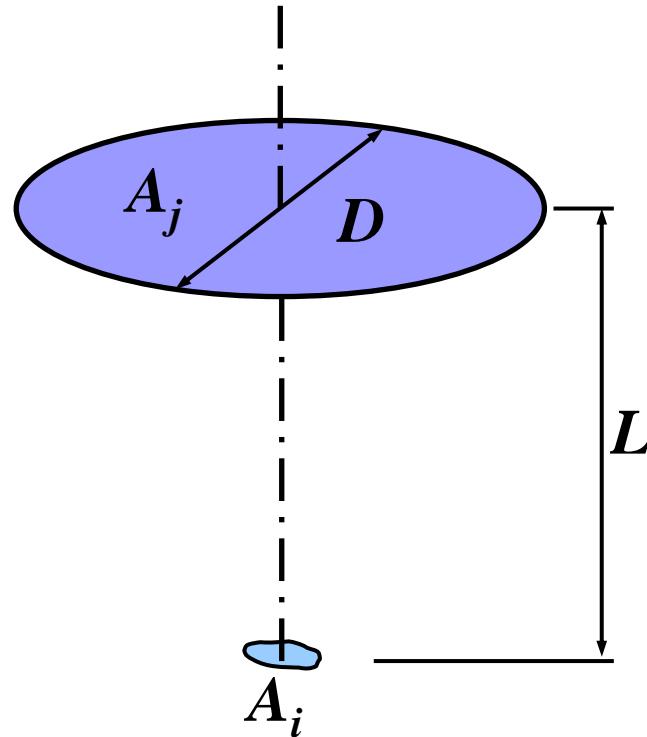


# Methods of View Factor Evaluation

- Direct integration
  - Area integral
  - Contour integral
- Flux algebra
  - Cross-string method: 2D only
  - Decomposition of shapes
- Sphere method
  - Unit sphere method:  
only from a differential area
  - Inside sphere method

# Area Integral

## Example 13.1



Find:

View factor of small surface w.r.t. disk,  $F_{ij}$

Assumptions:

1) Diffuse surfaces.

2)  $A_i \ll A_j$

## The view factor

$$F_{ij} = \frac{1}{A_i} \int_{A_j} \int_{A_i} \frac{\cos \theta_i \cos \theta_j}{\pi R^2} dA_i dA_j$$

$\theta_i$ ,  $\theta_j$  and  $R$  independent of position on  $A_i$

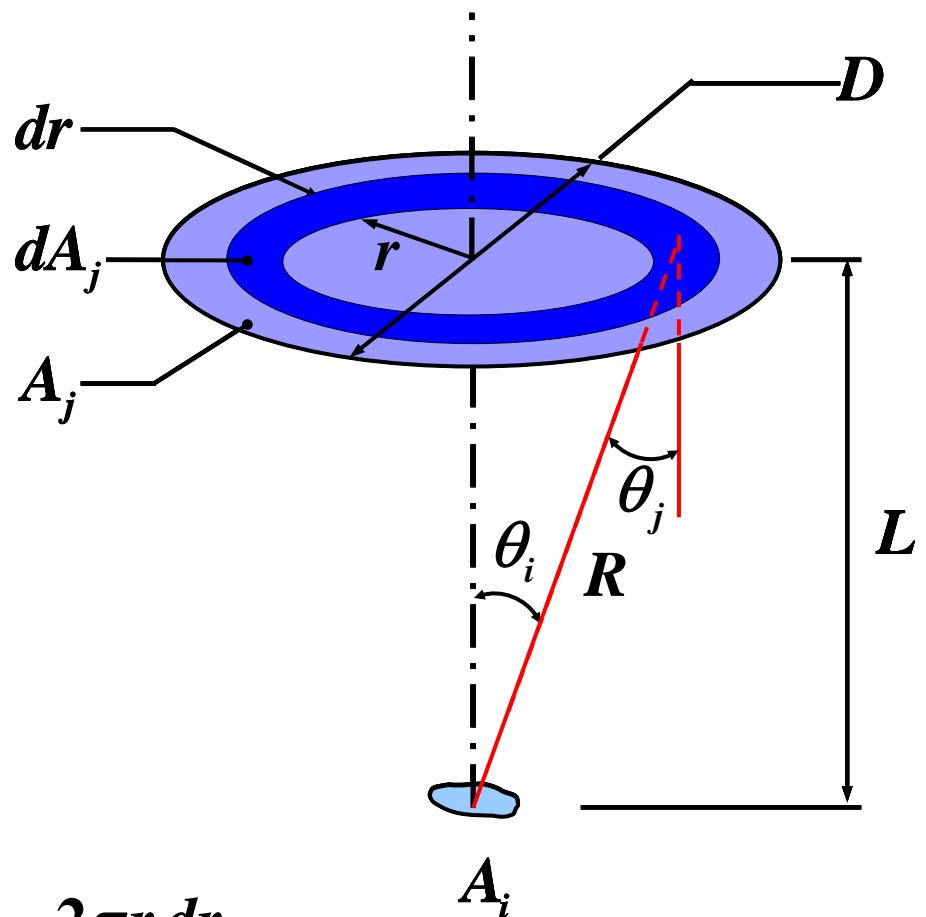
$$F_{ij} = \int_{A_j} \frac{\cos \theta_i \cos \theta_j}{\pi R^2} dA_j$$

since  $\theta_i = \theta_j \equiv \theta$

$$F_{ij} = \int_{A_j} \frac{\cos^2 \theta}{\pi R^2} dA_j$$

$$R^2 = r^2 + L^2, \quad \cos \theta = \frac{L}{R}, \quad dA_j = 2\pi r dr$$

$$F_{ij} = \int_0^{D/2} \frac{(L/R)^2}{\pi R^2} (2\pi r dr) = 2L^2 \int_0^{D/2} \frac{r dr}{(r^2 + L^2)^2} = \frac{D^2}{D^2 + 4L^2}$$



# Cross-String Method : 2-D

For an enclosure with 3 planes or convex surfaces

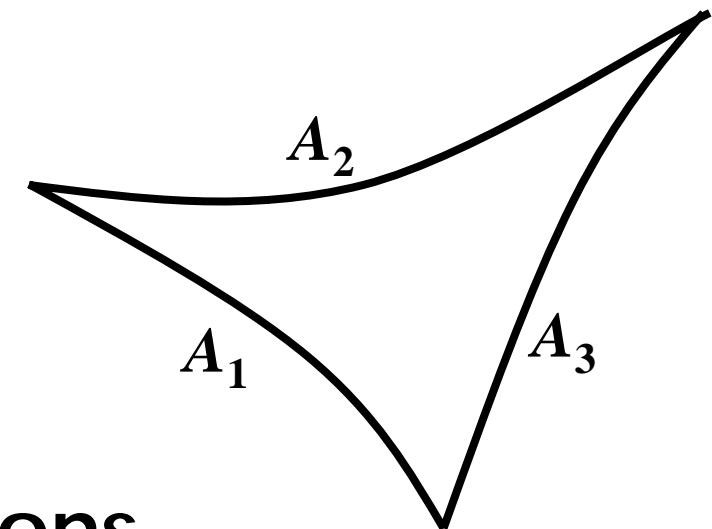
$$A_1 F_{12} = A_2 F_{21}, \quad F_{12} + F_{13} = 1$$

$$A_1 F_{13} = A_3 F_{31}, \quad F_{21} + F_{23} = 1$$

$$A_2 F_{23} = A_3 F_{32}, \quad F_{31} + F_{32} = 1$$

6 unknowns and 6 equations

$$\rightarrow F_{12} = \frac{A_1 + A_2 - A_3}{2A_1}$$



# cross-string method

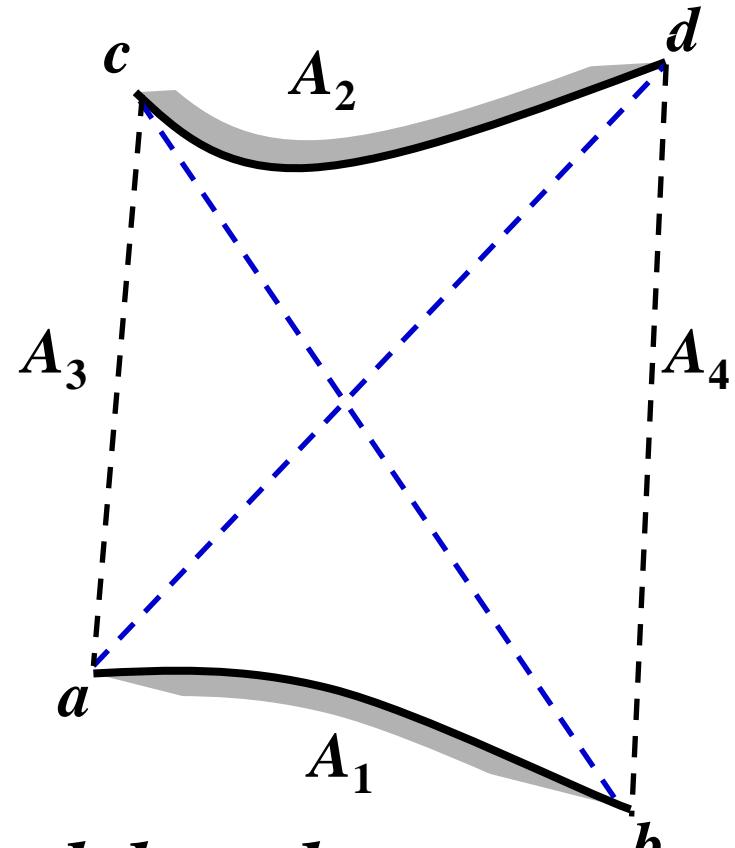
$$F_{12} = 1 - F_{13} - F_{14}$$

$$F_{13} = \frac{ab + ac - bc}{2ab}$$

$$F_{14} = \frac{ab + bd - ad}{2ab}$$

$$F_{12} = 1 - \frac{ab + ac - bc + ab + bd - ad}{2ab}$$

$$= \frac{(bc + ad) - (ac + bd)}{2ab}$$



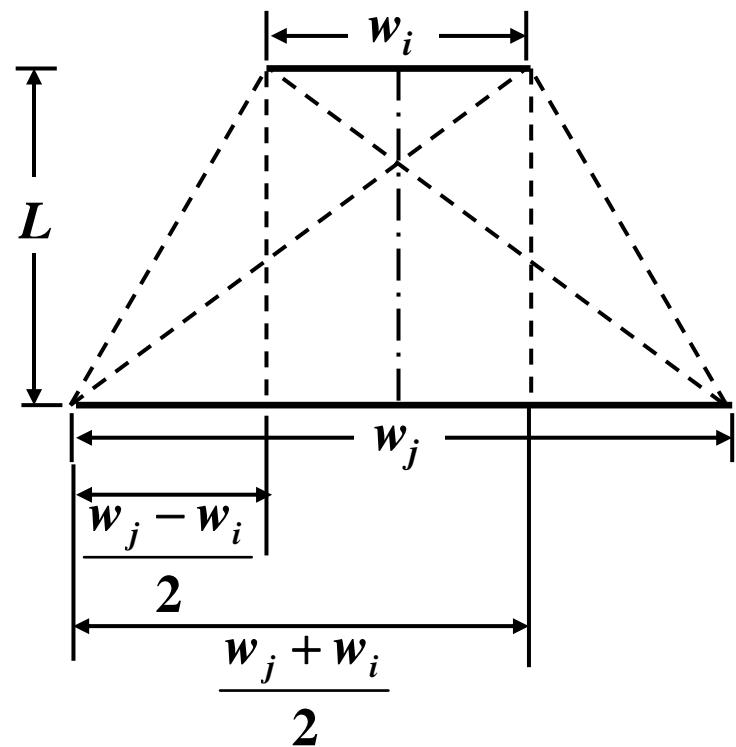
ex) view factor between parallel plates with midlines connected by perpendicular

$$F_{ij} = \frac{2 \left[ \left\{ (w_j + w_i)/2 \right\}^2 + L^2 \right]^{1/2} - 2 \left[ \left\{ (w_j - w_i)/2 \right\}^2 + L^2 \right]^{1/2}}{2w_i}$$

$$= \frac{\left[ (w_j + w_i)^2 + 4L^2 \right]^{1/2} - \left[ (w_j - w_i)^2 + 4L^2 \right]^{1/2}}{2w_i}$$

$$= \frac{\left[ (W_j + W_i)^2 + 4 \right]^{1/2} - \left[ (W_j - W_i)^2 + 4 \right]^{1/2}}{2W_i}$$

where  $W_i = w_i / L$ ,  $W_j = w_j / L$



# Decomposition of Shapes

$F_{12}$ : known,  $F_{14}$  : known,  $F_{13} = ?$

$$F_{12} = F_{1-(3+4)} = F_{13} + F_{14}$$

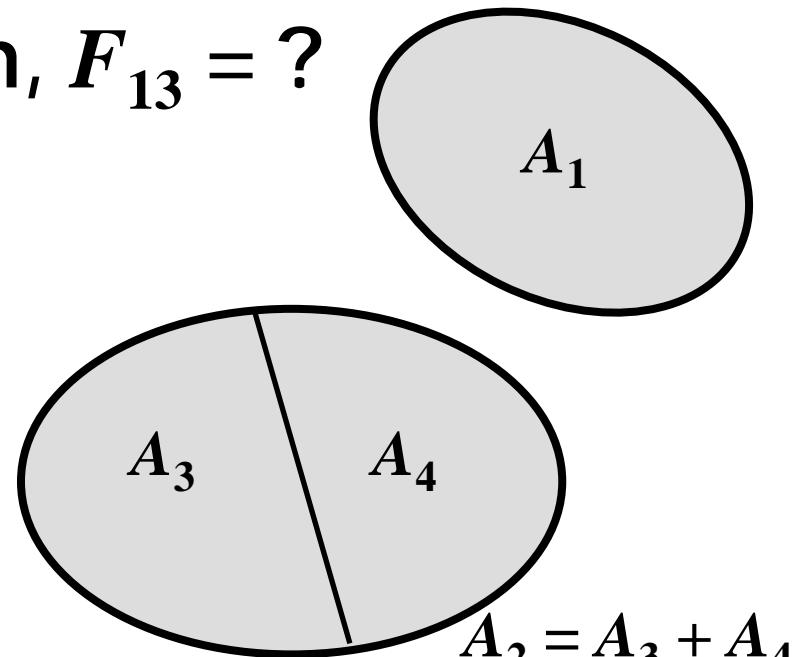
$$F_{13} = F_{12} - F_{14}$$

**Remark:**  $F_{(3+4)-1} \neq F_{31} + F_{41}$

$$F_{(3+4)-1} = \frac{A_1}{A_{(3+4)}} F_{1-(3+4)}$$

$$= \frac{A_1}{A_2} [F_{13} + F_{14}]$$

$$= \frac{A_1}{A_2} \left[ \frac{A_3}{A_1} F_{31} + \frac{A_4}{A_1} F_{41} \right] = \frac{A_3}{A_2} F_{31} + \frac{A_4}{A_2} F_{41}$$



ex)  $F_{12} = ?$

known:  $F_{(1+3)-(2+4)}$ ,  $F_{(1+3)-4}$ ,  $F_{3-(2+4)}$ ,  $F_{34}$

$$F_{(1+3)-(2+4)} = F_{(1+3)-2} + F_{(1+3)-4}$$

$$= \frac{A_2}{A_{13}} F_{2-(1+3)} + F_{(1+3)-4}$$

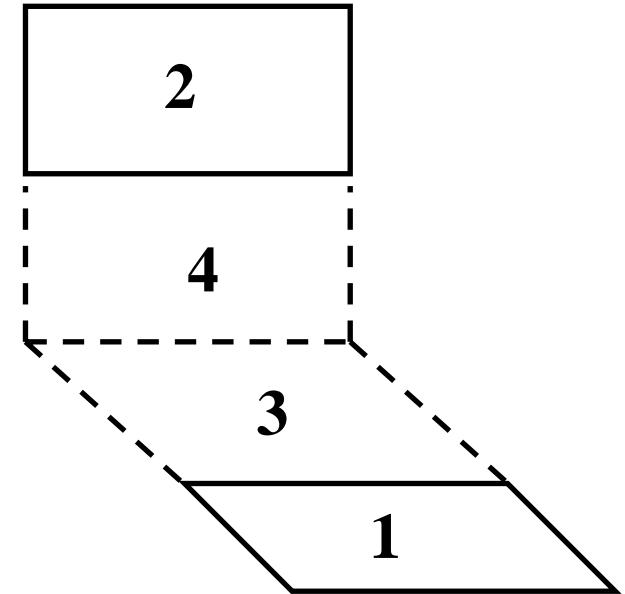
$$= \frac{A_2}{A_{13}} (F_{21} + F_{23}) + F_{(1+3)-4}$$

$$F_{21} = \frac{A_1}{A_2} F_{12}$$

$$F_{3-(2+4)} = F_{32} + F_{34} = \frac{A_2}{A_3} F_{23} + F_{34} \rightarrow F_{23} = \frac{A_3}{A_2} (F_{3-(2+4)} - F_{34})$$

$$F_{(1+3)-(2+4)} = \frac{A_2}{A_{13}} \left[ \frac{A_1}{A_2} F_{12} + \frac{A_3}{A_2} (F_{3-(2+4)} - F_{34}) \right] + F_{(1+3)-4}$$

$$F_{12} = \frac{A_{13} F_{(1+3)-(2+4)} + A_3 F_{34} - A_3 F_{3-(2+4)} - A_{13} F_{(1+3)-4}}{A_1}$$



# Blackbody Radiation Exchange

Between two black surfaces

$$J_b = \int_0^\infty \int_{\cap} I_{\lambda b} \cos \theta d\omega d\lambda = \pi I_b = E_b = \sigma T^4$$

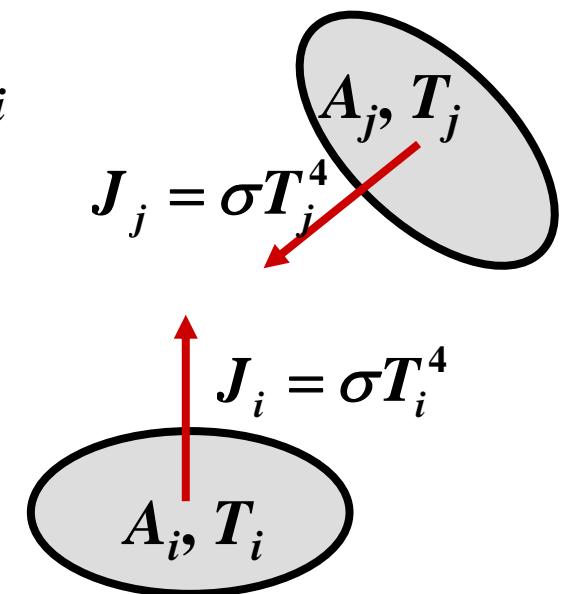
$$q_{i \rightarrow j} = \sigma T_i^4 A_i F_{ij}, \quad q_{j \rightarrow i} = \sigma T_j^4 A_j F_{ji}$$

$$q_i \equiv q_{ij} = q_{i \leftrightarrow j} = q_{i \rightarrow j} - q_{j \rightarrow i}$$

$$= \sigma T_i^4 A_i F_{ij} - \sigma T_j^4 A_j F_{ji}$$

$$= \sigma T_i^4 A_i F_{ij} - \sigma T_j^4 A_i F_{ij}$$

$$= \sigma A_i F_{ij} (T_i^4 - T_j^4)$$



# enclosure with $N$ surfaces

$$q_i = (J_i - G_i) A_i = J_i A_i - G_i A_i$$

$$G_i A_i = \sigma T_1^4 A_1 F_{1i} + \sigma T_2^4 A_2 F_{2i}$$

$$+ \cdots + \sigma T_N^4 A_N F_{Ni}$$

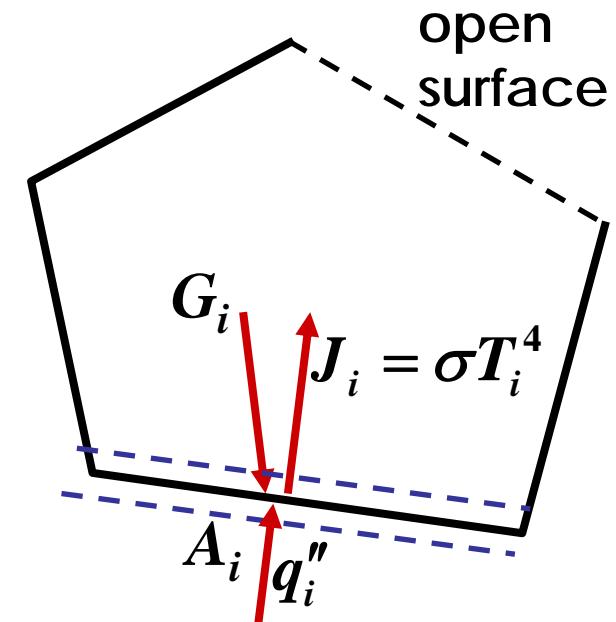
$$q_i = \sigma T_i^4 A_i$$

$$- (\sigma T_1^4 A_1 F_{1i} + \sigma T_2^4 A_2 F_{2i} + \cdots + \sigma T_N^4 A_N F_{Ni})$$

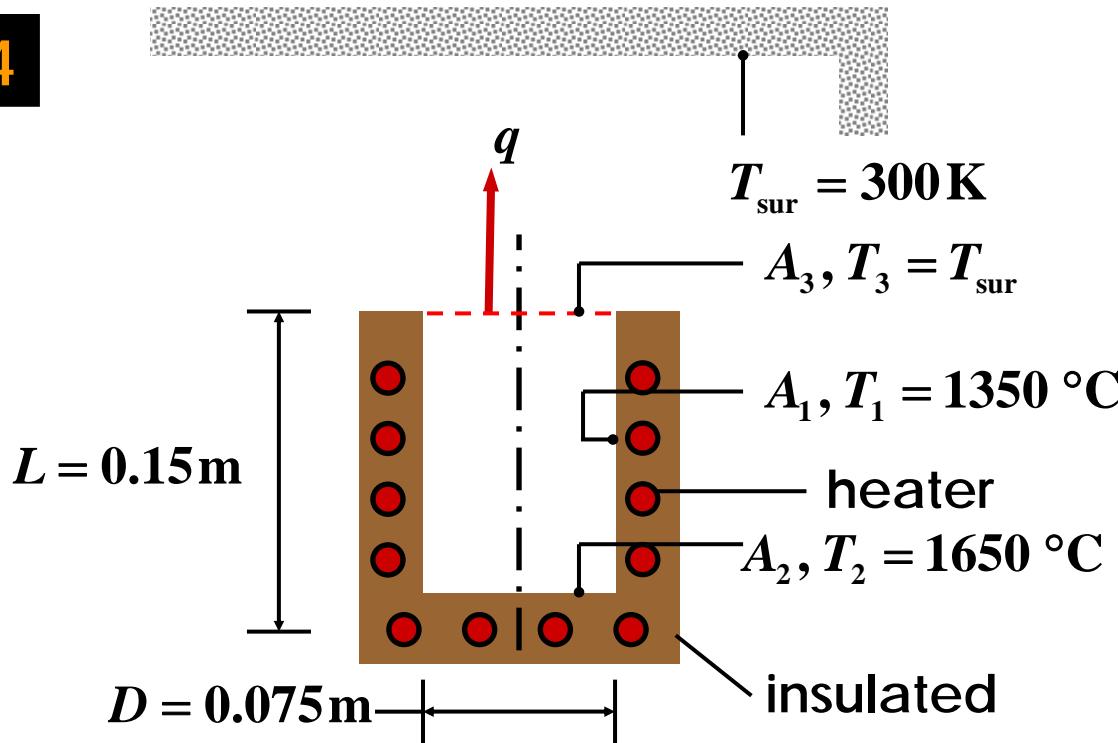
$$= \sigma T_i^4 A_i - \sum_{j=1}^N \sigma T_j^4 A_j F_{ji}$$

$$= \sigma T_i^4 A_i \sum_{j=1}^N F_{ij} - \sum_{j=1}^N \sigma T_j^4 A_i F_{ij}$$

$$= \sum_{j=1}^N \sigma A_i F_{ij} (T_i^4 - T_j^4)$$



## Example 13.4



Find:

Power required to maintain prescribed temperatures

Assumptions:

- 1) Interior surfaces behave as blackbodies.
- 2) Heat transfer by convection is negligible.
- 3) Outer surface of furnace is adiabatic.

Heat loss

$$\begin{aligned} q_3 &= (J_3 - G_3) A_3 \\ &= \sigma T_3^4 A_3 \\ &\quad - (\sigma T_1^4 A_1 F_{13} + \sigma T_2^4 A_2 F_{23}) \end{aligned}$$

$F_{23}$ : From Fig. 13.5,

$$r_j / L = 0.0375 \text{ m} / 0.15 \text{ m} = 0.25$$

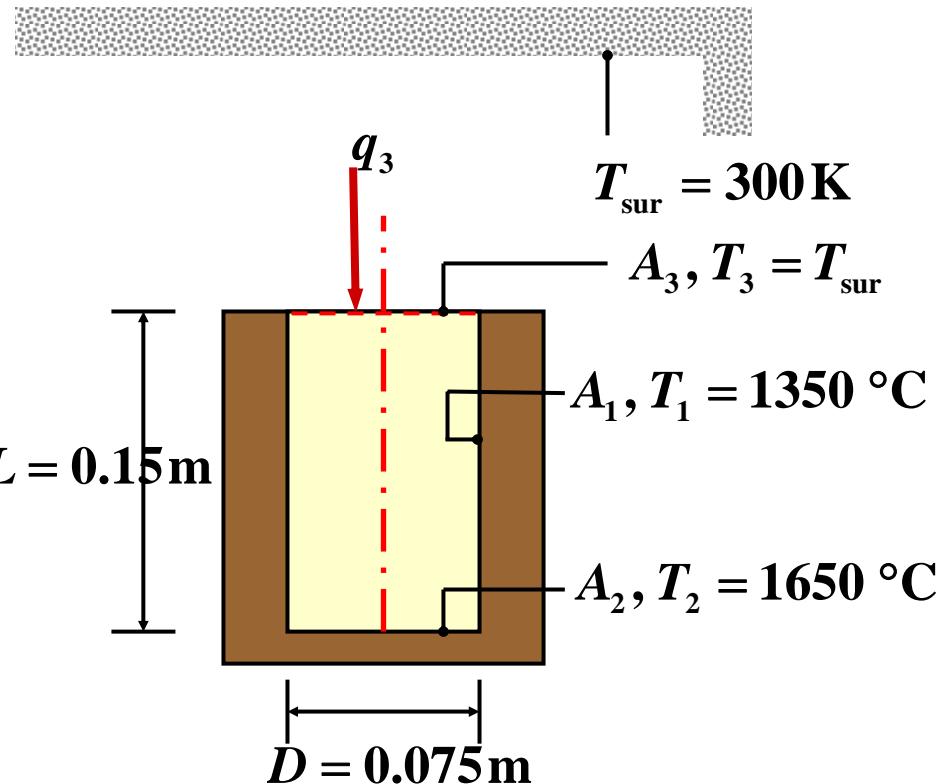
$$L / r_i = 0.15 \text{ m} / 0.0375 \text{ m} = 4$$

$$F_{23} = 0.06$$

$F_{13}$ :  $F_{21} = 1 - F_{23} = 0.94$

$$F_{13} = F_{12} = \frac{A_2}{A_1} F_{21} = \frac{\pi D^2 / 4}{\pi D L} F_{21} = \frac{0.075}{4 \times 0.15} \times 0.94 = 0.118$$

$$q_3 = -1844 \text{ W}$$



# Radiation Exchange between Diffuse, Gray Surfaces in an Enclosure

- Ray tracing method
- Net-radiation method

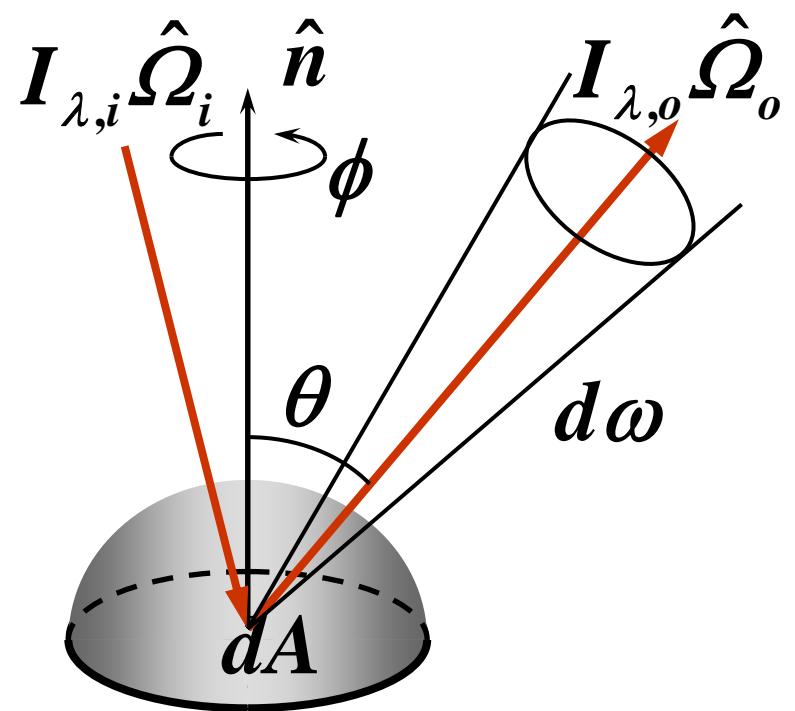
Irradiation and radiosity

$G$ : irradiation,  $\text{W/m}^2$

$J$ : radiosity,  $\text{W/m}^2$

$$J = \int_0^\infty \int_{\cap} I_{\lambda,o} \cos \theta d\omega d\lambda$$

$$G = \int_0^\infty \int_{\cap} I_{\lambda,i} \cos \theta d\omega d\lambda$$



$$J = \varepsilon\sigma T^4 + \rho G$$

$$q'' = J - G = (\varepsilon\sigma T^4 + \rho G) - G$$

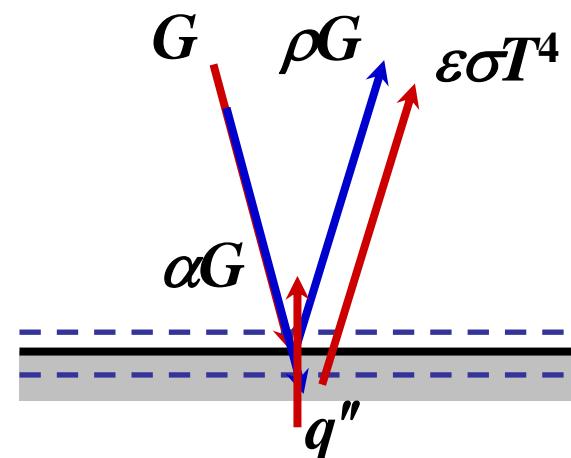
$$= \varepsilon\sigma T^4 - (1 - \rho)G$$

$$= \varepsilon\sigma T^4 - \alpha G$$

$$= \varepsilon(\sigma T^4 - G)$$

$$q'' = J - \frac{1}{\rho} (J - \varepsilon\sigma T^4) = \frac{\varepsilon}{\rho} (\sigma T^4 - J)$$

$$= \frac{\varepsilon}{1-\varepsilon} (\sigma T^4 - J)$$



# Radiation Exchange in an Enclosure

enclosure with  $n$  surfaces

$$q_k'' = J_k - G_k$$

$$J_k = \varepsilon_k \sigma T_k^4 + (1 - \varepsilon_k) G_k$$

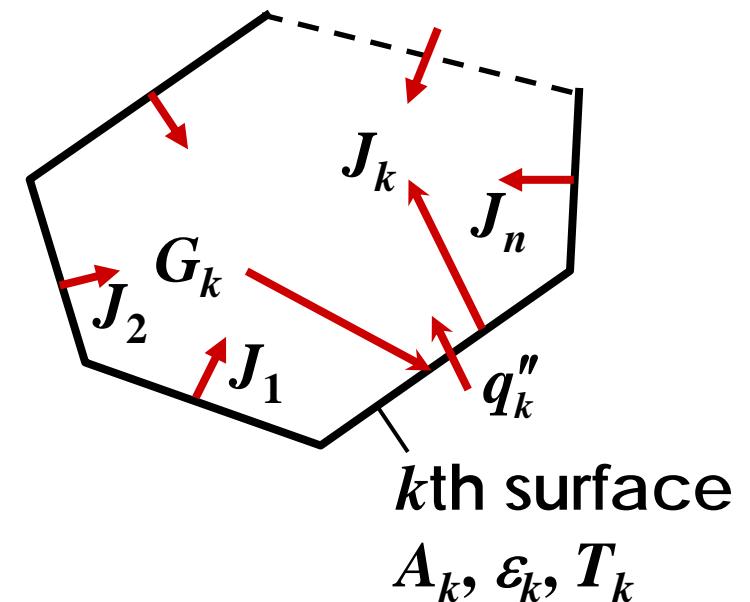
$$q_k'' = \frac{\varepsilon_k}{1 - \varepsilon_k} (\sigma T_k^4 - J_k)$$

irradiation

$$G_k A_k = J_1 A_1 F_{1k} + J_2 A_2 F_{2k} + \cdots + J_n A_n F_{nk}$$

$$= J_1 A_k F_{k1} + J_2 A_k F_{k2} + \cdots + J_n A_k F_{kn}$$

$$= \sum_{i=1}^n J_i A_k F_{ki} = A_k \sum_{i=1}^n J_i F_{ki} \quad \text{or} \quad G_k = \sum_{i=1}^n J_i F_{ki}$$

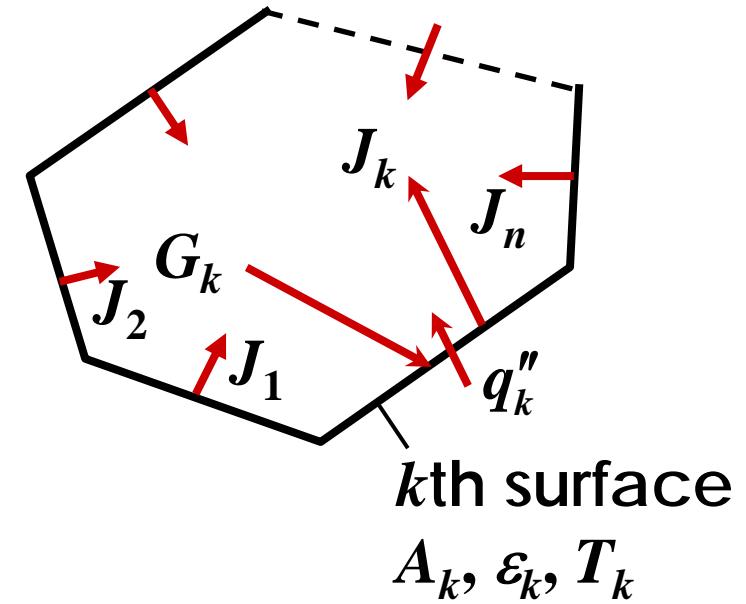


## Summary

$$q_k'' = \frac{\varepsilon_k}{1 - \varepsilon_k} (\sigma T_k^4 - J_k)$$

$$J_k = \varepsilon_k \sigma T_k^4 + (1 - \varepsilon_k) \sum_{i=1}^n J_i F_{ki}$$

$$k = 1, 2, 3, \dots, n$$



at the boundary  $T_k$  or  $q_k$  specified

$2n$  unknowns:  $J_k$  and  $q_k$  or  $T_k$

When all  $T_k$ 's are specified, the two equations are decoupled.

$n$  unknowns:  $J_k$

# Electric Network Analogy

$$q''_k = \frac{\varepsilon_k}{1 - \varepsilon_k} \left( \sigma T_k^4 - J_k \right), \quad G_k = \sum_{i=1}^n J_i F_{ki}$$

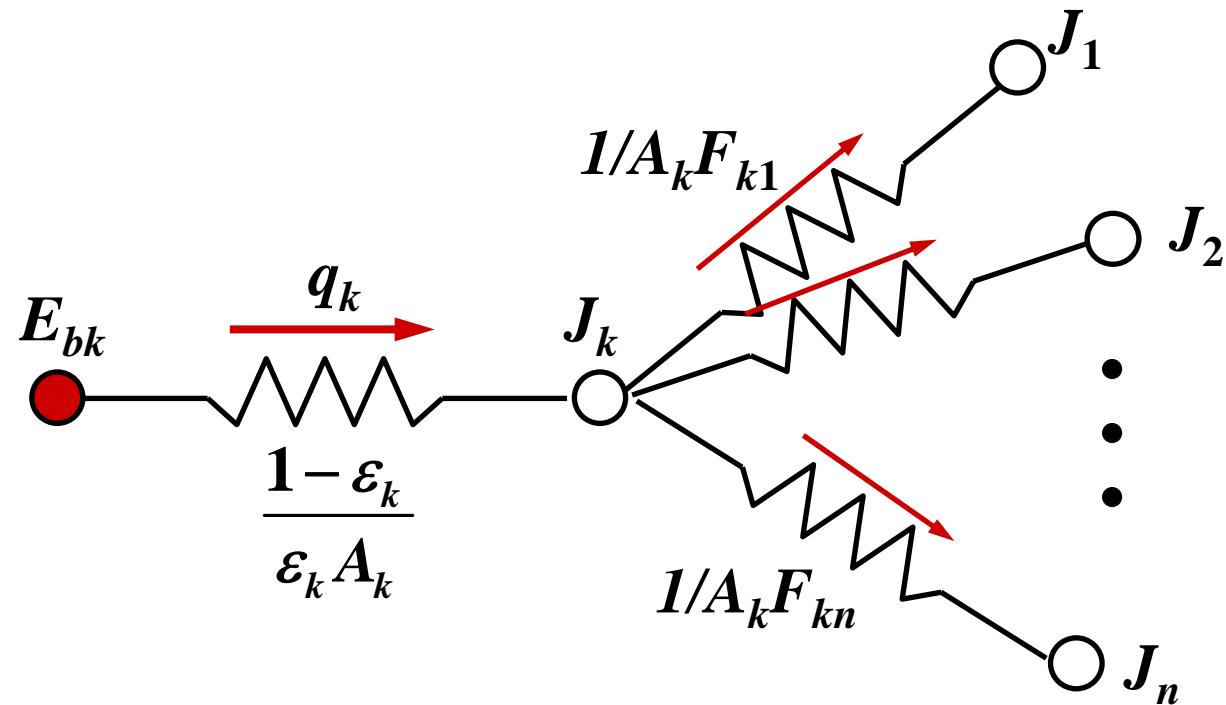
$$q_k = q''_k A_k = \frac{\sigma T_k^4 - J_k}{(1 - \varepsilon_k) / \varepsilon_k A_k} \equiv \frac{E_{bk} - J_k}{R}$$

$$= A_k (J_k - G_k) = A_k \left( J_k \sum_{i=1}^n F_{ki} - \sum_{i=1}^n J_i F_{ki} \right)$$

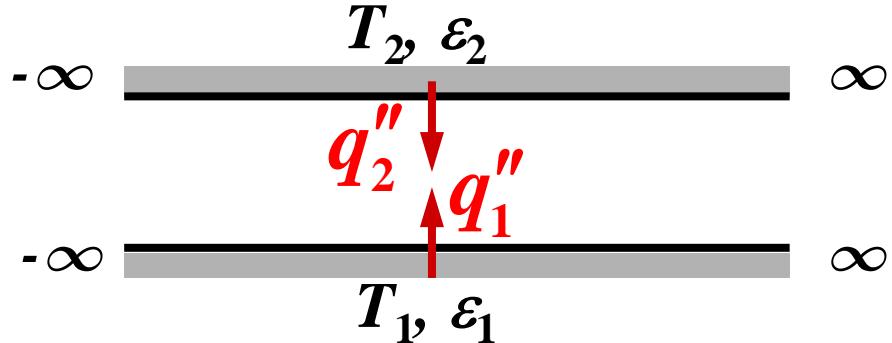
$$= A_k \sum_{i=1}^n (J_k F_{ki} - J_i F_{ki})$$

$$= \sum_{i=1}^n A_k F_{ki} (J_k - J_i) = \sum_{i=1}^n \frac{J_k - J_i}{1 / A_k F_{ki}}$$

$$q_k = \frac{E_{bk} - J_k}{\frac{1 - \varepsilon_k}{\varepsilon_k A_k}} = \sum_{i=1}^n \frac{J_k - J_i}{A_k F_{ki}}$$



ex) two infinite parallel plates



$$q''_k = \frac{\varepsilon_k}{1 - \varepsilon_k} (\sigma T_k^4 - J_k)$$

$$q''_1 = \frac{\varepsilon_1}{1 - \varepsilon_1} (\sigma T_1^4 - J_1), \quad q''_2 = \frac{\varepsilon_2}{1 - \varepsilon_2} (\sigma T_2^4 - J_2)$$

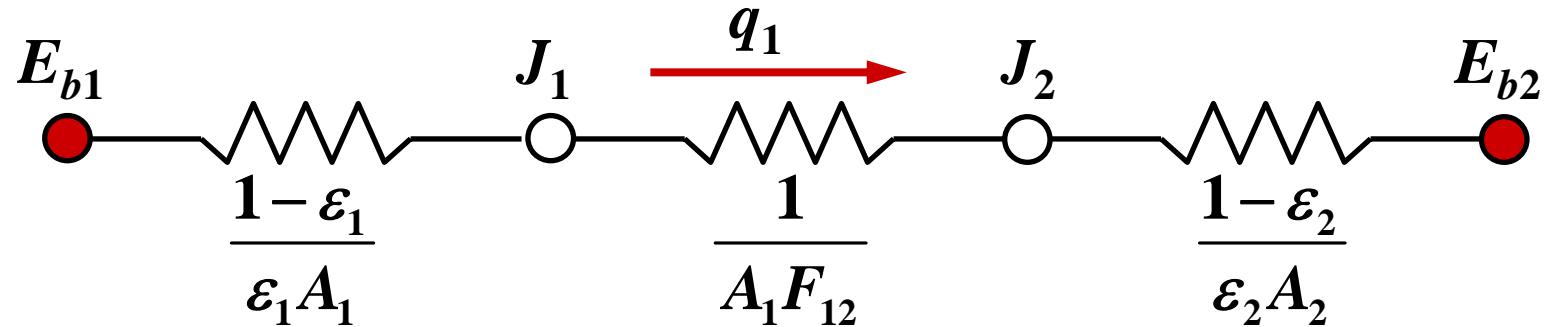
$$J_k = \varepsilon_k \sigma T_k^4 + (1 - \varepsilon_k) \sum_{i=1}^n J_i F_{ki}$$

$$J_1 = \varepsilon_1 \sigma T_1^4 + (1 - \varepsilon_1) J_2, \quad J_2 = \varepsilon_2 \sigma T_2^4 + (1 - \varepsilon_2) J_1$$

$$q''_1 = -q''_2 = \frac{\sigma (T_1^4 - T_2^4)}{\frac{1}{\varepsilon_1} + \frac{1}{\varepsilon_2} - 1}$$

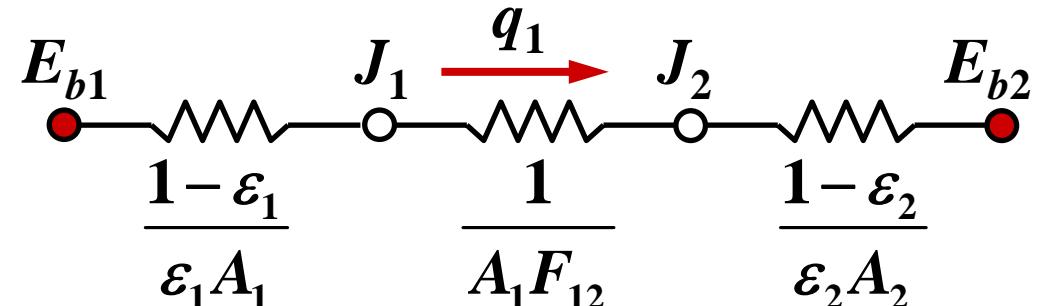
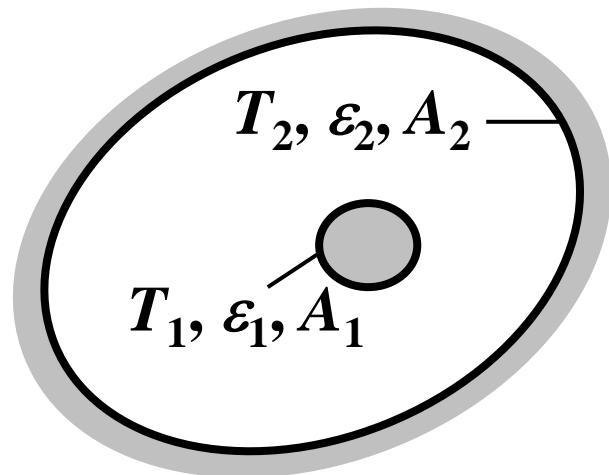
# Using network analogy

$$\begin{array}{c}
 -\infty \xrightarrow[T_2, \varepsilon_2]{\quad} \infty \\
 \hline
 -\infty \xrightarrow[T_1, \varepsilon_1]{\quad} \infty
 \end{array}
 \quad q_k = \frac{E_{bk} - J_k}{1 - \varepsilon_k} = \sum_{i=1}^n \frac{J_k - J_i}{A_k F_{ki}}$$

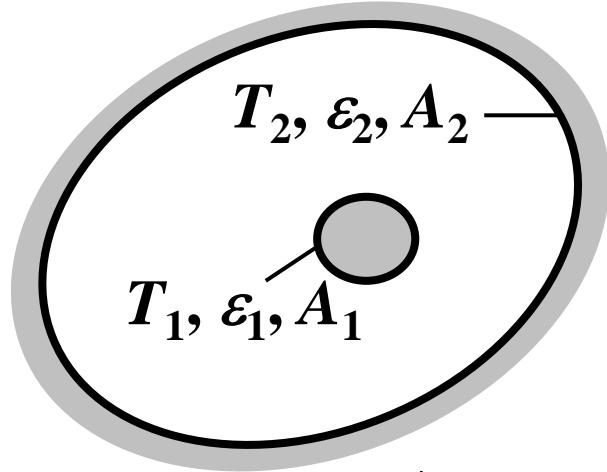


$$q''_1 = \frac{\sigma(T_1^4 - T_2^4)}{\frac{1 - \varepsilon_1}{\varepsilon_1} + 1 + \frac{1 - \varepsilon_2}{\varepsilon_2}} = \frac{\sigma(T_1^4 - T_2^4)}{\frac{1}{\varepsilon_1} + \frac{1}{\varepsilon_2} - 1}$$

ex) a body in an enclosure



$$\begin{aligned}
 q_1 &= \frac{\sigma(T_1^4 - T_2^4)}{\frac{1-\varepsilon_1}{A_1\varepsilon_1} + \frac{1}{A_1} + \frac{1-\varepsilon_2}{A_2\varepsilon_2}} = \frac{A_1\sigma(T_1^4 - T_2^4)}{\frac{1-\varepsilon_1}{\varepsilon_1} + 1 + \frac{A_1}{A_2}\left(\frac{1}{\varepsilon_2} - 1\right)} \\
 &= \frac{A_1\sigma(T_1^4 - T_2^4)}{\frac{1}{\varepsilon_1} + \frac{A_1}{A_2}\left(\frac{1}{\varepsilon_2} - 1\right)}
 \end{aligned}$$



$$q_1 = \frac{A_1 \sigma (T_1^4 - T_2^4)}{\frac{1}{\epsilon_1} + \frac{A_1}{A_2} \left( \frac{1}{\epsilon_2} - 1 \right)}$$

When  $\frac{A_1}{A_2} \ll 1$ ,  $q_1 = \epsilon_1 \sigma A_1 (T_1^4 - T_2^4)$

The enclosure acts like a black cavity.

Remark: when  $A_2$  is a black enclosure

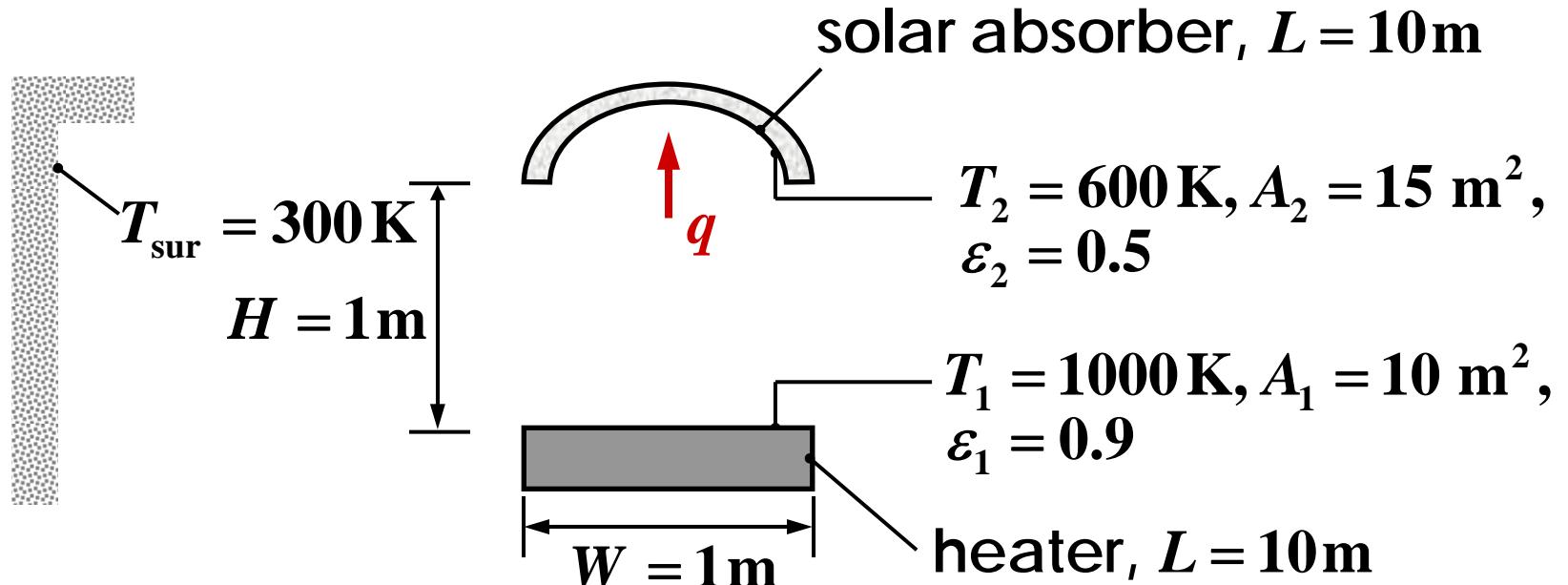
$$q_1 = \epsilon_1 \sigma T_1^4 A_1 - \alpha_1 G_1 A_1$$

$$G_1 A_1 = \sigma T_2^4 A_2 F_{21} = \sigma T_2^4 A_1 F_{12} = \sigma T_2^4 A_1$$

$$q_1 = \epsilon_1 \sigma T_1^4 A_1 - \epsilon_1 \sigma T_2^4 A_1 = \epsilon_1 \sigma A_1 (T_1^4 - T_2^4)$$

### Example 13.3

Coating on a curved solar absorber surface

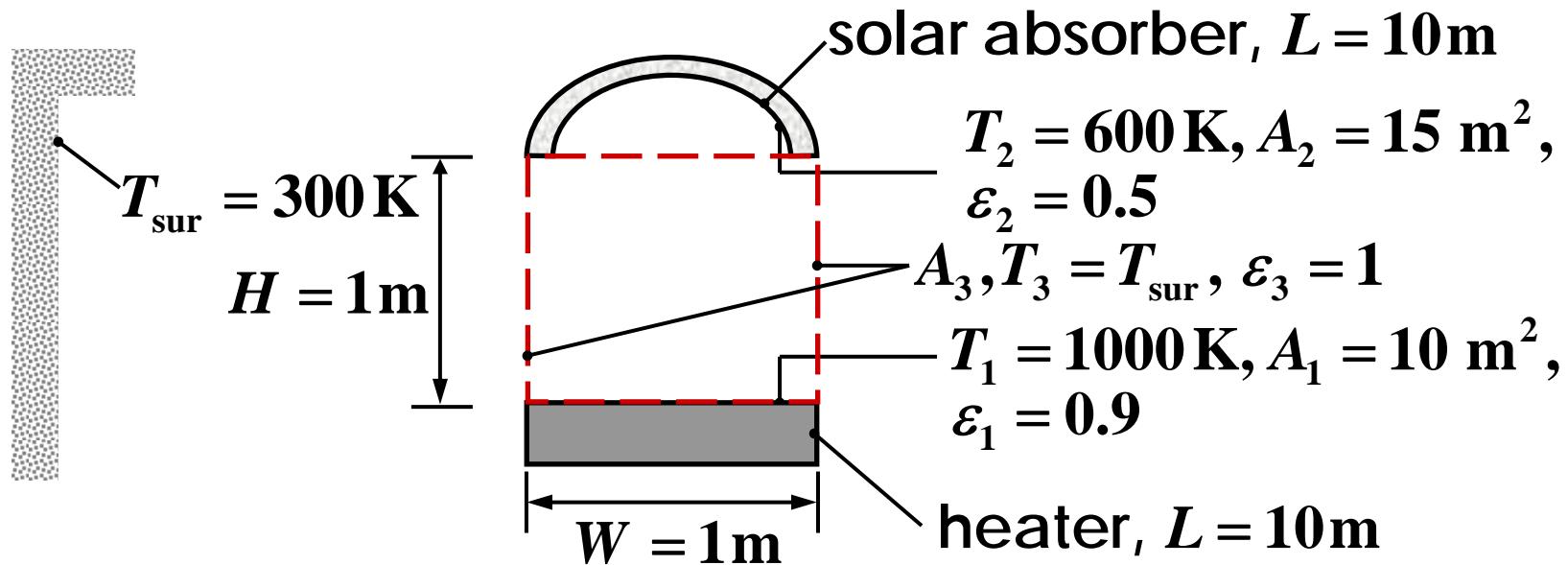


Find:

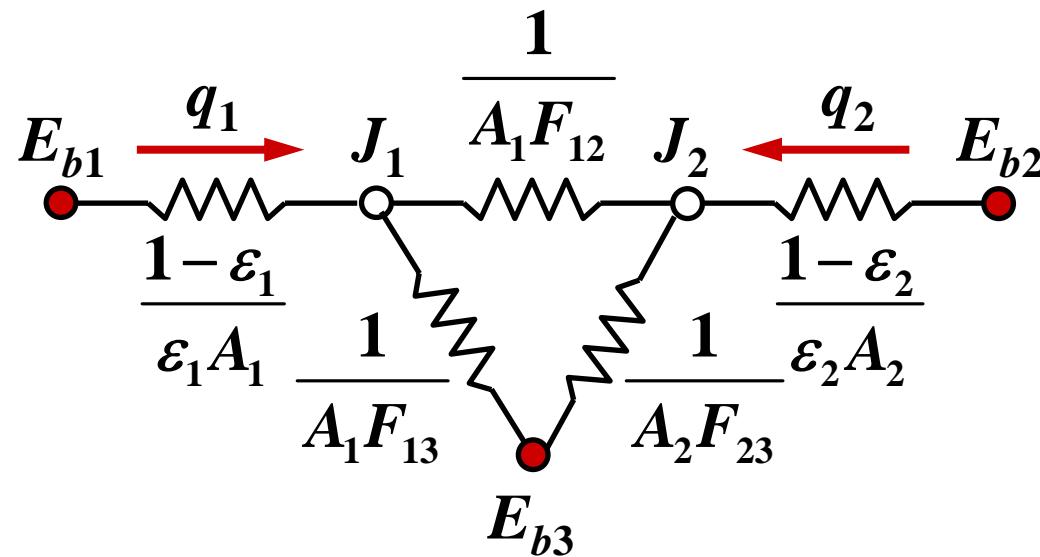
Net rate of heat transfer to the absorber surface

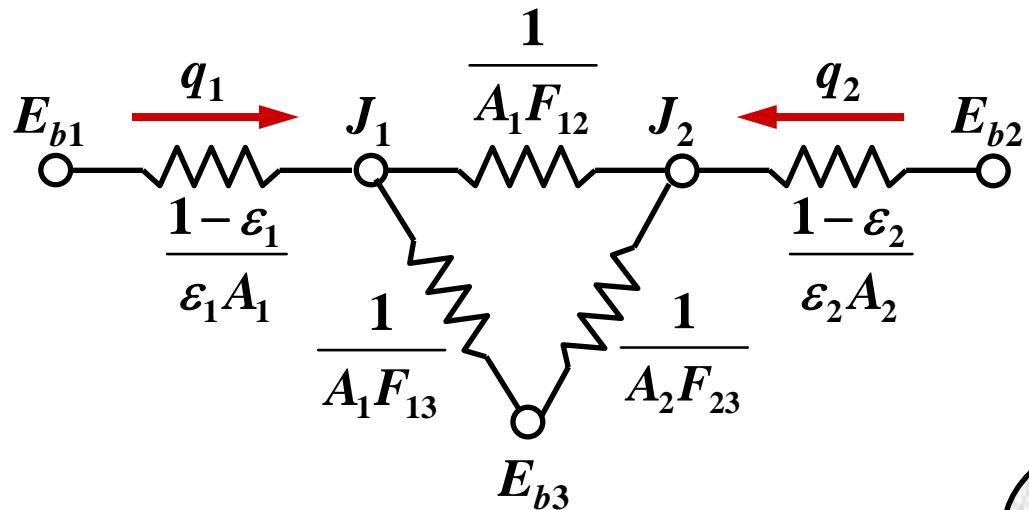
Assumptions:

- 1) Convection effects are negligible.
- 2) Absorber and heater surfaces are diffuse and gray.



## Electric network: 3-surface enclosure system

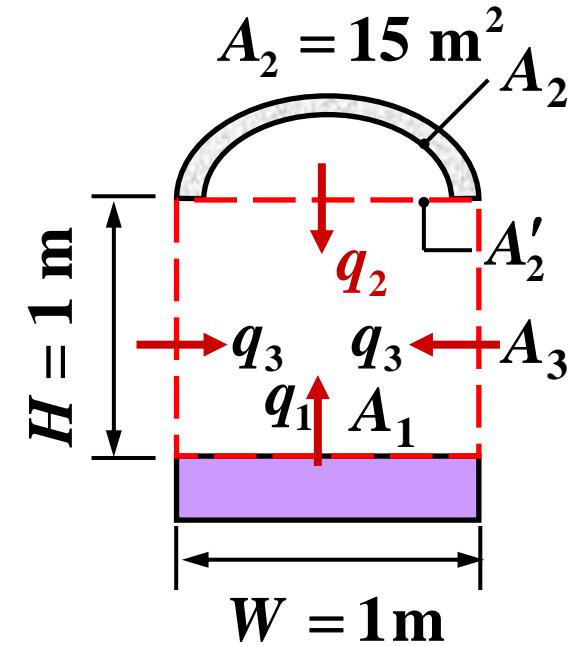




$$q_1 = \frac{E_{b1} - J_1}{(1 - \varepsilon_1) / \varepsilon_1 A_1} = \frac{J_1 - J_2}{1 / A_1 F_{12}} + \frac{J_1 - E_{b3}}{1 / A_1 F_{13}}$$

$$q_2 = \frac{E_{b2} - J_2}{(1 - \varepsilon_2) / \varepsilon_2 A_2} = \frac{J_2 - J_1}{1 / A_2 F_{21}} + \frac{J_2 - E_{b3}}{1 / A_2 F_{23}}$$

$$F_{12}: \quad F_{12} = F_{12'} \quad (F_{12} + F_{13} = 1, \quad F_{12'} + F_{13} = 1)$$



From Fig. 13.4:  $Y/L = 10$ ,  $X/L = 1 \rightarrow F_{12} = 0.39$

$$F_{21}: \quad A_2 F_{21} = A_1 F_{12}, \quad F_{21} = \frac{A_1}{A_2} F_{12} = \frac{1 \times 10}{15} \times 0.39 = 0.26$$

$$\textcolor{blue}{F_{13}}: F_{13} = 1 - F_{12} = 0.61$$

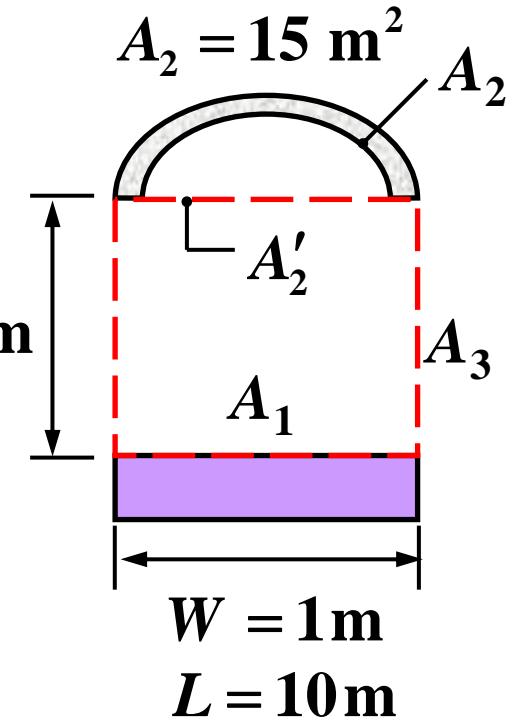
$$\textcolor{blue}{F_{23}}: F_{32} = F_{32'} = F_{31} = \frac{A_1}{A_3} F_{13}$$

$$F_{32} = \frac{A_1}{A_3} F_{13} = \frac{1 \times 10}{2(10 \times 1)} \times 0.61 = 0.305$$

$$F_{23} = \frac{A_3}{A_2} F_{32} = \frac{20}{15} \times 0.305 = 0.41$$

$$\textcolor{blue}{q_1} = \frac{E_{b1} - \textcolor{blue}{J}_1}{(1 - \varepsilon_1) / \varepsilon_1 A_1} = \frac{\textcolor{blue}{J}_1 - \textcolor{blue}{J}_2}{1 / A_1 F_{12}} + \frac{\textcolor{blue}{J}_1 - E_{b3}}{1 / A_1 F_{13}}$$

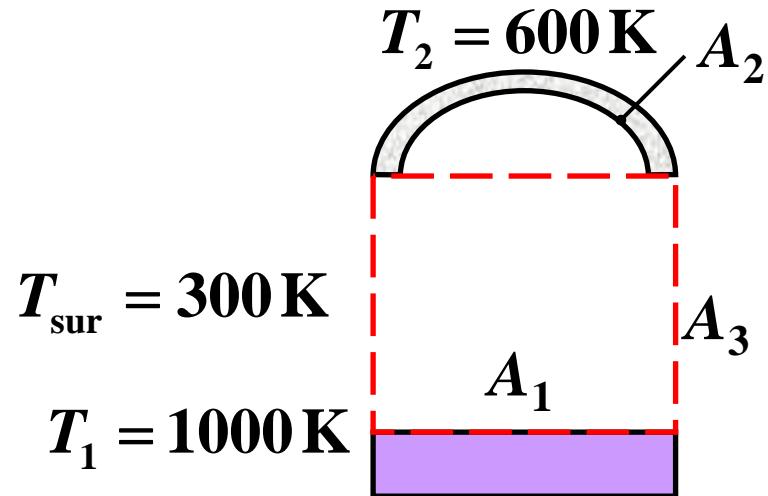
$$\textcolor{red}{q_2} = \frac{E_{b2} - \textcolor{blue}{J}_2}{(1 - \varepsilon_2) / \varepsilon_2 A_2} = \frac{\textcolor{blue}{J}_2 - \textcolor{blue}{J}_1}{1 / A_2 F_{21}} + \frac{\textcolor{blue}{J}_2 - E_{b3}}{1 / A_2 F_{23}}$$



$$E_{b1} = \sigma T_1^4 = 56,700 \text{ W/m}^2$$

$$E_{b2} = \sigma T_2^4 = 7,348 \text{ W/m}^2$$

$$E_{b3} = \sigma T_3^4 = 459 \text{ W/m}^2$$



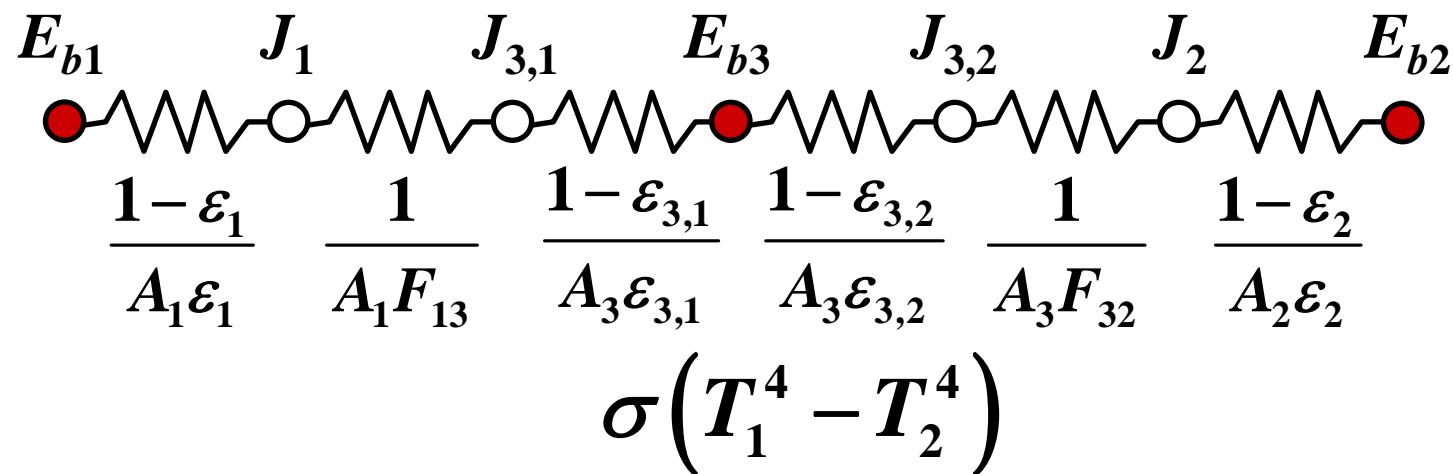
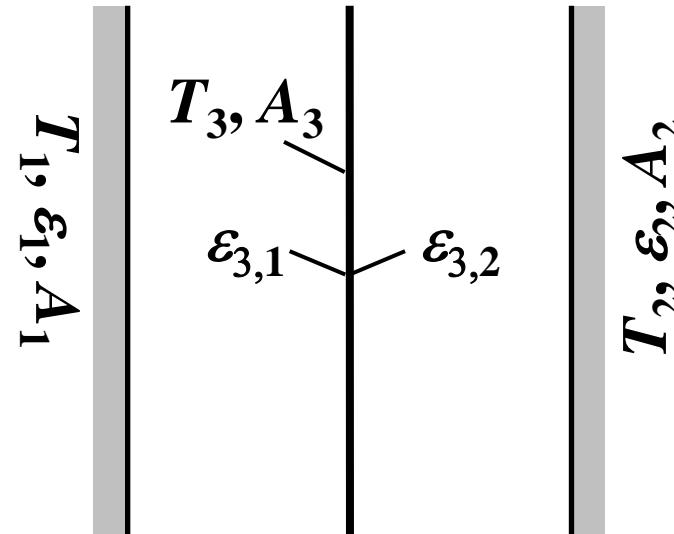
$$\frac{56,700 - J_1}{(1 - 0.9)/0.9} = \frac{J_1 - J_2}{1/0.39} + \frac{J_1 - 459}{1/0.61} \rightarrow -10J_1 + 0.39J_2 = -510,002$$

$$\frac{7,348 - J_2}{(1 - 0.5)/0.5} = \frac{J_2 - J_1}{1/0.26} + \frac{J_2 - 459}{1/0.41} \rightarrow 0.26J_1 - 1.67J_2 = -7536$$

$$\therefore J_2 = 12,528 \text{ W/m}^2$$

$$q_2 = \frac{E_{b2} - J_2}{(1 - \varepsilon_2)/A_2 \varepsilon_2} = \frac{7,348 - 12,528}{(1 - 0.5)/0.5 \times 15} = -77.7 \text{ kW}$$

# Radiation Shield



$$q_1 = \frac{\frac{1}{1-\varepsilon_1} + \frac{1}{A_1 F_{13}} + \frac{1}{A_3 \varepsilon_{3,1}} + \frac{1}{1-\varepsilon_{3,1}} + \frac{1}{A_3 \varepsilon_{3,2}} + \frac{1}{A_3 F_{32}} + \frac{1}{1-\varepsilon_2}}{\frac{1}{A_1 \varepsilon_1} + \frac{1}{A_1 F_{13}} + \frac{1}{A_3 \varepsilon_{3,1}} + \frac{1}{1-\varepsilon_{3,1}} + \frac{1}{A_3 \varepsilon_{3,2}} + \frac{1}{A_3 F_{32}} + \frac{1}{A_2 \varepsilon_2}}$$

when  $A_1 = A_2 = A_3$  and  $F_{13} = F_{32} = 1$

$$q_1 = \frac{A_1 \sigma (T_1^4 - T_2^4)}{\frac{1 - \varepsilon_1}{\varepsilon_1} + 1 + \frac{1 - \varepsilon_{3,1}}{\varepsilon_{3,1}} + \frac{1 - \varepsilon_{3,2}}{\varepsilon_{3,2}} + 1 + \frac{1 - \varepsilon_2}{\varepsilon_2}}$$

$$= \frac{A_1 \sigma (T_1^4 - T_2^4)}{\frac{1}{\varepsilon_1} + \frac{1}{\varepsilon_2} + \frac{1}{\varepsilon_{3,1}} + \frac{1}{\varepsilon_{3,2}} - 2}$$

$$\text{when } \varepsilon_1 = \varepsilon_2 = \varepsilon_{3,1} = \varepsilon_{3,2} \equiv \varepsilon, \quad q_1 = \frac{A_1 \sigma (T_1^4 - T_2^4)}{2 \left( \frac{2}{\varepsilon} - 1 \right)}$$

for  $N$  shields,  $(q_1)_N = \frac{1}{N+1} (q_1)_0$

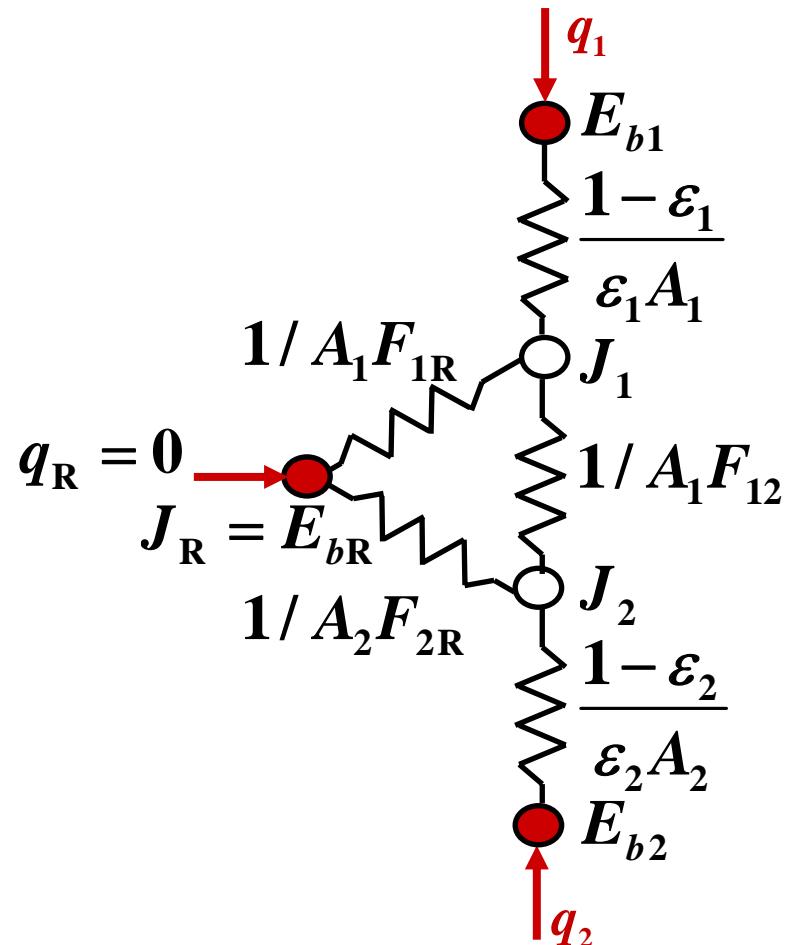
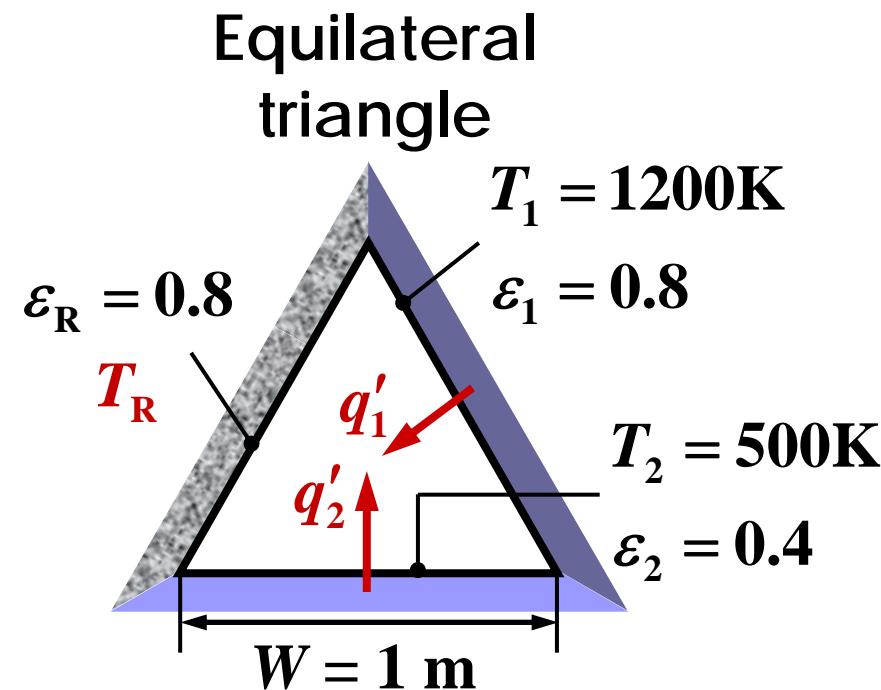
# Reradiating Surface

a surface with zero net radiation transfer

$$q_i = A_i (J_i - G_i) = \frac{A_i \varepsilon_i}{1 - \varepsilon_i} (\sigma T_i^4 - J_i) = 0$$

$$J_i = G_i = \sigma T_i^4$$

## Example 13.6



Find:

- 1) Rate at which heat must be supplied per unit length of duct,  $q'_1$ ,  $q'_2$
- 2) Temperature of the insulated surface,  $T_R$

Assumption: All surfaces are opaque, diffuse, gray, and of uniform radiosity.

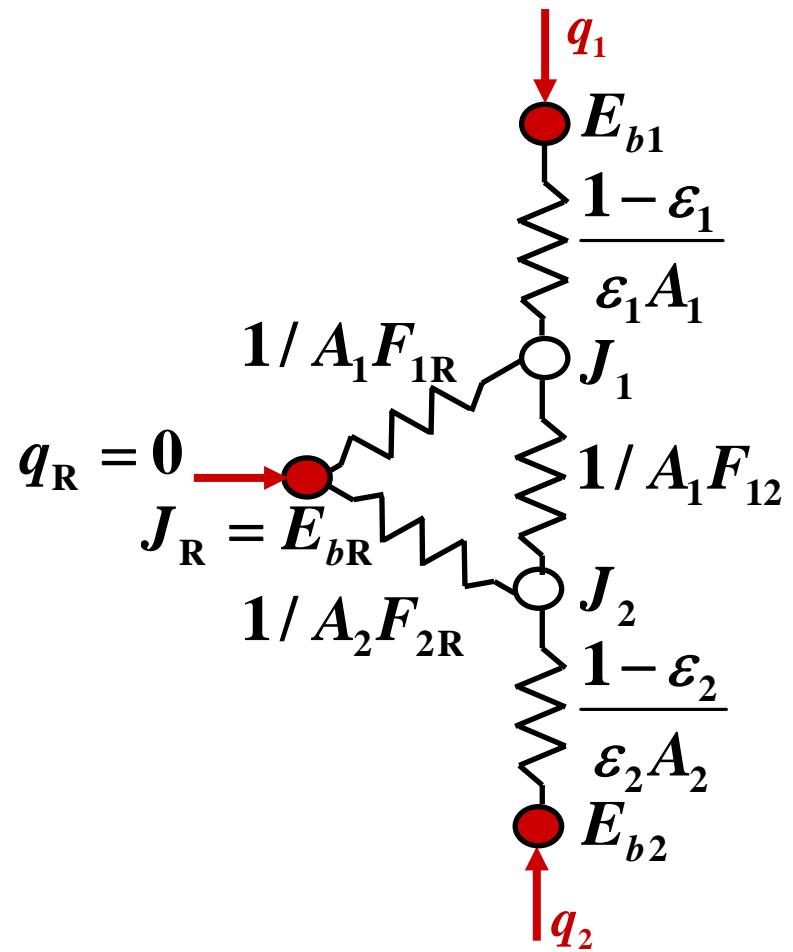
$$1) \ q_1, q_2$$

$$q_1 = \frac{E_{b1} - J_1}{\frac{1-\varepsilon_1}{\varepsilon_1 A_1}} = \frac{J_1 - J_2}{R} = \frac{J_2 - E_{b2}}{\frac{1-\varepsilon_2}{\varepsilon_2 A_2}}$$

$$q_1 = \frac{E_{b1} - E_{b2}}{\frac{1-\varepsilon_1}{\varepsilon_1 A_1} + R + \frac{1-\varepsilon_2}{\varepsilon_2 A_2}}$$

$$\frac{1}{R} = A_1 F_{12} + \frac{1}{1/A_1 F_{1R} + 1/A_2 F_{2R}}$$

$$q_1 = \frac{E_{b1} - E_{b2}}{\frac{1-\varepsilon_1}{\varepsilon_1 A_1} + \frac{1}{A_1 F_{12} + \left[ (1/A_1 F_{1R}) + (1/A_2 F_{2R}) \right]^{-1}} + \frac{1-\varepsilon_2}{\varepsilon_2 A_2}}$$

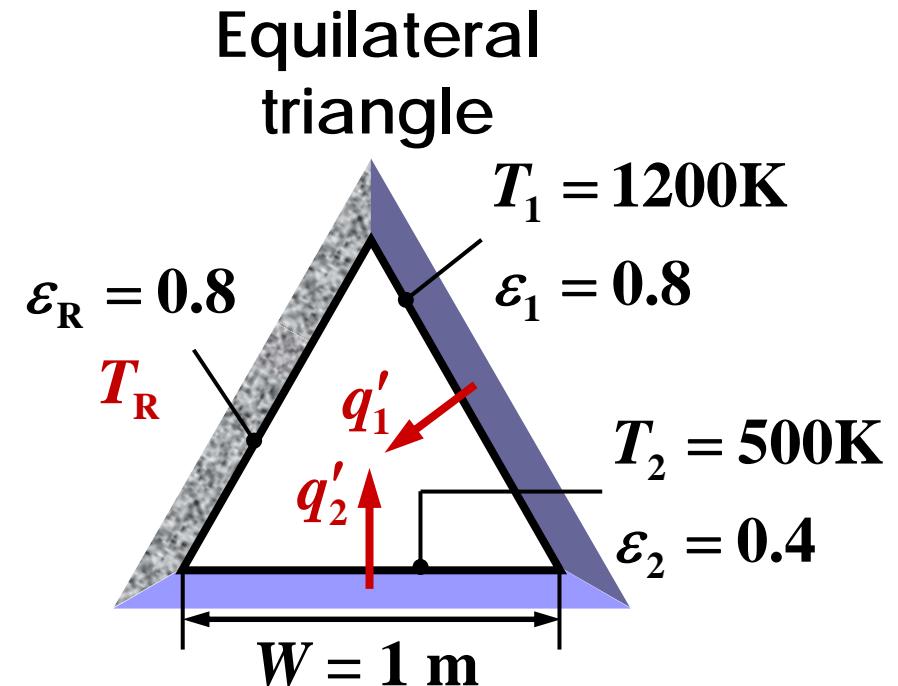


From symmetry,

$$F_{12} = F_{1R} = F_{2R} = 0.5$$

$$A_1 = A_2 = W \cdot L$$

$$\begin{aligned} q'_1 &= \frac{q_1}{L} = \frac{5.67 \times 10^{-8} (1200^4 - 500^4)}{\frac{1-0.8}{0.8 \times 1} + \frac{1}{1 \times 0.5 + (2+2)^{-1}} + \frac{1-0.4}{0.4 \times 1}} \\ &= 37 \text{ kW/m} = -q'_2 \end{aligned}$$



$$2) T_R$$

$$\frac{J_1 - E_{bR}}{1/A_1 F_{1R}} = \frac{E_{bR} - J_2}{1/A_2 F_{2R}}$$

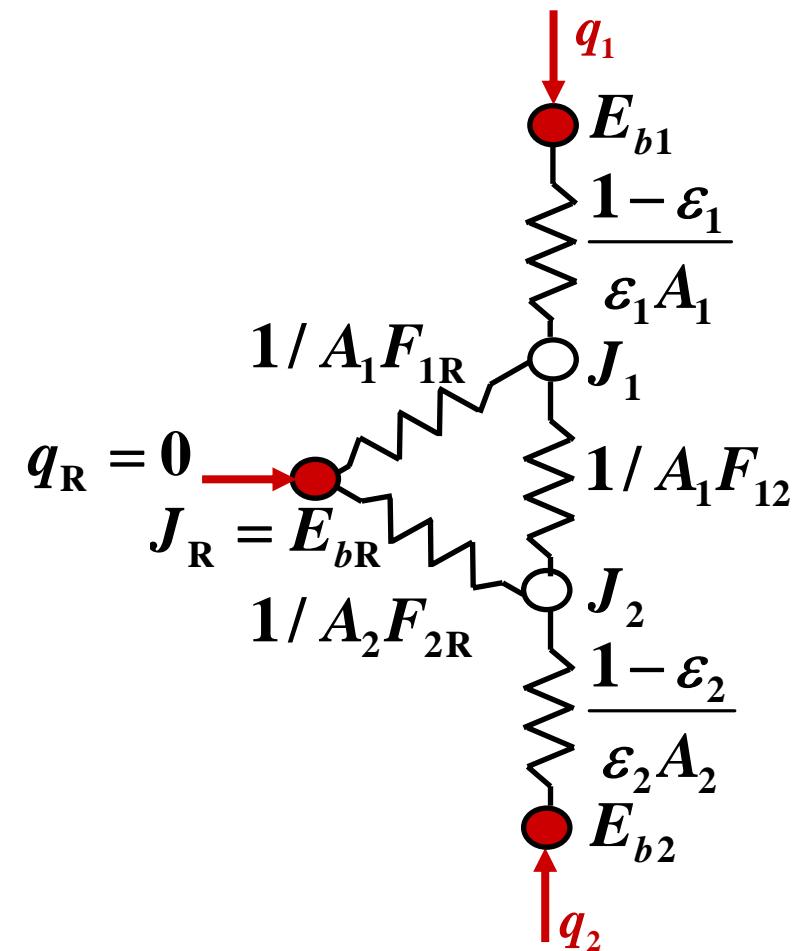
$$q_1 = \frac{E_{b1} - J_1}{\frac{1-\varepsilon_1}{\varepsilon_1 A_1}} = \frac{J_1 - J_2}{R} = \frac{J_2 - E_{b2}}{\frac{1-\varepsilon_2}{\varepsilon_2 A_2}}$$

$$J_1 = E_{b1} - \frac{1-\varepsilon_1}{\varepsilon_1 A_1} q_1 = 108,323 \text{ W/m}^2$$

$$J_2 = E_{b2} + \frac{1-\varepsilon_2}{\varepsilon_2 A_2} q_1 = 59,043 \text{ W/m}^2$$

$$E_{bR} = \sigma T_R^4 = 83,683 \text{ W/m}^2$$

$$T_R = \left( \frac{83,683}{5.67 \times 10^{-8}} \right)^{1/4} = 1102 \text{ K}$$



## Comments:

- 1) The results are independent of the value of  $\varepsilon_R$ .
- 2) This problem may also be solved using the matrix inversion method.

$$\frac{E_{b1} - J_1}{(1-\varepsilon_1)/\varepsilon_1 A_1} = \frac{J_1 - J_2}{1/A_1 F_{12}} + \frac{J_1 - J_R}{1/A_1 F_{1R}}$$

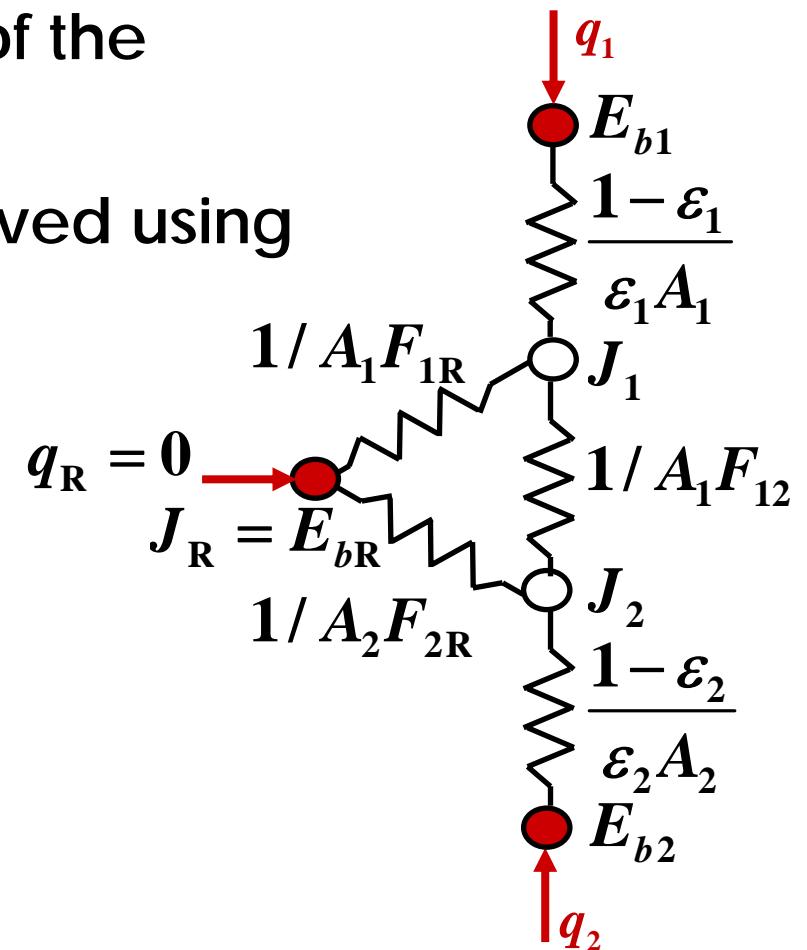
$$\frac{E_{b2} - J_2}{(1-\varepsilon_2)/\varepsilon_2 A_2} = \frac{J_2 - J_1}{1/A_2 F_{21}} + \frac{J_2 - J_R}{1/A_2 F_{2R}}$$

$$0 = \frac{J_R - J_1}{1/A_R F_{R1}} + \frac{J_R - J_2}{1/A_R F_{R2}}$$

$$10J_1 - J_2 - J_R = 940,584$$

$$-J_1 + 3.33J_2 - J_R = 4725$$

$$-J_1 - J_2 + 2J_R = 0$$



From these equations, the matrices are

$$\begin{bmatrix} 10 & -1 & -1 \\ -1 & 3.33 & -1 \\ -1 & -1 & 2 \end{bmatrix} \begin{bmatrix} J_1 \\ J_2 \\ J_R \end{bmatrix} = \begin{bmatrix} 940,584 \\ 4725 \\ 0 \end{bmatrix}$$

Solving the equation, it follows that

$$J_1 = 108,328 \text{ W/m}^2$$

$$J_2 = 59,018 \text{ W/m}^2$$

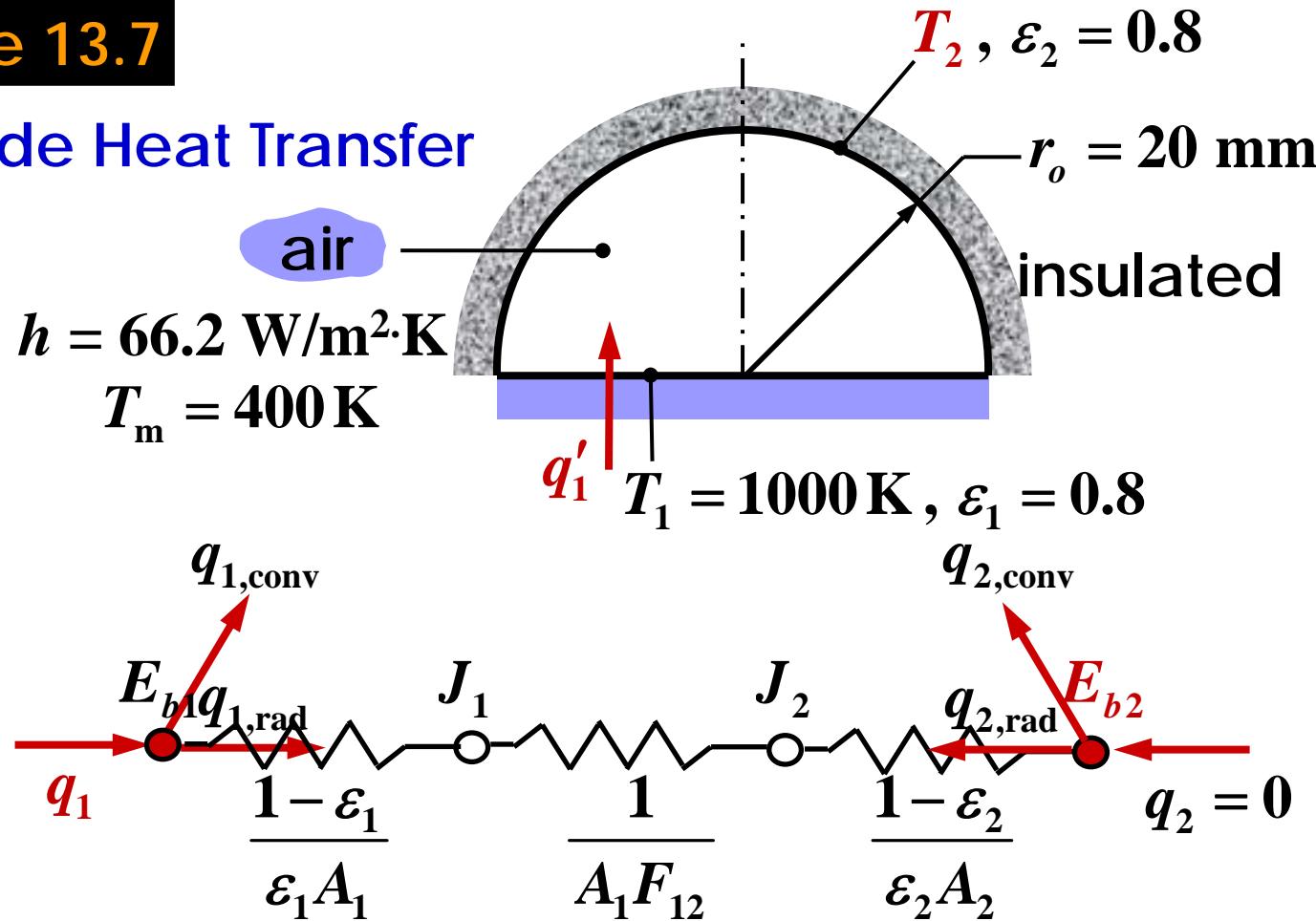
$$J_R = 83,673 \text{ W/m}^2$$

Recognizing that  $J_R = \sigma T_R^4$ ,

$$T_R = \left( \frac{J_R}{\sigma} \right)^{1/4} = \left( \frac{83,673}{5.67 \times 10^{-8}} \right)^{1/4} = 1102 \text{ K}$$

## Example 13.7

### Multimode Heat Transfer

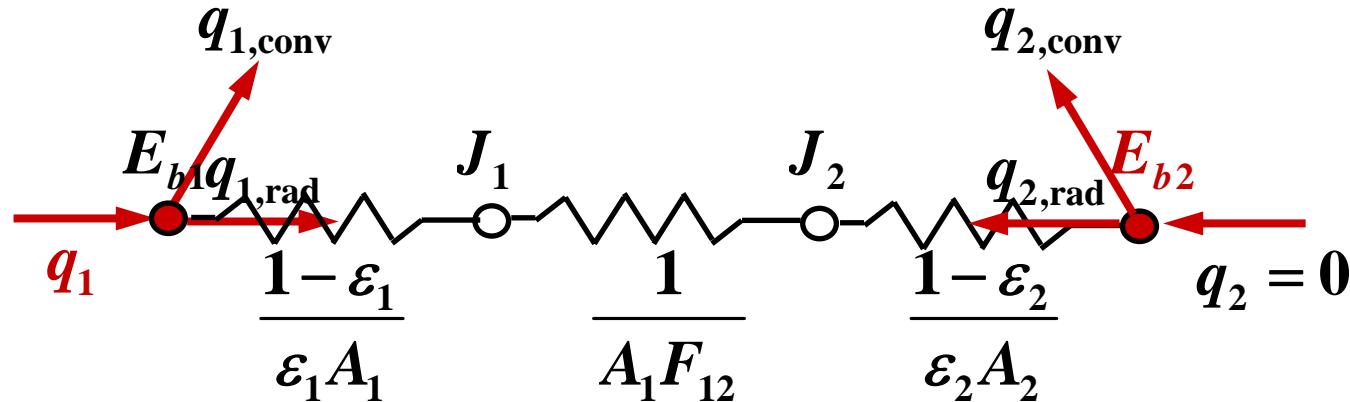


Find:

Rate at which heat must be supplied and temperature of insulated surface.

Assumption:

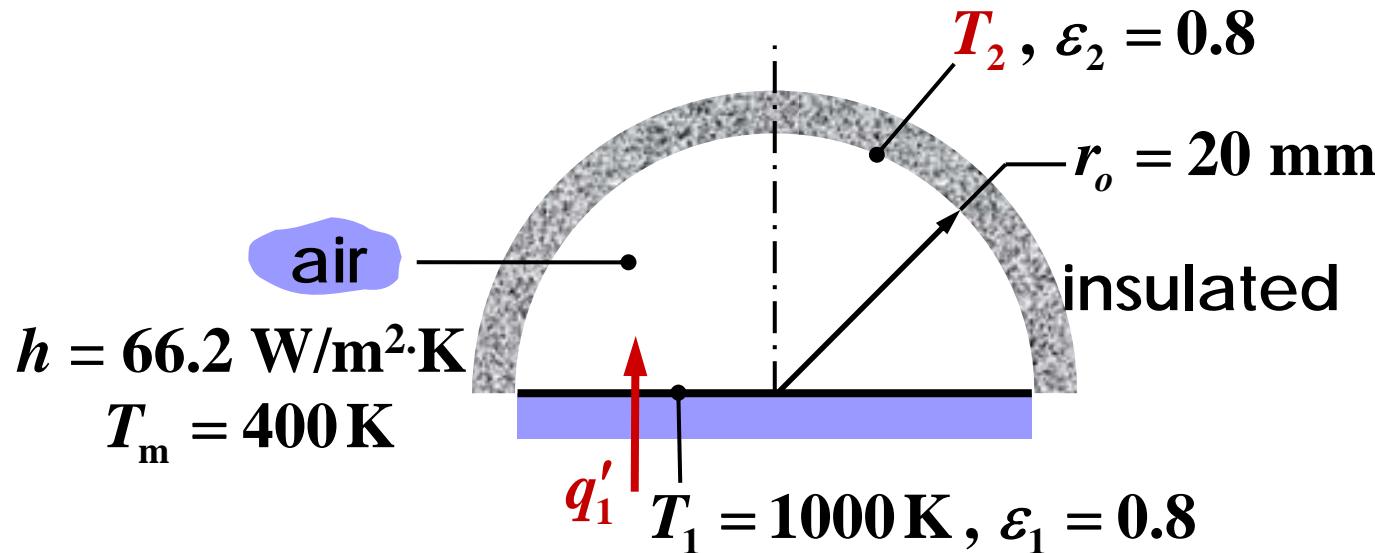
Diffuse, gray surfaces



$$\mathbf{q}_1 = \mathbf{q}_{1,\text{rad}} + \mathbf{q}_{1,\text{conv}}, \quad q_2 = q_{2,\text{rad}} + q_{2,\text{conv}} = 0$$

$$\mathbf{q}_1 = \frac{\sigma(T_1^4 - \mathbf{T}_2^4)}{\frac{1-\varepsilon_1}{\varepsilon_1 A_1} + \frac{1}{A_1 F_{12}} + \frac{1-\varepsilon_2}{\varepsilon_2 A_2}} + h A_1 (T_1 - T_m)$$

$$q_2 = \frac{\sigma(\mathbf{T}_2^4 - T_1^4)}{\frac{1-\varepsilon_1}{\varepsilon_1 A_1} + \frac{1}{A_1 F_{12}} + \frac{1-\varepsilon_2}{\varepsilon_2 A_2}} + h A_2 (\mathbf{T}_2 - T_m) = 0$$



$$\frac{\sigma(T_2^4 - T_1^4)}{\frac{1-\epsilon_1}{\epsilon_1 A_1} + \frac{1}{A_1 F_{12}} + \frac{1-\epsilon_2}{\epsilon_2 A_2}} + h A_2 (T_2 - T_m) = 0, \quad F_{12} = 1$$

$$5.67 \times 10^{-8} T_2^4 + 146.5 T_2 - 115,313 = 0 \rightarrow T_2 = 696 \text{ K}$$

$$q_1 = \frac{\sigma(T_1^4 - T_2^4)}{\frac{1-\epsilon_1}{\epsilon_1 A_1} + \frac{1}{A_1 F_{12}} + \frac{1-\epsilon_2}{\epsilon_2 A_2}} + h A_1 (T_1 - T_m) = 2820 \text{ W/m}$$

# Radiation in Participating Media

participating:

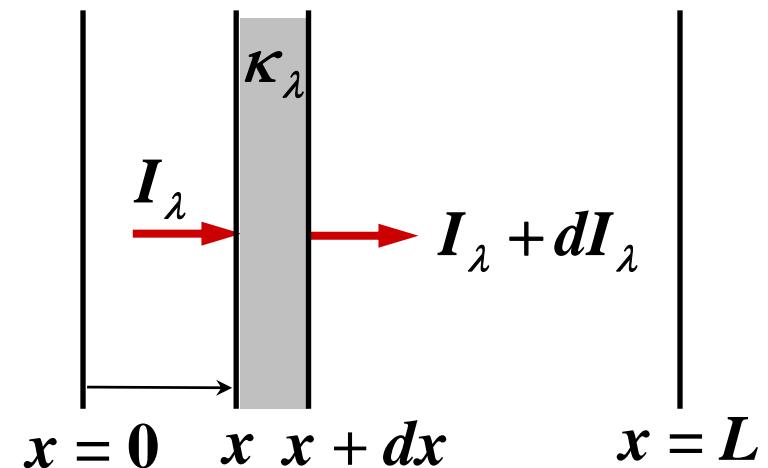
absorbing, emitting and scattering

## Attenuation by Absorption and Scattering

$$dI_\lambda = -\kappa_\lambda I_\lambda dx \quad (\text{experimental observation})$$

or  $\frac{dI_\lambda}{dx} = -\kappa_\lambda I_\lambda$

$\kappa_\lambda$ : extinction coefficient  
[cm<sup>-1</sup>]



$$\kappa_\lambda = \kappa_\lambda(\lambda, T, P, C_i)$$

$$\kappa_\lambda = a_\lambda + \sigma_\lambda$$

$a_\lambda$ : absorption coefficient

$\sigma_\lambda$ : scattering coefficient

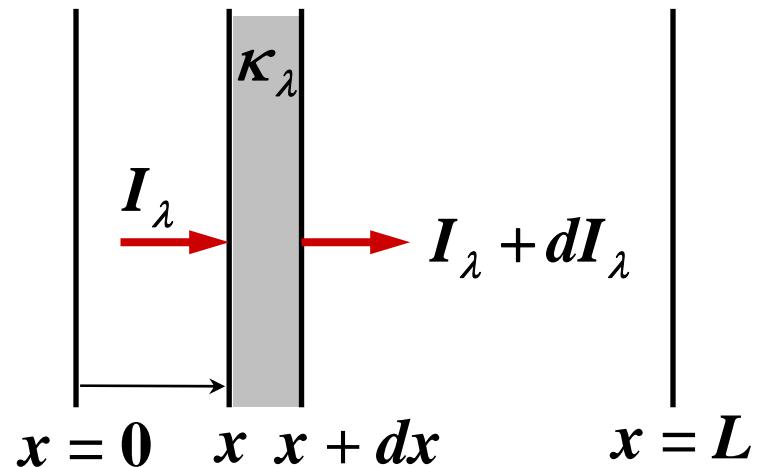
$$dI_\lambda = -\kappa_\lambda I_\lambda dx$$

$$\int_{I_\lambda(0)}^{I_\lambda(L)} \frac{dI_\lambda}{I_\lambda} = - \int_0^L \kappa_\lambda(x) dx$$

$$\ln \frac{I_\lambda(L)}{I_\lambda(0)} = - \int_0^L \kappa_\lambda(x) dx$$

$$I_\lambda(L) = I_\lambda(0) \exp \left[ - \int_0^L \kappa_\lambda(x) dx \right] : \text{Bouguer's law}$$

$$\text{When } \kappa_\lambda = \text{constant}, \quad I_\lambda(L) = I_\lambda(0) e^{-\kappa_\lambda L}$$



# Transmittance, Absorptance and Emittance

$$I_\lambda(L) = I_\lambda(0)e^{-\kappa_\lambda L}$$

transmittance

$$\tau_\lambda = \frac{I_\lambda(L)}{I_\lambda(0)} = e^{-\kappa_\lambda L}$$

absorptance

$$\alpha_\lambda = \frac{I_\lambda(0) - I_\lambda(L)}{I_\lambda(0)} = 1 - e^{-\kappa_\lambda L} = 1 - \tau_\lambda$$

emittance: when Kirchhoff's law is assumed

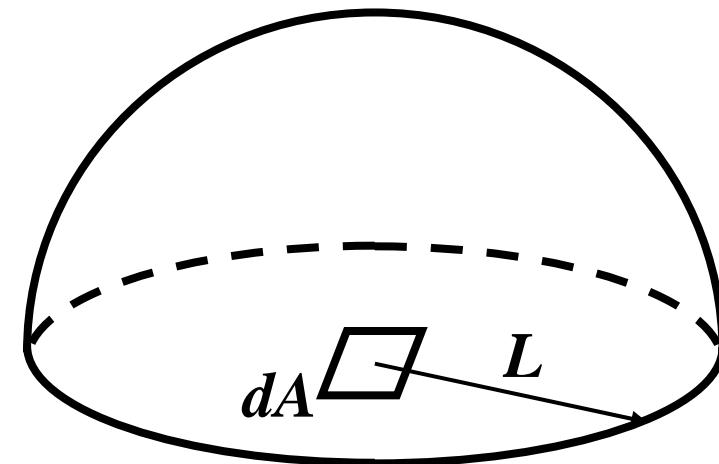
$$\alpha_\lambda = \epsilon_\lambda$$

# Gaseous Emission and Absorption

radiation emission from a hemispherical gas mass of temperature  $T_g$  to a surface element  $dA$ , which is located at the center of the hemisphere's base

$$E_g = \varepsilon_g \sigma T_g^4$$

$$\varepsilon_g = \varepsilon_g(T_g, P_g L)$$

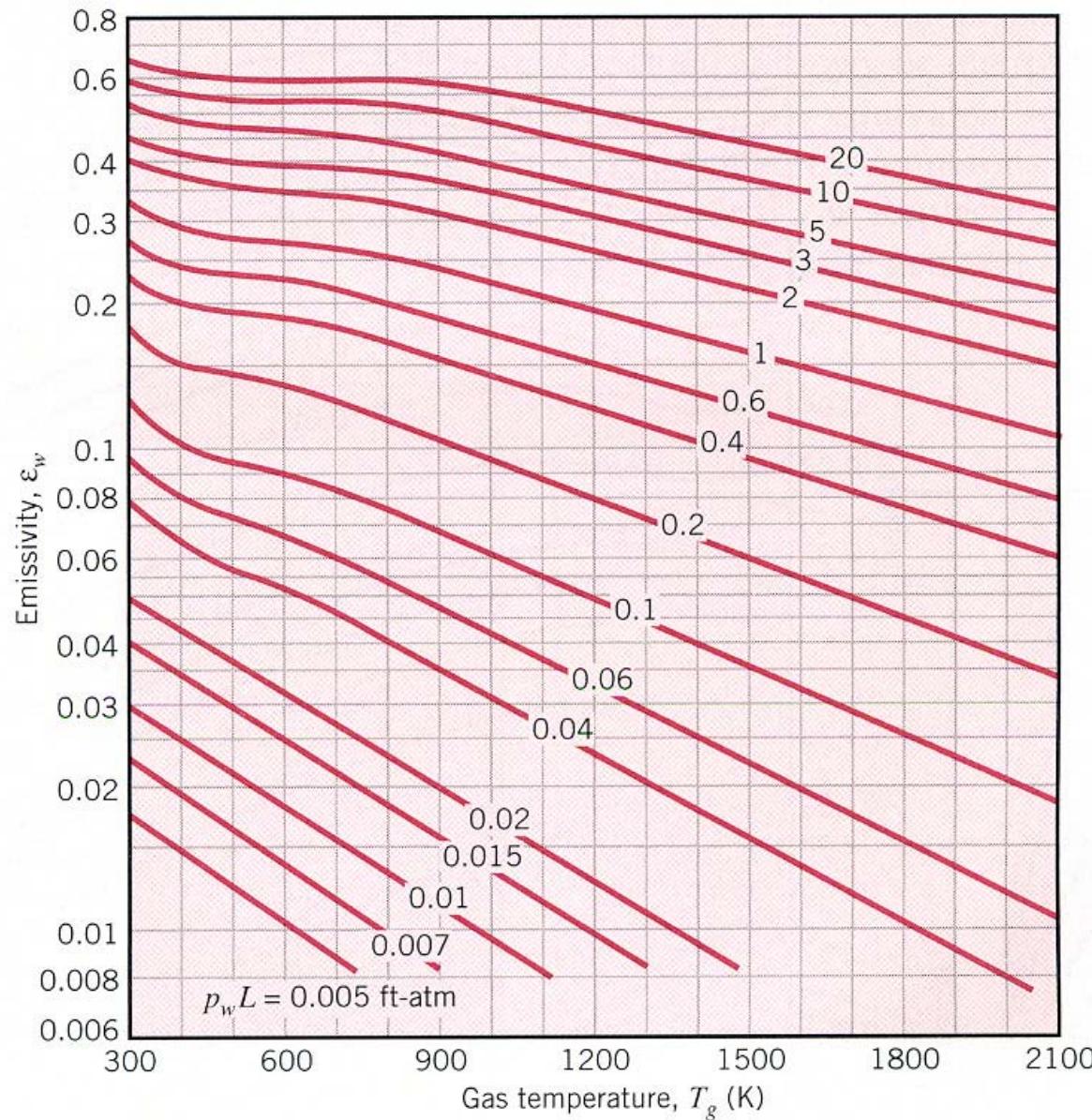


mixtures of water and carbon dioxide:

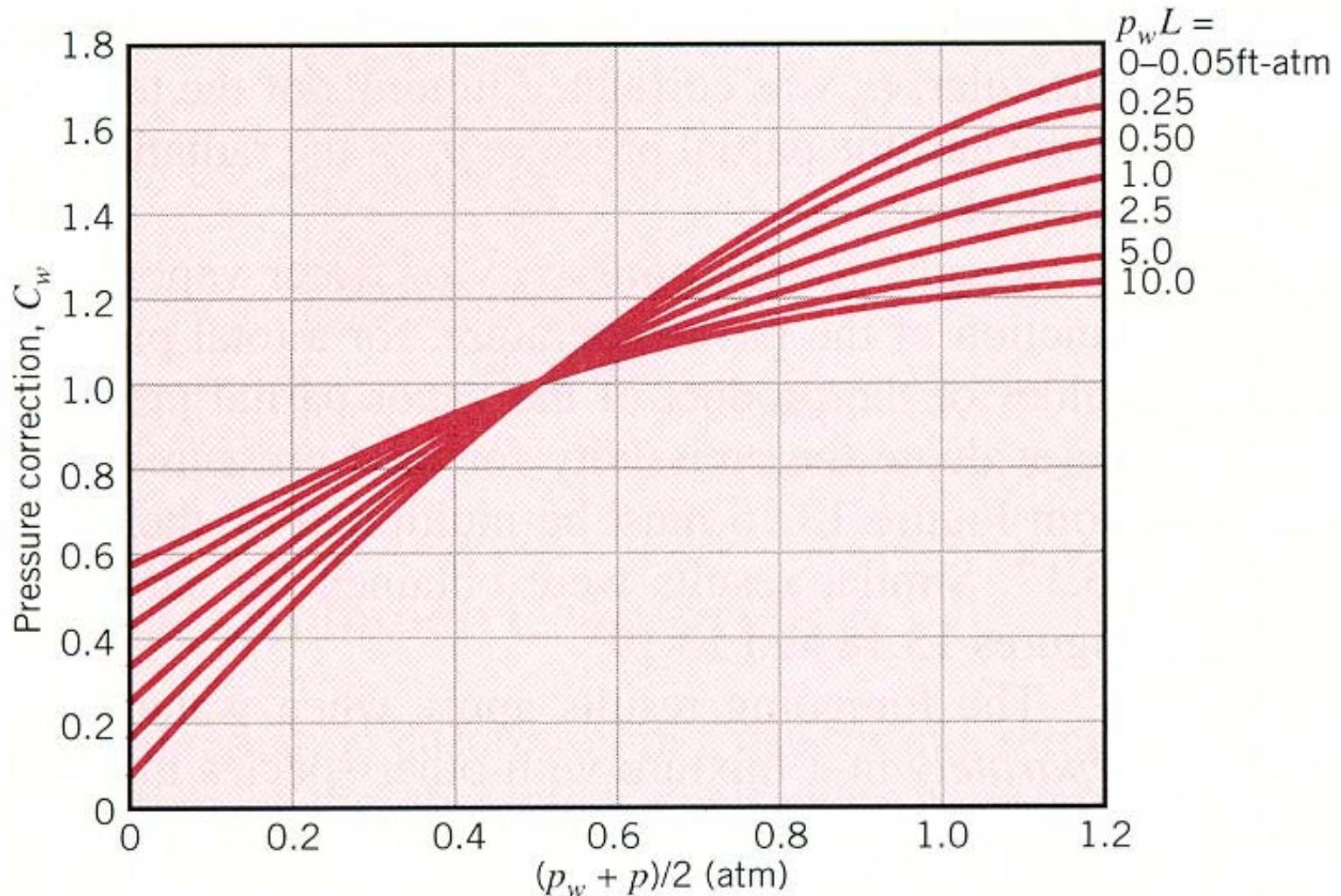
$$\varepsilon_g = \varepsilon_w + \varepsilon_c - \Delta\varepsilon$$

For geometries other than hemisphere:  
use mean beam length  $L_e$

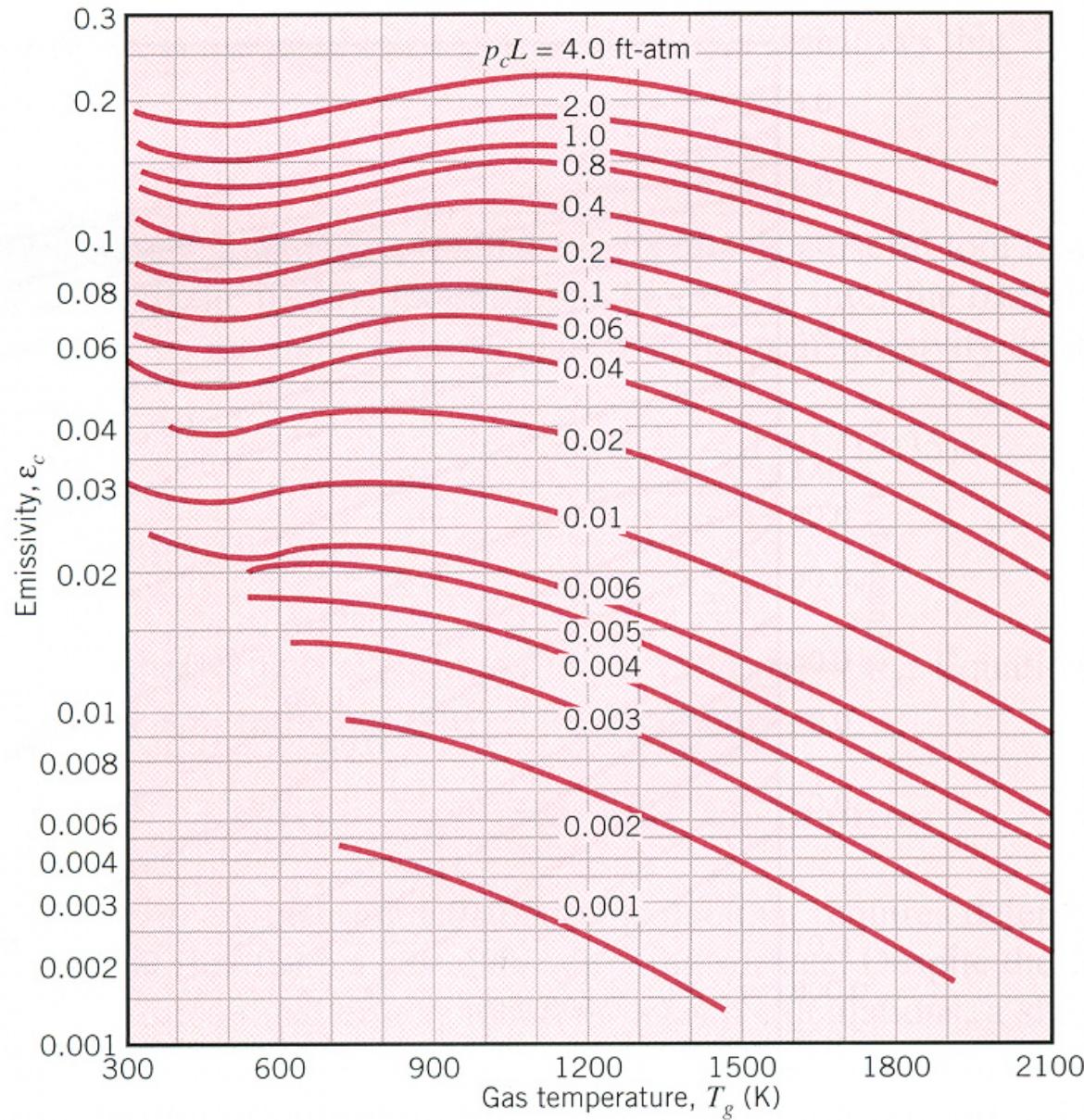
# Emissivity of water vapor in a mixture with nonradiating gases at 1-atm total pressure and of hemispherical shape



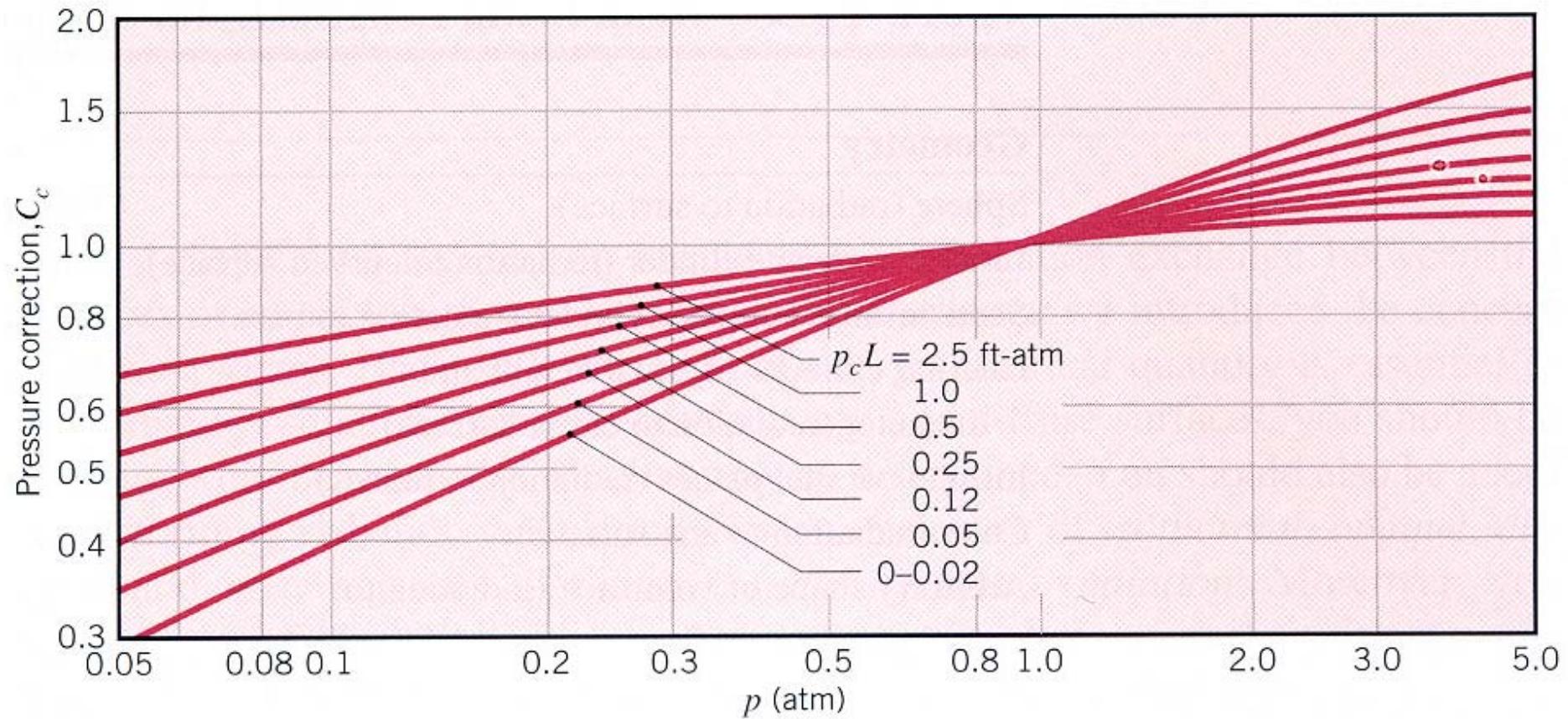
## Correction factor for obtaining water vapor emissivities at pressure other than 1 atm



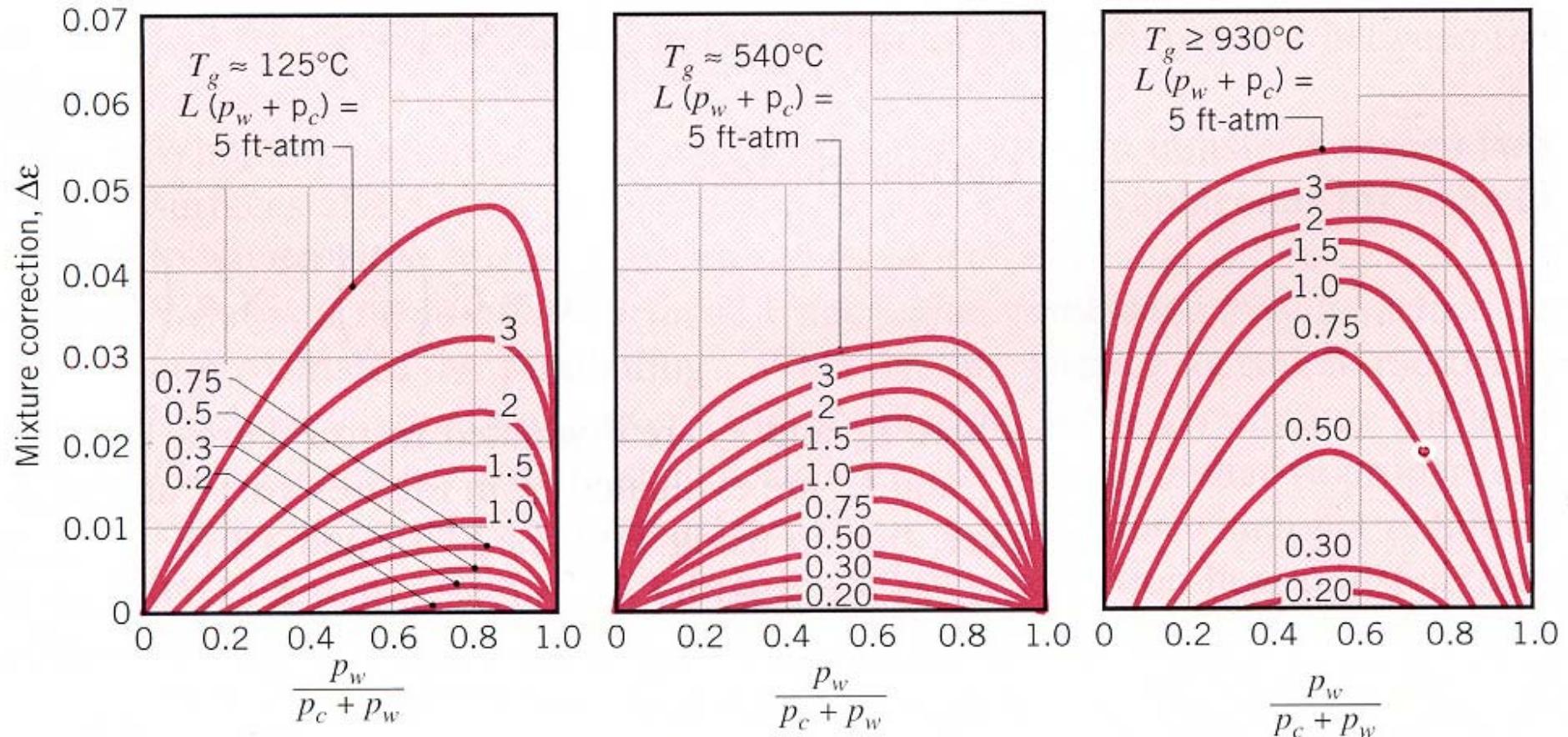
# Emissivity of carbon dioxide in a mixture with nonradiating gases at 1-atm total pressure and of hemispherical shape



# Correction factor for obtaining carbon dioxide emissivities at pressure other than 1 atm



# Correction factors associated with mixtures of water vapor and carbon dioxide



# Net Radiation Transfer from Gas Mass to Black Surfaces

$$q_{\text{net}} = A_s \sigma \left( \varepsilon_g T_g^4 - \alpha_g T_s^4 \right)$$

water:

$$\alpha_w = C_w \left( \frac{T_g}{T_s} \right)^{0.45} \times \varepsilon_w(T_s, P_w L_e \frac{T_s}{T_g})$$

carbon dioxide:

$$\alpha_c = C_c \left( \frac{T_g}{T_s} \right)^{0.65} \times \varepsilon_c(T_s, P_c L_e \frac{T_s}{T_g})$$