

# Yield Coefficient

$$Y_{X/S} = \frac{\Delta X}{\Delta S} = - \frac{dX}{dS}$$

$$\Delta S = \Delta S_{\text{assimilation into biomass}} + \Delta S_{\text{assimilation into an extracellular product}} + \Delta S_{\text{growth energy}} + \Delta S_{\text{maintenance energy}}$$

$$Y_{X/O_2} = \frac{\Delta X}{\Delta O_2} \quad Y_{P/S} = \frac{\Delta P}{\Delta S}$$

# Growth Yield

- For organisms growing aerobically on glucose
  - $Y_{x/s} = 0.4 - 0.6 \text{ g/g}$
  - $Y_{x/o_2} = 0.9 - 1.4 \text{ g/g}$
- In most cases the yield of biomass on a carbon-energy source is  $1.0 \pm 0.4 \text{ g biomass/g}$  of carbon consumed.

# Maintenance Coefficient

$$m \equiv \frac{[dS/dt]_m}{X}$$

- Maintenance
  - To repair damaged cellular components
  - To transfer some nutrients and products
  - For motility
  - To adjust the osmolarity

# Product Formation

- Growth-associated product formation
  - Specific rate of product formation

$$q_p = \frac{1}{X} \frac{dP}{dt} = Y_{p/x} \mu$$

$$\frac{dP}{dt} = Y_{p/x} \frac{dX}{dt}$$

- Nongrowth-associated product formation

$$q_p = \beta = \text{constant}$$

- Ex) many secondary metabolites such as antibiotics

# Product Formation

- Mixed-growth-associated product formation
  - Specific rate of product formation

$$q_p = \alpha \mu + \beta$$

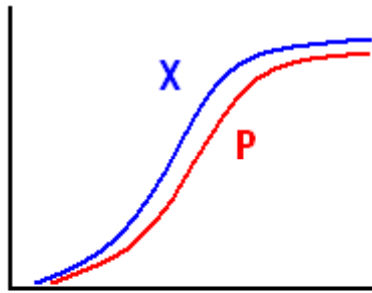
$$\frac{dP}{dt} = \alpha \frac{dX}{dt} + \beta X$$

(Luedeking-Piret Equation)

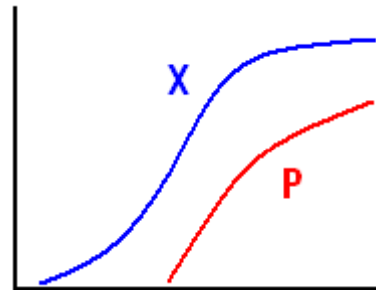
- Ex) lactic acid, xanthan gum, some secondary metabolites

# Kinetic Pattern of Product Formation

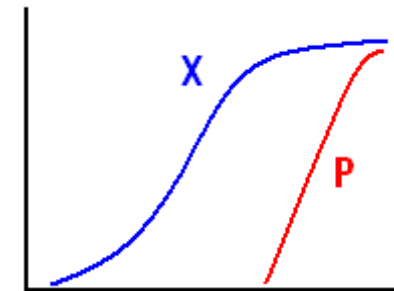
- Fig. 6.6



(a) growth-associated



(b) mixed-growth-associated



(c) nongrowth-associated

## 6.2.3. How Environmental Conditions Affect Growth Kinetics

- Effect of Temperature
  - Eqs. (6.19) and (6.20)
    - $E_a$ : activation energy for growth (10-20 kcal/mol)
    - $E_d$ : activation energy for thermal death (60-80 kcal/mol)
  - Thermal death is more sensitive to temperature changes than microbial growth.
  
- Fig. 6.7

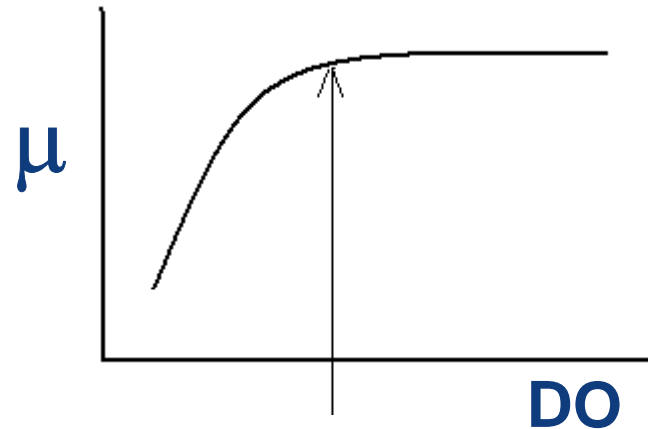
# Effect of pH

- pH optimum
  - Bacteria: 3~8
  - Yeast: 3~6
  - Mold: 3~7
  - Plant cell: 5~6
  - Animal cell: 6.5~7.5
- Fig. 6.8
- pH controller



# Effect of DO (dissolved oxygen)

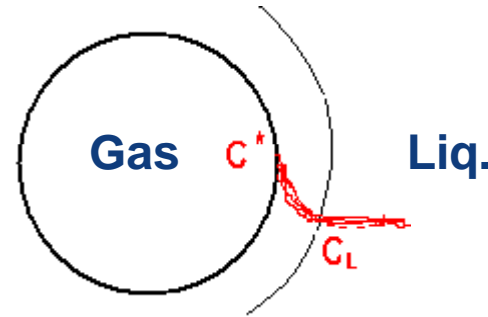
- Fig. 6.9



- Critical oxygen concentration
  - The growth rate is independent of DO above a critical oxygen concentration.
    - Bacteria and yeasts: 5%~10% of the saturated DO
    - Molds: 10~50% of the saturated DO  
(depending on the pellet size of molds)
  - Saturated DO in H<sub>2</sub>O at 25°C and 1 atm  $\approx$  7ppm
    - Salts and organic material alter the saturation value.

# Oxygen Transfer Rate (OTR)

- OTR from gas to liquid



$$\text{OTR} = N_{\text{O}_2} = k_L a (C^* - C_L)$$

- $N_{\text{O}_2}$  : OTR (mg  $\text{O}_2$  / L / h)
- $k_L$  : oxygen transfer coefficient (cm/h)
- $a$  : gas-liquid interfacial area ( $\text{cm}^2/\text{cm}^3$ )
- $k_L a$  : volumetric oxygen transfer coefficient (1/h)
- $C^*$  : saturated DO concentration (mg/L)
- $C_L$  : DO concentration in the broth (mg/L)

# Oxygen Uptake Rate (OUR)

- OUR from liquid to cell

$$\text{OUR} = q_{\text{O}_2} X = (\mu X) / Y_{\text{X/O}_2}$$

- $q_{\text{O}_2}$  : specific rate of oxygen consumption (mg O<sub>2</sub>/g cell/h)
- $Y_{\text{X/O}_2}$  : oxygen yield coefficient (g cell/g O<sub>2</sub>)

- When oxygen transfer is the rate-limiting step,



$$\text{OTR} (\rightarrow) = \text{OUR} (\rightarrow)$$

$$(\mu X) / Y_{\text{X/O}_2} = k_L a (C^* - C_L)$$

$$dX / dt = Y_{\text{X/O}_2} k_L a (C^* - C_L)$$