

[Case Study]

***E. coli* Fed-Batch Operation
with Exponential Feeding**

Productivity (g product/L hr)

- **Productivity**

$$Pd = \frac{\frac{CellMass}{Volume} (X) \times SpecificExpression(Ps)}{CultureTime}$$

- **Necessary condition**

- High cell density culture
- High specific expression

To Maximize Productivity

- **High cell density culture**
 - **By-product: acetic acid**
 - **Synthetic media: $\mu = 0.35 \text{ hr}^{-1}$**
 - **Complex media: $\mu = 0.2 \text{ hr}^{-1}$**
- **High specific expression**
 - **Expression vs. specific growth rate**
 - **Low μ , high product**
 - **Proteolytic degradation**

Feed Flow Rate Control in Fed-Batch Operation

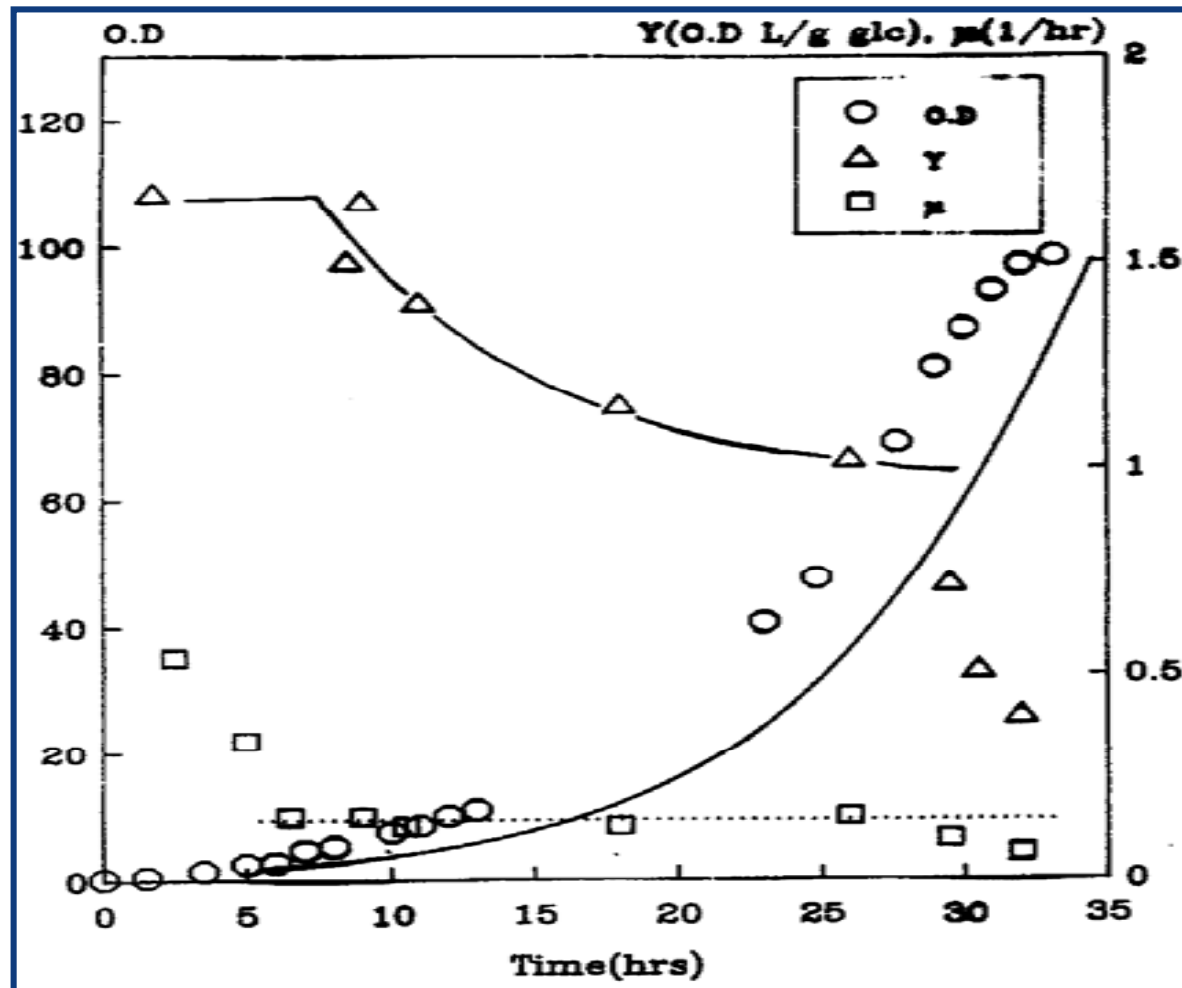
- **Feedback Control**
- **Feed Forward Control**
 - $\mu \uparrow$, acetic acid \uparrow , growth \downarrow , expression \downarrow

$$\mu = \frac{\mu_m S}{K_S + S}$$

Exponential Feeding

$$F = \frac{X_0 \times V_0 \times \mu \times e^{\mu t}}{S_F \times Y}$$

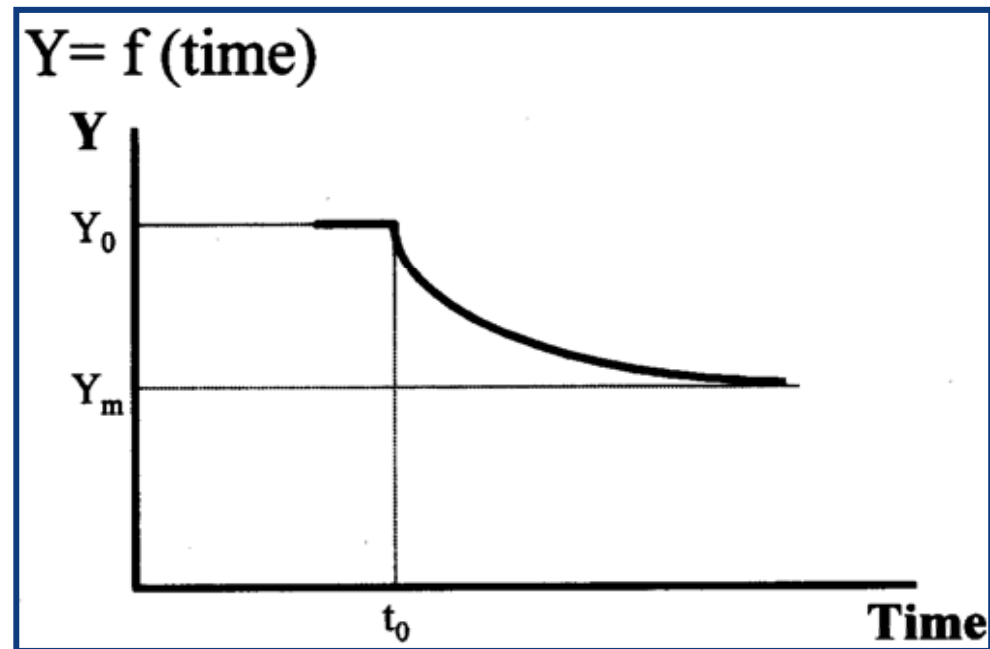
Fed-Batch Operation



Growth Yield

Yield

Time Variable



Growth Yield

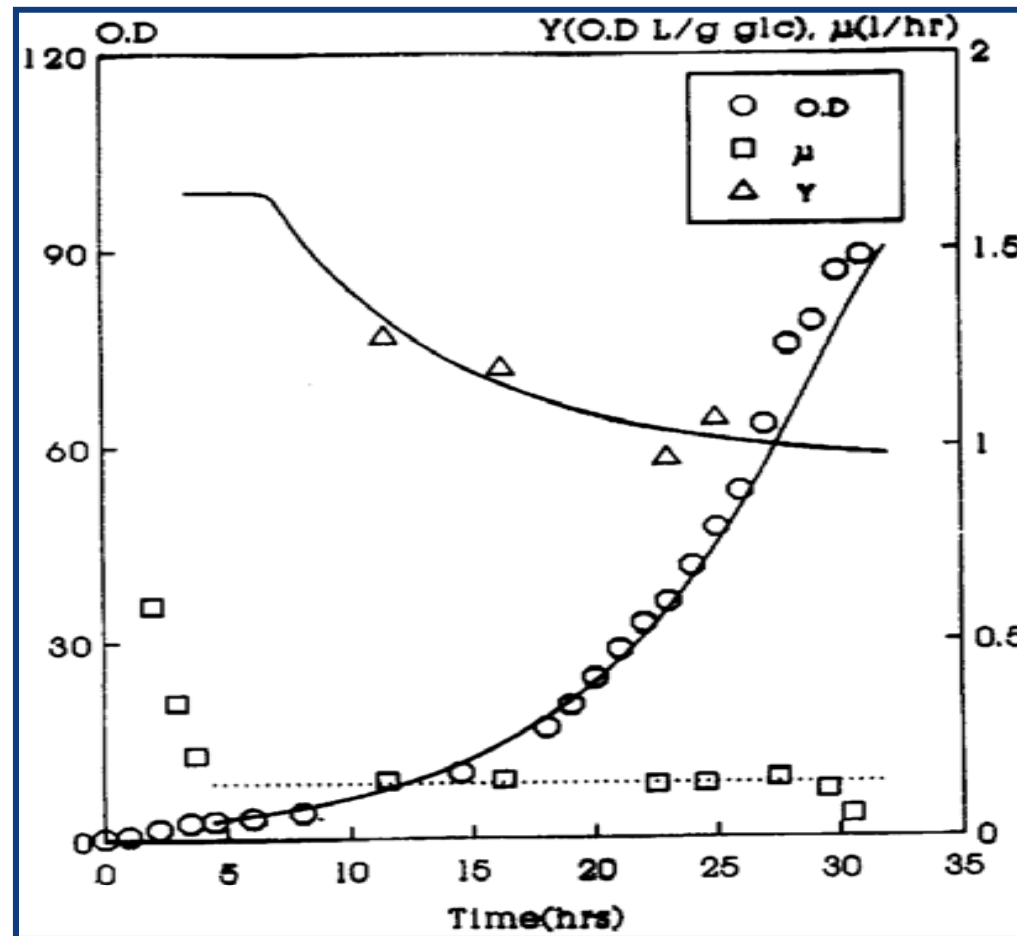
Yield

Time Variable

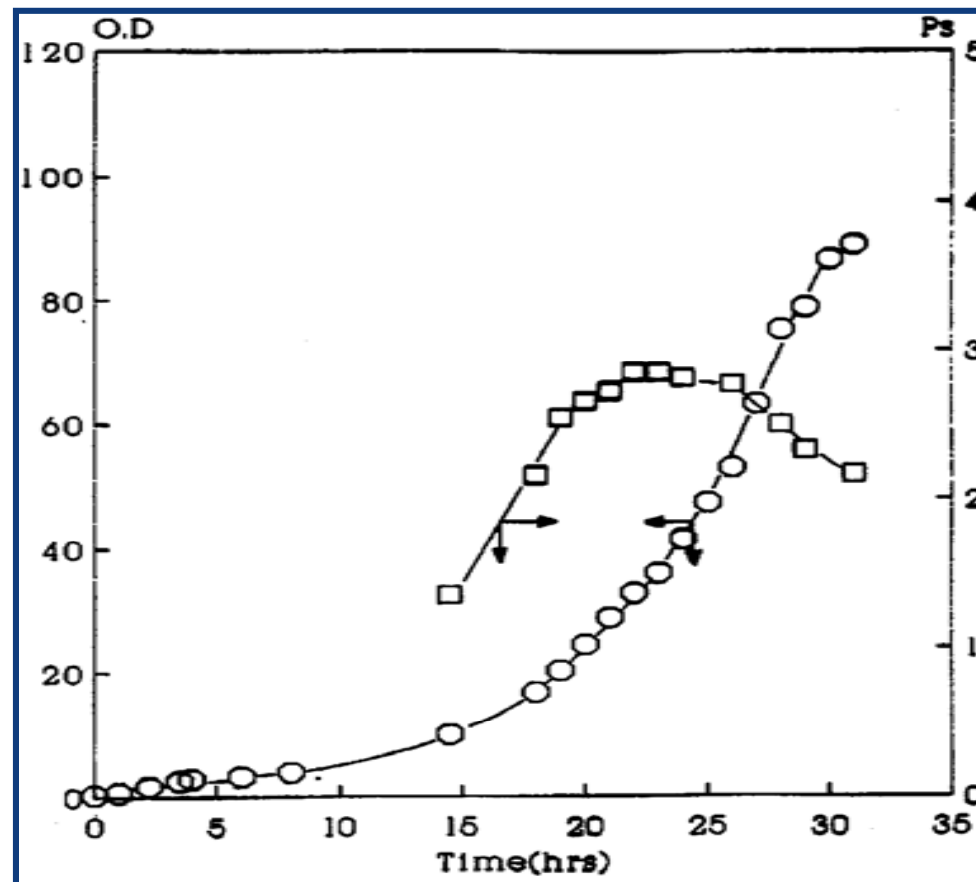
$$\frac{dY}{dt} = \frac{1}{ty} (Ym - Y), t = t_0, Y = Y_0$$

$$Y = 0.7 \text{Exp} \{ -(t - 8) / 8 \} + 0.95$$

Fed-Batch Operation



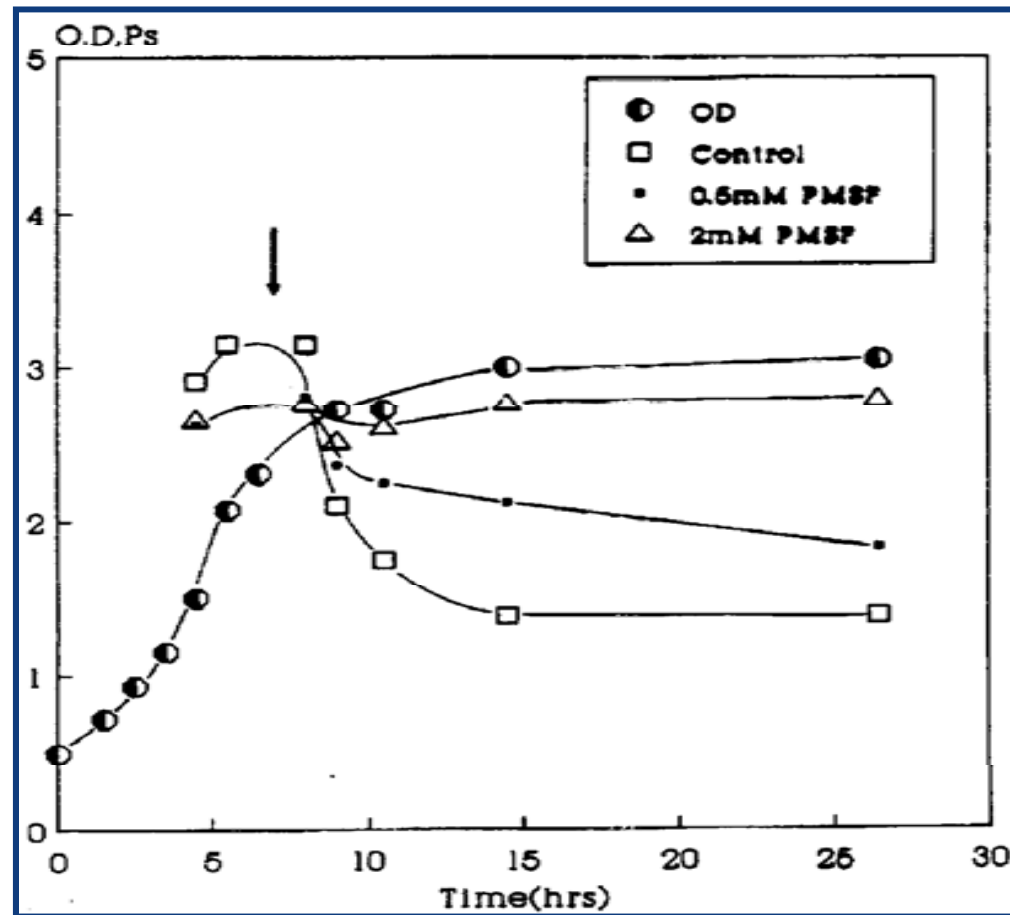
Fed-Batch Operation



Why does the specific expression rate decrease with the increase of cell density?

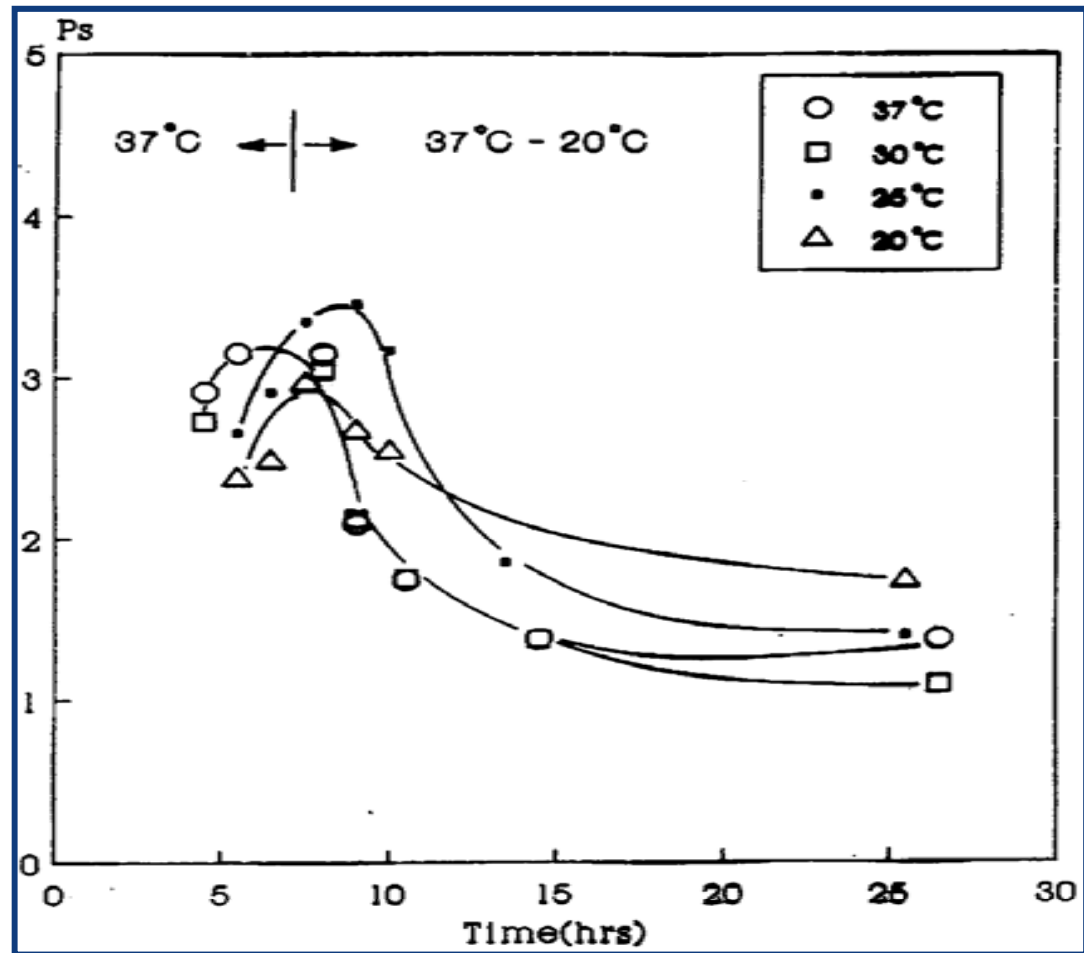
1. P_{O_2} limitation
 2. Glucose accumulation
 3. Acetic acid accumulation
 4. N source limitation
 5. P source limitation
 6. $MgSO_4$ limitation
 7. Plasmid instability
 8. Degradation by protease
- Low μ ,
Slow feeding,
Pure oxygen
- Ammonium phosphate
feeding
- $MgSO_4$ feeding
-

Effect of PMSF on Protein Degradation.



PMSF (Phenyl Methane Sulfonyl Fluoride)

Effect of Culture Temperature on Protein Degradation



Product Degradation by Protease

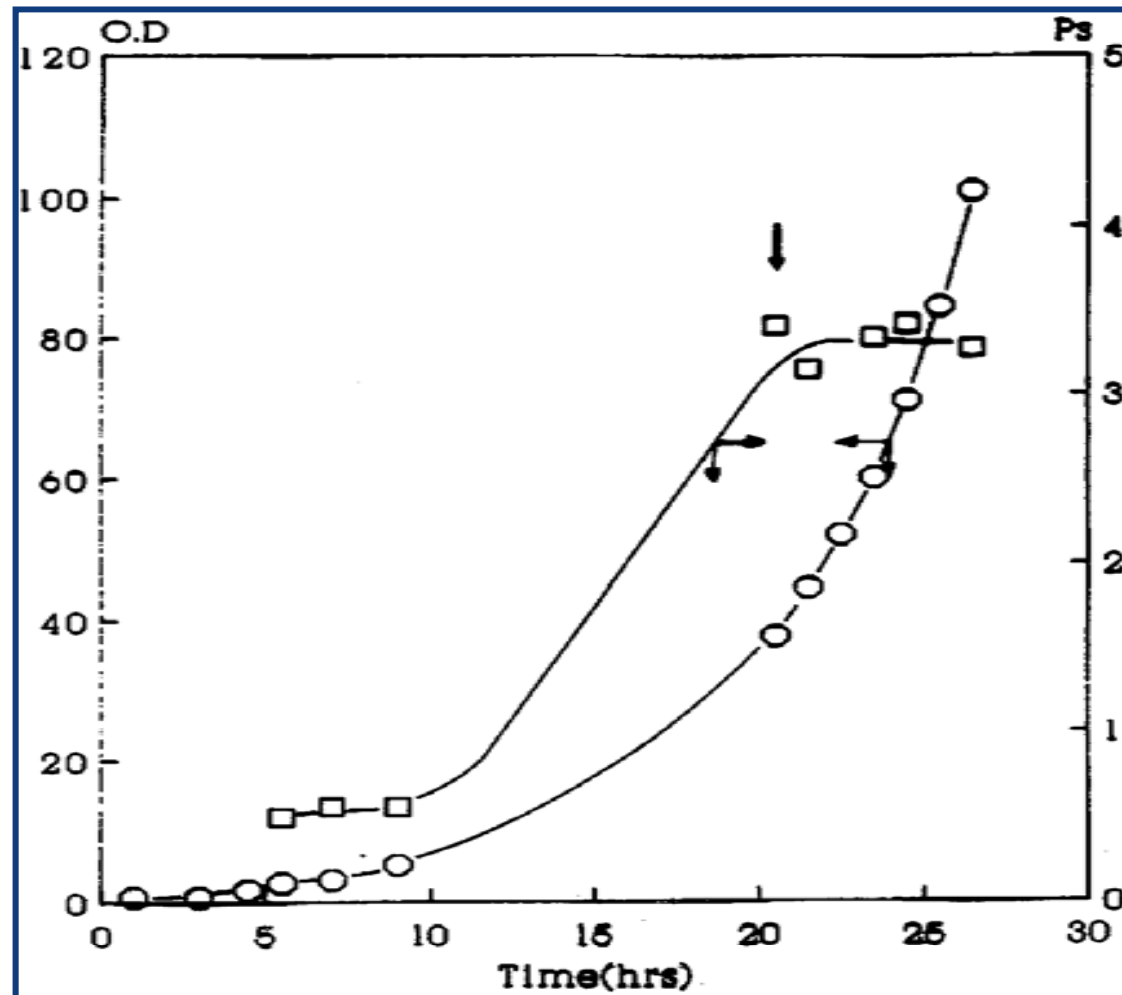
- Protease is induced under stressful conditions

- Depletion of Carbon or Nitrogen source
- High Temperature
- Expose to ethanol, UV

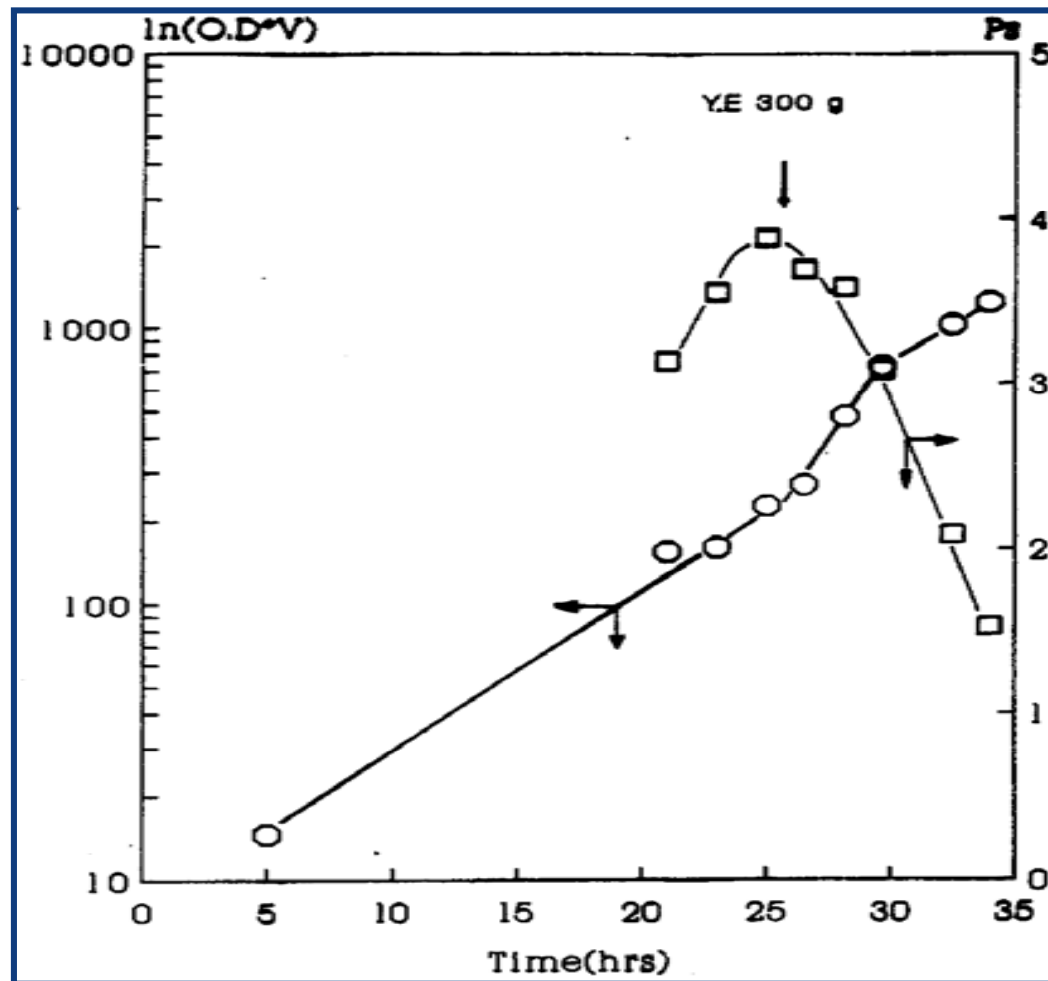
Composition of Modified Medium

Component	Concentration		
	Starting medium	Feeding medium 1	Feeding medium 2
Yeast Extract (g/L)	1.0	-	100
KH_2PO_4 (g/L)	15.0	-	-
$\text{MgSO}_4 \cdot 7\text{H}_2\text{O}$ (g/L)	4.0	-	15.5
Glucose	2.0	400	400
$\text{FeSO}_4 \cdot 7\text{H}_2\text{O}$ (mg/L)	-	200	200
$\text{CaCl}_2 \cdot 2\text{H}_2\text{O}$ (mg/L)	-	1300	1300
$\text{MnSO}_4 \cdot 5\text{H}_2\text{O}$ (mg/L)	-	67	67
$\text{CoCl}_2 \cdot 6\text{H}_2\text{O}$ (mg/L)	-	13	13
$\text{ZnSO}_4 \cdot 7\text{H}_2\text{O}$ (mg/L)	-	67	67
$\text{CuCl}_2 \cdot 5\text{H}_2\text{O}$ (mg/L)	-	13	13
$\text{Na}_2\text{MoO}_4 \cdot 2\text{H}_2\text{O}$ (mg/L)	-	13	13

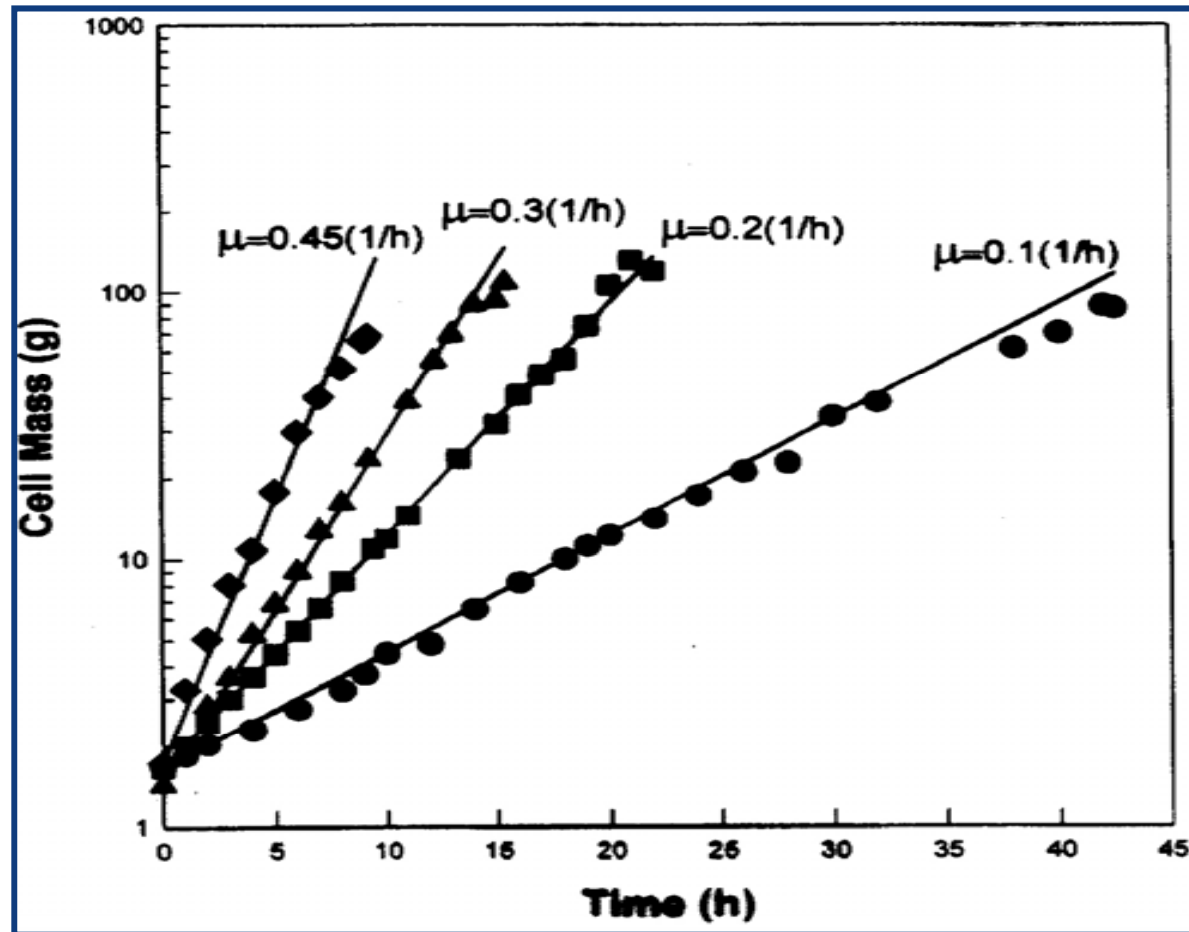
Fed-Batch Operation with YE



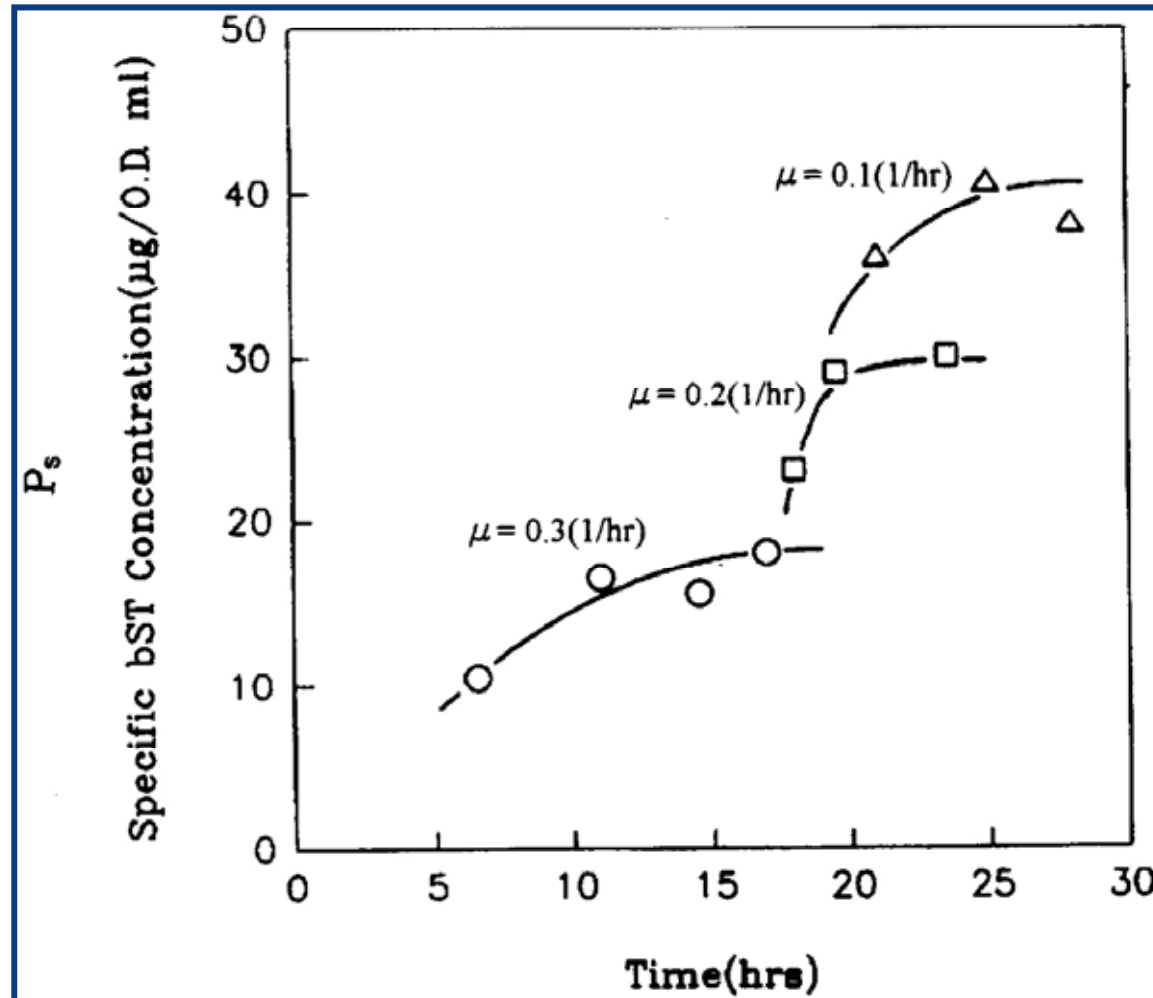
Fed-Batch Operation with YE



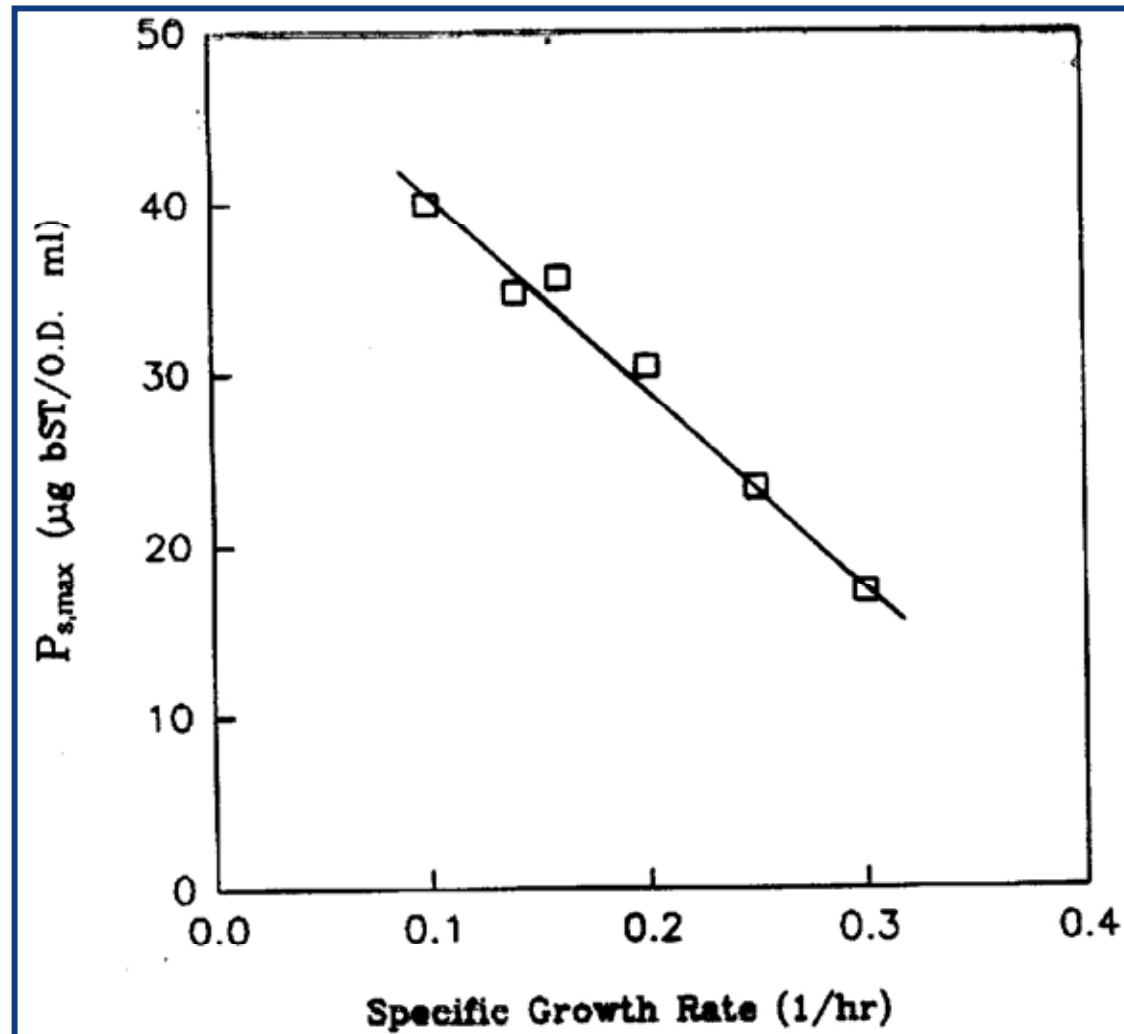
Fed-Batch Operation with Controlled Specific Growth Rate



Fed-Batch Operation with Controlled Specific Growth Rate



Effect of Specific Growth Rate on Expression



Productivity Maximization

$$P_{s,max} = -13.2\mu + 5.96$$

$$Pd = \frac{XP_{s,max}}{t}$$

$$[XV = X_0V_0e^{\mu t} \quad t = \frac{1}{\mu} \ln\left(\frac{XV}{X_0V_0}\right)]$$

$$= \frac{X\mu P_{s,max}}{\ln\left(\frac{XV}{X_0V_0}\right)}$$

- *Maximization of Pd*

Maximization of ($\mu P_{s,max}$)

$$\mu P_{s,max} = -13.2\mu^2 + 5.96\mu$$

$$\text{Optimum } \mu = 0.23 \text{ (1/hr)}$$

Optimum Specific Growth Rate for Maximum Productivity

