Chapter 2 Fluid Statics

- 2.1 Pressure-Density-Height Relationship
- 2.2 Absolute and Gage Pressure
- 2.3 Manometry
- 2.4 Forces on Submerged Plane Surfaces
- 2.5 Forces on Submerged Curved Surfaces
- 2.6 Buoyancy and Floatation
- 2.7 Fluid Masses Subjected to Acceleration

2.1 Pressure-Density-Height Relationship

Fluid statics

- ~ study of fluid problems in which there is no relative motion between fluid elements
 - → no velocity gradients
 - \rightarrow no shear stress
 - → only normal pressure forces are present

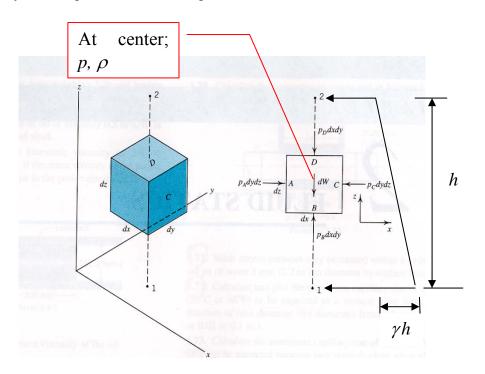
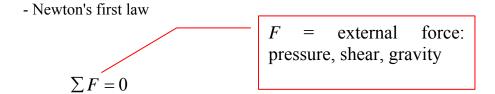


Fig. 2.1

- Static equilibrium of a typical differential element of fluid
 - vertical axis = z axis = direction parallel to the gravitational force field



$$\sum F_{x} = 0: \qquad \sum F_{x} = p_{A} dz - p_{c} dz = 0$$
Assume unit thickness in y direction; $dy = 1$

$$\sum F_z = 0: \quad \sum p_B dx - p_D dx - dW = 0 \tag{2.2}$$

in which p = f(x, z)

ch
$$p = f(x, z)$$

$$p_A = p - \frac{\partial p}{\partial x} \frac{dx}{2}$$

$$p_c = p + \frac{\partial p}{\partial x} \frac{dx}{2}$$
(1) $\frac{\partial p}{\partial x}$ = variation of pressure with x direction

$$p_B = p - \frac{\partial p}{\partial z} \frac{dz}{2}$$
 $p_D = p + \frac{\partial p}{\partial z} \frac{dz}{2}$ (2)

$$dW = \rho g dx dz = \gamma dx dz \tag{3}$$

Substituting (1) and (3) into (2.1) yields

$$dF_{x} = \left(p - \frac{\partial p}{\partial x}\frac{dx}{2}\right)dz - \left(p + \frac{\partial p}{\partial x}\frac{dx}{2}\right)dz = -\frac{\partial p}{\partial x}dxdz = 0$$

$$\rightarrow \frac{\partial p}{\partial x} = 0$$
(A)

Substituting (2) and (3) into (2.2) yields

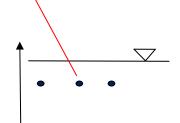
$$dF_z = \left(p - \frac{\partial p}{\partial z} \frac{dz}{2}\right) dx - \left(p + \frac{\partial p}{\partial z} \frac{dz}{2}\right) dx - \gamma dx dz = -\frac{\partial p}{\partial z} dz dx - \gamma dx dz = 0$$

$$\rightarrow \frac{\partial p}{\partial z} = \frac{dp}{dz} = -\gamma = -\rho g \quad \text{(partial derivative} \rightarrow \text{total derivative because of (A))}$$

$$\frac{\partial p}{\partial x} = 0 \quad (:. \ p = fn(z \ only))$$

$$(1) \quad \frac{\partial p}{\partial x} = 0$$

$$p_1 = p_2 = p_3$$



- ~ no variation of pressure with horizontal distance
- ~ pressure is constant in a horizontal plane in a static fluid

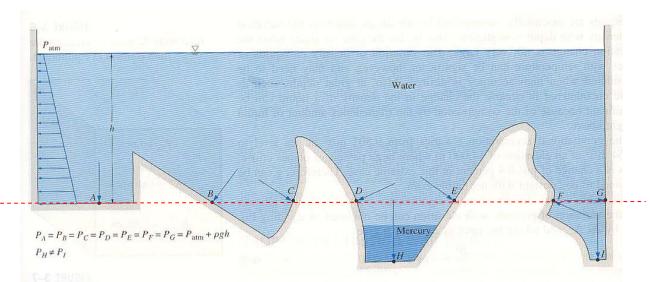


FIGURE 3-9

The pressure is the same at all points on a horizontal plane in a given fluid regardless of geometry, provided that the points are interconnected by the same fluid.

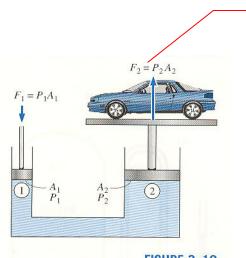


FIGURE 3–10 Lifting of a large weight by a small force by the application

of Pascal's law.

 $p_1 = p_2$

 $\frac{F_1}{A_1} = \frac{F_2}{A_2}$

 $F_2 = \frac{A_2}{A_1} F_1$

 $\frac{A_2}{A_1}$ = mechanical advantage

of hydraulic lift

(2) $\frac{dp}{dz} = -\gamma$ (minus sign indicates that as z gets larger, the pressure gets smaller)

$$\rightarrow -dz = \frac{dp}{\gamma}$$

$$\int_{z_1}^{z_2} -dz = \int_{p_1}^{p_2} \frac{dp}{\gamma}$$

Integrate over depth

$$(z_2 - z_1) = -\int_{p_1}^{p_2} \frac{dp}{\gamma} = \int_{p_2}^{p_1} \frac{dp}{\gamma}$$
 (2.4)

For fluid of constant density (incompressible fluid; $\gamma = \text{const.}$)

$$z_2 - z_1 = h = \frac{p_1 - p_2}{\gamma}$$

$$\therefore p_1 - p_2 = \gamma (z_2 - z_1) = \gamma h$$

$$\therefore p_1 = p_2 + \gamma h$$

$$(2.5)$$

- \sim increase of pressure with depth in a fluid of constant density \rightarrow <u>linear increase</u>
- \sim expressed as a head h of fluid of specific weight γ
- ~ heads in millimeters of mercury, meters of water; $\frac{\Delta p}{\gamma} = h$ (m)
- [Cf] For compressible fluid, $\gamma = fn(z \ or \ p)$
- [Re] External forces
 - 1) body force forces acting on the fluid element
 - gravity force, centrifugal force, Corioli's force (due to Earth's rotation)
 - 2) surface force forces transmitted from the surrounding fluid and acting at right angles

against sides of the fluid element

- pressure, shear force

• Manometer or Piezometer

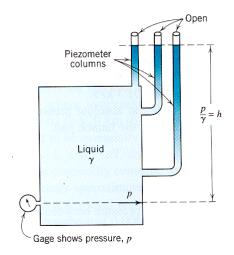


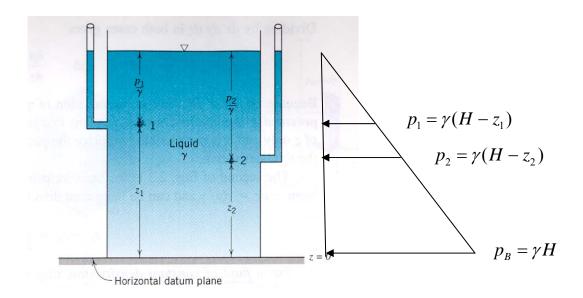
Fig. 2.2

h = height of a column of any fluid

$$h \text{ (m of H2O)} = \frac{p \text{ (kN/m}^2)}{9.81 \text{ kN/m}^3} = 0.102 \times p \text{ (kN/m}^2)$$

• For a static fluid

$$\frac{p_1}{\gamma} + z_1 = \frac{p_2}{\gamma} + z_2 = \text{const.}$$
 (2.6)



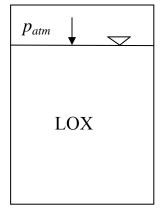
- For a fluid of variable density (compressible fluid)
 - ~ need to know a relationship between p and γ
 - ~ oceanography, meteorology

[IP 2.1] The liquid oxygen (LOX) tank of space shuttle booster is filled to a depth of 10 m with LOX at -196°C. The absolute pressure in the vapor above the liquid surface is 101.3 kPa. Calculate absolute pressure at the inlet valve.

[Sol]

From App. 2 (Table A2.1) $\rho \text{ of LOX at -196°C} = 1,206 \text{ kg/m}^3$ $p_2 = p_{atm} + \gamma_{LOX} h$ $p_2 = 101.3 \text{ kPa+ (1,206 kg/m}^3) \text{ (9.81 m/s}^2\text{) (10 m)}$ $= 101.3 \text{ kPa+ } 118,308 \text{ kg} \cdot \text{m/s}^2/\text{m}^2$ = 101.3 kPa+ 118,308 kPa

= 219.6 kPa absolute



2.2 Absolute and Gage Pressure

1) absolute pressure =
$$\begin{cases} \text{atmospheric pressure + gage pressure for } p > p_{atm} \\ \text{atmospheric pressure - vacuum for } p < p_{atm} \end{cases}$$

2) relative (gage) pressure $\rightarrow p_{atm} = 0$

Bourdon pressure gage ~ measure gage pressure ⇒ open U-tube manometer
 Aneroid pressure gage ~ measure absolute pressure ⇒ mercury barometer

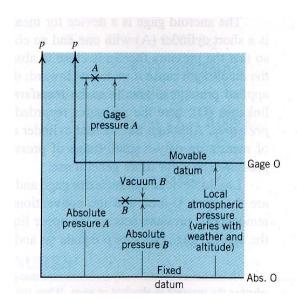


Fig. 2.6

- gage pressure is normally substituted by "pressure"
- Mercury barometer (Fig. 2.5)
 - ~ invented by Torricelli (1643) measure absolute pressure/local atmospheric pressure
 - ~ filling tube with air-free mercury
 - ~ inverting it with its open end beneath the mercury surface in the receptacle

[IP 2.4] A Bourdon gage registers a vacuum of 310 mm of mercury;

$$p_{atm} = 100$$
 kPa, absolute. Gage pressure

Find Absolute pressure.

[Sol] absolute pressure = 100 kPa - 310 mm Hg

$$=100 \text{ kPa} - 310 \left(\frac{101.3 \text{ kPa}}{760} \right) = 58.7 \text{ kPa}$$

[Re] App. 1

$$760 \text{ mmHg} = 101.3 \text{ kPa} = 1,013 \text{ mb} \rightarrow 1 \text{ mmHg} = 101,300 / 760 = 133.3 \text{ Pa}$$

1 bar =
$$100 \text{ kPa} = 10^3 \text{ mb}$$

$$760 \text{ mmHg} = 760 \times 10^{-3} \text{ m} \times 13.6 \times 9,800 \text{ N/m}^3 = 101.3 \text{ kN/m}^2$$

=
$$101,300 \text{ N/m}^2 / 9,800 \text{ N/m}^3 = 10.3 \text{ m of H}_2\text{O}$$

2.3 Manometry

~ more precise than Bourdon gage (mechanical gage)

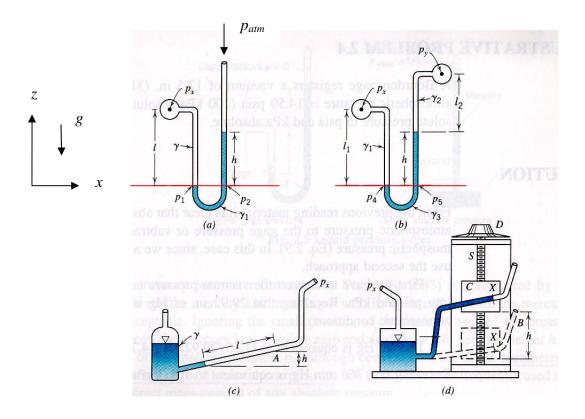


Fig. 2.7

(i) U-tube manometer

~ over horizontal planes within continuous columns of the same fluid,

pressures are equal
$$\left(\because \frac{\partial p}{\partial x} = 0\right)$$

$$\rightarrow p_1 = p_2$$

$$p_1 = p_x + \gamma l$$

$$p_2 = 0 + \gamma_1 h$$

$$P_{atm} \to 0$$

$$p_1 = p_2$$
; $p_x + \gamma l = 0 + \gamma_1 h$

$$\therefore p_x = \gamma_1 h - \gamma l$$

(ii) Differential manometer

~ measure difference between two unknown pressures

$$p_4 = p_5$$

$$p_4 = p_x + \gamma_1 l_1 \qquad p_5 = p_y + \gamma_2 l_2 + \gamma_3 h$$

$$p_x + \gamma_1 l_1 = p_y + \gamma_2 l_2 + \gamma_3 h$$

$$\therefore p_x - p_y = \gamma_2 l_2 + l_3 h - \gamma_1 l_1$$

If $\gamma_1 = \gamma_2 = \gamma_w$ and x and y are horizontal

$$p_x - p_y = \gamma_3 h + \gamma_w (\underline{l_2 - l_1})$$

$$= \gamma_3 h + \gamma_w (-h) = (\gamma_3 - \gamma_w) h$$

head:
$$\frac{p_x - p_y}{\gamma_w} = \left(\frac{\gamma_3}{\gamma_w} - 1\right)h$$

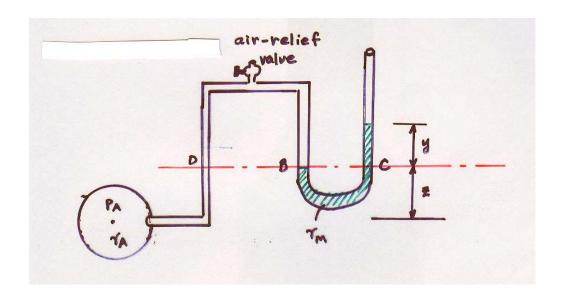
(iii) Inclined gages

~ measure the comparatively small pressure in low-velocity gas flows

$$p_{x} = \gamma h = \gamma l \sin \theta$$

reading of $l > \text{reading of } h \rightarrow \text{accurate}$

(iv) Open-end manometer



$$p_D = p_B = p_C$$

$$p_D = p_A - \gamma_A z$$

$$p_c = p_{atm} + \gamma_M y$$

$$p_{\scriptscriptstyle A} = p_{\scriptscriptstyle atm} + \gamma_{\scriptscriptstyle M} \, y + \gamma_{\scriptscriptstyle A} z$$

head:
$$\frac{p_A}{\gamma_A} = \frac{p_{atm}}{\gamma_A} + \frac{\gamma_M}{\gamma_A} y + z$$

(v) Measure vacuum

$$p_{1} = p_{2}$$

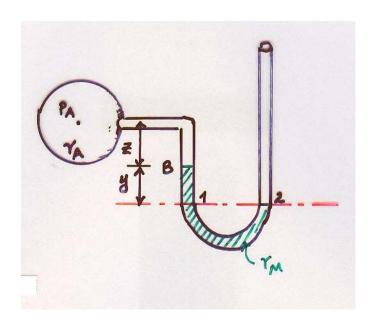
$$p_{1} = p_{A} + \gamma_{A}z + \gamma_{M}y$$

$$p_{2} = p_{atm}$$

$$p_{A} + \gamma_{A}z + \gamma_{M}y = p_{atm}$$

$$p_{A} = p_{atm} - \gamma_{A}z - \gamma_{M}y$$

$$p_{A} < p_{atm} \rightarrow vacuum$$



(vi) Differential manometer

$$p_{1} = p_{2}$$

$$p_{1} = p_{A} - \gamma z_{A}$$

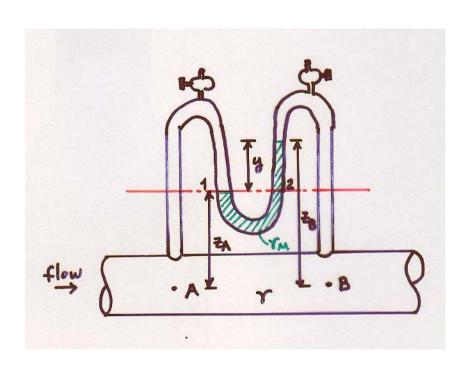
$$p_{2} = p_{B} - \gamma z_{B} + \gamma_{M} y$$

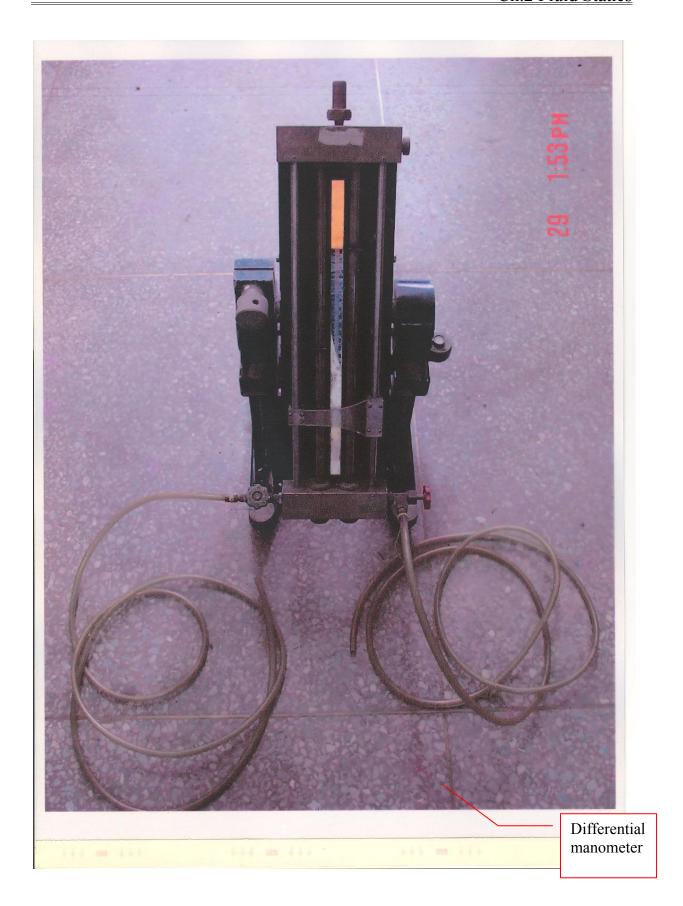
$$\therefore p_{A} - \gamma z_{A} = p_{B} - \gamma z_{B} + \gamma_{M} y$$

$$p_{A} - p_{B} = \gamma(z_{A} - z_{B}) + \gamma_{M} y$$

$$= -\gamma y + \gamma_{M} y = (\gamma_{M} - \gamma) y$$

$$\frac{p_{A} - p_{B}}{\gamma} = \left(\frac{\gamma_{M}}{\gamma} - 1\right) y$$
If $\gamma = \gamma_{w} \to \frac{p_{A} - p_{B}}{\gamma_{w}} = (s.g._{M} - 1) y$



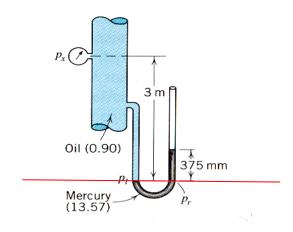




For measuring large pressure difference,

- \rightarrow use heavy measuring liquid, such as mercury $s.g. = 13.55 \rightarrow$ makes y small For a small pressure difference,
 - \rightarrow use a light fluid such as oil, or even air s.g. < 1
- Practical considerations for manometry
 - ① Temperature effects on densities of manometer liquids should be appreciated.
 - ② Errors due <u>to capillarity</u> may frequently be canceled by selecting manometer tubes of uniform sizes.

[IP 2.5] The vertical pipeline shown contains oil of specific gravity 0.90. Find p_x



[Sol]

2.4 Forces on Submerged Plane Surfaces

- Calculation of magnitude, direction, and location of the total forces on surfaces submerged in a liquid is essential.
 - → design of dams, bulkheads, gates, tanks, ships
- Pressure variation for non-horizontal planes

$$\frac{\partial p}{\partial z} = -\gamma$$

$$\therefore p = \gamma h$$

→ The pressure varies linearly with depth.

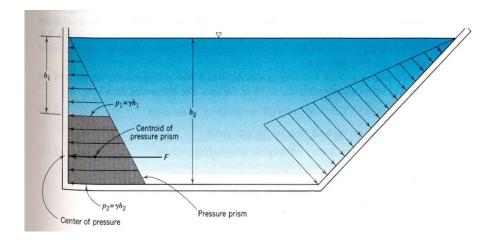


Fig. 2.8

Dams & gates

Spillway



Arch dam

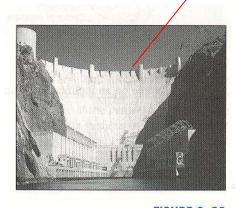
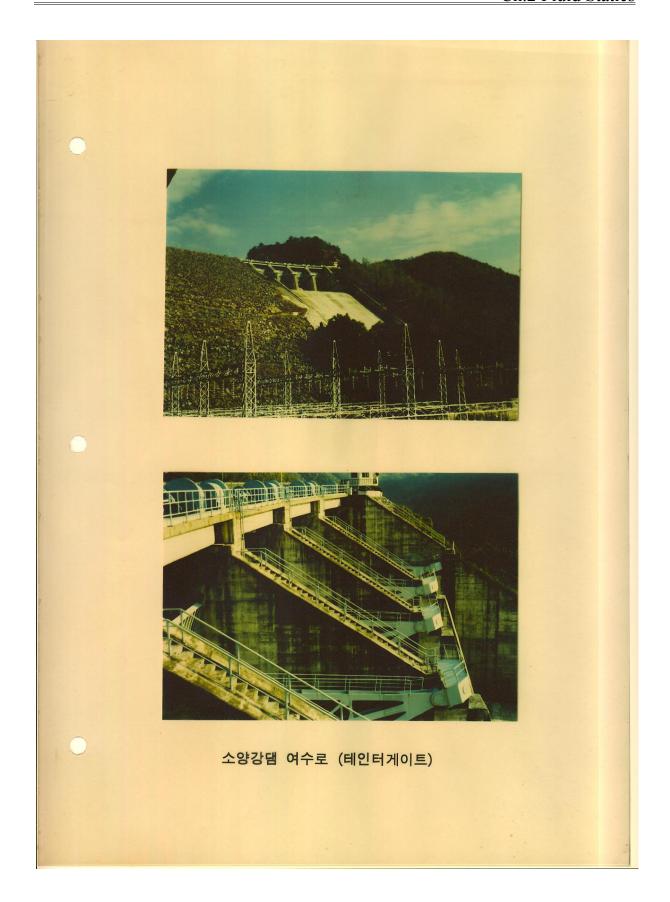
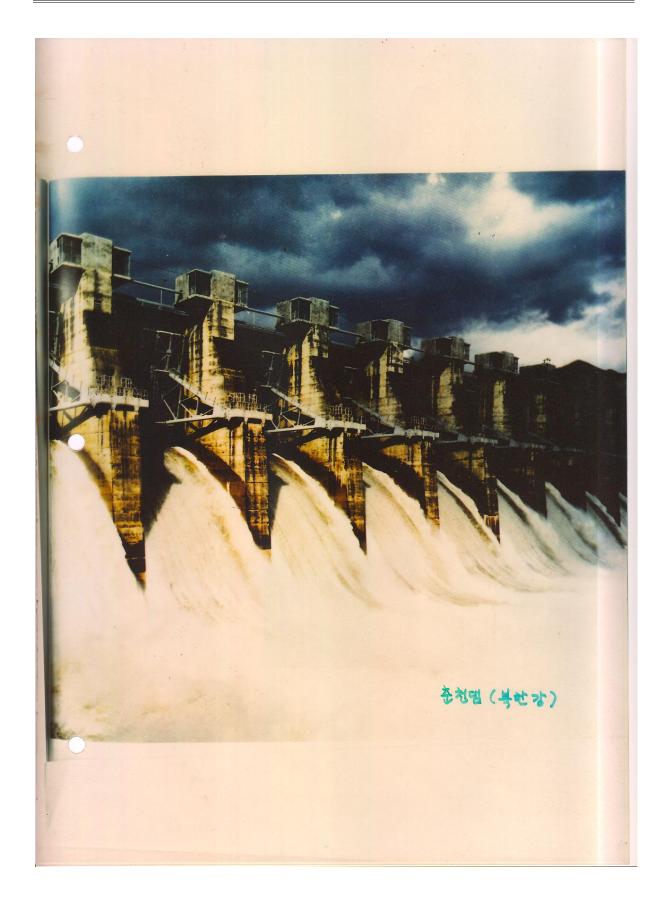
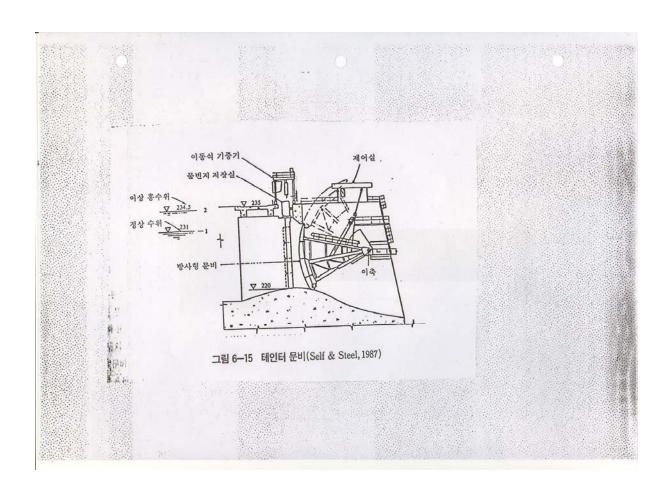


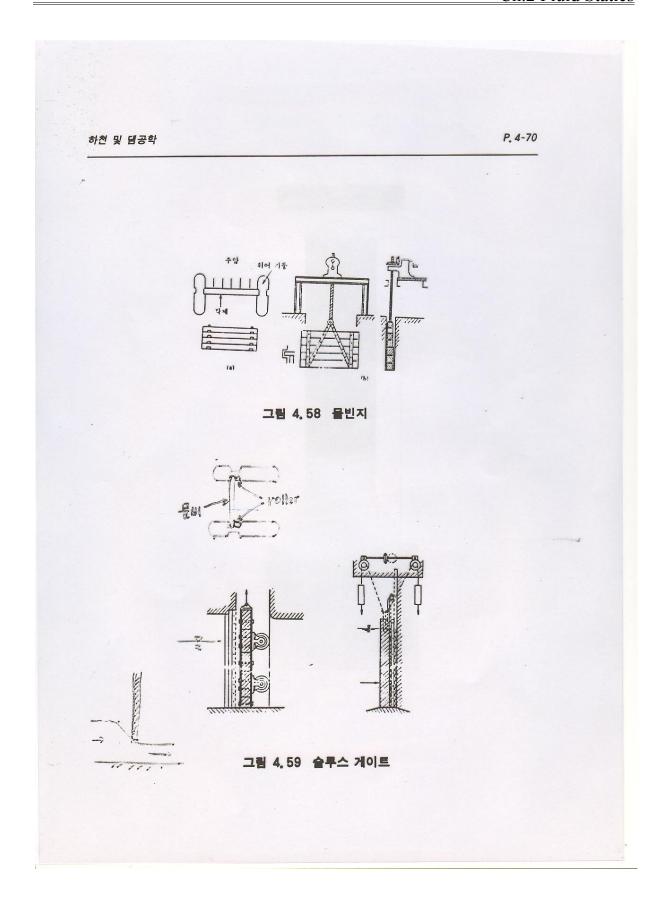
FIGURE 3–23 Hoover Dam.

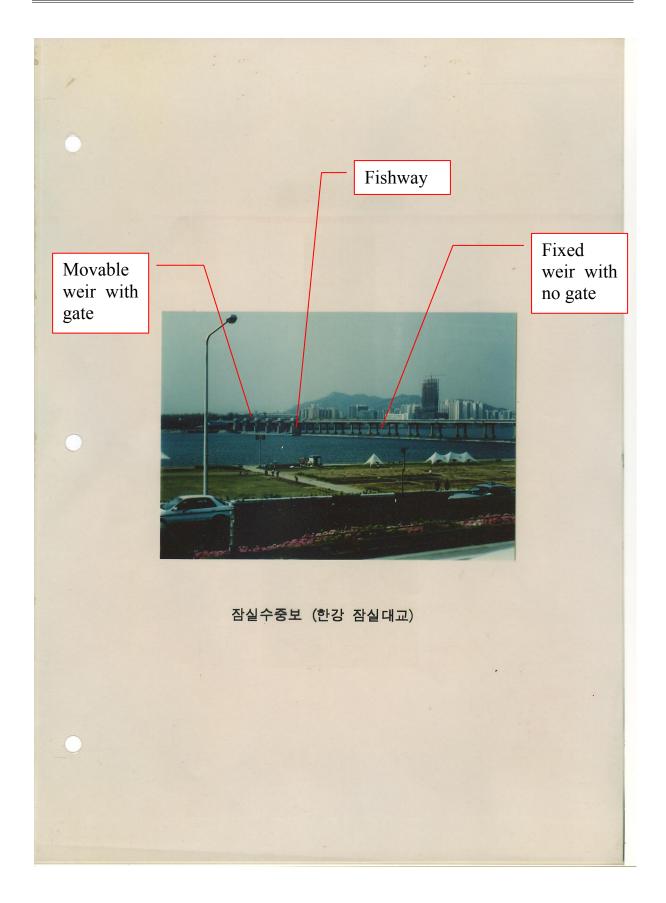
Courtesy United States Department of the Interior, Bureau of Reclamation-Lower Colorado Region.



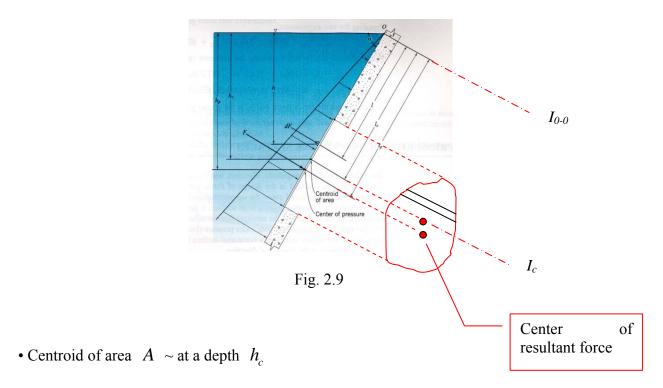








• Pressure on the inclined plane



 \sim at a distance $\;l_{c}\;$ from the line of intersection 0-0

(i)Magnitude of total force

First, consider differential force dF

$$dF = pdA = \gamma hdA$$

$$h = l \sin \alpha$$

$$\to dF = \gamma l \sin \alpha \, dA \tag{2.10}$$

Then, integrate dF over area A

$$F = \int_{-\alpha}^{A} dF = \gamma \sin \alpha \int_{-\alpha}^{A} l dA$$
 (2.11)

in which
$$\int_{-1}^{A} l dA = 1$$
st moment of the area A about the line 0-0
$$= A \cdot l_{c}$$

in which l_c = perpendicular distance from 0-0 to the centroid of area

 $F = \gamma A l_c \sin \alpha$ (pressure at centroid) × (area of plane) $F = \gamma h_c A$ (2.12)

(ii) Location of total force

$$dF = \gamma l \sin \alpha dA$$

Consider moment of force about the line 0-0

$$dM = d\vec{F} \cdot l = \gamma l^2 d \sin \alpha$$

$$M = \int_{-1}^{1} dM = \gamma \sin \alpha \int_{-1}^{1} l^2 dA$$

where $\int_{-\infty}^{A} l^2 dA = \underline{\text{second moment of the area } A}$, about the line 0-0 = I_{0-0}

$$\therefore M = \gamma \sin \alpha I_{0-0} \tag{a}$$

By the way,

$$M = F \cdot l_p$$
 (total force × moment arm) (b)

 $l_p = \text{unknown}$

Combine (a) and (b)

$$Fl_p = \gamma I_{0-0} \sin \alpha \tag{c}$$

Substitue $F = \gamma l_c \sin \alpha A$ into (c)

$$\gamma l_c \sin \alpha A l_p = \gamma I_{0-0} \sin \alpha$$

$$\therefore l_p = \frac{I_{0-0}}{l_c A} = \frac{I_c + l_c^2 A}{l_c A} = l_c + \frac{I_c}{l_c A}$$
(2.14)

 \rightarrow Center of pressure is always below the centroid by $\frac{I_c}{l_c A}$

$$l_p - l_c = \frac{I_c}{l_c A}$$

 \rightarrow as $\ l_{c}$ (depth of centroid) increases $\ l_{p}-l_{c}$ decreases

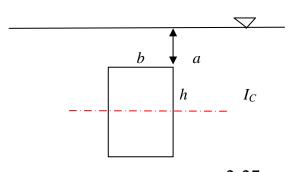
• Second moment transfer equation

$$I_{0-0} = I_c + l_c^2 A$$

 I_c = 2nd moment of the area A about a axis through the centroid, parallel to 0-0

→ Appendix 3

1) Rectangle



$$A = bh$$
, $y_c = \frac{h}{2}$, $I_c = \frac{bh^3}{12}$

$$\therefore h_c = a + (h - y_c) = a + \frac{h}{2}$$

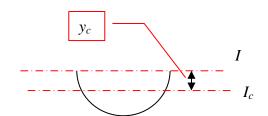
$$F = \gamma h_c A = \gamma \left(a + \frac{h}{2} \right) (bh)$$

$$h_p = h_c + \frac{I_c}{h_c A}$$

If
$$a = 0$$
; $h_c = \frac{h}{2}$

$$h_p = \frac{h}{2} + \frac{\frac{bh^3}{12}}{\frac{h}{2}bh} = \frac{h}{2} + \frac{h}{6} = \frac{2}{3}h$$

2) Semicircle



$$I = \frac{\pi d^4}{128}, \ y_c = \frac{4r}{3\pi}$$

$$I = I_c + y_c^2 A$$

$$\therefore I_c = I - y_c^2 A$$

$$= \frac{\pi d^4}{128} - \left(\frac{4r}{3\pi}\right)^2 \left(\frac{\pi d^2}{8}\right)$$

$$= \left(\frac{\pi}{128} - \frac{1}{18\pi}\right)d^4 = 0.10976r^4$$

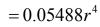
3) Quadrant

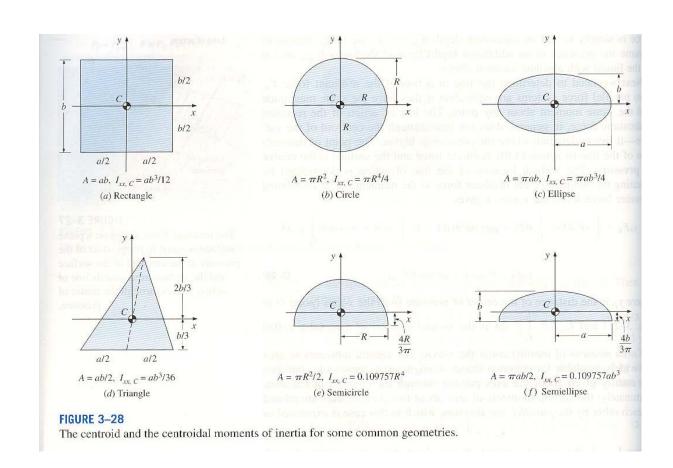
$$I = \frac{\pi d^4}{256}, y_c = \frac{4r}{3\pi}$$

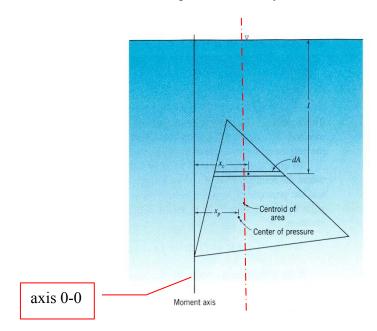
$$I_c = I + y_c^2 A$$

$$= \frac{\pi d^4}{256} - \left(\frac{4r}{3\pi}\right)^2 \left(\frac{\pi d^2}{16}\right)$$

$$= \left(\frac{\pi}{256} - \frac{1}{36\pi}\right) d^4$$







(iii) Lateral location of the center of pressure for asymmetric submerged area

Fig. 2.10

a. For regular plane

- (i) divide whole area into a series of elemental horizontal strips of area dA
- (ii) center of pressure for each strip would be at the midpoint of the strip (the strip is a rectangle in the limit)
 - (iii) apply moment theorem about a vertical axis 0-0

$$dF = \gamma h_c dA = \gamma l \sin \alpha dA$$
 (a)
$$dM = x_c dF = x_c \gamma l \sin \alpha dA$$

Integrate (a)

$$M = \int_{A} dM = \int x_{c} \gamma l \sin \alpha dA$$
 (b)

By the way,
$$M = x_p F$$
 (c)

Equate (b) and (c)

$$x_p F = \int x_c \gamma l \sin \alpha dA$$

$$x_p = \frac{1}{F} \gamma \sin \alpha \int x_c l dA \tag{2.15}$$

- b. For irregular forms
 - ~ divide into simple areas
 - ~ use methods of statics

[Re] Moment theorem

 \rightarrow The moment of the resultant force is equal to the sum of the moments of the individual forces.

[IP 2.9] A vertical gate: quarter circle

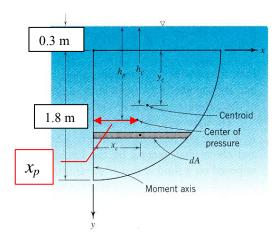


Fig. Problem 2.9

[Sol]

(i) Magnitude

$$y_c$$
)_{quadrant} = $\frac{4r}{3\pi} = \frac{4}{3\pi} (1.8) = 0.764;$

$$h_c = 0.3 + 0.764 = 1.064$$

$$F_{quad} = \gamma h_c A = 9,800(1.064) \left(\frac{\pi}{4}(1.8)^2\right) = 26.53 \text{ kN}$$

(ii) Vertical location of resultant force

$$\left(\frac{I_c}{l_c A}\right)_{quad} = \frac{0.05488(1.8)^4}{(1.064)\left(\frac{\pi}{4}(1.8)^2\right)} = 0.213 \,\mathrm{m}$$

$$\rightarrow l_p = 1.064 + 0.213 = 1.277 \,\mathrm{m}$$

(iii) Lateral location of the center of pressure

Divide quadrant into horizontal strips

Take a moment of the force on dA about y-axis

$$dM = \gamma h dA \cdot (\text{moment arm}) = 9800(y + 0.3)(x dy) \left(\frac{x}{2}\right)$$

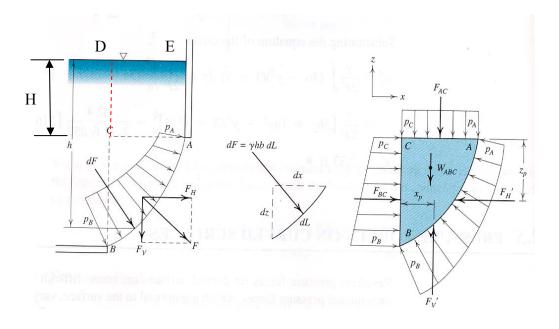
$$\frac{9800}{2} (y + 0.3)x^2 dy = \frac{9800}{2} (y + 0.3)(1.8^2 - y^2) dy$$

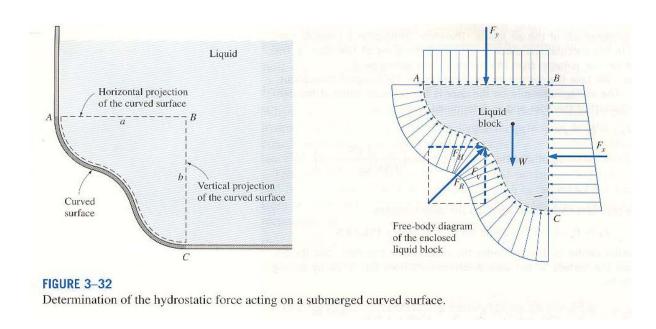
$$\therefore M = \int_0^{1.8} \frac{9800}{2} (y + 0.3)(1.8^2 - y^2) dy = 18575 \,\text{N} \cdot \text{m}$$

By the way,
$$M = F_{quad} x_p$$

$$x_p = 18575 / 26.53 \times 10^3 = 0.7m$$
 right to the y-axis

2.5 Forces on Submerged Curved Surfaces





- Resultant pressure forces on curved surfaces are more difficult to deal with because the incremental pressure forces vary continually in direction.
 - → Direct integration

 Method of basic mechanics

- 1) Direct integration
- Represent the curved shape functionally and integrate to find horizontal and vertical components of the resulting force
 - i) Horizontal component

$$F_H = \int dF_H = \int \gamma h b \, dz$$

where b = the width of the surface; dz = the vertical projection of the surface element dL

location of F_H : take moments of dF about convenient point, e.g., point C

$$z_p F_H = \int z \, dF_H = \int z \, \gamma h b \, dz$$

where z_p = the vertical distance from the moment center to F_H

ii) Vertical component

$$F_V = \int dF_V = \int \gamma h b \, dx$$

where dx = the horizontal projection of the surface element dL

location of F_V : take moments of dF about convenient point, e.g., point C

$$x_p F_V = \int x \, dF_V = \int x \, \gamma h b \, dx$$

where x_p = the horizontal distance from the moment center to F_V

- 2) Method of basic mechanics
- Use the basic mechanics concept of a free body and the equilibrium of a fluid mass
- Choose a convenient volume of fluid in a way that one of the fluid element boundaries coincide with the curved surface under consideration

- Isolate the fluid mass and show all the forces acting on the mass to keep it in equilibrium
- Static equilibrium of free body ABC

$$\sum F_x = F_{BC} - F_H' = 0$$

$$\therefore F_H' = F_{BC} = \gamma h_c A_{BC}$$

$$\sum F_z = F_V' - W_{ABC} - F_{AC} = 0$$

$$\therefore F_V' = F_{AC} + W_{ABC}$$

$$F_{AC} = \gamma h_c A_{AC} = \gamma H A_{AC} = W_{ACDE}$$

$$W_{ABC} = \text{weight of free body } ABC$$

$$\therefore F_V' = \text{weight of } ABDE$$

• Location

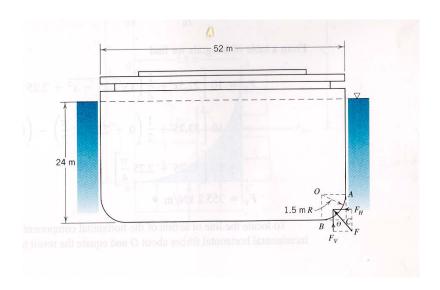
From the inability of the free body of fluid to support shear stress,

- ightarrow $F_{H^{'}}$ must be colinear with F_{BC}
- $\rightarrow F_{V^{'}}$ must be colinear with the resultant of $\,W_{{\scriptscriptstyle ABC}}\,$ and $\,F_{{\scriptscriptstyle AC}}\,.$

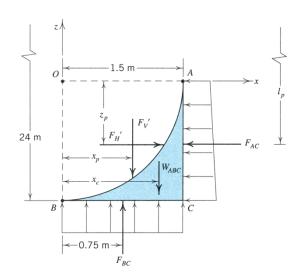
[IP 2.10] p. 59

Oil tanker
$$W = 330,000 \text{ tone} = 330,000 \times 10^3 \text{kg}$$

Calculate magnitude, direction, and location of resultant force/meter exerted by seawater $(\gamma = 10 \times 10^3 \, \text{N/m}^3)$ on the curved surface AB (quarter cylinder) at the corner.



[Sol] Consider a free body ABC



(i) Horizontal Comp.

$$h_c = 22.5 + \frac{h}{2} = 22.5 + \frac{1.5}{2} = 23.25$$

$$F_H = F_{AC} = \gamma h_c A = 10^4 \times \left(22.5 + \frac{1.5}{2}\right) \times (1.5 \times 1) = 348.8 \text{ kN/m}$$

$$l_p = l_c + \frac{I_c}{l_c A} = 23.25 + \frac{\frac{1 \times (1.5)^3}{12}}{23.25 \times 1.5} = 23.25 + 0.0081 = 23.258 \text{ m}$$

$$\therefore z_p = 23.258 - 22.5 = 0.758 \,\text{m}$$
 below line OA

$$= 24 - 23.258 = 0.742$$
 m above line BC

(ii) Vertical Comp.

$$\sum F_z = F_{BC} - F_V' - W_{ABC} = 0$$

$$\therefore F_V' = F_{BC} - W_{ABC} = \gamma h_c A - \gamma Vol.$$

$$= 10^4 \times 24 \times (1.5 \times 1) - 10^4 \left(1.5 \times 1.5 - \frac{1}{4} \pi (1.5)^2 \right) \times 1 = 355.2 \, kN / m$$

• To find the location of F_{ν} , we should first find center of gravity of ABC using statics

Take a moment of area about line OB

$$\frac{4(1.5)}{3\pi} \times \frac{1}{4}\pi (1.5)^2 + x_c \times 0.483 = 2.25 \times \frac{1.5}{2}$$

$$x_c = 1.1646 \text{ m}$$

[Cf] From App. 3, for segment of square

$$x_c = \frac{2}{3} \frac{r}{4 - \pi} = \frac{2}{3} \frac{1.5}{4 - \pi} = 1.165 m$$

Now, find location of force F_{V}

Take a moment of force about point O

$$F_{V} \times x_{p} = F_{BC} \times 0.75 - W_{ABC} \times 1.1646$$

$$355.2 \times x_p = 360 \times 0.75 - 4.83 \times 1.1646$$

$$\therefore x_p = 0.744 \text{ m right of } OB$$

[Summary]

i) Magnitude of Resultant force F

$$F = \sqrt{(348.8)^2 + (355.2)^2} = 497.8 \,\text{kN/m}$$

ii) Direction θ

$$\theta = \tan^{-1} \left(\frac{F_V}{F_H} \right) = \tan^{-1} \left(\frac{355.2}{348.8} \right) = 45.5^{\circ}$$

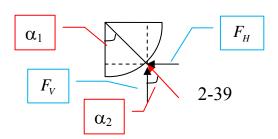
iii) Location

Force acting through a point 0.742 m above line BC and 0.744 m right of B

$$\alpha_1 = \tan^{-1} \left(\frac{0.744}{0.758} \right) = 44.47^{\circ}$$

$$\alpha_2 = \tan^{-1} \left(\frac{348.8}{355.2} \right) = 44.47^{\circ}$$

 $\alpha_1 = \alpha_2 \rightarrow F$ act through point O.

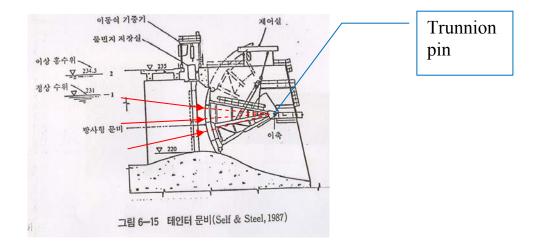


- Pressure acting on the cylindrical or spherical surface
 - The pressure forces are all normal to the surface.
 - For a circular arc, all the lines of action would pass through the center of the arc.
 - → Hence, the resultant would also pass through the center.
- Tainter gate (Radial gate) for dam spillway

All hydrostatic pressures are radial, passing through the trunnion bearing.

→ only pin friction should be overcome to open the gate

pin friction (radial gate) < roller friction (lift gate)



2.6 Buoyancy and Floatation

- Archimedes' principle
 - I. A body immersed in a fluid is buoyed up by a force equal to the weight of fluid displaced.
 - II. A floating body displaces its own weight of the liquid in which it floats.
- → Calculation of draft of surface vessels, lift of airships and balloons

(i) Immersed body

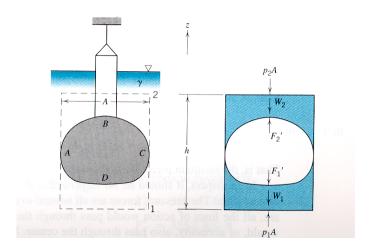


Fig. 2.12

Isolate a free body of fluid with vertical sides tangent to the body

 \rightarrow F_1'' = vertical force exerted by the lower surface (ADC) on the surrounding fluid F_2'' = vertical force exerted by the upper surface (ABC) on the surrounding fluid $F_1'' - F_2'' = F_B$

 F_B = buoyancy of fluid; act vertically upward.

For upper portion of free body

$$\sum F_z = F_2' - W_2 - P_2 A = 0 \tag{a}$$

For lower portion

$$\sum F_z = F_1' - W_1 + P_1 A = 0 \tag{b}$$

Combine (a) and (b) γh

$$F_B = F_1' - F_2' = (P_1 - P_2)A - (W_1 + W_2)$$

$$(P_1 - P_2)A = \gamma hA$$
 = weight of free body

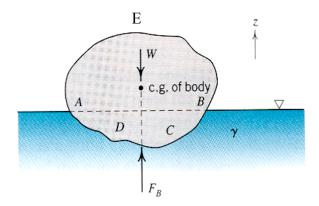
 $W_1 + W_2 =$ weight of dashed portion of fluid

 $\therefore (P_1 - P_2)A - (W_1 + W_2)$ = weight of a volume of fluid equal to that of the body

ABCD

$$\therefore F_B = \gamma_{fluid} \text{ (volume of submerged object)}$$
 (2.16)

(ii) Floating body



For floating object

$$F_{\rm B} = \gamma_{\rm f} \quad {\rm (volume\ displaced,} \quad ABCD \, {\rm)} \qquad \qquad F_{\rm B} = \gamma_{\rm f} ABCD \, {\rm)} \label{eq:FB}$$

$$W_{ABCDE} = \gamma_s V_{ABCDE}$$

$$W = \gamma_s ABCDE$$

where γ_s = specific weight of body

From static equilibrium: $F_B = W_{ABCDE}$

$$\gamma_f V_{ABCD} = \gamma_s V_{ABCDE}$$

$$\therefore V_{ABCD} = \frac{\gamma_s}{\gamma_f} V_{ABCDE}$$

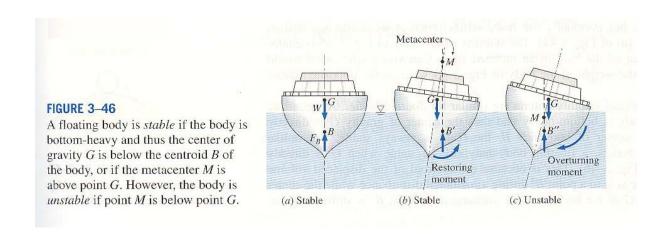
[Ex] Iceberg in the sea

Ice s.g.=
$$0.9$$

Sea water s.g.= 1.03

$$V_{sub} = \frac{0.9(9800)}{1.03(9800)} V_{total} = 0.97 V_{total}$$

• Stability of submerged or floating bodies



 $G_1 < M \rightarrow$ stable, righting moment

 $G_2 > M$ \rightarrow unstable, overturning moment

 G_1, G_2 = center of gravity

M = metacenter

2.7 Fluid Masses Subjected to Acceleration

- Fluid masses can be subjected to various types of <u>acceleration without the occurrence of</u>
 relative motion between fluid particles or between fluid particles and boundaries.
 - → laws of fluid statics modified to allow for the effects of acceleration
- A whole tank containing fluid system is accelerated.

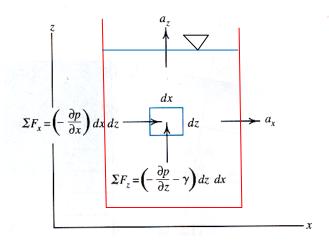


Fig. 2.15

• Newton's 2nd law of motion (Sec. 2.1)

$$\sum F = Ma$$

First, consider force

$$\sum F_{x} = \left(p - \frac{\partial p}{\partial x} \frac{dx}{2}\right) dz - \left(p + \frac{\partial p}{\partial x} \frac{dx}{2}\right) dz = \left(-\frac{\partial p}{\partial x}\right) dx dz \tag{2.18a}$$

$$\sum F_z = \left(-\frac{\partial p}{\partial z} - \gamma\right) dxdz$$
Then, consider acceleration

(2.18b)

$$z: \left(-\frac{\partial p}{\partial z} - \gamma\right) dxdz = \left(\frac{\gamma}{g} dxdz\right) a_z$$

where mass = $\rho vol. = \frac{\gamma}{g} dxdz \times 1$

$$\frac{\partial p}{\partial x} = -\frac{\gamma}{g} a_x \tag{2.19}$$

$$\frac{\partial p}{\partial z} = -\frac{\gamma}{g}(g + a_z) \tag{2.20}$$

→ pressure variation through an accelerated mass of fluid

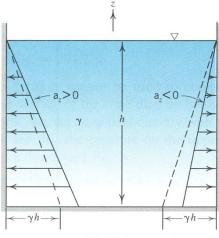


Fig. 2.16

[Cf] For fluid at rest,

$$\frac{\partial p}{\partial x} = 0$$

$$\frac{\partial p}{\partial z} = -\gamma$$

• Chain rule for the total differential for dp (App. 5)

$$dp = \frac{\partial p}{\partial x}dx + \frac{\partial p}{\partial z}dz \tag{a}$$

Combine (2.19), (2.20), and (a)

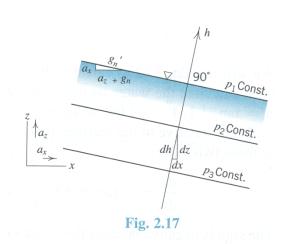
$$dp = -\frac{\gamma}{g} a_x dx - \frac{\gamma}{g} (g + a_z) dz \tag{2.21}$$

• Line of constant pressure dp = 0

$$-\frac{\gamma}{g}a_x dx - \frac{\gamma}{g}(g + a_z)dz = 0$$

$$\therefore \frac{dz}{dx} = -\left(\frac{a_x}{g + a_x}\right) \tag{2.22}$$

→ slope of a line of constant pressure



1) No horizontal acceleration: $a_x = 0$

$$\frac{\partial p}{\partial x} = 0$$

$$\therefore \frac{dp}{dz} = -\gamma \left(\frac{g + a_z}{g} \right)$$

• For free falling fluid, $a_z = -g$

$$\frac{dp}{dz} = 0$$

2) Constant linear acceleration

Divide (2.21) by dh

$$\frac{dp}{dh} = -\gamma \left(\frac{a_x}{g} \frac{dx}{dh} + \frac{g + a_z}{g} \frac{dz}{dh} \right) \tag{a}$$

Use similar triangles

$$\frac{dx}{dh} = \frac{a_x}{g} \tag{b.1}$$

$$\frac{dz}{dh} = \frac{a_z + g}{g} \tag{b.2}$$

$$g' = \left[a_x^2 + (a_z + g)^2\right]^{1/2}$$

Substitute (b) into (a)

$$\frac{dp}{dh} = -\gamma \frac{g'}{g}$$

 \rightarrow pressure variation along h is linear.

[IP 2.13] p. 70

An open tank of water is accelerated vertically upward at 4.5 m/s^2 . Calculate the pressure at a depth of 1.5 m.

[Sol]

$$\frac{dp}{dz} = -\gamma \left(\frac{g + a_z}{g}\right) = (-9,800 \text{ N/m}^3) \left(\frac{9.81 + 4.5}{9.81}\right) = -14,300 \text{ N/m}^3$$
$$dp = -14,300dz$$

integrate

$$\int_0^p dp = \int_0^{-1.5} -14,300 dz$$

$$p = -14,300[z]_0^{-1.5} = 14,300(-1.5 - 0) = 21,450 \text{ N/m}^2 = 21.45 \text{ kPa}$$

[Cf] For
$$a_z = 0$$

 $p = \gamma h = 9800(1.5) = 14.7 \text{ kPa}$

Homework Assignment # 2

Due: 1 week from today

- Prob. 2.4
- Prob. 2.6
- Prob. 2.11
- Prob. 2.26
- Prob. 2.31
- Prob. 2.39
- Prob. 2.52
- Prob. 2.59
- Prob. 2.63
- Prob. 2.76
- Prob. 2.91
- Prob. 2.98
- Prob. 2.129