

# System Control

## 5. Basic Control Actions and Response of Control Systems

(1) PID Control

(2) Routh's stability tests

(3) Systems Type

Open loop and closed loop : model sensitivity

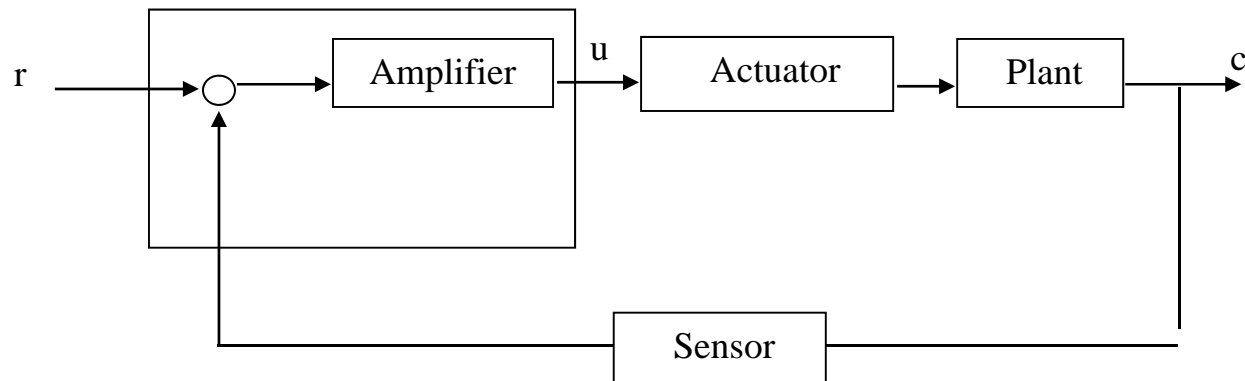
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**Vehicle Dynamics and Control Laboratory**  
**Seoul National University**



# Control Systems

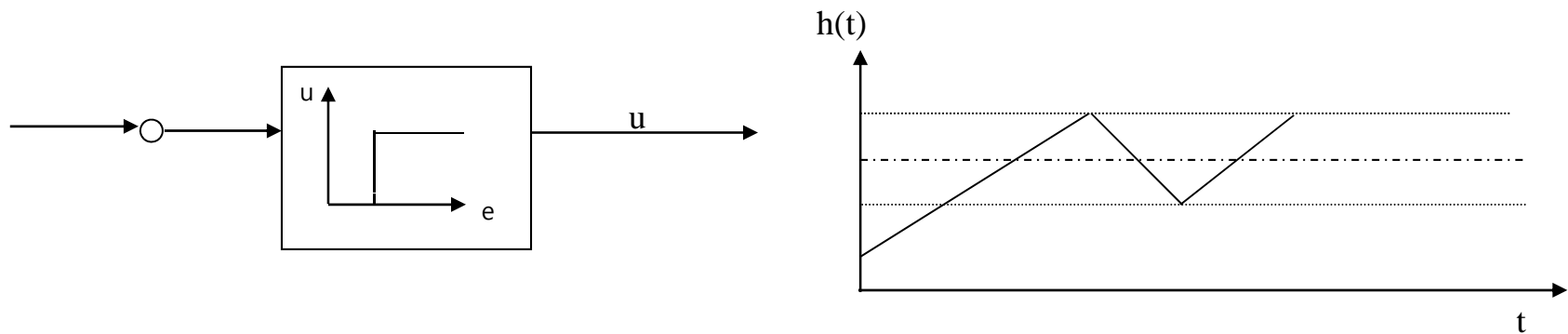
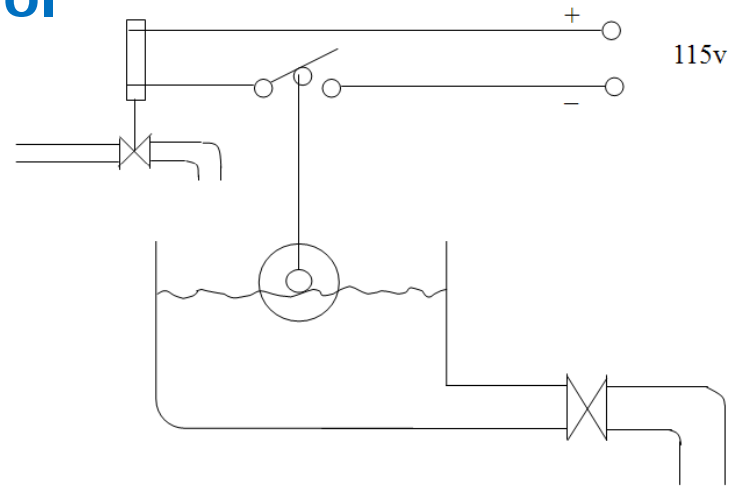


$$u=f(r,c)$$



# Classifications of controllers

## 1. ON-OFF control

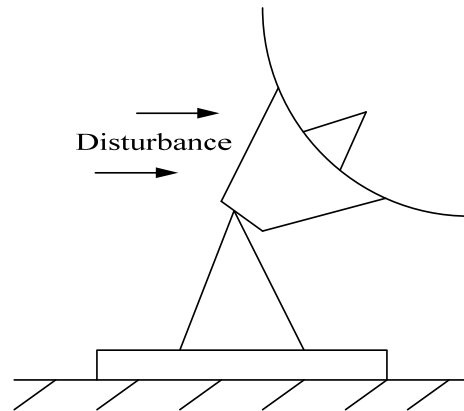
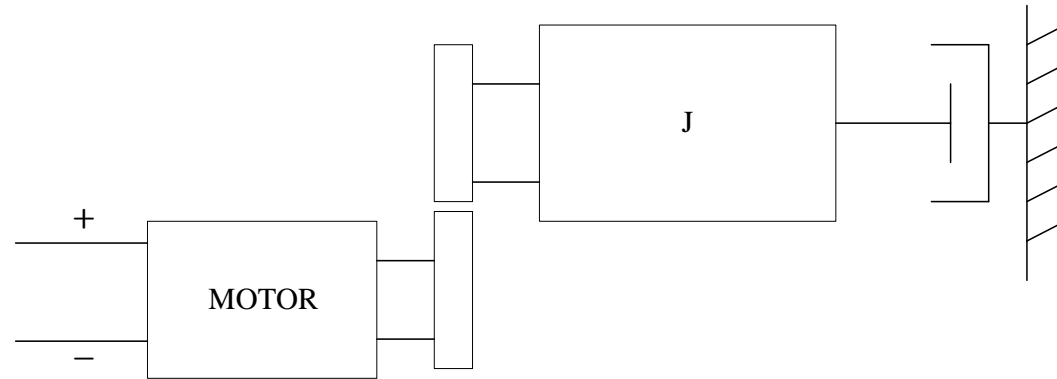


# Classifications of controllers

## 2. Proportional Control

$$U = k_p e$$

$k_p$  : The proportional Gain



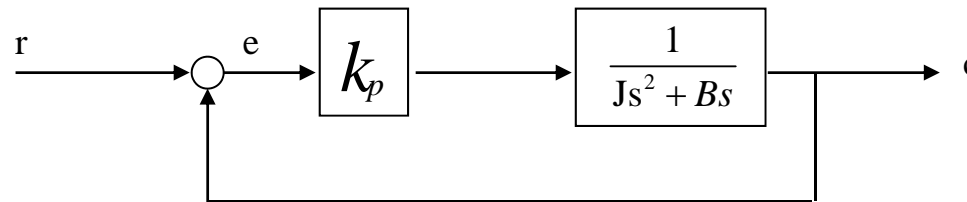
Antenna Position Control System



# Classifications of controllers

## 2. Proportional Control

$$U = k_p e \quad k_p : \text{The proportional Gain}$$



$$\frac{c(s)}{r(s)} = \frac{\frac{K_p}{Js^2 + Bs}}{1 + \frac{K_p}{Js^2 + Bs}} = \frac{K_p}{Js^2 + Bs + K_p}$$



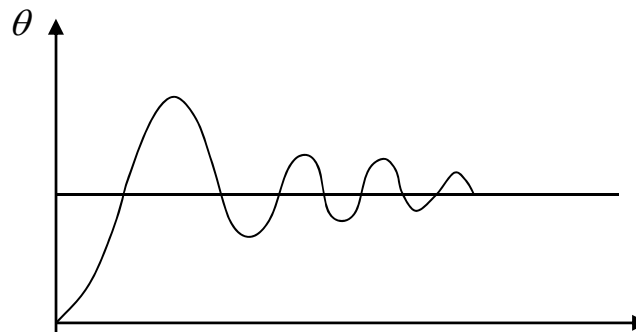
# Classifications of controllers

## 2. Proportional Control

- Step input response  $r(s) = \frac{1}{s}$

- steady state response  $c(t) = \lim_{s \rightarrow 0} sC(s)$

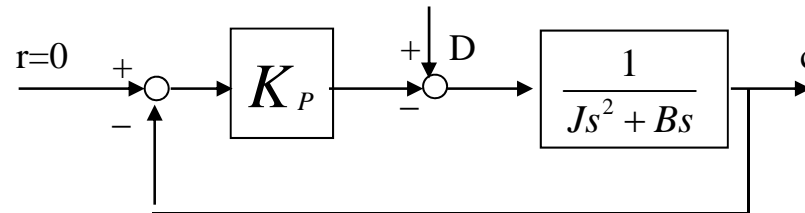
$$= \lim_{s \rightarrow 0} s \frac{K_p}{Js^2 + Bs + K_p} \frac{1}{s} = 1$$



# Classifications of controllers

## 2. Proportional Control

- Response to torque disturbance



$$C(s) = \frac{K_p}{Js^2 + Bs + K_p} r(s) + \frac{1}{Js^2 + Bs + K_p} D(s)$$

Assume that  $D(s) = \frac{1}{s}$  steady state response

$$c(t) = \lim_{s \rightarrow \infty} s \cdot \frac{1}{Js^2 + Bs + K_p} \cdot \frac{1}{s} = \frac{1}{K_p} : \text{steady-state error}$$

Large  $K_p$  → small steady-state error

→ large motor power is needed

→ oscillations

→ large  $w_n$   $\left( w_n = \sqrt{\frac{K_p}{J}} \right)$

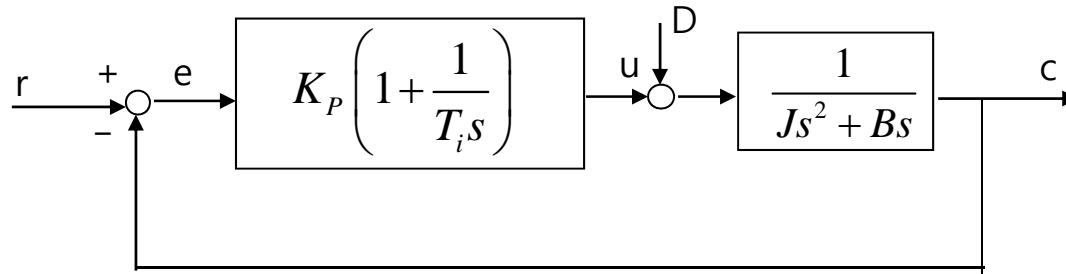
→ small damping ratio  $\zeta = \frac{B}{2\sqrt{JK_p}}$



# Classifications of controllers

## 3. Proportional-Integral Control (PI control)

- Response to torque disturbance



$$\frac{U(s)}{E(s)} = K_P \left(1 + \frac{1}{T_i s}\right)$$

$$u(t) = K_p e(t) + \frac{K_P}{T_i} \int_0^t e(t) dt$$

$$\frac{C(s)}{R(s)} = \frac{K_P s + \frac{1}{T_i} K_P}{Js^3 + Bs^2 + K_P s + \frac{K_P}{T_i}}$$

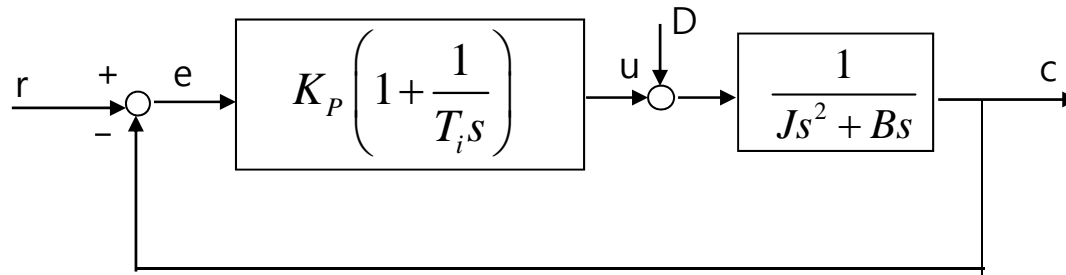
No steady-state error for reference input





# Classifications of controllers

## 3. Proportional-Integral Control (PI control)



$$\frac{C(s)}{D(s)} = \frac{\frac{1}{Js^2 + Bs}}{1 + K_P \left(1 + \frac{1}{T_i s}\right) \frac{1}{Js^2 + Bs}}$$
$$= \frac{s}{Js^3 + Bs^2 + K_P s + \frac{K_P}{T_i}}$$

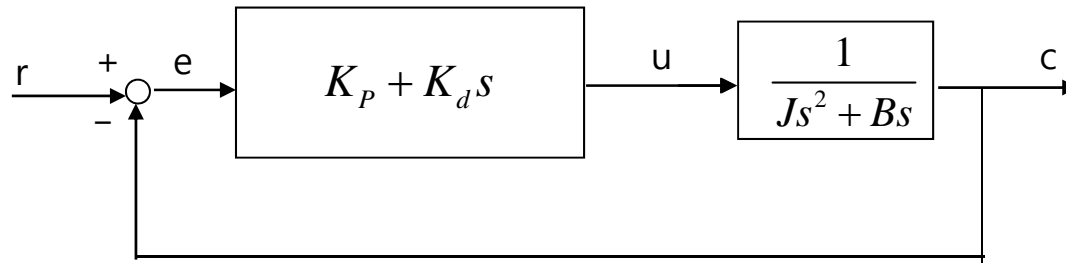
$$D(s) = \frac{1}{s}$$
$$C(t) = \lim_{s \rightarrow 0} s \frac{s}{Js^3 + Bs^2 + K_P s + \frac{K_P}{T_i}} \frac{1}{s} = 0$$

No steady-state error for step disturbance



# Classifications of controllers

## 4. Proportional-Derivative Control (PD control)



$$u(t) = K_P e(t) + K_d \frac{d}{dt} e(t)$$

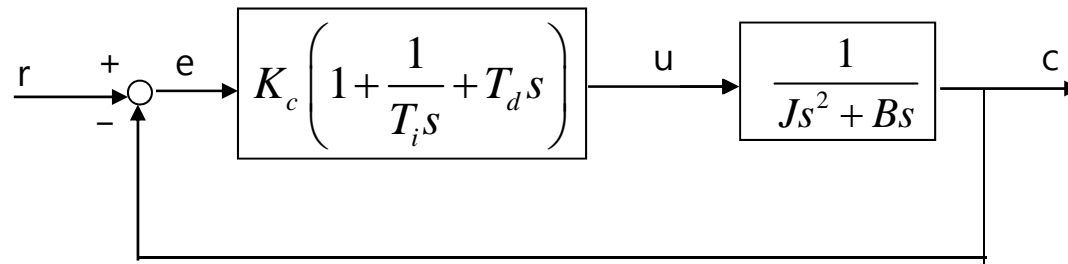
$$\frac{C(s)}{R(s)} = \frac{K_P + K_d s}{J s^2 + (B + K_d) s + K_P}$$

$$\zeta = \frac{B + K_d}{2\sqrt{JK_P}} : \text{increased effective damping}$$

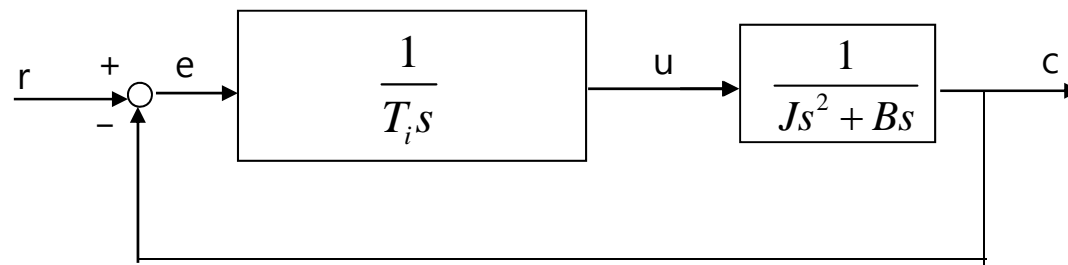


# Classifications of controllers

## 5. Proportional-Integral-Derivative Control (PID control)



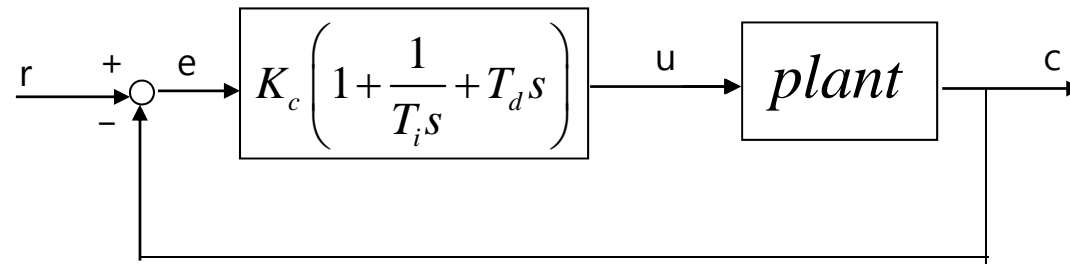
## 6. I control



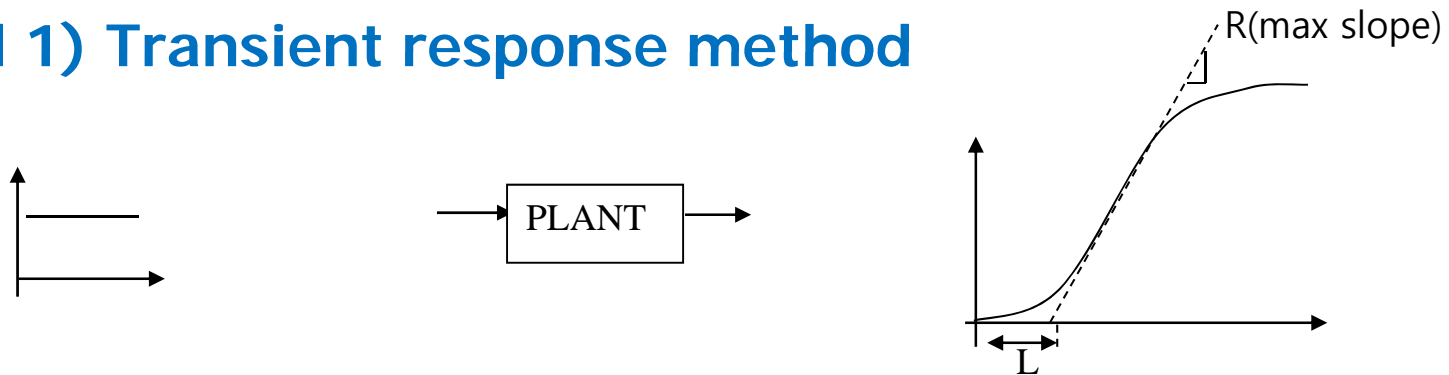
$$\frac{C(s)}{R(s)} = \frac{\frac{1}{T_i s} \frac{1}{Js^2 + Bs}}{1 + \frac{1}{T_i s} \frac{1}{Js^2 + Bs}} = \frac{\frac{1}{T_i}}{Js^3 + Bs^2 + \frac{1}{T_i}}$$



# Ziegler-Nicholas Tuning Rules for PID controllers



## Method 1) Transient response method



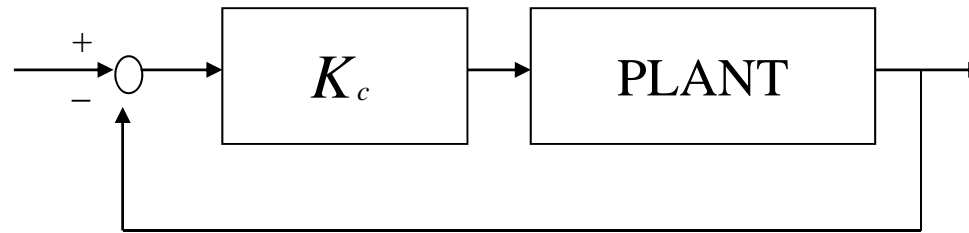
$$\text{Step input} \left\{ \begin{array}{l} K_c = \frac{1}{RL} \quad \text{for } P\text{-control} \\ K_c = \frac{0.9}{RL}, \quad T_i = 3.3L \quad \text{for } PI\text{-control} \\ K_c = \frac{1.2}{RL}, \quad T_i = 2L, \quad T_d = 0.5L \quad \text{for } PID\text{-control} \end{array} \right.$$

- This method works good if the unit step response is  $\int$  (sigmod) shaped

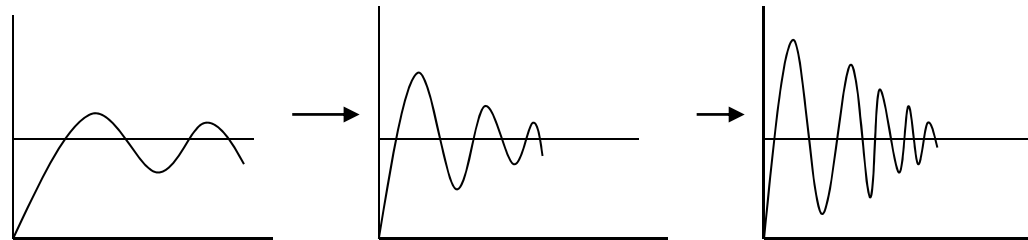


# Ziegler-Nicholas Tuning Rules for PID controllers

## Method 2) Ultimate sensitivity method



$K_c \gg 1, \omega_n \rightarrow \text{increase}$   
 $\zeta \rightarrow \text{decrease}$

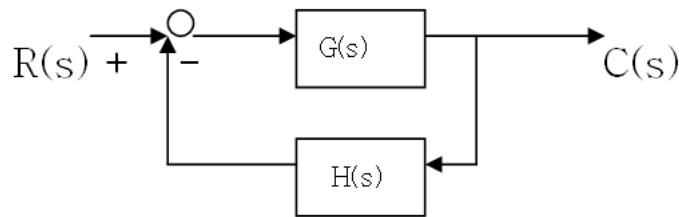


- Increase  $K_c$  until you hit the stability limit

$$\begin{cases} K_c = 0.5K_U & \text{for } P\text{-control} \\ K_c = 0.45K_U, T_i = 0.83P_U & \text{for } PI\text{-control} \\ K_c = 0.6K_U, T_i = 0.5P_U, T_d = 0.125P_U & \text{for } PID\text{-control} \end{cases}$$



# Higher Order Systems



$$\frac{C(s)}{R(s)} = \frac{G(s)}{1 + G(s)H(s)} = \frac{b_0 s^m + b_1 s^{m-1} + \dots + b_{m-1} s + b_m}{a_0 s^n + a_1 s^{n-1} + \dots + a_{n-1} s + a_n}$$

• unit step response  $R(s) = \frac{1}{s}$

$$C(s) = \frac{b_0 s^m + \dots + b_m}{a_0 s^n + \dots + a_0} \cdot \frac{1}{s}$$

characteristic equation

$$a_0 s^n + a_1 s^{n-1} + \dots + a_{n-1} s + a_n = 0$$

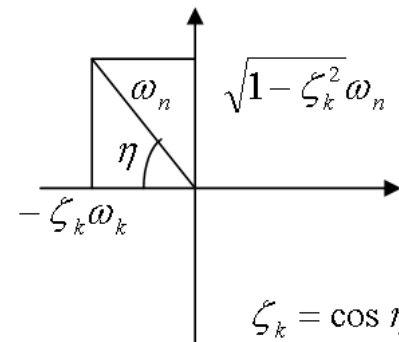
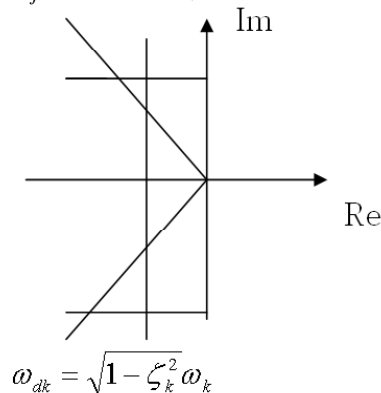
$$s = p_i \quad i = 1, \dots, q$$

$$s = -\zeta_k \omega_k \pm \sqrt{1 - \zeta_k^2} \omega_k j \quad k = 1, \dots, r$$

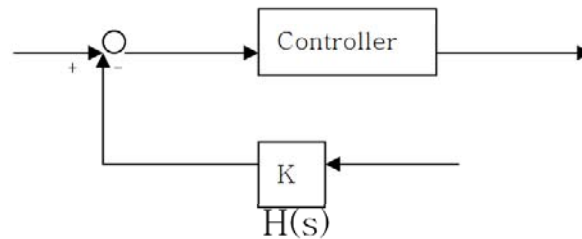
zero ;  $s = Z_i \quad i = 1, \dots, m$

$$C(s) = \frac{k \prod_{i=1}^m (s - z_i)}{s \prod_{j=1}^q (s - p_j) \prod_{k=1}^r (s^2 + 2\zeta_k \omega_k s + \omega_k^2)} = \frac{a}{s} + \sum_{j=1}^q \frac{a_j}{s - p_j} + \sum_{r=1}^r \frac{b_k (s + \zeta_k \omega_k) + C_k \omega_k \sqrt{1 - \zeta_k^2}}{s^2 + 2\zeta_k \omega_k s + \omega_k^2}$$

$$C(t) = a + \sum_{j=1}^q a_j e^{p_j t} + \sum_{k=1}^r b_k e^{-\zeta_k \omega_k t} \cos \omega_k \sqrt{1 - \zeta_k^2} t + \sum_{k=1}^r C_k e^{-\zeta_k \omega_k t} \sin \omega_k \sqrt{1 - \zeta_k^2} t$$

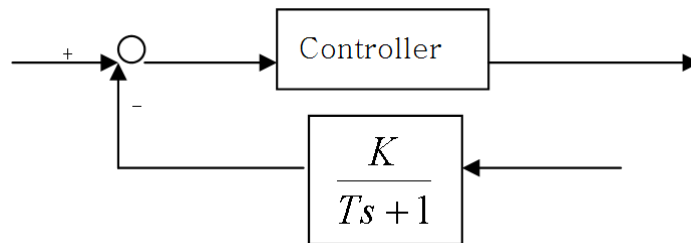


# Effect of sensors on system performance

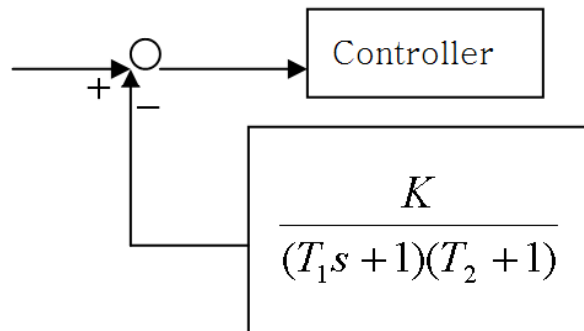


- **Fast sensor dynamics** ;  $H(s)=\text{constant}$

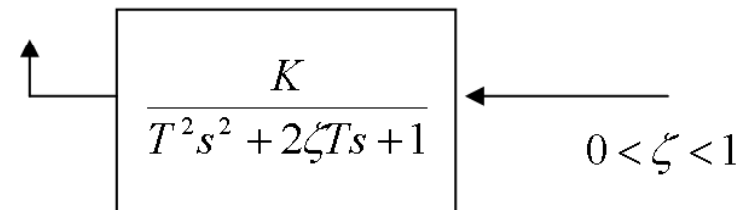
- First order sensor



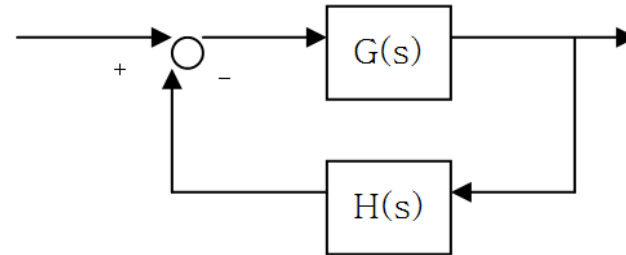
- Overdamped second order



- underdamped second order



# Stability of Feedback Systems



$$\frac{C(s)}{R(s)} = \frac{G(s)}{1 + G(s)H(s)} = \frac{P(s)}{Q(s)}$$

Poles :  $s_i$

$\text{Re}(s_i) < 0$  ; stable

Characteristic equation  $Q(s) = 0$

$$b_n s^n + b_{n-1} s^{n-1} + \dots + b_1 s + b_0 = 0$$





# Routh's Stability Criterion

Characteristic equation

$$b_n s^n + b_{n-1} s^{n-1} + \dots + b_1 s + b_0 = 0$$

$s^n$	$b_n$	$b_{n-2}$	$b_{n-4}$	$\dots$
$s^{n-1}$	$b_{n-1}$	$b_{n-3}$	$b_{n-5}$	$\dots$
$s^{n-2}$	$c_1$	$c_2$		
$s^{n-3}$	$d_1$	$d_2$		
$\cdot$	$\cdot$	$\cdot$		
$s_0$				

$$c_1 = \frac{b_{n-1}b_{n-2} - b_n b_{n-3}}{b_{n-1}}, \quad c_2 = \frac{b_{n-1}b_{n-4} - b_n b_{n-5}}{b_{n-1}}$$

$$d_1 = \frac{c_1 b_{n-3} - b_{n-1} c_2}{c_1}, \quad d_2 = \frac{c_1 b_{n-5} - b_{n-1} c_3}{c_1}$$

- Routh's Criterion

Number of the characteristic roots with positive real parts

= Number of sign changes of the first column have the same sign



# Routh's Stability Criterion

Example 1)

$$\frac{C}{R} = \frac{P(s)}{s^5 + s^4 + 10s^3 + 72s^2 + 152s + 240}$$

$s^5$	1	10	152
$s^4$	1	72	240
$s^3$	-62	-88	
$s^2$	70.6	240	
$s^1$	122.6		
$s^0$	240		

Two sign change

- $Q(s)=0$  has two roots with positive real parts
- unstable



# Routh's Stability Criterion

Example 2)

$s^4$	1	2	5
$s^3$	1	2	
$s^2$	0		
$s^1$	?		

→ prevents completion of the array

method 1)  $s = \frac{1}{x}$

$$Q(s) = \frac{5x^4 + 2x^3 + 2x^2 + x + 1}{x^4}$$

$x^4$	5	2	1
$x^3$	2	1	
$x^2$	-0.5    1		
$x^1$	-1	2	
$x^0$	5		

two sign change → unstable

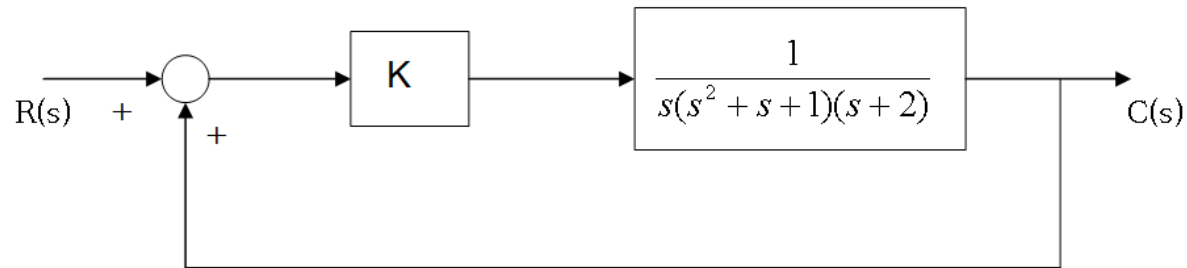
method 2)

set  $Q(s)(s+1) = 0$



# Routh's Stability Criterion

Example 3)



$$\frac{C(s)}{R(s)} = \frac{\frac{K}{s(s^2 + s + 1)(s + 2)}}{1 + \frac{K}{s(s^2 + s + 1)(s + 2)}} = \frac{K}{s(s^2 + s + 1)(s + 2) + K} = \frac{K}{s^4 + 3s^3 + 3s^2 + 2s + K}$$

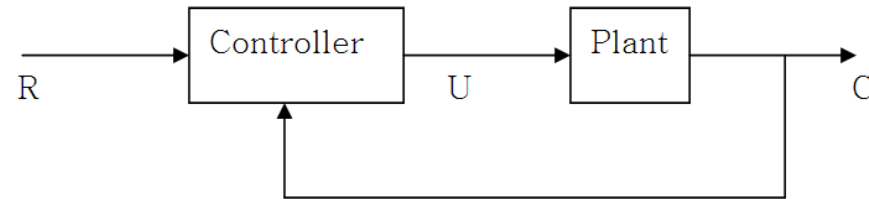
$s^4$	1	3	K
$s^3$	3	2	
$s^2$	$\frac{7}{3}$	K	
$s^1$	$\left(2 - \frac{9}{7}K\right)$		
$s^0$	K		

$$2 - \frac{9}{7}K > 0 \Rightarrow K < \frac{14}{9} \quad K > 0$$

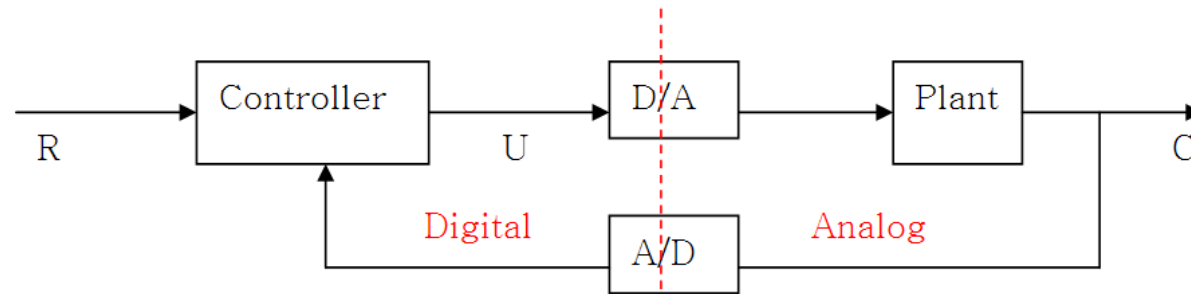
$$\therefore 0 < K < \frac{14}{9}$$



# Analog/Digital Controller



[Analog Controller]



[Digital Controller]

Analog Controller	Digital Controller
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Pneumatic controller  
(compressed air)

Hydraulic controller  
(oil)

Electronic controller

Microprocessor

- flexible
- modern control algorithm
- reliable



# Pneumatic vs Hydraulic

- ① Air and gases are compressible, whereas oil is incompressible.
- ② Air lacks lubricating property,  
Oil functions as a hydraulic fluid as well as a lubricator.
- ③ Operating pressure
  - Pneumatic ; low
  - Hydraulic ; high
- ④ Output power
  - Pneumatic ; low
  - Hydraulic ; high
- ⑤ Accuracy
  - Pneumatic ; poor at low velocity
  - Hydraulic ; satisfactory at all velocities
- ⑥ Pneumatic
  - External leakage : permissible
  - Internal leakage ; make be avoidHydraulic
  - External leakage ; make be avoid
  - Internal leakage ; permissible
- ⑦ Pneumatic ; no return pipe  
Hydraulic ; always needed
- ⑧ Pneumatic ; 5<sup>o</sup> ~ 60<sup>o</sup> C (0<sup>o</sup> ~ 200<sup>o</sup> C) insensitive  
Hydraulic ; Hydraulic : 20<sup>o</sup> ~ 70<sup>o</sup> C sensitive (viscosity)
- ⑨ Pneumatic ; fire-and explosion-proof  
Hydraulic ; not



# Hydraulic Control Systems

- Characteristics

- ① high horsepower-to-weight
- ② accurate
- ③ fast response
- ④ machine tool, aircraft, industrial

- Advantages

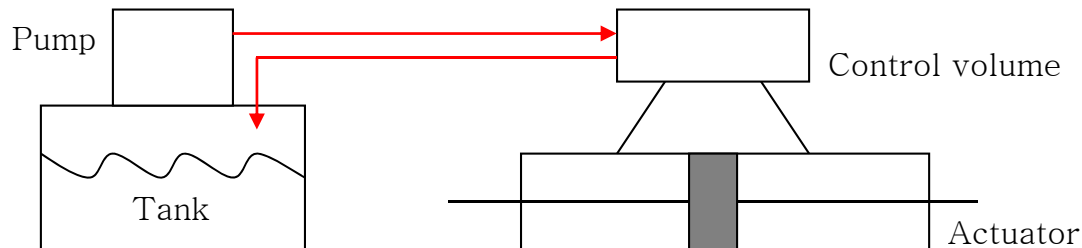
- ① hydraulic fluid ; lubricant, heat exchanger
- ② small size – large force actuators
- ③ higher speed of response,  
fast starts, stops and speed reversals.
- ④ hydraulic actuators can be operated under continuous, intermittent, reversing and stalled conditions without damage
- ⑤ linear and rotary actuators ; flexibility in design
- ⑥ low leakage in actuators  
⇒ speed drop when loads are applied is small



# Hydraulic Control Systems

- Disadvantages

- ① hydraulic power is not readily available compared to electric power



- ② cost ; higher than a comparable electric system performing a similar function

- ③ fire and explosion hazards exist unless fire-resistant fluids are used

- ④ system tends to be messy (leakage)

- ⑤ contaminated oil  $\Rightarrow$  failure

- ⑥ highly nonlinear – sophisticated design

- ⑦ hydraulic systems – poor damping characteristics

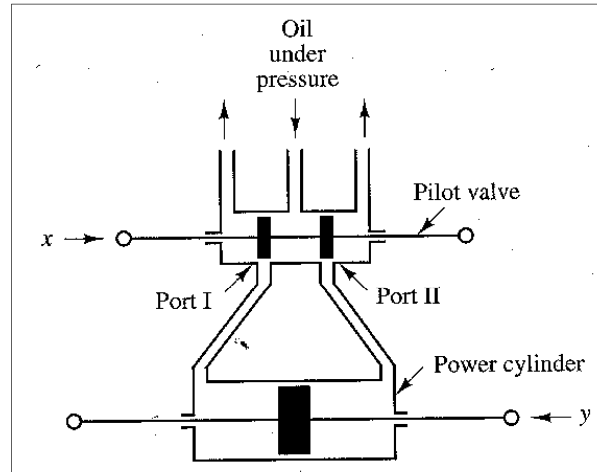
if properly design  $\Rightarrow$  some unstable phenomena may occur or disappear depending on operating condition.





# Hydraulic Control Systems

- Hydraulic Integral Controller



$$q = K_1 x \quad [\text{kg/sec}]$$

$$q dt = \rho A dy$$

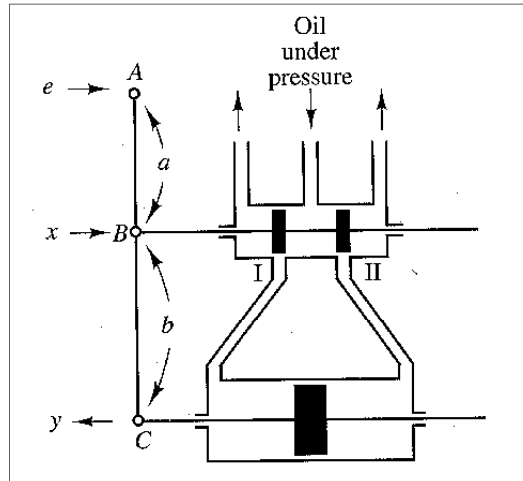
$$\frac{dy}{dt} = \frac{1}{\rho A} q = \frac{K_1}{\rho A} x = Kx$$

$$sY(s) = KX(s) \quad \Rightarrow \quad \frac{Y(s)}{X(s)} = \frac{K}{s}$$



# Hydraulic Control Systems

- Hydraulic Proportional Controller



Steady State

$$\frac{y}{e} = \frac{b}{a}$$

$$x = \frac{b}{a+b} e - \frac{a}{a+b} y$$

$$\frac{Y(s)}{E(s)} = \frac{\frac{b}{a+b} \cdot \frac{K}{s}}{1 + \frac{K}{s} \cdot \frac{a}{a+b}} = \frac{bK}{s(a+b) + Ka} = \frac{\frac{bK}{a+b}}{s + \frac{aK}{a+b}} \approx \frac{b}{a}$$

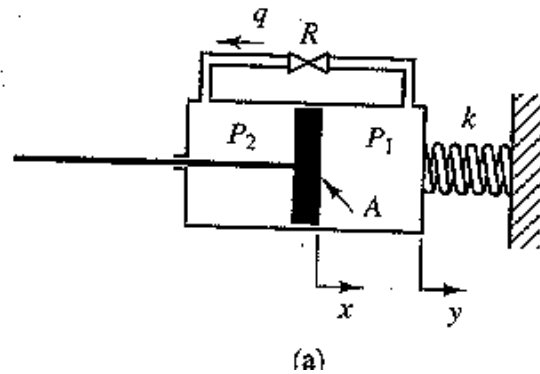
Time constant  $\frac{a+b}{Ka}$  (large K)

Unit Step Response  $E(s) = \frac{1}{s}$

$$\lim_{t \rightarrow \infty} y(t) = \lim_{s \rightarrow 0} s \cdot \frac{bK}{s(s+b) + Ka} \cdot \frac{1}{s} = \frac{b}{a}$$



# Hydraulic Control Systems



$$q = \frac{P_1 - P_2}{R}$$

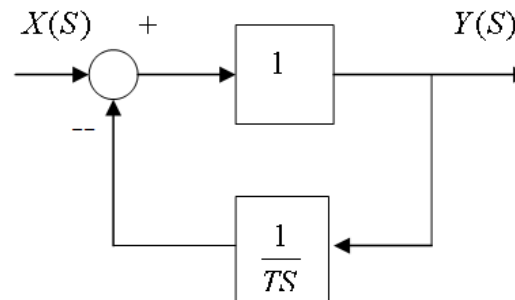
$$F = A(P_1 - P_2) = ky$$

$$q = A \frac{d(x - y)}{dt} \rho$$

$$\frac{dx}{dt} - \frac{dy}{dt} = \frac{1}{A\rho} q = \frac{1}{A\rho} \frac{1}{R} (P_1 - P_2) = \frac{k}{A^2 \rho R} y$$

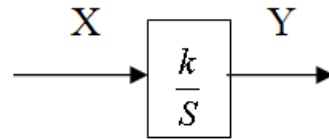
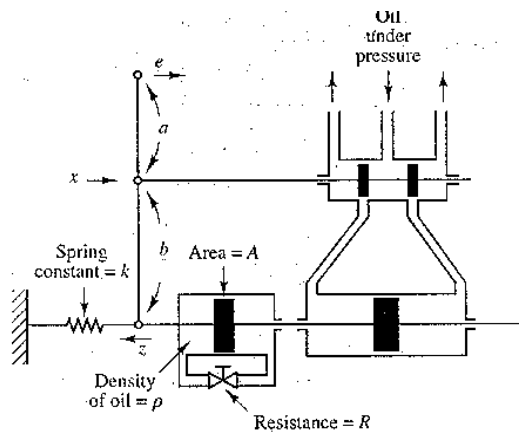
$$sY(s) + \frac{1}{T} Y(s) = sX(s)$$

$$\frac{Y(s)}{X(s)} = \frac{s}{s + \frac{1}{T}} = \frac{1}{1 + \frac{1}{Ts}}$$



# Hydraulic Control Systems

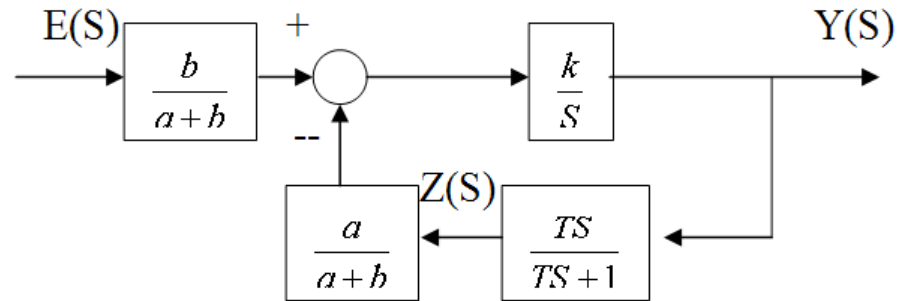
- Hydraulic PI Controller



$$x = \frac{b}{a+b}e - \frac{a}{a+b}z$$

$$\frac{Z(s)}{Y(s)} = \frac{Ts}{Ts+1}$$

(a)



$$\frac{Y}{E} = \frac{\frac{b}{a+b} \frac{k}{s}}{1 + \frac{ka}{a+b} \frac{k}{s} \frac{TS}{TS+1}}$$

$$k = \frac{k_1}{A\rho} \quad A\rho \frac{dy}{dt} = k_1 x$$

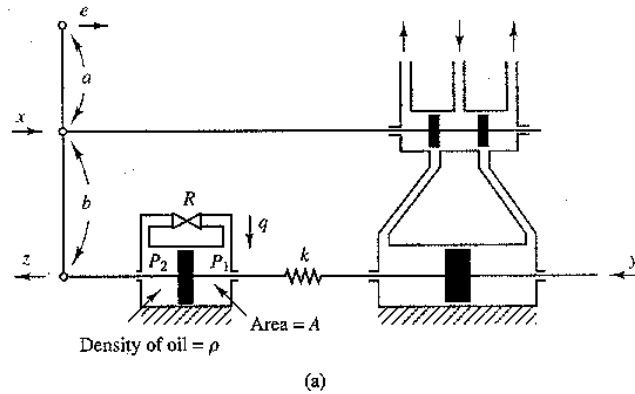
$$\Rightarrow \left| \frac{kaT}{(a+b)(Ts+1)} \right| \gg 1$$

$$\frac{Y}{E} = \frac{\frac{b}{a+b} \frac{k}{s}}{\frac{a}{a+b} \frac{k}{s} \frac{T}{Ts+1}} = k_p \left( 1 + \frac{1}{T_i s} \right) \quad \left( k_p = \frac{b}{a}, T_i = T = \frac{RA\rho^2}{k} \right)$$



# Hydraulic Control Systems

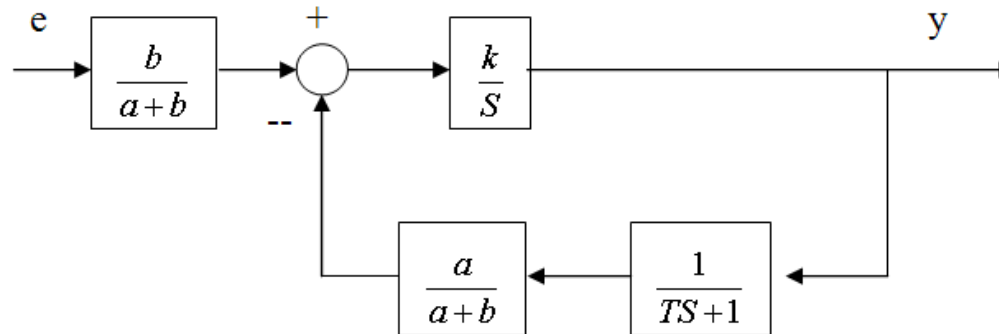
- Hydraulic PD Controller



$$A(P_2 - P_1) = k(y - z)$$

$$q = \frac{P_2 - P_1}{R} \quad q = A\rho \frac{dz}{dt}$$

$$\frac{Z(s)}{y(s)} = \frac{1}{Ts + 1} \quad T = \frac{RA\rho^2}{k}$$



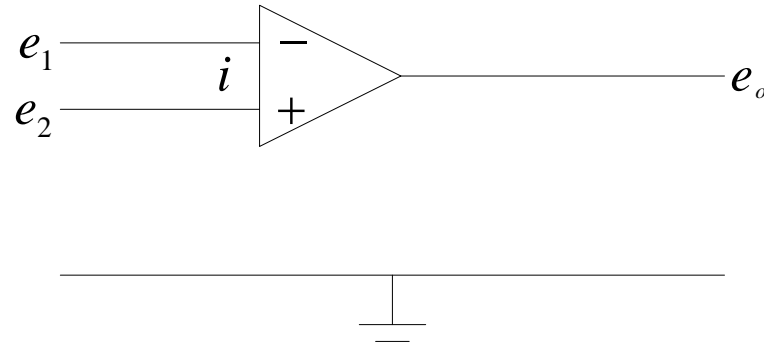
$$x = \frac{b}{a+b} e - \frac{a}{a+b} z$$

$$\frac{Y(s)}{E(s)} = \frac{\frac{b}{a+b} \frac{k}{s}}{1 + \frac{a}{a+b} \frac{1}{s} \frac{1}{Ts+1}} \approx k_p (1 + Ts) \quad \left( k_p = \frac{b}{a}, T = \frac{RA\rho^2}{k} \right)$$



# Electronic Controllers

- Operation Amplifiers



$$e_o \approx k(e_2 - e_1) \quad k: \text{very large-}10^5 \sim 10^6 \text{ (for signals less than 10 Hz)}$$

$$i \approx 0$$

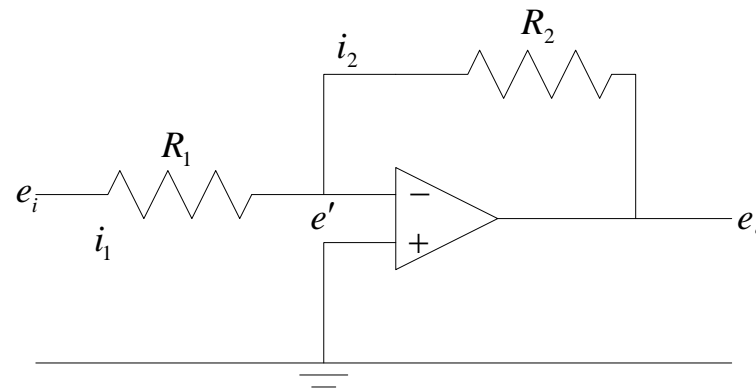
$$e_1 \approx e_2 (k = \infty)$$



# Electronic Controllers

- Operation Amplifiers

- Inverting Amplifiers

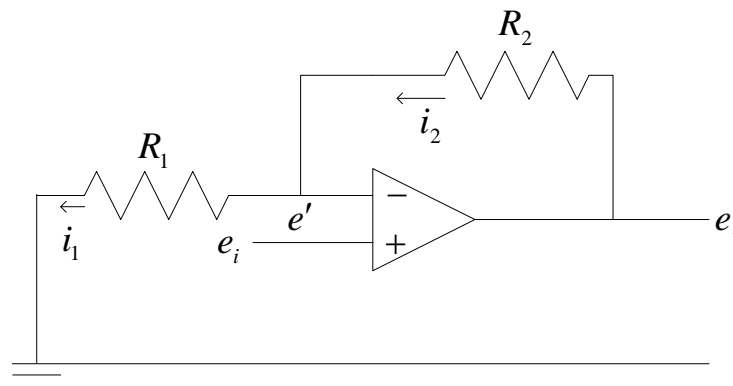


$$i_1 = i_2, e' = 0$$

$$i_1 = \frac{e_i}{R_1} = i_2 = \frac{0 - e_o}{R_2}$$

$$e_o = -\frac{R_2}{R_1} e_i$$

- Non-inverting Amplifiers



$$i_1 = i_2$$

$$i_1 = \frac{e_i}{R_1} = \frac{e_o - e_i}{R_2}$$

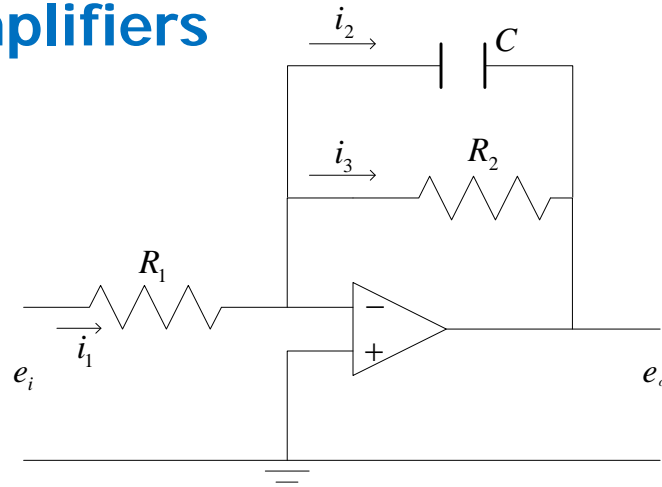
$$e_o = \left(1 + \frac{R_2}{R_1}\right) \cdot e_i$$



# Electronic Controllers

- Operation Amplifiers

Example)



$$i_1 = i_2 + i_3 \qquad i_1 = \frac{e_i}{R_1} \quad 2) \quad \frac{dv_c}{dt} = \frac{1}{C} i_2 = -\frac{de_0}{dt} \quad 3) \quad i_3 = \frac{0 - e_0}{R_2}$$

$$\frac{e_i}{R_1} = -C \frac{de_0}{dt} + \frac{-e_0}{R_2} \qquad \text{Laplace} \rightarrow \frac{1}{\sqrt{R_1}} E_i(s) = -(cs + \frac{1}{R_2}) E_0(s)$$

$$\therefore \frac{E_0(s)}{E_i(s)} = -\frac{\frac{1}{R_1}}{cs + \frac{1}{R_2}} = -\frac{R_2}{R_1} \frac{1}{R_2 cs + 1}$$

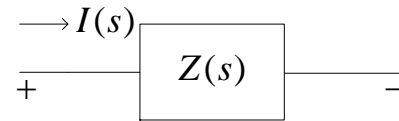




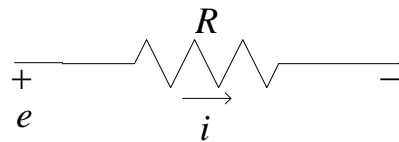
# Electronic Controllers

- Impedance approach for obtaining transfer functions

- Impedance



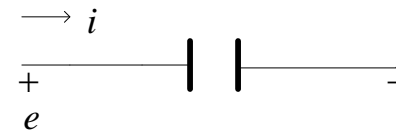
Laplace tranceform 된 I(s) 와 E(s)의 relation을 impedance라 한다.



$$e = iR$$

$$E(s) = I(s)R$$

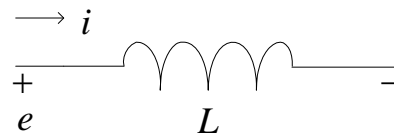
$$Z(s) = \frac{E(s)}{I(s)} = R$$



$$\frac{de}{dt} = \frac{1}{c}i$$

$$sE(s) = \frac{1}{c}I(s)$$

$$Z(s) = \frac{E(s)}{I(s)} = \frac{1}{cs}$$



$$e = L \frac{di}{dt}$$

$$E(s) = LsI(s)$$

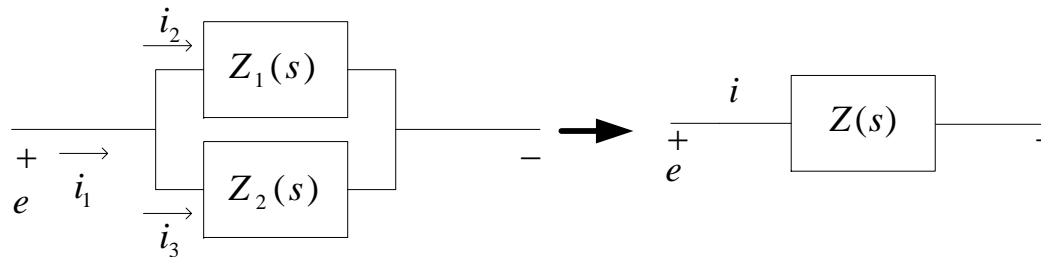
$$Z(s) = \frac{E(s)}{I(s)} = Ls$$



# Electronic Controllers

- Impedance approach for obtaining transfer functions

Example 1)



$$I_2(s) = \frac{E(s)}{Z_1(s)}, I_3(s) = \frac{E(s)}{Z_2(s)}$$

$$i_1 = i_2 + i_3$$

$$I_1(s) = \frac{E(s)}{Z(s)}$$

$$I_1(s) = \frac{E(s)}{Z(s)} = \frac{E(s)}{Z_1(s)} + \frac{E(s)}{Z_2(s)}$$

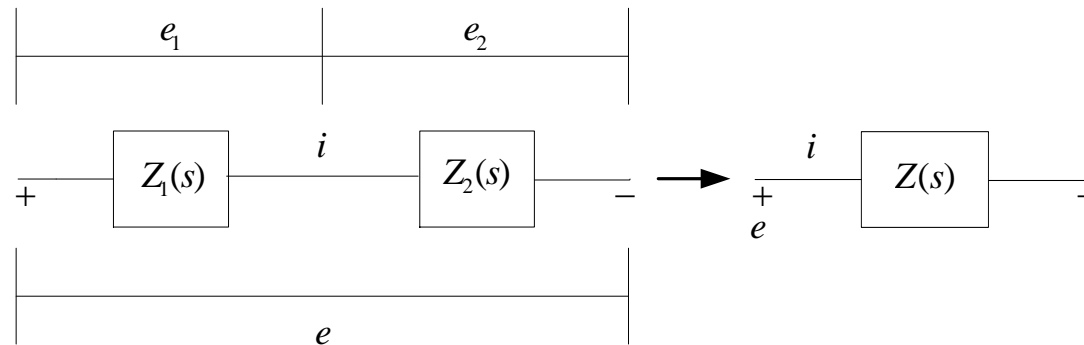
$$\frac{1}{Z(s)} = \frac{1}{Z_1(s)} + \frac{1}{Z_2(s)}$$



# Electronic Controllers

- Impedance approach for obtaining transfer functions

Example 2)



$$E(s) = E_1(s) + E_2(s)$$

$$I(s) \cdot Z(s) = Z_1(s) \cdot I(s) + Z_2(s) \cdot I(s)$$

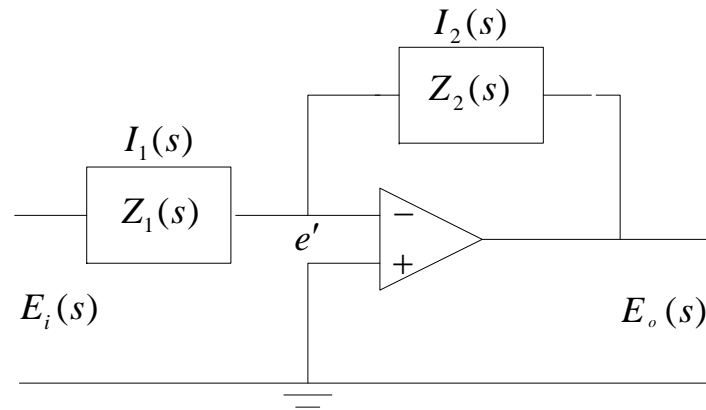
$$\therefore Z(s) = Z_1(s) + Z_2(s)$$



# Electronic Controllers

- Impedance approach for obtaining transfer functions

Example 3)



$$I_1(s) = I_2(s)$$

$$\frac{E_i(s)}{Z_1(s)} = -\frac{E_o(s)}{Z_2(s)}$$

$$\frac{E_o(s)}{E_i(s)} = -\frac{Z_2(s)}{Z_1(s)}$$

앞의 예에서

$$Z_1(s) = R_1$$

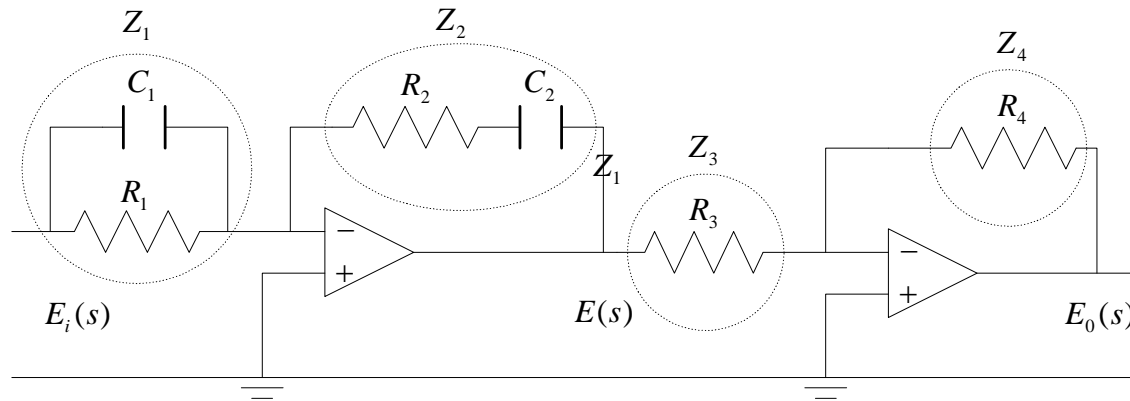
$$\frac{1}{Z_2(s)} = \frac{1}{R_2} + \frac{1}{1/CS}$$

$$\frac{E_o(s)}{E_i(s)} = -\frac{1/(CS + 1/R_2)}{R_1} = -\frac{R_2}{R_1} \cdot \frac{1}{R_2CS + 1}$$



# Electronic Controllers

## • OP-amp 로 PID 만들기



$$\frac{1}{Z_1(s)} = \frac{1}{R_1} + \frac{1}{1/C_1 S}$$

$$Z_2(s) = R_2 + \frac{1}{C_2 S}$$

$$Z_3(s) = R_3$$

$$Z_4(s) = R_4$$

$$\frac{E(s)}{E_i(s)} = -\frac{Z_2(s)}{Z_1(s)}, \quad \frac{E_0(s)}{E(s)} = -\frac{Z_4(s)}{Z_3(s)}$$

양변을 곱하면

$$\frac{E_0(s)}{E_i(s)} = \frac{Z_2(s)Z_4(s)}{Z_1(s)Z_3(s)} = k_p \left( 1 + \frac{1}{T_i s} + T_d s \right)$$

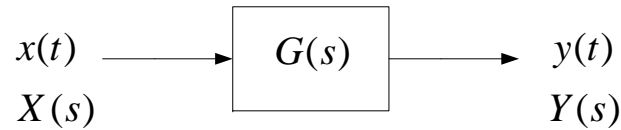
$$K_p = \frac{R_4(R_1 C_1 + R_2 C_2)}{R_3 R_1 C_2}, \quad T_i = R_1 C_1 + R_2 C_2, \quad T_d = \frac{R_1 C_1 R_2 C_2}{R_1 C_1 + R_2 C_2}$$

→ PID



# Phase Lead and Phase Lag in Sinusoidal Response

Linearsystem



$$G(s) = \frac{P(s)}{g(s)} = \frac{P(s)}{(S + S_1)(S + S_2) + \dots + (S + S_n)}$$

위 system에  $x(t) = X \sin \omega t$  를 넣어주면  $y(t)$ 는 ?

$$X(s) = \frac{X\omega}{s^2 + \omega^2}$$

$$\Rightarrow Y(s) = G(s)X(s) = G(s) \frac{X\omega}{s^2 + \omega^2}$$

$$= \frac{b_1}{s + s_1} + \frac{b_2}{s + s_2} + \dots + \frac{b_n}{s + s_n} + \frac{a}{s + j\omega} + \frac{\bar{a}}{s - j\omega}$$

1) Transient response  $\rightarrow$  Stable system인 경우 = 0

2) Stable system인 경우 Steady state response 는

$$y(t) = ae^{-j\omega t} + \bar{a}e^{j\omega t}$$

$$a = G(s) \frac{\omega}{s^2 + \omega^2} (-s + j\omega)_{s=-j\omega} = -\frac{XG(-j\omega)}{2j}$$

$$\bar{a} = G(s) \frac{X\omega}{s^2 + \omega^2} (s - j\omega)_{s=j\omega} = \frac{XG(j\omega)}{2j}$$

$$G(j\omega) = |G(j\omega)|e^{j\phi}$$

$$G(-j\omega) = |G(j\omega)|e^{-j\phi}, \phi = \text{phase}$$

$$\therefore y(t) = X|G(j\omega)| \frac{e^{j(\omega t + \phi)} - e^{-j(\omega t + \phi)}}{2j} = X|G(j\omega)| \sin(\omega t + \phi)$$

$$= Y \sin(\omega t + \phi), Y = X|G(j\omega)|, \phi = \angle G(j\omega)$$



# Phase Lead and Phase Lag in Sinusoidal Response

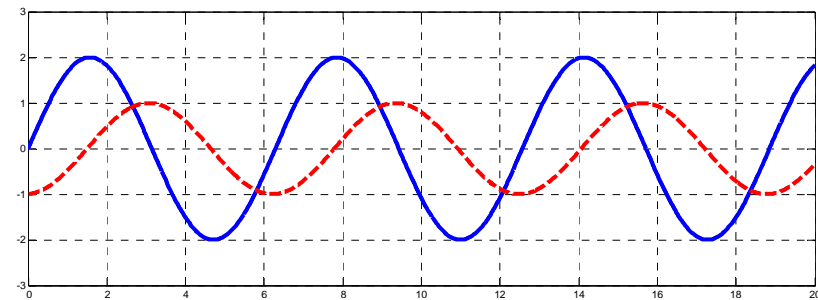
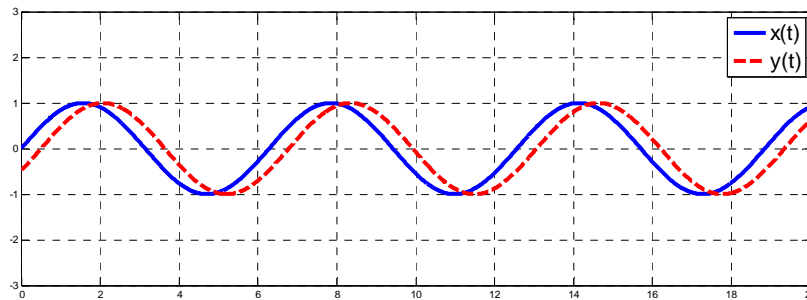
Example) First order system

$$G(s) = \frac{K}{Ts + 1}$$

$$G(j\omega) = \frac{K}{Tj\omega + 1}, |G(j\omega)| = \frac{K}{\sqrt{1 + T^2\omega^2}}$$

$$G(j\omega) = \frac{K}{Tj\omega + 1}, |G(j\omega)| = \frac{K}{\sqrt{1 + T^2\omega^2}}, \angle G(j\omega) = -\tan^{-1} T\omega$$

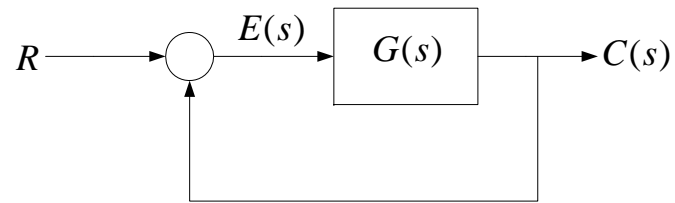
$$\therefore y_{ss}(t) = X \frac{K}{\sqrt{1 + T^2\omega^2}} \sin(\omega t + \phi), \quad \phi = -\tan^{-1} T\omega$$



$\phi < 0$  : phase lag,  $\phi > 0$  : phase lead



# Steady state Error in Unity Feedback control systems



$$G(s) = \frac{K(T_a s + 1)(T_b s + 1) \cdots (T_n s + 1)}{S^N (T_1 s + 1)(T_2 s + 1) \cdots (T_p s + 1)}$$

N=0 ; Type 0, N=1 ; Type 1, N=2 ; Type 2

Steady state Error 를 생각해 보자

$$E(s) = \frac{1}{1 + G(s)} R(s)$$

1)  $R(s) = \frac{1}{s}$  일 경우 (unit step input),

$$e_{ss} = \lim_{s \rightarrow 0} s E(s) = \lim_{s \rightarrow 0} s \frac{1}{1 + G(s)} \frac{1}{s} = \frac{1}{1 + G(0)}$$

Static position error constant  $k_p$   $k$  ; Type 0 system

$$k_p = \lim_{s \rightarrow 0} G(s) = G(0) = \infty \quad ; \text{Type 1 system}$$

$\infty$  ; Type 2 system

$$e_{ss} = \frac{1}{1 + k_p} = \frac{1}{0} \quad ; \text{Type 0 system}$$

$$0 \quad ; \text{Type 1, 2, ... system}$$





# Steady state Error in Unity Feedback control systems

2)  $R(s) = \frac{1}{s^2}$  일 경우 (unit step input),

$$e_{ss} = \lim_{s \rightarrow 0} s \frac{1}{1+G(s)} \frac{1}{s^2} = \lim_{s \rightarrow 0} \frac{1}{s(G(s)+1)} = \lim_{s \rightarrow 0} \frac{1}{sG(s)}$$

Static velocity error constant  $k_v$

$$k_v = \lim_{s \rightarrow 0} sG(s) = G(0) = \begin{cases} 0 & ; \text{Type 0 system} \\ k & ; \text{Type 1 system} \\ \infty & ; \text{Type 2, 3.. system} \end{cases} \quad e_{ss} = \frac{1}{k_v} = \begin{cases} \infty & ; \text{Type 0 system} \\ \frac{1}{k} & ; \text{Type 1 system} \\ 0 & ; \text{Type 2, 3,.. system} \end{cases}$$

3)  $R(s) = \frac{1}{s^3}$  일 경우 (unit step input),

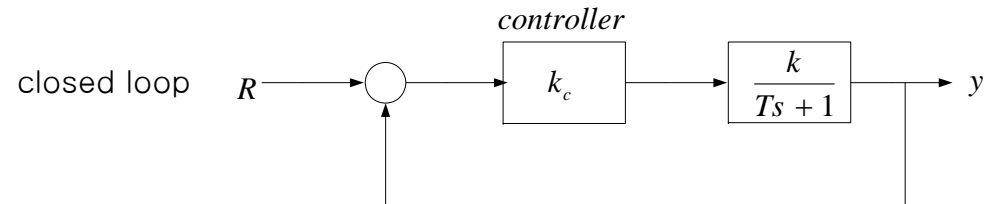
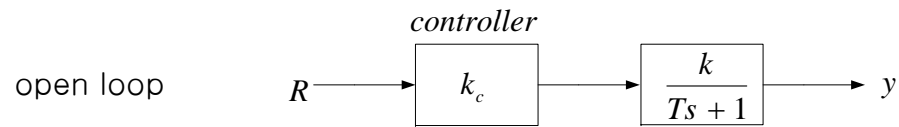
$$e_{ss} = \lim_{s \rightarrow 0} s \frac{1}{1+G(s)} \frac{1}{s^3} = \lim_{s \rightarrow 0} \frac{1}{s^2 G(s)}$$

Static acceleration error constant  $k_a$

$$k_a = \lim_{s \rightarrow 0} s^2 G(s) = G(0) = \begin{cases} 0 & ; \text{Type 0 system} \\ 0 & ; \text{Type 1 system} \\ k & ; \text{Type 2 system} \\ \infty & ; \text{Type 3 system} \end{cases} \quad e_{ss} = \frac{1}{k_a} = \begin{cases} \infty & ; \text{Type 0, 1 system} \\ \frac{1}{k} & ; \text{Type 2 system} \\ 0 & ; \text{Type 3, 4,.. system} \end{cases}$$



# Open/Closed loop control systems



Open loop Transfer function 에서

$$\frac{y}{R} = k_c \frac{1}{Ts + 1} \rightarrow k_c = \frac{1}{k} \text{ 이 되어야 error}=0 \text{ 이 된다.}$$

Closed loop Transfer function 에서

$$\frac{y}{R} = \frac{k_p \frac{k}{Ts + 1}}{1 + k_p \frac{k}{Ts + 1}} = \frac{k_p k}{Ts + 1 + k_p k}$$

Steady/ state error for  $R(s) = \frac{1}{s}$

Open loop Transfer function 에서  $e_{ss} = 0$

Closed loop Transfer function 에서  $e_{ss} = 1 - \frac{k_p k}{1 + k_p k} = \frac{1}{1 + k_p k}$



# Open/Closed loop control systems

예외의 경우에 대한 예>

$k = 10, \Delta k = 1$  인 model error 가 있을 경우

Open loop Transfer function 에서

$$\frac{y}{R} = \frac{1}{k_c} \frac{k + \Delta k}{Ts + 1}, \quad y(t) = \frac{k + \Delta k}{k} = 1.1 \quad (10\% \text{ steady state error})$$

Closed loop Transfer function 에서

$$e_{ss} = \frac{1}{1 + k_p k} \quad \text{let } k_p = \frac{100}{k} \Rightarrow e_{ss} = \frac{1}{1 + \frac{100}{k} k} = \frac{1}{101}$$

$$k + \Delta k, \quad e_{ss} = \frac{1}{1 + \frac{100}{k}(k + \Delta k)} = \frac{1}{1 + 10(11)} = \frac{1}{111} = 0.009$$

