

Ch.2 Equations of fluid motion

노트 제목

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- continuum Kn = mean free path (λ) / flow length scale (l)
Knudsen number $\ll 1$

- Eulerian & Lagrangian fields

$$\underbrace{\frac{D}{Dt}}_{\text{material derivative}} \equiv \frac{\partial}{\partial t} + \underline{U} \cdot \nabla = \underbrace{\frac{\partial}{\partial t}}_{\text{time derivative}} + \underbrace{U_j \frac{\partial}{\partial x_j}}_{\text{convective derivative}}$$

- Continuity equation

$$\frac{\partial \rho}{\partial t} + \nabla \cdot (\rho \underline{U}) = 0 \quad \underline{\nabla \cdot U} : \text{dilatation}$$

For constant ρ , $\nabla \cdot \underline{U} = 0$

(incomp. flow)

\underline{U} is solenoidal or divergence free.

- momentum equation

τ_{ij} : stress tensor, $\tau_{ij} = \tau_{ji}$

$$\rho \frac{DU_j}{Dt} = \frac{\partial \tau_{ij}}{\partial x_i} - \rho g_j$$

For constant-property
Newtonian fluids,

$$\left(= \frac{\partial U_j}{\partial t} + U_i \frac{\partial U_j}{\partial x_i} \right)$$

$$\tau_{ij} = -p \delta_{ij} + \mu \left(\frac{\partial U_i}{\partial x_j} + \frac{\partial U_j}{\partial x_i} \right)$$

↑ pressure ↑ viscosity

$$\overrightarrow{(\partial u_i / \partial x_i = 0)} \quad \rho \frac{DU_j}{Dt} = \mu \nabla^2 U_j - \frac{\partial p}{\partial x_j} - \rho g_j$$

($\underline{g} = -\nabla\psi$ ψ : gravitational potential)

$\rho' = \rho + \rho\psi$ ν : kinematic viscosity

$$\rightarrow \frac{DU_j}{Dt} = -\frac{1}{\rho} \frac{\partial p'}{\partial x_j} + \left(\frac{\mu}{\rho}\right) \nabla^2 U_j \quad \text{Navier-Stokes equation}$$

$$\rightarrow \frac{DU}{Dt} = -\frac{1}{\rho} \nabla p + \nu \nabla^2 \underline{U} \quad (\text{drop prime})$$

For inviscid fluid ($\mu=0$), $\tau_{ij} = -p\delta_{ij}$

$$\rightarrow \frac{DU}{Dt} = -\frac{1}{\rho} \nabla p : \text{Euler equation}$$

• Role of pressure

$$\nabla \cdot \left[\left(\frac{D}{Dt} - \nu \nabla^2 \right) \underline{U} = -\frac{1}{\rho} \nabla p \right]$$

$$= \frac{\partial}{\partial t} + (\underline{U} \cdot \nabla) \underline{U}$$

$$\rightarrow \left(\frac{D}{Dt} - \nu \nabla^2 \right) \nabla \cdot \underline{U} = -\frac{1}{\rho} \nabla^2 p - \frac{\partial U_i}{\partial x_j} \frac{\partial U_j}{\partial x_i}$$

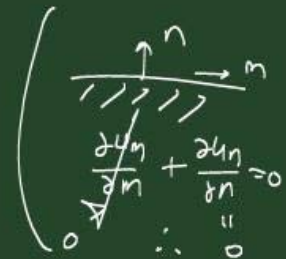
when $\nabla \cdot \underline{U} = 0$, $\nabla^2 p = -\rho \frac{\partial U_i}{\partial x_j} \frac{\partial U_j}{\partial x_i}$

At solid surface, $\frac{\partial p}{\partial n} = \mu \frac{\partial^2 U_n}{\partial n^2}$

If p is a sol., $p+c$ is sol. too.

Using Green ft., \rightarrow homo. sol.

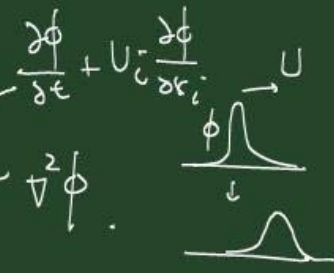
$$p(\underline{x}, t) = p^{(h)}(\underline{x}, t) + \frac{\rho}{4\pi} \iint_V \left(\frac{\partial U_i}{\partial x_j} \frac{\partial U_j}{\partial x_i} \right)_{\underline{y}, t} \frac{d\underline{y}}{|\underline{x} - \underline{y}|}$$



• Conserved passive scalars.

$\phi(\underline{x}, t)$: conserved passive scalar

In a constant-property flow, $\frac{D\phi}{Dt} = \Gamma \nabla^2 \phi$.



Γ : (const & uniform) diffusivity

ϕ is conserved because there is no source and sink in the equation.

ϕ is passive because it does not change the flow.

ϕ : temperature $\rightarrow \Gamma$: thermal diffusivity
 $Pr = \nu/\Gamma$ (Prandtl number)

concentration $\rightarrow \Gamma$: molecular diffusivity
 $Sc = \nu/\Gamma$ (Schmidt number)

boundedness : if the initial & boundary values of ϕ lie within a given range


$$\phi_{min} \leq \phi \leq \phi_{max}$$

then $\phi(\underline{x}, t)$ for all (\underline{x}, t) also lies in this range.

i.e., values of ϕ greater than ϕ_{max} or less than ϕ_{min} cannot occur.

• Vorticity equation

turbulent flow \rightarrow rotational \rightarrow non-zero vorticity

vorticity $\underline{\omega} = \nabla \times \underline{U}$: twice the rotation rate 

$\nabla \times [N-S \text{ eq.}] \rightarrow$ vortex stretching : increase $(\underline{\omega})$

$$\rightarrow \frac{D\underline{\omega}}{Dt} = \boxed{\underline{\omega} \cdot \nabla \underline{U}} + \nu \nabla^2 \underline{\omega}$$

$$\frac{D\omega_i}{Dt} = \omega_1 \frac{\partial U_1}{\partial x_1} + \omega_2 \frac{\partial U_1}{\partial x_2} + \omega_3 \frac{\partial U_1}{\partial x_3} + \nu \nabla^2 \omega_i$$

For the material line : $\frac{d\xi}{dt} = (\xi \cdot \nabla) \underline{U}$

\therefore In inviscid flow, the vorticity vector behaves in the same way as an infinitesimal material line element. \rightarrow Helmholtz theorem.

In 2-D (1, 2) $\Rightarrow (U_1, U_2 \neq 0, \omega_3 \neq 0)$

$$\frac{D\omega_3}{Dt} = \omega_1 \frac{\partial U_3}{\partial x_1} + \omega_2 \frac{\partial U_3}{\partial x_2} + \omega_3 \frac{\partial U_3}{\partial x_3} + \nu \nabla^2 \omega_3$$

\rightarrow no vortex stretching \rightarrow decays

- Rates of strain and rotation

$$\frac{\partial U_i}{\partial x_j} = \underbrace{\frac{1}{2} \left(\frac{\partial U_i}{\partial x_j} + \frac{\partial U_j}{\partial x_i} \right)}_{S_{ij} \text{ " strain rate tensor (symmetric ")}} + \underbrace{\frac{1}{2} \left(\frac{\partial U_i}{\partial x_j} - \frac{\partial U_j}{\partial x_i} \right)}_{\Omega_{ij} \text{ " rotation rate tensor (anti-symmetric ")}}$$

$$\hat{T}_{ij} = -p\delta_{ij} + 2\mu S_{ij} \quad (\text{not a ft. of } \Omega_{ij})$$
$$\omega_i = -\epsilon_{ijk} \Omega_{jk} \quad (\text{not a ft. of } S_{ij})$$
$$\Omega_{ij} = -\frac{1}{2} \epsilon_{ijk} \omega_k$$