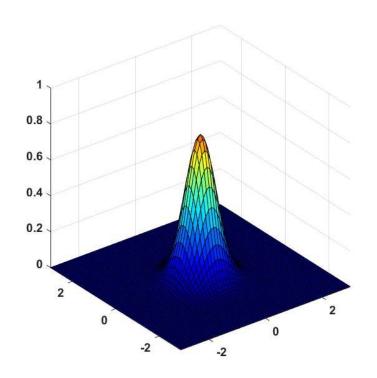


Diffusion Equation and Its Solutions







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Chapter 2 Diffusion Equation and Its Solutions

Contents

- 2.1 Fick's Law for Molecular Diffusion
- 2.2 The Random Walk and Molecular Diffusion
- 2.3 Mathematics of Diffusion Equation





Chapter 2 Diffusion Equation and Its Solutions

Objectives

- Present equations and concepts for molecular diffusion processes
- Present two different rationalizations for the molecular diffusion equation
- Introduce statistical aspects of concentration distributions
- Discuss boundary conditions for various inputs of the pollutants in rivers
- Derive <u>analytical solutions</u> to the diffusion equations for different BCs





2.1.1 Diffusion Equation

Diffusion and Advection

fluids at rest \rightarrow diffusion

moving fluids \rightarrow diffusion + advection

• molecular diffusion versus turbulent diffusion



- molecular diffusion ~ only important in microscopic scale; not much important in environmental problems
- turbulent diffusion ~ large scale; analogous to molecular diffusion
- Fick (1855) adopted Fourier's law of heat flow (1822) to diffusion

	Fourier	Fick
transport	heat	mass
gradient	temp.	conc.





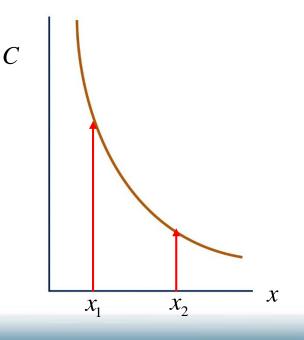
1) Fick's law

 $q \propto \frac{\partial C}{\partial x}$

- \rightarrow <u>flux of solute mass</u>, that is, the mass of a solute crossing a unit area per unit time in
- a given direction, is proportional to the gradient of solute concentration in that direction.

q = solute mass flux (mass per unit area and per unit time; 질량전달률)

C = mass concentration of dispersing solute



time rate of heat per unit area in a

temperature gradient in direction

given direction is proportional to the





Since mass transport is from high to low concentrations 따라서 q를 양의 값으로 나타내기 위해서는 – 부호를 붙여야 함.

$$q \propto \frac{\Delta C}{\Delta x} = \frac{C_1 - C_2}{x_2 - x_1} = -\frac{C_2 - C_1}{x_2 - x_1} = -\frac{\partial C}{\partial x} = -slope$$

$$q = -D\frac{\partial C}{\partial x}$$
(2.1)

- → Fick's law of diffusion
- D = coefficient of proportionality
- \rightarrow diffusion coefficient (m²/s), molecular diffusivity
- → distributed parameter





[Re] Two basic models for diffusion

1) Diffusion model (Fick's law)

$$q = -D\frac{\partial C}{\partial x}$$

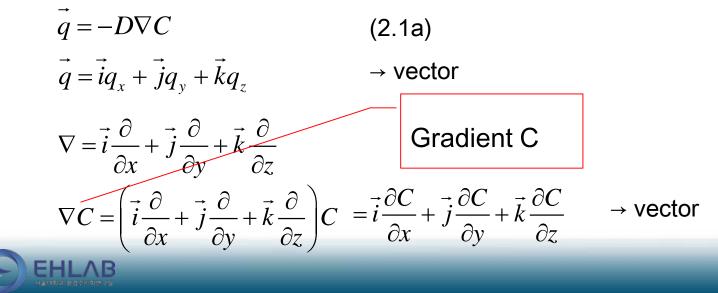
q = mass flux per unit time and unit area $q_c =$ mass transfer per unit time per unit volume

2) Mass transfer model

 $q_c = k \Delta C$

 $k = mass transfer coefficient \rightarrow lumped parameter$

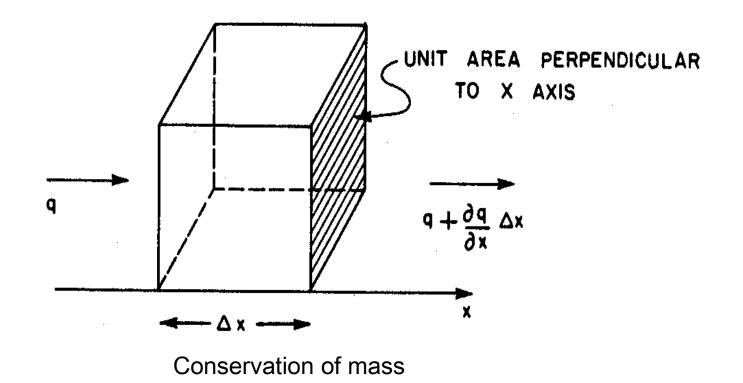
[Re] Fick's law in 3D





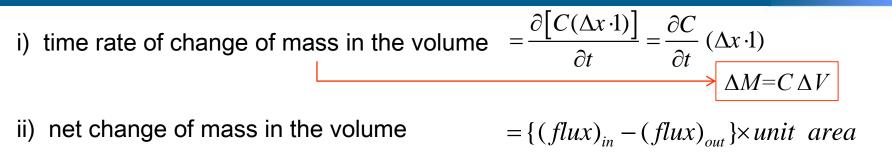
2) Conservation of Mass

Consider mass conservation for 1-D transport process of the infinitesimal control volume









$$= q - \left(q + \frac{\partial q}{\partial x}\Delta x\right)$$
$$= -\frac{\partial q}{\partial x}\Delta x$$

Now, combine (i) and (ii)

$$\frac{\partial C}{\partial t} \Delta x = -\frac{\partial q}{\partial x} \Delta x$$

 $\frac{\partial C}{\partial t} = -\frac{\partial q}{\partial x}$

(2.2)

→ Mass conservation equation





3) Diffusion Equation

Combine Eq. (2.1) and (2.2) $\frac{\partial C}{\partial t} = -\frac{\partial}{\partial x} \left(-D \frac{\partial C}{\partial x} \right)$ $\frac{\partial C}{\partial t} = D \frac{\partial^2 C}{\partial x^2}$ (2.3)

⇒ Diffusion Equation (Heat Equation)

Diffusion Equation = Fick's law of diffusion + Conservation of mass

Differentiate Eq. (2.2) w.r.t. x $\frac{\partial}{\partial x} \left(\frac{\partial C}{\partial t} \right) = -\frac{\partial^2 q}{\partial x^2}$ $LHS = \frac{\partial}{\partial t} \left(\frac{\partial C}{\partial x} \right) = \frac{\partial}{\partial t} \left(-\frac{q}{D} \right) = -\frac{1}{D} \frac{\partial q}{\partial t}$

$$\frac{\partial q}{\partial t} = D \frac{\partial^2 q}{\partial x^2}$$





[Re] Vector and Tensor

Scalar: 크기만 있는 양

~ pressure, density, temperature, concentration

Vector : 크기와 방향이 있는 양

~ velocity, force

Tensor: 스칼라와 벡터를 확장시킨 양, n차 텐서로 표현

0차 텐서 → 스칼라; 1차텐서 → 벡터

2차 텐서: 응력, 변형률, 확산계수

Vector \overline{F}

 $\overline{F} = F_x \overline{e_x} + F_y \overline{e_y} + F_z \overline{e_z}$ $\overline{e_x}, \overline{e_y}, \overline{e_z} = \text{unit vectors}$

 F_x, F_y, F_z = projections of the magnitude of \overline{F} on the *x*, *y*, *z* axes





(1) Magnitude of \overline{F}

$$F = \left| \overline{F} \right| = \left(F_x^2 + F_y^2 + F_z^2 \right)^{1/2}$$

(2) Dot product = Scalar product $S = \overline{F \cdot G} = \left| \overline{F} \right| \left| \overline{G} \right| \cos \phi$

(3) Vector product = Cross product

 $\overline{V} = \overline{F} \times \overline{G} \longrightarrow \text{vector}$

magnitude of
$$\overline{V} = |\overline{V}| = |\overline{F}||\overline{G}|\sin\phi$$

direction of \overline{V} = perpendicular to the plane of \overline{F} and \overline{G}
 \rightarrow right hand rule





(4) Derivatives of vectors

$$\frac{\partial F}{\partial s} = \frac{\partial F_x}{\partial s} \overline{e_x} + \frac{\partial F_y}{\partial s} \overline{e_y} + \frac{\partial F_z}{\partial s} \overline{e_z}$$

(5) Gradient of F (scalar) \rightarrow vector

grad
$$F = \nabla F = \frac{\partial F}{\partial x} \overline{e_x} + \frac{\partial F}{\partial y} \overline{e_y} + \frac{\partial F}{\partial y} \overline{e_z} \rightarrow \text{vector}$$

 $[\nabla] = \text{ pronounced as 'del' or 'nabla'}$
 $\nabla = \overline{e_i} \frac{\partial}{\partial x_i}$

[Re] $grad(scalar) \rightarrow vector$ $grad(vector) \rightarrow tensor$ grad(F+G) = grad F + grad Ggrad CF = C grad F





(6) Divergence of \overline{F} (vector): 벡터의 내적 \rightarrow scalar

(7)

$$div\overline{F} = \nabla \cdot \overline{F} = \left(\frac{\partial}{\partial x}\overline{e_x} + \frac{\partial}{\partial y}\overline{e_y} + \frac{\partial}{\partial z}\overline{e_z}\right) \cdot \overline{F}$$

$$= \left(\frac{\partial}{\partial x}\overline{e_x} + \frac{\partial}{\partial y}\overline{e_y} + \frac{\partial}{\partial z}\overline{e_z}\right) \cdot \left(F_x\overline{e_x} + F_y\overline{e_y} + F_z\overline{e_z}\right)$$

$$= \left|\frac{\partial}{\partial x}\overline{e_x}\right| F_x\overline{e_x} |\cos 0 + \frac{\partial F_y}{\partial x}\overline{e_x}\overline{e_y}\cos 90^\circ + \frac{\partial F_z}{\partial x}\overline{e_x}\overline{e_z}\cos 90^\circ$$

$$+ \left|\frac{\partial F}{\partial y}\overline{e_y}\right| F_y\overline{e_y} |\cos 0 + \left|\frac{\partial}{\partial z}\overline{e_z}\right| F_z\overline{e_z} |\cos 0$$

$$= \frac{\partial F_x}{\partial x} + \frac{\partial F_y}{\partial y} + \frac{\partial F_z}{\partial z} \longrightarrow \text{scalar}$$

$$Curl \ \overline{V} = \nabla \times \overline{V} = \left| \begin{array}{c}\overline{i} & \overline{j} & \overline{k} \\ \frac{\partial}{\partial x} & \frac{\partial}{\partial x} & \frac{\partial}{\partial x} \\ u & v & w \end{array} \right| = \left(\frac{\partial w}{\partial y} - \frac{\partial v}{\partial z}\right) \overline{i} + \left(\frac{\partial u}{\partial z} - \frac{\partial w}{\partial x}\right) \overline{j} + \left(\frac{\partial v}{\partial x} - \frac{\partial u}{\partial y}\right) \overline{k}$$



(8)
$$div(grad F) = \nabla \cdot \nabla F = \nabla^2 F \equiv Laplacian of F$$

$$= \frac{\partial^2 F_x}{\partial x^2} + \frac{\partial^2 F_y}{\partial y^2} + \frac{\partial^2 F_z}{\partial z^2}$$

$$\begin{aligned} \text{Pf]} \quad & div (grad \ F) = div \left(\frac{\partial F}{\partial x} \overline{e_x} + \frac{\partial F}{\partial y} \overline{e_y} + \frac{\partial F}{\partial z} \overline{e_z} \right) \\ &= \frac{\partial}{\partial x} \left(\frac{\partial F}{\partial x} \right) + \frac{\partial}{\partial y} \left(\frac{\partial F}{\partial y} \right) + \frac{\partial}{\partial z} \left(\frac{\partial F}{\partial z} \right) \\ &= \frac{\partial^2 F_x}{\partial x^2} + \frac{\partial^2 F_y}{\partial y^2} + \frac{\partial^2 F_z}{\partial z^2} \\ \nabla \cdot \nabla = \left(\overline{i} \frac{\partial}{\partial x} + \overline{j} \frac{\partial}{\partial y} + \overline{k} \frac{\partial}{\partial z} \right) \left(\overline{i} \frac{\partial}{\partial x} + \overline{j} \frac{\partial}{\partial y} + \overline{k} \frac{\partial}{\partial z} \right) \\ &= \frac{\partial^2}{\partial x^2} + \frac{\partial^2}{\partial y^2} + \frac{\partial^2}{\partial z^2} = \nabla^2 \end{aligned}$$





텐서식의 표기

1차 텐서: 벡터량 $a_i b_i = a_1 b_1 + a_2 b_2 + a_3 b_3$ $\frac{\partial u_i}{\partial x_i} = \frac{\partial u_1}{\partial x_1} + \frac{\partial u_2}{\partial x_2} + \frac{\partial u_3}{\partial x_3} = \frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} + \frac{\partial w}{\partial z}$

2차 텐서

$$a_{ij}b_{ij} = a_{11}b_{11} + a_{12}b_{12} + a_{13}b_{13} + a_{21}b_{21} + a_{22}b_{22} + a_{23}b_{23}$$
$$+a_{31}b_{31} + a_{32}b_{32} + a_{33}b_{33}$$

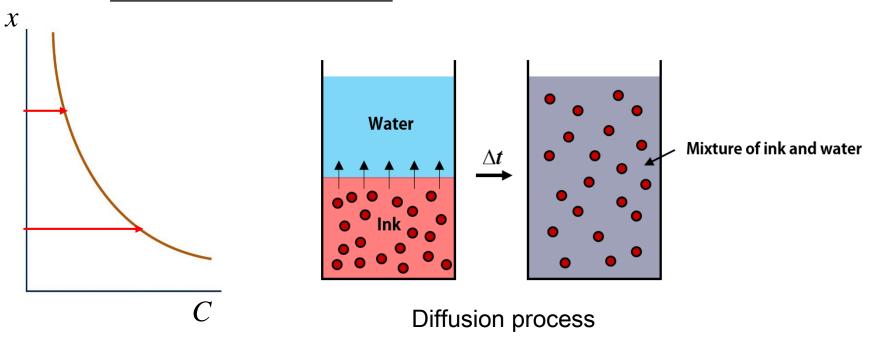




2.1.2 Diffusion Process

1. Diffusion process

= process by which matter is transported from one part of a system to another as a result of <u>random molecular motions</u>







(i) Watch individual molecules of ink

- \rightarrow Motion of each molecule is a random one.
- → Each molecule of ink behaves independently of the others.
- \rightarrow Each molecule of ink is constantly undergoing collision with other.
- → As a result of collisions, if moves sometimes towards a region of higher, sometimes of lower concentrations, having <u>no preferred direction of motion</u>.
- \rightarrow The motion of a single molecule is described in terms of **random walk model**
- → It is possible to calculate the mean-square distance travelled in given interval of time.

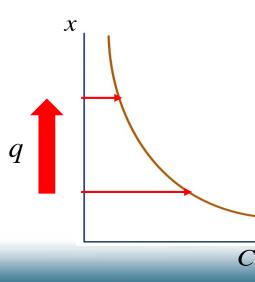
It is not possible to say in what direction a given molecule will move in that time





- (ii) <u>On the average</u> some <u>fraction</u> of the molecules in the lower element of volume will cross the interface from below, and <u>the same fraction</u> of molecule in the upper element will cross the interface from above in a given time.
- (iii) Thus, simply because there are <u>more ink molecules</u> in the lower element than in the upper one, there is a <u>net transfer from the lower to the upper side</u> of the section as a result of random molecular motions.
- (iv) Transfer of ink molecules from the region of higher to that of lower concentration

is observed.







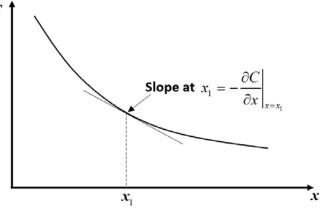
2. Molecular Diffusion

- (i) Fick's 1st Law:
- → Rate of mass transport of material or flux through the liquid, by molecular diffusion

is proportional to the concentration gradient of the material in the liquid.

Diffusive mass flux,
$$q = -D \frac{\partial C}{\partial x}$$
 (1)

(negative sign arises because diffusion occurs in the direct opposite to that of increasing concentration)



Fick's law of molecular diffusion





(ii) Fick's 2nd Law:

Conservation of mass + Fick's 1st Law
$$\rightarrow \frac{\partial C}{\partial t} = D \frac{\partial^2 C}{\partial x^2}$$

Assumption for Fick's Law

 \rightarrow Fick's 1st law is consistent only for an isotropic medium, whose structure and diffusion properties in the neighborhood of any point are the same relative to all directions.

In molecular diffusion: In turbulent diffusion: In shear flow dispersion:

$$D_{x} = D_{y} = D_{z} = D$$
$$\mathcal{E}_{x}, \mathcal{E}_{y}, \mathcal{E}_{z}$$
$$K_{x}, K_{y}, K_{z}$$

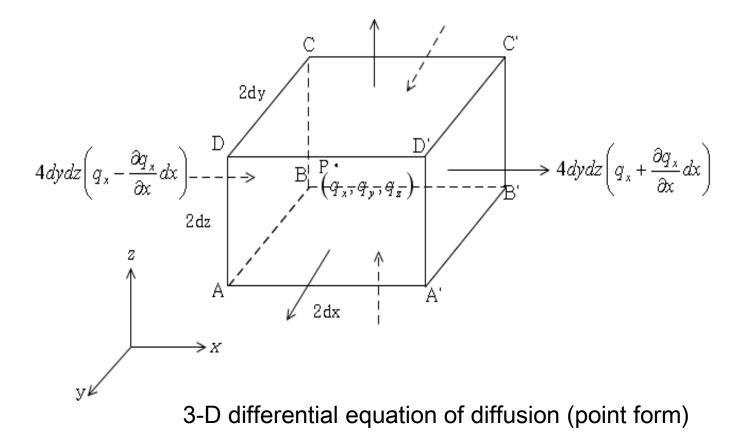
[Cf] anisotropic medium

 \rightarrow diffusion properties depend on the direction in which they are measured





3. 3D differential equation of diffusion – point form







(i) Rate at which diffusing substance enters the element through the face ABCD in the x direction

$$Influx = 4dydz \left(q_x - \frac{\partial q_x}{\partial x} dx \right)$$

In which q_x = rate of transfer through unit area of the corresponding plane through P

(ii) Rate of loss of diffusing substance through the face A'B'C'D'

$$Outflux = 4dydz \left(q_x + \frac{\partial q_x}{\partial x}dx\right)$$

(iii) Contribution to the rate of increase of diffusing substance in the element from these two faces

$$Netflux = 4dydz \left(q_x - \frac{\partial q_x}{\partial x} dx \right) - 4dydz \left(q_x + \frac{\partial q_x}{\partial x} dx \right) = -8dxdydz \frac{\partial q_x}{\partial x}$$





(iv) Similarly from the other faces we obtain

$$-8dxdydz\frac{\partial q_y}{\partial y}$$
 and $-8dxdydz\frac{\partial q_z}{\partial z}$

(v) Time rate at which the amount of diffusing substance in the element increases

$$\frac{\partial}{\partial t}(mass) = \frac{\partial}{\partial t}(volume \times conc.)$$
$$= 8dxdydz \frac{\partial c}{\partial t}$$

(vi) Combine (iii), (iv), and (v)

$$8dxdydz\frac{\partial c}{\partial t} = -8dxdydz\left(\frac{\partial q_x}{\partial x} + \frac{\partial q_y}{\partial y} + \frac{\partial q_z}{\partial z}\right)$$
$$\frac{\partial c}{\partial t} + \frac{\partial q_x}{\partial x} + \frac{\partial q_y}{\partial y} + \frac{\partial q_z}{\partial z} = 0$$
(2)





(vii) Substitute Fick's law into Eq.(2)

$$\frac{\partial C}{\partial t} = -\frac{\partial}{\partial x} \left(-D\frac{\partial C}{\partial x} \right) - \frac{\partial}{\partial y} \left(-D\frac{\partial C}{\partial y} \right) - \frac{\partial}{\partial z} \left(-D\frac{\partial C}{\partial z} \right) = \frac{\partial}{\partial x} \left(D\frac{\partial C}{\partial x} \right) + \frac{\partial}{\partial y} \left(D\frac{\partial C}{\partial y} \right) + \frac{\partial}{\partial z} \left(D\frac{\partial C}{\partial z} \right)$$

Remember *D* is isotropic for molecular diffusion.

For homogeneous medium; $D \neq f_n(x, y, z)$

$$\frac{\partial C}{\partial t} = D\left(\frac{\partial^2 C}{\partial x^2} + \frac{\partial^2 C}{\partial y^2} + \frac{\partial^2 C}{\partial z^2}\right)$$

→ Fick's 2nd law of diffusion





2.1.3 Advection-Diffusion Equation

Consider fluid moving with velocity \vec{u}

 $\vec{u} = u\vec{i} + v\vec{j} + w\vec{k}$

- Advection = transport by the mean motion of the fluid
- Assume the transports by advection and by diffusion are <u>separate and additive</u> processes.
- \rightarrow rate of mass transport through unit area (y-z plane) by x component of velocity, q_u

$$q_u = uC \tag{2.4}$$

[Re] advective flux

mass = volume · concentration

mass rate = volume rate \cdot conc. = discharge \cdot conc. = velocity \cdot area \cdot conc.

advective flux = mass rate /area = velocity \cdot conc.





Total rate of mass transport

$$q = uC + \left(-D\frac{\partial C}{\partial x}\right) \tag{2.5}$$

= advective flux + diffusive flux

Substitute (2.5) into mass conservation equation, (2.3)

$$\frac{\partial C}{\partial t} + \frac{\partial q}{\partial x} = 0$$
$$\frac{\partial C}{\partial t} + \frac{\partial}{\partial x} \left(uC - D\frac{\partial C}{\partial x} \right) = 0$$
$$\frac{\partial C}{\partial t} + \frac{\partial}{\partial x} (uC) = D\frac{\partial^2 C}{\partial x^2}$$

→ 1-D advection-diffusion equation (1차원 이송-확산 방정식)

 \rightarrow linear, 2nd order PDE





[Re] Conservation of mass in 3D

$$\frac{\partial C}{\partial t} = -\nabla \cdot \vec{q} = -\left(\frac{\partial q_x}{\partial x} + \frac{\partial q_y}{\partial y} + \frac{\partial q_z}{\partial z}\right)$$
$$\frac{\partial C}{\partial t} + \nabla \cdot \vec{q} = 0$$
(i)

Then consider q by various transport mechanisms

- molecular diffusion (Fickian diffusion) $\rightarrow \vec{q} = -D\nabla C$
- advection by ambient current $\rightarrow \vec{q} = C\vec{u}$

$$\vec{q} = C\vec{u} - D\nabla C$$

Substitute (ii) into (i)

$$\frac{\partial C}{\partial t} + \nabla \cdot \left(\vec{Cu} - D\nabla C \right) = 0$$
$$\frac{\partial C}{\partial t} + \nabla \cdot \left(\vec{Cu} \right) = D\nabla^2 C$$

(iii) \rightarrow conservative form

(ii)





$$\nabla \cdot \left(C\vec{u}\right) = \left(\nabla C\right) \cdot \vec{u} + C\left(\nabla \cdot \vec{u}\right)$$

$$\nabla \cdot \vec{u} = \frac{\partial u_x}{\partial x} + \frac{\partial u_y}{\partial y} + \frac{\partial u_z}{\partial z} = 0$$
Continuity eq. for
incompressible fluid
$$\therefore \nabla \cdot (C\vec{u}) = \nabla C \cdot \vec{u}$$

$$= \left(\frac{\partial C}{\partial x}\vec{i} + \frac{\partial C}{\partial y}\vec{j} + \frac{\partial C}{\partial z}\vec{k}\right) \cdot \left(u_x\vec{i} + u_y\vec{j} + u_z\vec{k}\right)$$

$$= u_x \frac{\partial C}{\partial x} + u_y \frac{\partial C}{\partial y} + u_z \frac{\partial C}{\partial z}$$

$$(\because \vec{i} \cdot \vec{i} = \vec{j} \cdot \vec{j} = \vec{k} \cdot \vec{k} = |\vec{i}| |\vec{i}| \cos 0^\circ = 1$$

$$\vec{i} \cdot \vec{j} = \vec{j} \cdot \vec{k} = \vec{k} \cdot \vec{i} = 0$$

Thus, (iii) becomes

$$\frac{\partial C}{\partial t} + \nabla C \cdot \vec{u} = D \nabla^2 C$$

 \rightarrow non-conservative form





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write out fully in Cartisian coordinates

$$\frac{\partial C}{\partial t} + u_x \frac{\partial C}{\partial x} + u_y \frac{\partial C}{\partial y} + u_z \frac{\partial C}{\partial z} = D\left(\frac{\partial^2 C}{\partial x^2} + \frac{\partial^2 C}{\partial y^2} + \frac{\partial^2 C}{\partial z^2}\right)$$

 \rightarrow 3D advection-diffusion equation

텐서식으로 표기하면

$$\frac{\partial C}{\partial t} + u_i \frac{\partial C}{\partial x_i} = D \frac{\partial^2 C}{\partial x_i^2}$$





[Re] Vector notation of conservation of mass

Consider a fixed volume V with surface area S

total mass in the volume =
$$\int_{V} \vec{C(x,t)} dV$$

mass flux = q(x,t)

Consider conservation of mass

$$\frac{\partial}{\partial t} \int_{V} C(\vec{x}, t) dV + \int_{S} \vec{q}(\vec{x}, t) \cdot \vec{n} dS = 0$$
 (a)

 \vec{n} = unit vector normal to surface element dS

Green's theorem

$$\int_{S} \vec{q} \cdot \vec{n} dS = \int_{V} \nabla \cdot \vec{q} dV$$
 (b)

Substitute (b) into (a)

$$\int_{V} \left(\frac{\partial C}{\partial t} + \nabla \cdot \vec{q} \right) dV = 0$$
$$\frac{\partial C}{\partial t} + \nabla \cdot \vec{q} = 0$$
$$\mathbf{HLAB}$$



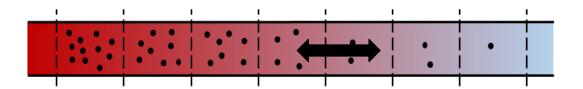
2.2 The Random Walk and Molecular Diffusion

- Two different ways for the molecular diffusion
 - 1) study the statistics of motion of single molecule or particle and generalize it
 - → random walk model
 - 2) study the integrated effect of random motion of a large number of particles simultaneously → gradient-flux equation

2.2.1 The Random Walk

Think motion of a tracer molecule consists of a series of random steps

 \rightarrow whether the step is <u>forward or backward is entirely random</u>







2.2 The Random Walk and Molecular Diffusion

Use **central limit theorem** \rightarrow in the limit of many steps, probability of the particle being

between $m\Delta x$ and $(m+1)\Delta x$ is the <u>normal distribution</u>

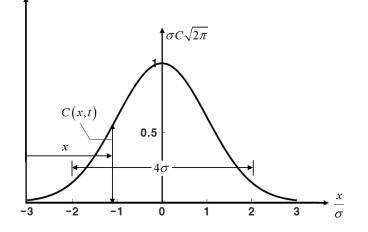
mean: $\mu = 0$ variance: $\sigma^2 = \frac{t(\Delta x)^2}{\Delta t}$ Normal distribution: $p(x,t)dx = \frac{1}{\sigma\sqrt{2\pi}} \exp\left(-\frac{x^2}{2\sigma^2}\right)$

Designate

$$\sigma^2 = \frac{t(\Delta x)^2}{\Delta t} = 2Dt$$

Then

$$p(x,t)dx = \frac{1}{\sqrt{4\pi Dt}} \exp\left(-\frac{x^2}{4Dt}\right)dx$$





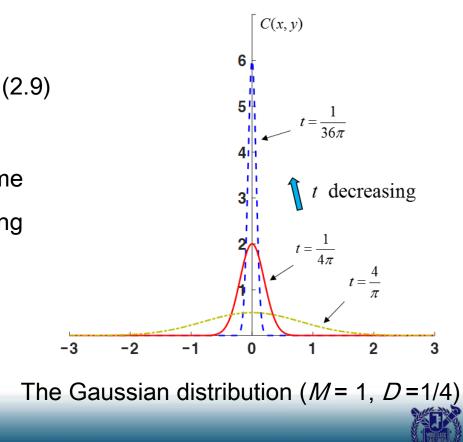


Now think whole group of particles, N

$$C(x,t) = \iint p(x,t) dx dn = \iint \frac{1}{\sqrt{4\pi Dt}} \exp\left(-\frac{x^2}{4Dt}\right) dx dn$$

$$C(x,t) = \frac{M}{\sqrt{4\pi Dt}} \exp\left(-\frac{x^2}{4Dt}\right)$$

 \rightarrow Random walk process leads to the same result that a slug of tracer diffuses according to the diffusion equation, Eq. (2.17).



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2.2 The Random Walk and Molecular Diffusion

2.2.2 The Gradient-Flux Relationship

Think random motion of large number of molecules at the same time.

 \rightarrow probability of a molecule passing through the surface is proportional to the average number of molecule near the surface \rightarrow mass transfer model

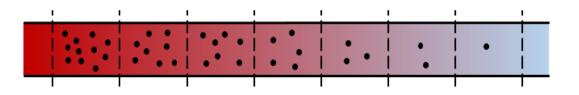
 \rightarrow differences in mean concentration are, on the average, always reduced, never increased.

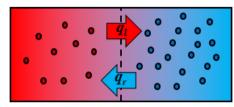
Consider flux of material across the bounding surface



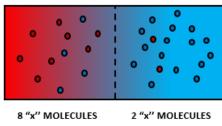


2.2 The Random Walk and Molecular Diffusion





10 "x" MOLECULES 20 "y" MOLECULES t = 0



4 "y" MOLECULES 16 "y" MOLECULES

 $t = \Delta t$

Transfer of molecules





2.2 The Random Walk and Molecular Diffusion

 $q_l = kM_l$ - flux of material from left to right

 $q_r = kM_r$ - flux of material from right to left

where $k = \text{transfer probability } [1/t] \rightarrow \text{mass transfer coefficient}$

$$M_{l}$$
 = mass of the tracer in the left-hand box

 M_r = mass of the tracer in the right-hand box

q =net flux = net rate at which tracer mass is exchange per unit time

$$q = k(M_{l} - M_{r})$$
(a)
Define

$$C_{l} = \frac{\overline{M}_{l}}{\Delta x}$$
(b)

$$\overline{M}_{l} = C_{l} Vol = C_{l} \Delta x$$

$$C_{r} = \frac{\overline{M}_{r}}{\Delta x}$$
(c)



 \overline{M}_r = average masses in the right-hand box

Mass transfer per unit time

2.2 The Random Walk and Molecular Diffusion

Combine (b) and (c)

$$\overline{M}_{l} - \overline{M}_{r} = \Delta x (C_{l} - C_{r})$$
$$= (\Delta x)^{2} \left[-\frac{C_{r} - C_{l}}{\Delta x} \right]$$
$$\approx (\Delta x)^{2} \left[-\frac{\partial C}{\partial x} \right] if \Delta x$$

is small

(d)

Substitute (d) into (a)

$$q = -k(\Delta x)^{2} \frac{\partial C}{\partial x}$$
$$q = -D \frac{\partial C}{\partial x}$$
$$D = k(\Delta x)^{2}$$

 \Rightarrow Fick's law

 \Rightarrow Diffusion coefficient (constant)

→ Convert mass transfer model to diffusion model





2.2 The Random Walk and Molecular Diffusion

[Re] Two basic models for diffusion

1) Diffusion model (Fick's law)

$$q = -D\frac{\partial C}{\partial x}$$

q = mass flux per unit time and unit area

 $D = \text{diffusion coefficient } [L^2/t] \rightarrow \text{distributed parameter}$

2) Mass transfer model

 $q_c = k \Delta C$

- q_c = mass transfer per unit time <u>per unit volume</u>
- $k = mass transfer coefficient [1/t] \rightarrow lumped parameter$

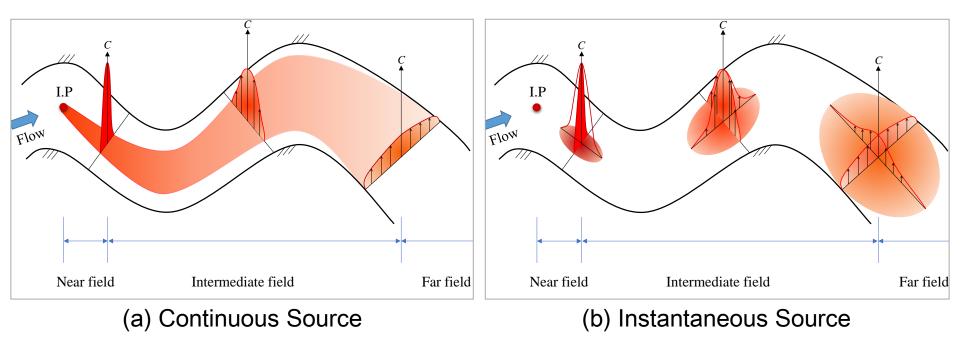




2.3.1 Analytical Solution of 1D Diffusion Equation

2.3.1.1 Boundary Conditions for Various Inputs

· Types of pollutants input



Stages of pollutant mixing in natural streams





Problem 1: Consider diffusion of an initial slug of mass *M* introduced <u>instantaneously</u> at time zero at the *x* origin

[Cf] Continuous input \rightarrow <u>initial concentration</u> specified as a function of time

i) Governing equation:

$$\frac{\partial C}{\partial t} = D \frac{\partial^2 C}{\partial x^2}$$
(2.10)

ii) Initial & Boundary conditions:

- Spreading of an initial slug of mass *M* introduced instantaneously at time zero at

the *x* origin can be expressed as

$$C(x=0,t=0) = M\delta(x)$$

 $C(x = \pm \infty, t) = 0 \tag{2.11}$





- where $\delta(x) =$ Dirac delta function
- = representing a unit mass of tracer concentrated into an

infinitely small space with an infinitely large concentrati

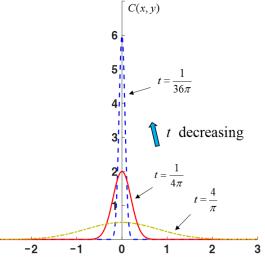
- = spike function $\neq \frac{1}{\Lambda r}$
- \cdot mass *M* in the 1D model = mass/area

[Re] Boundary conditions

For the 1-D models, three boundary conditions are commonly

encountered;

$$C(x = 0)$$
$$C(x = -\infty)$$
$$C(x = +\infty)$$



-3



• Types of boundary conditions:

1) Constant concentration \rightarrow Dirichlet (1st type)

 $C(x=0,t) = C_0$

2) Constant mass flux \rightarrow Neumann (2nd type) a) Finite flux: $J_0 = -D \frac{\partial C}{\partial x}\Big|_{x=0}$ b) No flux: $\frac{\partial C}{\partial x}\Big|_{x=0} = 0 \rightarrow$ reflecting (impermeable) boundary

3) Advective mass flux

$$J_0 = -D \frac{\partial C}{\partial x} \bigg|_{x=o} = k_m [C(0,t) - C_{\infty}]$$

where k_m = mass transfer coefficient





2.3.1.2 Analytical Solution

To obtain an analytical solution, we can apply

- Dimensional analysis
- Separation of variables
- Laplace transformation

Now, apply dimensional analysis

$$C(x,t) = f(M, D, x, t)$$

$$C = \frac{M}{\sqrt{4\pi Dt}} f\left(\frac{x}{\sqrt{4Dt}}\right)$$
(2.12)

Now find function f

Set
$$\eta = \frac{x}{\sqrt{4Dt}}$$

(2.13)





Then,

$$\frac{\partial \eta}{\partial t} = \frac{\eta}{2t}$$
$$\frac{\partial \eta}{\partial x} = \frac{1}{\sqrt{4Dt}}$$

Substitute Eq. (2.13) into Eq. (2.12) and then into Eq. (2.10)

Eq. (2.12): C_p

$$C = \frac{M}{\sqrt{4\pi Dt}} f\left(\frac{x}{\sqrt{4Dt}}\right) = \frac{M}{\sqrt{4\pi Dt}} f(\eta)$$

Thus, each term in Eq. (2.10) become

$$\frac{\partial C}{\partial t} = \frac{M}{\sqrt{4\pi Dt}} \frac{\partial f}{\partial t} + \left(\frac{M}{\sqrt{4\pi D}} \frac{1}{\sqrt{t}}\right) f = C_p \frac{\partial f}{\partial \eta} \frac{\partial \eta}{\partial t} + C_p \left(-\frac{1}{2t}\right) f$$
$$= C_p \frac{\partial f}{\partial \eta} \left(-\frac{\eta}{2t}\right) + C_p \left(-\frac{1}{2t}\right) f$$
(a)





$$\begin{aligned} \frac{\partial C}{\partial x} &= C_p \frac{\partial f}{\partial x} = C_p \frac{\partial f}{\partial \eta} \frac{\partial \eta}{\partial x} = C_p \frac{\partial f}{\partial \eta} \frac{1}{\sqrt{4Dt}} \end{aligned} \tag{b} \\ \frac{\partial^2 C}{\partial x^2} &= \frac{\partial}{\partial x} \left(\frac{\partial C}{\partial x} \right) = \frac{\partial}{\partial x} \left(C_p \frac{\partial f}{\partial \eta} \frac{1}{\sqrt{4Dt}} \right) = C_p \frac{1}{\sqrt{4Dt}} \frac{\partial}{\partial x} \left(\frac{\partial f}{\partial \eta} \right) \\ &= C_p \frac{1}{\sqrt{4Dt}} \frac{\partial}{\partial \eta} \frac{\partial \eta}{\partial x} \left(\frac{\partial f}{\partial \eta} \right) = C_p \frac{1}{4Dt} \frac{\partial^2 f}{\partial \eta^2} \end{aligned} \tag{b}$$

Substitute (a) and (c) into Eq. (2.10)

$$C_{p} \frac{\partial f}{\partial \eta} \left(-\frac{\eta}{2t} \right) + C_{p} \left(-\frac{1}{2t} \right) f = DC_{p} \frac{\partial^{2} f}{\partial \eta^{2}} \frac{1}{4Dt}$$
$$2\eta \frac{\partial f}{\partial \eta} + 2f + \frac{\partial^{2} f}{\partial \eta^{2}} = 0$$
$$\frac{\partial}{\partial \eta} \left(2\eta f \right) + \frac{\partial^{2} f}{\partial \eta^{2}} = 0$$





(2.14)

2.3 Mathematics of Diffusion Equation

Integrate once w.r.t. η

$$2\eta f + \frac{df}{d\eta} = 0$$

Apply separation of variables to Eq. (2.14)

$$\frac{df}{f} = -2\eta d\eta$$

Integrate both sides

$$\ln f = -\eta^{2} + C$$

$$f = e^{-n^{2} + C} = C_{0}e^{-n^{2}}$$
(2.15)

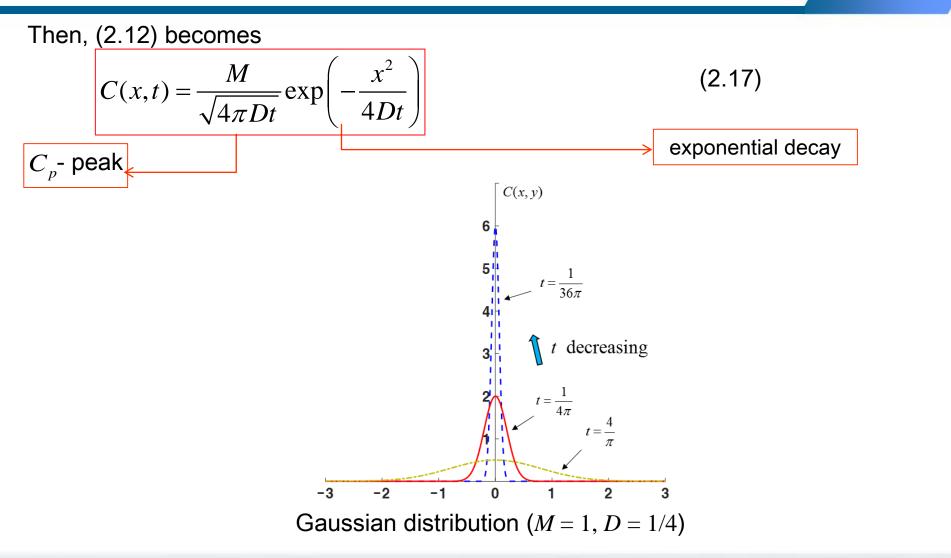
Total mass, M is

 $\int_{-\infty}^{\infty} C dx = M \tag{2.16}$

Substituting Eq. (2.12) and Eq. (2.15) into Eq. (2.16) yields $C_0 = 1$

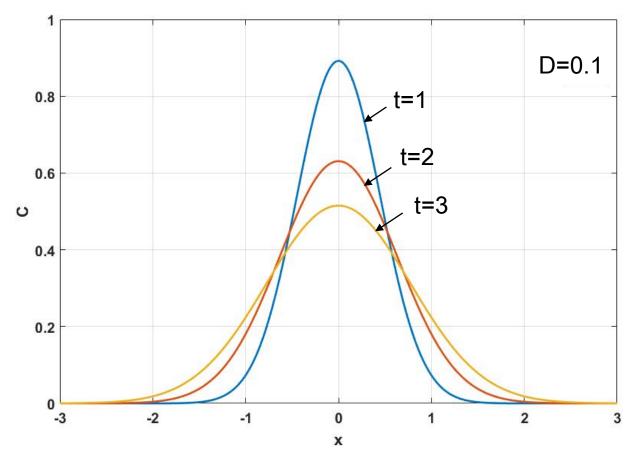








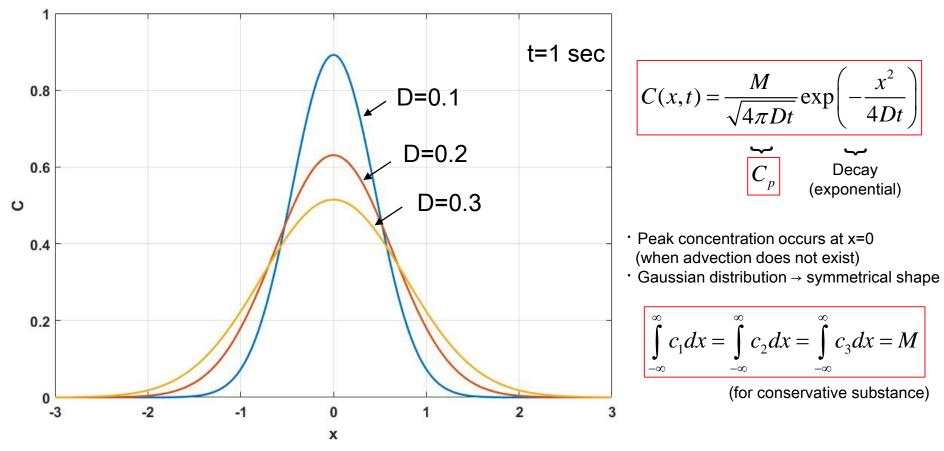




Gaussian concentration distributions with elapsed time







Gaussian concentration distributions with varying dispersion coefficient





[Re] Analytical solution by separation of variables

$$\frac{\partial C}{\partial t} = D \frac{\partial^2 C}{\partial x^2}$$
(2.18)

$$C(x,t=0) = M\delta(x)$$
(2.19a)

$$C(x = \pm \infty, t) = 0 \tag{2.19b}$$

$$M = \lim_{\varepsilon \to 0} \int_{-\varepsilon}^{\varepsilon} f(x) dx \qquad \qquad M = \lim$$
 (2.1)

Separation of variables

$$C(x,t) = F(x)G(t)$$
(2.20)

Substitute Eq. (2.20) into Eq. (2.10)

$$F(x)\frac{\partial G}{\partial t} = DG(t)\frac{\partial^2 F}{\partial x^2}$$
 $FG' = DGF'$

$$\frac{1}{D}\frac{G'}{G} = \frac{F''}{F} = k$$
$$F'' - \omega^2 F = 0$$
$$G' - D\omega^2 g = 0$$

9c)





where
$$k = const. \neq f_n(x \text{ or } t)$$

i) $k > 0$
 $k = \omega^2$
 $\frac{1}{D}\frac{G'}{G} = \frac{F''}{F} = \omega^2$
 $\rightarrow \begin{bmatrix} F'' - \omega^2 F = 0 & (2.21a) \\ G' - D\omega^2 g = 0 & (2.21b) \end{bmatrix}$
Solution of (2.21a) is $F = C_1 e^{wx} + C_2 e^{-wx}$ (a)

Substituting (2.19b) into (a) yields $C_1 = 0$

Then

$$F = C_2 e^{-wx}$$





- Solution of (2.21b) is $G = C_3 e^{\sqrt{D\omega t}}$
- Substituting B.C. (2.19b) gives $C_3 = 0$
- This means that $C = F \cdot G = 0$ at all points, which is not true.

Therefore, $k \leq 0$

ii) k = 0 $F'' = 0 \rightarrow F = ax + b \rightarrow a = 0$ $\therefore F = b$ $G' = 0 \rightarrow G = k$ $\therefore C = FG = bk = const. \rightarrow not true$

Therefore, k < 0





iii) k < 0

$$k = -p^{2}$$

$$\frac{1}{D}\frac{G'}{G} = \frac{F''}{F} = -p^{2}$$
(2.21c)
$$F'' + p^{2}F = 0$$
(2.21d)
$$G' + Dp^{2}G = 0$$

Assume solution of Eq. (2.21c) as $F = e^{\lambda x}$

Substitute this into Eq. (2.21c) and derive characteristic equation (2.22)

$$\lambda^{2} + p^{2} = 0$$

$$\therefore \lambda = \pm pi$$

$$\therefore F = C_{1}e^{pxi} + C_{2}e^{-pxi}$$

$$= C_{1}(\cos pz + i\sin px) + C_{2}(\cos px - i\sin px)$$

$$= A\cos px + B\sin px$$

(2.22)



Assume solution of Eq. (2.21d) as and $G = e^{\lambda x}$

Substitute this into Eq. (2.21d) and derive characteristic equation

$$\lambda + Dp^{2} = 0$$

$$\therefore \lambda = -Dp^{2}$$

$$\therefore G = C_{1}e^{-Dp^{2}t}$$
(2.23)

Substitute Eq. (2.22) and (2.23) into Eq. (2.20)

$$C(x,t) = F(x)G(t) = (A\cos px + B\sin px)e^{-Dp^{2}t}$$
(2.24)

Use Fourier integral for non-periodic function.

Assume

$$A, B = f_n(p)$$

$$C(x, t, p) = \{A(p)\cos px + B(p)\sin px\}(-Dp^2t)$$
(2.25)





$$C(x,t) = \int_0^\infty C(x,t;p)dp$$

=
$$\int_0^\infty \{A(p)\cos px + B(p)\sin px\}\exp(-Dp^2t)dp$$
 (2.26)

Since Eq. (2.10) is linear and homogeneous, integral of Eq. (2.26) exists I.C.: Eq. (2.19a) and Eq. (2.19c)

$$C(x,t=0) = \int_0^\infty \{A(p)\cos px + B(p)\sin px\}dp = f(x)$$

Where f(x) = Fourier integral

$$= \frac{1}{\pi} \int_0^\infty \left\{ \cos px \int_0^\infty f(v) \cos(pv) dv + \sin px \int_{-\infty}^\infty f(v) \sin(pv) dv \right\} dp$$
$$A(p) = \frac{1}{\pi} \int_{-\infty}^\infty f(v) \cos(pv) dv$$
$$B(p) = \frac{1}{\pi} \int_{-\infty}^\infty f(v) \sin(pv) dv$$
HEAB



Use Trigonometric rule

$$C(x,0) = \frac{1}{\pi} \int_0^\infty \left\{ \int_0^\infty f(v) \cos px \sin pv dv + \int_{-\infty}^\infty f(v) \sin px \sin pv dv \right\} dp$$
$$= \frac{1}{\pi} \int_{-\infty}^\infty \left\{ \int_{-\infty}^\infty f(v) \cos(px - pv) dv \right\} dp$$
(2.27)

Substitute Eq. (2.27) into Eq. (2.26)

$$C(x,t) = \frac{1}{\pi} \int_0^\infty \left\{ \int_{-\infty}^\infty f(v) \cos(px - pv) \exp(-Dp^2 t) dv \right\} dp$$

Switch order of integral

$$C(x,t) = \frac{1}{\pi} \int_0^\infty f(v) \left\{ \underbrace{\int_{-\infty}^\infty \exp(-Dp^2 t) \cos(px - pv) dv}_{(e)} \right\} dp$$
(2.28)

Let

$$(e) = \int_{-\infty}^{\infty} \exp(-Dp^2 t) \cos(px - pv) dp$$





(2.29)

2.3 Mathematics of Diffusion Equation

Use <u>Residue theorem</u> to get integral of (e)

$$\int_{-\infty}^{\infty} e^{-s^2} \cos 2bs ds = \frac{\sqrt{\pi y}}{2} e^{-b^2}$$

Set
$$s = p\sqrt{Dt}, b = \frac{x-v}{2\sqrt{Dt}}$$

Then $2bs = (x-v)p, ds = \sqrt{Dt}dp$

(e) becomes

$$\int_{0}^{\infty} \exp(-Dp^{2}t) \cos(px - pv) dp = \frac{\sqrt{x}}{2\sqrt{Dt}} \exp\left\{-\frac{(x - v)^{2}}{4Dt}\right\}$$
(2.30)

Substitute Eq. (2.30) into Eq. (2.28)

$$C(x,t) = \frac{1}{\sqrt{4\pi Dt}} \int_{-\infty}^{\infty} f(v) \exp\left\{-\frac{(x-v)^2}{4Dt}\right\} dv = \frac{1}{\sqrt{4\pi Dt}} \lim_{\varepsilon \to 0} \int_{-\varepsilon}^{\varepsilon} f(v) \exp\left\{-\frac{(x-v)^2}{4Dt}\right\} dv$$

$$= \frac{M}{\sqrt{4\pi Dt}} \exp\left(-\frac{x^2}{4Dt}\right)$$
(2.31)
CHLAB

2.3.2.1 Concentration Distribution

G.E. and BCs for instantaneous point source

$$\frac{\partial C}{\partial t} = D \frac{\partial^2 C}{\partial x^2}$$
$$C(x,0) = M \delta(x)$$

 δ = Dirac delta function (= $\frac{1}{\Delta x}$)

(2.32)

→ representing a unit mass of tracer concentrated into an infinitely small space with an infinitely large conc.

 \rightarrow spike distribution

[Ex] bucket of concentrated dye dumped into a large river





The solution is

$$C(x,t) = \frac{M}{\sqrt{4\pi Dt}} \exp\left(-\frac{x^2}{4Dt}\right)$$

 \rightarrow Gaussian distribution (Normal distribution if M = 1)

[Re] *M*

- For 1D model, M = total mass / area
- For 2D model, M = total mass / length
- For 3D model, M = total mass

- \rightarrow plane source
- \rightarrow line source
- \rightarrow point source

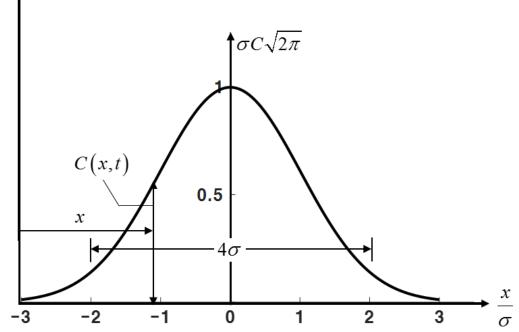




2.3.2.2 Moments of Concentration Distribution

Moments of concentration distributions are defined as

0th moment = $M_{0=} \int_{-\infty}^{\infty} C(x,t) dx$ 1st moment = $M_{1=} \int_{-\infty}^{\infty} C(x,t) x dx$ 2nd moment = $M_{2=} \int_{-\infty}^{\infty} C(x,t) x^2 dx$ p^{th} moment = $M_{p=} \int_{-\infty}^{\infty} C(x,t) x^p dx$







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2.3.2 Statistical Analysis of the Diffusion Equation

i) Mass: $M = M_0$

ii) Mean: $\mu = M_1 / M_0$ iii) Variance: $\sigma^2 = \frac{\int_{-\infty}^{\infty} (x - \mu)^2 C(x, t) dx}{M_0} = \frac{M_2}{M_0} - \mu^2$ iv) Skewness $S_1 = \frac{\frac{M_3}{M_0} - 3\mu \frac{M_2}{M_0} + 2\mu^3}{(\sigma^2)^{3/2}}$

- measure of skew

- For normal dist., $S_t = 0$

Normal distribution is given as

$$N(\mu,\sigma^2); \quad f(x) = \frac{1}{\sigma\sqrt{2\pi}} \exp\left\{-\frac{(x-\mu)^2}{2\sigma^2}\right\}, \quad -\infty < x < \infty$$

$$E(x) = \mu$$
; $Var(x) = \sigma^2$





For concentration distribution, substitute $\mu = 0, \sigma = \sqrt{2Dt}$ $C(x,t) = \frac{1}{\sqrt{4\pi Dt}} \exp\left(\frac{x^2}{-4Dt}\right)$

Then, $M_0 = 1$

- $\mu = 0 \rightarrow$ location of centroid of concentration distribution
- $\sigma^2 = 2Dt \rightarrow$ measure of the <u>spread of the distribution</u>



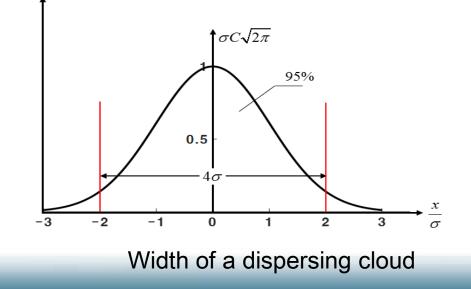


2.3.2.3 Calculation of Diffusion Coefficients

(1) Measure of spread of dispersing tracer

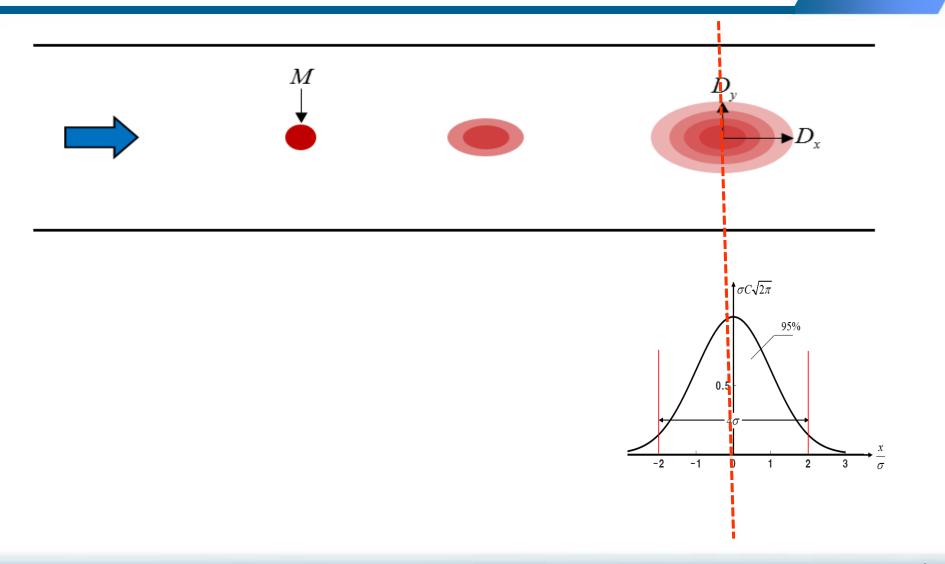
- $\sigma = \sqrt{2Dt}$ $4\sigma = 4\sqrt{2Dt}$
- $[Cf] \quad 6\sigma = 6\sqrt{2Dt}$

- \Rightarrow standard deviation (a)
- \Rightarrow estimate of the <u>width of a dispersing cloud</u>
- \Rightarrow include 95% of the total mass
- \Rightarrow include 99.5% of the total mass









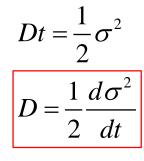




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- (2) Calculation of diffusion coefficient
- → Change of moment method

Differentiate Eq. (a) w.r.t. time



(2.34)

- i) For normal distribution: it is obvious
- ii) Eq. (2.34) can be also true for any distribution, provided that it is dispersing in accord with the Fickian diffusion equation.





Proof: Start with Fickian diffusion equation

$$\frac{\partial C}{\partial t} = D \frac{\partial^2 C}{\partial x^2}$$

Multiply each side by x^2

$$x^2 \frac{\partial C}{\partial t} = Dx^2 \frac{\partial^2 C}{\partial x^2}$$

Integrate from to $-\infty$ and $+\infty$ w.r.t x

$$\int_{-\infty}^{\infty} \frac{\partial C}{\partial t} x^2 dx = \int_{-\infty}^{\infty} Dx^2 \frac{\partial^2 C}{\partial x^2} dx$$

Apply integration by parts into right hand side

$$\int uv' = uv - \int u'v$$

(a)





$$\frac{\partial}{\partial t} \int_{-\infty}^{\infty} Cx^2 dx = D \left\{ \begin{bmatrix} x^2 \frac{\partial C}{\partial x} \end{bmatrix}_{-\infty}^{\infty} - \int_{-\infty}^{\infty} 2x \frac{\partial C}{\partial x} dx \end{bmatrix} \\ = -2D \int_{-\infty}^{\infty} x \frac{\partial C}{\partial x} dx \qquad \left[\because \frac{\partial C}{\partial x} \right]_{\pm\infty} \approx 0 \right\} \\ = -2D \left\{ \begin{bmatrix} xC \end{bmatrix}_{-\infty}^{\infty} - \int_{-\infty}^{\infty} Cdx \right\} \\ = 2D \int_{-\infty}^{\infty} Cdx \qquad (\because C]_{-\infty}^{\infty} \approx 0) \end{bmatrix} \\ 2D = \frac{\frac{\partial}{\partial t} \int_{-\infty}^{\infty} Cx^2 dx}{\int_{-\infty}^{\infty} Cdx} = \frac{\frac{\partial}{\partial t} M_2}{M_0} = \frac{\partial}{\partial t} \left(\frac{M_2}{M_0} \right) \\ D = \frac{1}{2} \frac{\partial}{\partial t} \left(\frac{M_2}{M_0} \right) \end{bmatrix}$$





(b)

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Now, multiply each side of Eq. (a) by x $\int_{-\infty}^{\infty} x \frac{\partial C}{\partial t} dx = \int_{-\infty}^{\infty} Dx \frac{\partial^2 C}{\partial x^2} dx = D \left\{ x \frac{\partial C}{\partial x} \right\}_{-\infty}^{\infty} - \int_{-\infty}^{\infty} \frac{\partial C}{\partial x} dx \right\}$ $= -D \int_{-\infty}^{\infty} \frac{\partial C}{\partial x} dx = -D \left[C \right]_{-\infty}^{\infty} = 0$ $\therefore \frac{\partial}{\partial t} \int_{-\infty}^{\infty} C x dx = 0$ $\rightarrow \frac{\partial}{\partial t} M_1 = 0$ $\frac{\partial}{\partial t}(M_1 / M_0) = \frac{\partial}{\partial t}(\mu) = 0$

 \rightarrow μ is independent of time.





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By the way,

$$\sigma^{2} = \frac{M_{2}}{M_{0}} - \mu^{2}$$

$$\frac{\partial}{\partial t} \left(\sigma^{2}\right) = \frac{\partial}{\partial t} \left(\frac{M_{2}}{M_{0}}\right) - \frac{\partial}{\partial t} \left(\mu^{2}\right) = \frac{\partial}{\partial t} \left(\frac{M_{2}}{M_{0}}\right)$$

Combine Eq.(b) and Eq.(c)

$$D = \frac{1}{2} \frac{\partial \sigma^2}{\partial t}$$
(2.35)

→ Variance of a finite distribution increases linearly with time at the rate 2D no matter what its shape.

→ Property of the Fickian diffusion equation: any finite initial distribution eventually decays into Gaussian distribution.





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(C)

(3) Change of moment method

a) Calculate diffusion coefficient from two concentration curves

Start from Eq. (2.36)

$$\sigma^{2} = 2Dt + C$$

$$\sigma_{2}^{2} = 2Dt_{2} + C$$
(1)
$$\sigma_{1}^{2} = 2Dt_{1} + C$$
(2)

Subtract (1) from (2)

$$\sigma_2^2 - \sigma_1^2 = 2D(t_2 - t_1)$$

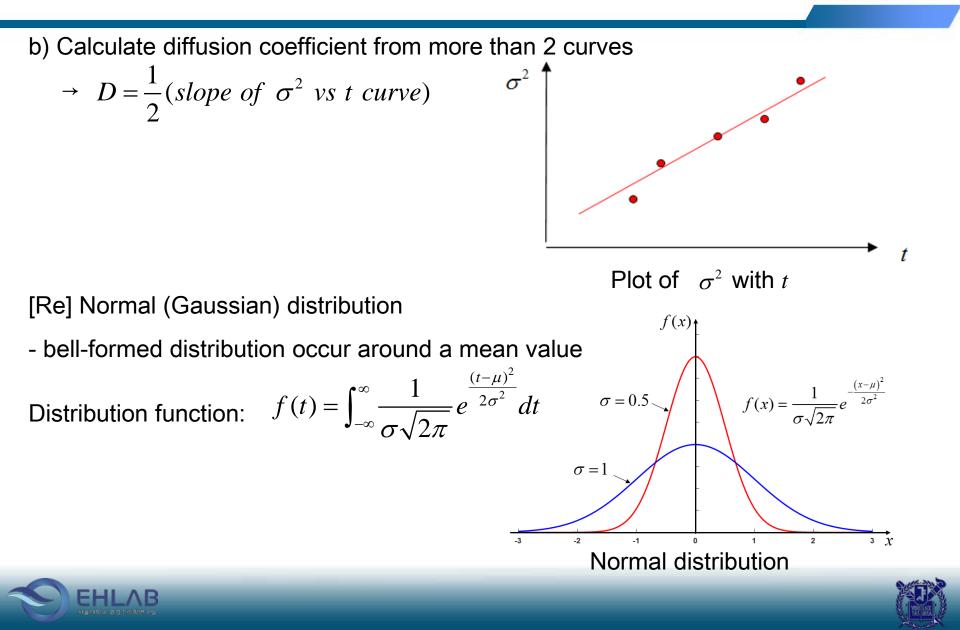
Rearrange $D = \frac{1}{2} \frac{\sigma_2^2 - \sigma_1^2}{t_2 - t_1}$ (2.36) σ_1^2 = variance of concentration distribution at $t = t_1$

 σ_2^2 = variance of concentration distribution at $t = t_2$





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Homework #1

Due: 1 week from today

Taking care to create as little disturbance as possible, a small sample of salt solution is released at the center of the large tank of motionless fluid.

(a) After 24 hours have elapsed a conductivity probe is used to measure the concentration distribution around the release location. It is found to be Gaussian with a variance of 1.53 centimeters squared. The experiment is repeated after a further 24 hours have elapsed and the variance is found to be 2.34 centimeters squared. Determine the diffusion coefficient indicated by the experimental data.

(b) Explain how the measured peak concentration at 24 hours and 48 hours could be used to check the result in (a).

(c) Must the distribution be Gaussian for the method used in (a) to apply?





G.E.:
$$\frac{\partial C}{\partial t} = D \frac{\partial^2 C}{\partial x^2}$$

(2.37)

B.C.:

- Series 1: Instantaneous inputs
- Series 2: Continuous inputs
- Series 3: Instantaneous inputs with boundary walls
- Series 4: Instantaneous inputs in 2D & 3D fluids
- Series 5: Advective diffusion
- Series 6: Maintained point discharges in 2D & 3D flows
- Series 7: Pollutant Mixing in Rivers





Problem 1-1:

initial slug of mass *M* introduced instantaneously at time zero at the *x* origin

$$C(x = 0, t = 0) = M\delta(x)$$

$$C(x = \pm \infty, t) = 0$$
(2.38)

Solution is

$$C(X,t) = \frac{M}{\sqrt{4\pi Dt}} \exp\left[\frac{-x^2}{4Dt}\right]$$





(2.39)

2.3.3.1 An Initial Spatial Distribution C(x, 0)

(1) Mass *M* released at time t = 0 at the point $x = \xi \rightarrow \text{Problem 1-2}$ *I.C.* $C(x,0) = M\delta(x-\xi)$ *B.C.* $C(\pm\infty,t) = 0$

For the <u>coordinate transformation</u>, set $X = x - \xi$

Then, I.C. becomes

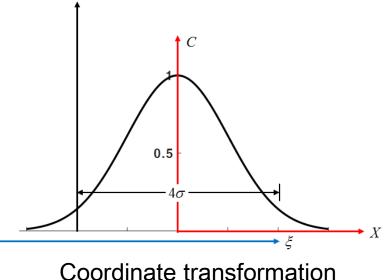
$$C(X,0) = M\delta(X)$$

The solution is

$$C(X,t) = \frac{M}{\sqrt{4\pi Dt}} \exp\left[\frac{X^2}{4Dt}\right]$$

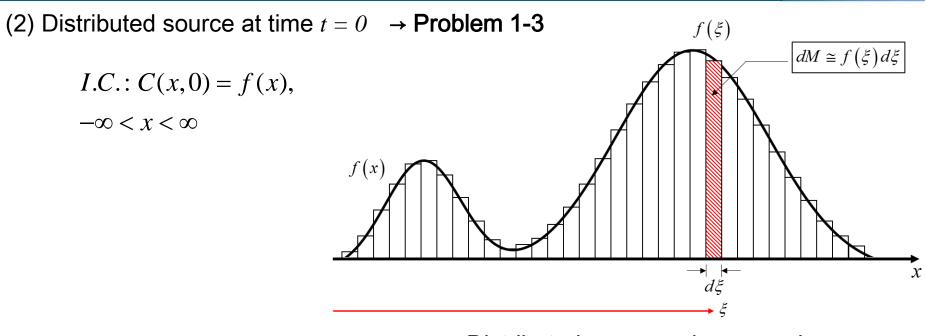
Convert X into x

$$C(x,t) = \frac{M}{\sqrt{4\pi Dt}} \exp\left[\frac{-(x-\xi)^2}{4Dt}\right]$$
(2.40)









f(x) ~ arbitrary function

Distributed sources along x axis

Assume that the initial input is composed from a distributed <u>series of separate</u> <u>slugs</u>, which all diffuse independently.

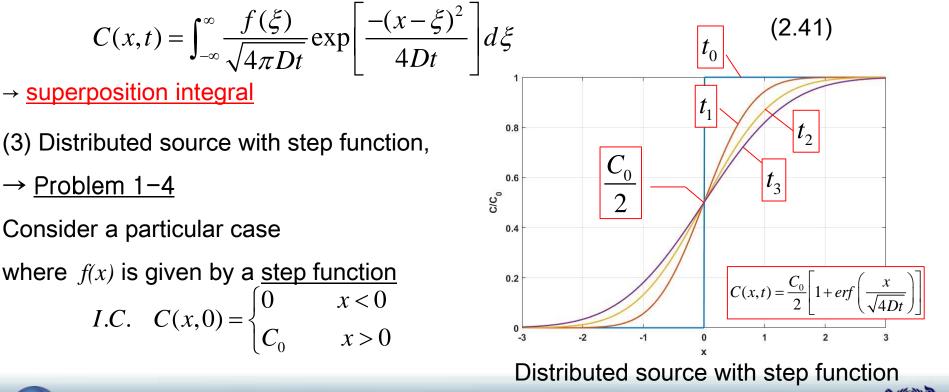
→ motion of individual particles is independent of the concentration of other particles





Concentration resulting from the slug containing the mass $dM = f(\xi)d\xi$ is given as $\frac{f(\xi)d\xi}{\sqrt{4\pi Dt}} \exp\left[\frac{-(x-\xi)^2}{4Dt}\right]$

Then, total contribution from all slugs is the integral sum of all the individual contributions



According to (2.41), solution is given as

$$C(x,t) = \int_{0}^{\infty} \frac{C_{0}}{\sqrt{4\pi Dt}} \exp\left[\frac{-(x-\xi)^{2}}{4Dt}\right] d\xi \qquad (a)$$
Set $u = \frac{(x-\xi)}{\sqrt{4Dt}}$ $\xi = 0$: $u = \frac{x}{\sqrt{4Dt}}$ $\xi = \infty$: $u = -\infty$
 $du = \frac{-d\xi}{\sqrt{4Dt}} \rightarrow d\xi = -\sqrt{4Dt} du$
Substitute (b) into (a)
 $C(x,t) = \frac{C_{0}}{\sqrt{\pi}} \int_{-\infty}^{\frac{x}{\sqrt{4Dt}}} e^{-u^{2}} du = \frac{C_{0}}{2} \left[\frac{2}{\sqrt{\pi}} \int_{-\infty}^{0} e^{-u^{2}} du + \frac{2}{\sqrt{\pi}} \int_{0}^{\frac{x}{\sqrt{4Dt}}} e^{-u^{2}} du\right]$
 $= \frac{C_{0}}{2} \left[1 + \frac{2}{\sqrt{\pi}} \int_{0}^{\frac{x}{\sqrt{4Dt}}} e^{-u^{2}} du\right] = \frac{C_{0}}{2} \left[1 + erf\left(\frac{x}{\sqrt{4Dt}}\right)\right]$
 $C(x,t) = \frac{C_{0}}{2} \left[1 + erf\left(\frac{x}{\sqrt{4Dt}}\right)\right] \qquad (2.42)$





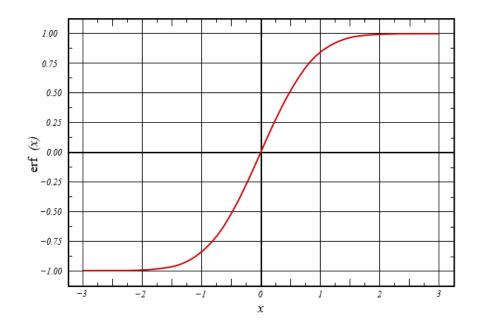
[Re] Error function (오차함수)

~ a <u>special function</u> of "S" shaped curve (sigmoid curve)

$$erf \ x = \frac{2}{\sqrt{\pi}} \int_0^x \exp(-\xi^2) d\xi$$
$$erf(\infty) = \frac{2}{\sqrt{\pi}} \int_0^\infty \exp(-\xi^2) d\xi = 1$$

complementary error function

$$erfc x = 1 - erf x$$







[Re] Normal distribution

- Most important distribution in statistical application since many <u>measured (random)</u> <u>data</u> have approximately normal distributions.

The <u>random variable</u> X has a normal distribution if its p.d.f. is defined by

$$f(x) = \frac{1}{\sigma\sqrt{2\pi}} \exp\left[-\frac{(x-\mu^2)}{2\sigma^2}\right], \quad -\infty < x < \infty$$

• Integral of normal distribution

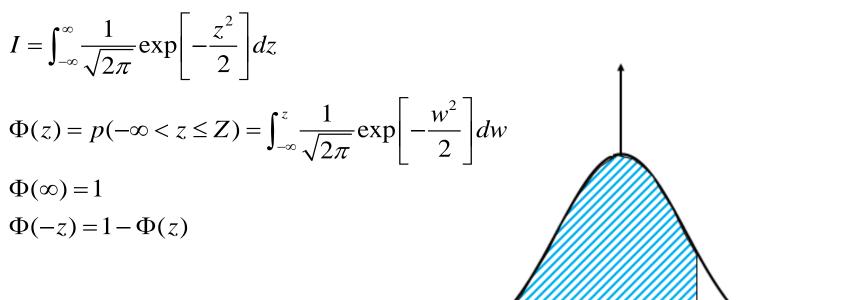
$$I = \int_{-\infty}^{\infty} \frac{1}{\sigma\sqrt{2\pi}} \exp\left[-\frac{(x-\mu^2)}{2\sigma^2}\right] dx$$

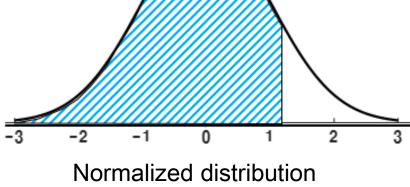




Let
$$z = \frac{x - \mu}{\sigma} \left(dz = \frac{1}{\sigma} dx \right)$$

Then,









(4) Distributed source with step function C_0 for $x < 0 \rightarrow$ <u>Problem 1-5</u>

Consider instantaneous input of step function

I.C.
$$C(x,0) = \begin{cases} C_0, & x < 0 \\ 0, & x > 0 \end{cases}$$

Solution by line source of $C_0 \delta \xi$ is given as

$$dC = \frac{C_0 \delta \xi}{\sqrt{4\pi Dt}} \exp\left[\frac{(x-\xi)^2}{-4Dt}\right]$$

Then, total contribution is

$$C(x,t) = \frac{C_0}{\sqrt{4\pi Dt}} \int_{-4Dt}^{0} \exp\left[-\frac{(x-\xi)^2}{-4Dt}\right] d\xi$$

Set
$$\eta = \frac{x - \xi}{\sqrt{4D}}$$

Then
$$d\eta = -\frac{d\xi}{\sqrt{4Dt}}$$
 $\xi = -\infty \rightarrow \eta = \infty$ $\xi = 0 \rightarrow \eta = \frac{x}{\sqrt{4Dt}}$





Substituting this relation yields

$$C(x,t) = \frac{C_0}{\sqrt{\pi}} \int_{\infty}^{\frac{x}{\sqrt{4Dt}}} \exp(-\eta^2) (-d\eta) = \frac{C_0}{\sqrt{\pi}} \int_{\frac{x}{\sqrt{4Dt}}}^{\infty} \exp(-\eta^2) d\eta$$
$$= \frac{C_0}{2} \left[\frac{2}{\sqrt{\pi}} \int_{\frac{x}{\sqrt{4Dt}}}^{\infty} \exp(-\eta^2) d\eta - \frac{2}{\sqrt{\pi}} \int_{0}^{\frac{x}{\sqrt{4Dt}}} \exp(-\eta^2) d\eta \right]$$
$$= \frac{C_0}{2} \left[\frac{2}{\sqrt{\pi}} \int_{0}^{\infty} \exp(-\eta^2) d\eta - \frac{2}{\sqrt{\pi}} \int_{0}^{\frac{x}{\sqrt{4Dt}}} \exp(-\eta^2) d\eta \right]$$
$$= \frac{C_0}{2} \left[1 - erf\left(\frac{x}{\sqrt{4Dt}}\right) \right] = \frac{C_0}{2} erfc\left(\frac{x}{\sqrt{4Dt}}\right)$$
$$C(x,t) = \frac{C_0}{2} \left[1 - erf\left(\frac{x}{\sqrt{4Dt}}\right) \right] = \frac{C_0}{2} erfc\left(\frac{x}{\sqrt{4Dt}}\right), -\infty \le x \le \infty$$
(2.43)

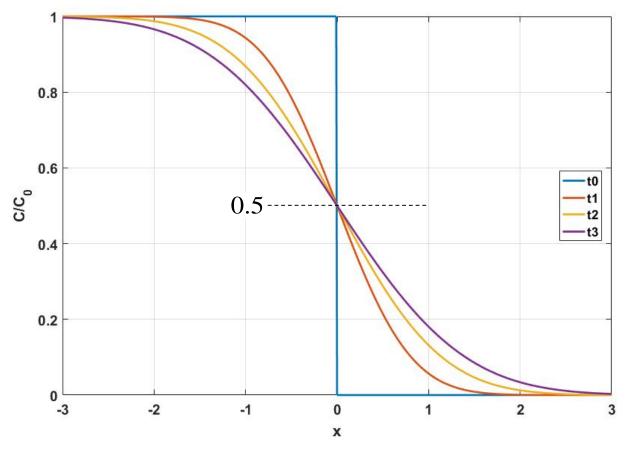
→ complementary error function

 \rightarrow summing the effect of a series of line sources, each yielding an exponential of





[Re] complementary error function



Analytical solution for step function





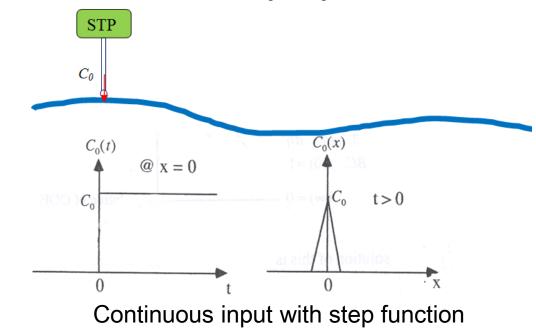
Case	Initial and boundary conditions	Solution
1-1	<i>M</i> introduced instantaneously at time zero at the <i>x</i> origin	$C(X,t) = \frac{M}{\sqrt{4\pi Dt}} \exp\left[\frac{-x^2}{4Dt}\right]$
1-2	<i>M</i> released at time $t = 0$ at the point $x = \xi$	$C(x,t) = \frac{M}{\sqrt{4\pi Dt}} \exp\left[\frac{-(x-\xi)^2}{4Dt}\right]$
1-3	Distributed source at time $t = 0$ $C(x,0) = f(x)$ for $-\infty < x < \infty$	$C(x,t) = \int_{-\infty}^{\infty} \frac{f(\xi)}{\sqrt{4\pi Dt}} \exp\left[\frac{-(x-\xi)^2}{4Dt}\right] d\xi$
1-4	Distributed source with step function $C(x,0) = C_0$ for $x > 0$	$C(x,t) = \frac{C_0}{2} \left[1 + erf\left(\frac{x}{\sqrt{4Dt}}\right) \right]$
1-5	Distributed source with step function $C(x,0) = C_0$ for $x < 0$	$C(x,t) = \frac{C_0}{2} \left[1 - erf\left(\frac{x}{\sqrt{4Dt}}\right) \right]$

Summary of solutions for instantaneous inputs (Series 1)





(1) <u>Continuous</u> input with step function $C_0 = C_0(t) \rightarrow \text{Problem 2-1}$



Consider continuous input with step input at x = 0

I.C.
$$C(x,t=0) = 0$$

B.C. $C(x=0,t>0) = C_0$





Solution by dimensional analysis

$$C = C_0 f\left(\frac{x}{\sqrt{Dt}}\right)$$

Set
$$\eta = \frac{x}{\sqrt{Dt}}$$

 $\frac{\partial \eta}{\partial t} = \frac{x}{\sqrt{D}} \left(-\frac{1}{2} \right) t^{-\frac{3}{2}} = -\frac{1}{2t} \frac{x}{\sqrt{Dt}} = -\frac{1}{2t} \eta$
 $\frac{\partial \eta}{\partial x} = \frac{1}{\sqrt{Dt}}$

Then
$$\frac{\partial C}{\partial t} = \frac{dC}{d\eta} \frac{\partial \eta}{\partial t} = -\frac{1}{2t} \eta \frac{dC}{d\eta}$$

 $\frac{\partial^2 C}{\partial x^2} = \frac{1}{Dt} \frac{d^2 C}{d\eta^2} \left(\because \frac{\partial^2 C}{\partial x^2} = \frac{d^2 C}{d\eta^2} \frac{\partial^2 \eta}{\partial x^2} \right)$





Substitute these into Eq. (2.10) to obtain O.D.E.

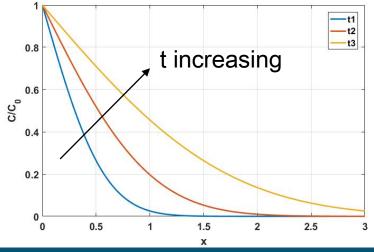
$$\frac{1}{2t}\eta \frac{dC}{d\eta} = \frac{1}{t}\frac{d^2f}{d\eta^2}$$
$$2f'' + \eta f' = 0$$

B.C.
$$f(0) = 1$$
 $f(\infty) = 0$

Solution of Eq. (a) is

$$C = C_0 \left[1 - erf\left(\frac{x}{\sqrt{4Dt}}\right) \right] = C_0 erfc\left(\frac{x}{\sqrt{4Dt}}\right), \quad x > 0$$
 (2.44)

Solution for continuous step function







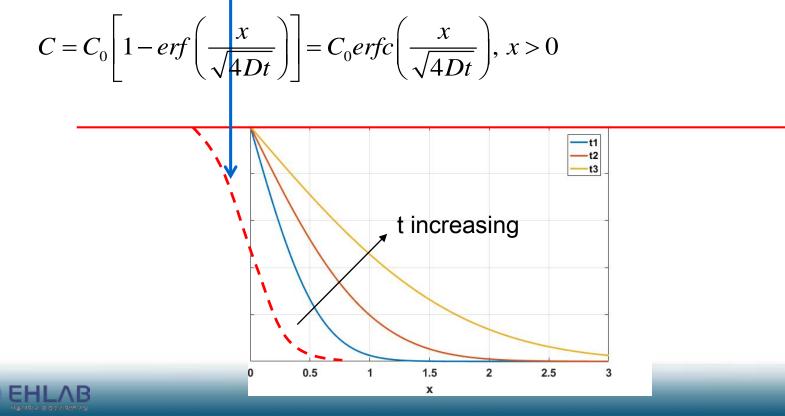
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(a)

Solution of Prob. 1-5

$$C(x,t) = \frac{C_0}{2} \left[1 - erf\left(\frac{x}{\sqrt{4Dt}}\right) \right] = \frac{C_0}{2} erfc\left(\frac{x}{\sqrt{4Dt}}\right), -\infty \le x \le \infty$$

Solution of Prob. 2-1





[Re] Laplace transformation

For ODE, it transforms ODE into algebraic problem.

For PDE, it transforms PDE into ODE.

i) Laplace transformation ("operational calculus")

$$F_n(x,s) = L(C) = \int_0^\infty e^{-st} C(x,t) dt = \overline{C}$$
$$L(C') = sL(C) - C(x,0) = s\overline{C} - C(x,0)$$
$$L(C'') = s^2 L(C) - sC(x,0) - C'(x,0)$$

ii) Inverse transform

$$C(x,t) = L^{-1}(F)$$

iii) Linearity of Laplace transformation

$$L\left\{af(t) + bg(t)\right\} = aL\left\{f(t) + bL\left\{g(t)\right\}\right\}$$

iv) Integration of f(t)

$$L\left\{\int_0^t f(\tau)d\tau\right\} = \frac{1}{s}L\left\{f(t)\right\}$$



[Re] Analytical solution by Laplace transformation

Consider advection-diffusion equation as G.E.

$$\frac{\partial C}{\partial t} + u \frac{\partial C}{\partial x} = D \frac{\partial^2 C}{\partial x^2}$$

B.C. & I.C. for continuous input are given as

$$C(x = 0, t > 0) = C_0$$
 (a)

$$C(x \ge 0, t = 0) = 0$$
 (b)

$$C(x = \pm \infty, t \ge 0) = 0$$
 (c)

Rewrite G.E.

$$D\frac{\partial^2 C}{\partial x^2} - U\frac{\partial C}{\partial x} - \frac{\partial C}{\partial t} = 0$$

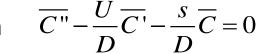




Apply Laplace transformation

$$D\frac{\partial^{2}C}{\partial x^{2}} - U\frac{\partial C}{\partial x} - s\overline{C} - C(t=0) = 0$$
$$D\frac{\partial^{2}C}{\partial x^{2}} - U\frac{\partial \overline{C}}{\partial x} - s\overline{C} = 0$$

Set,
$$\overline{C'} = \frac{\partial \overline{C}}{\partial x}$$
, $\overline{C''} = \frac{\partial^2 \overline{C}}{\partial x^2}$



C(t=0)=0

From I.C.

Assume $\overline{C} = e^{\lambda x}$

Derive characteristic equation as

$$\lambda^2 - \frac{U}{D}\lambda - \frac{s}{D} = 0$$

Solution is

$$\lambda = \frac{\frac{U}{D} \pm \sqrt{\left(\frac{U}{D}\right)^2 + 4\left(\frac{s}{D}\right)}}{2} = \frac{U \pm \sqrt{U^2 + 4sD}}{2D}$$



Then, \overline{C} is

$$\overline{C} = C_1 e^{-\lambda_1 x} + C_2 e^{-\lambda_2 x}$$

$$= C_1(s) \exp\left\{\frac{U \pm \sqrt{U^2 + 4sD}}{2D}x\right\} + C_2(s) \exp\left\{\frac{U \pm \sqrt{U^2 + 4sD}}{2D}x\right\}$$
(1)

Laplace transformation of B.C., Eq. (c) is

$$\lim_{x \to \infty} \overline{C}(x,s) = \lim_{x \to \infty} \int_0^\infty e^{-st} C(x,t) dt$$
$$= \int_0^\infty \left\{ e^{-st} \lim_{x \to \infty} C(x,t) dt \right\} = 0$$

If we apply this to Eq. (1)

$$\lim_{x \to \infty} \overline{C}(x,s) = \lim_{x \to \infty} \left[C_1(s) \exp\left\{ \frac{U \pm \sqrt{U^2 + 4sD}}{2D} x \right\} \right] + \lim_{x \to \infty} \left[C_2(s) \exp\left\{ \frac{U \pm \sqrt{U^2 + 4sD}}{2D} x \right\} \right] = 0$$

$$\therefore C_1(s) \quad \text{should be zero}$$

$$\therefore \ldots \overline{C} = C_2(s) \exp\left\{ \frac{U \pm \sqrt{U^2 + 4sD}}{2D} x \right\}$$





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2.3.4 Concentration Specified as a Function of Time

Apply B.C., Eq. (a)

Laplace transformation

$$\overline{C}(0,s) = \frac{1}{s}C_0$$

$$\therefore C_2(s) = C_0 / s$$

$$\therefore \overline{C} = \frac{C_0}{s} \exp\left(\frac{U \pm \sqrt{U^2 + 4sD}}{2D}x\right)$$

$$= C_0 \exp\left(\frac{Ux}{2D}\right) \frac{1}{s} \exp\left(-\frac{x}{\sqrt{D}}\sqrt{\frac{U^2}{4D}} + s\right)$$

Get inverse Laplace transformation using Laplace transform table

$$\frac{2}{s}\exp\left\{-a(s+b^2)^{\frac{1}{2}}\right\} \Leftrightarrow e^{-ab}erfc\left(\frac{a}{2\sqrt{t}}-b\sqrt{t}\right)+e^{ab}erfc\left(\frac{a}{2\sqrt{t}}-b\sqrt{t}\right)$$



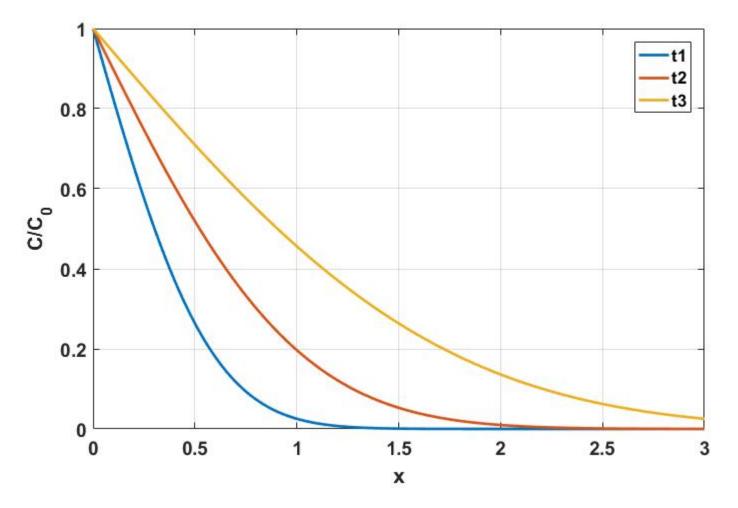


Set
$$a = \frac{x}{\sqrt{D}}, b = \frac{U}{2\sqrt{D}}$$

 $e^{-ab} = \exp\left\{-\left(\frac{x}{\sqrt{D}}, \frac{U}{2\sqrt{D}}\right)\right\} = \exp\left\{-\frac{xU}{2D}\right\}$ $e^{ab} = \exp\left\{\left(\frac{x}{\sqrt{D}}, \frac{U}{2\sqrt{D}}\right)\right\} = \exp\left\{\frac{xU}{2D}\right\}$
 $\frac{a}{2\sqrt{t}} - b\sqrt{t} = \frac{x/\sqrt{D}}{2\sqrt{t}} + \frac{U}{2\sqrt{D}}\sqrt{t} = \frac{x-Ut}{4\sqrt{Dt}}$
 $\frac{a}{2\sqrt{t}} + b\sqrt{t} = \frac{x/\sqrt{D}}{2\sqrt{t}} + \frac{U}{2\sqrt{D}}\sqrt{t} = \frac{x+Ut}{4\sqrt{Dt}}$
 $\therefore C = \frac{C_0}{2}\exp\left(\frac{Ux}{2D}\right)\left\{\exp\left(\frac{-Ux}{2D}\right)erfc\left(\frac{x-Ut}{\sqrt{4Dt}}\right) + \exp\left(\frac{Ux}{2D}\right)erfc\left(\frac{x+Ut}{\sqrt{4Dt}}\right)\right\}$
 $= \frac{C_0}{2}\left\{erfc\left(\frac{x-Ut}{\sqrt{4Dt}}\right) + \exp\left(\frac{Ux}{2D}\right)erfc\left(\frac{x+Ut}{\sqrt{4Dt}}\right)\right\}$
In case $U=0$
 $C = \frac{C_0}{2}\left\{erfc\left(\frac{x}{\sqrt{4Dt}}\right) + erfc\left(\frac{x}{\sqrt{4Dt}}\right)\right\} = C_0erfc\left(\frac{x}{\sqrt{4Dt}}\right)$ (2.45)







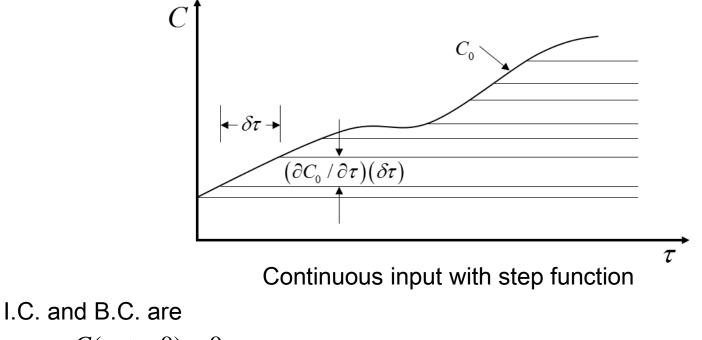
Solution for continuous step function





(2) Concentration specified as a function of time at fixed point \rightarrow Problem 2-2

Consider the case where $C_0(\tau)$ is a time variable concentration at x = 0



$$C(x,t=0) = 0$$

 $C(x=0,t>0) = C_0(\tau)$





The solution is obtained by a <u>superposition of solution</u>, (2.44).

In each time increment δ_{τ} the concentration at x = 0 changes by an amount $\frac{\partial C}{\partial \tau} \delta_{\tau}$.

Thus, for a change occurring at time τ the result for all future times, due to the

incremental changes, is given as

$$\delta C = \frac{\partial C_0}{\partial \tau} \delta \tau erfc \left(\frac{x}{\sqrt{4D(t-\tau)}} \right), \ t > \tau$$

Then, total contribution is

$$C(x,t) = \int_{-\infty}^{t} \frac{\partial C_0}{\partial \tau} erfc\left(\frac{x}{\sqrt{4D(t-\tau)}}\right) d\tau$$





2.3.5 Input of mass specified as a function of time

(1) Continuous injection of mass at the rate \dot{M} , $-\infty < t < \infty \rightarrow$ **Problem 2-3**

We can assume that a continuous injection of mass at the rate \dot{M} (*M*/*t*) is equivalent to injecting a slug of amount $\dot{M} \delta \tau$ after each time increment $\delta \tau$.

Then, the concentration resulting from the continuous injection is the <u>sum of the</u> <u>concentrations resulting from the individual slugs</u> injected at all time <u>prior to the</u> <u>time of observation</u>.

Thus, concentration resulting from the individual slug is

$$dC = \frac{\dot{M}(\tau)d\tau}{\sqrt{4\pi D(t-\tau)}} \exp\left[\frac{x^2}{4D(t-\tau)}\right]$$

Total contribution is

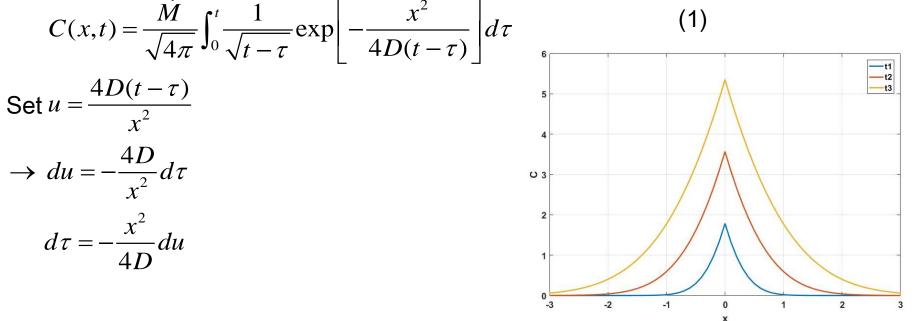
$$C = \int_{-\infty}^{t} \frac{\dot{M}(\tau)\tau}{\sqrt{4\pi D(t-\tau)}} \exp\left[-\frac{x^2}{4D(t-\tau)}\right] d\tau$$
(2.46)

where $\dot{M}(\tau)$ = rate of input mass at time τ and may vary with time = [ML⁻²t⁻¹]





(2) Continuous injection of mass of <u>constant strength</u> \dot{M} , $t > 0 \rightarrow$ <u>Problem 2-4</u> Eq. (2.46) gives



Continuous injection of mass of constant strength

(2.47)

Then, substituting this into (1) yields

$$C(x,t) = \frac{\dot{M}x}{4D\sqrt{\pi}} \int_{0}^{\frac{4Dt}{x^{2}}} u^{-\frac{1}{2}} \exp\left[-\frac{1}{u}\right] du$$





- (3) Continuous injection of distributed source of mass $m(x, t) \rightarrow \underline{\text{Problem 2-5}}$
- \rightarrow superposition in space and then in time to get solution
- m = mass per unit length per unit time= [ML⁻³t⁻¹]

$$C(x,t) = \int_{-\infty}^{t} \int_{-\infty}^{\infty} \frac{m(\xi,\tau)}{\sqrt{4\pi D(t-\tau)}} \exp\left[-\frac{(x-\xi)^2}{4D(t-\tau)}\right] d\xi d\tau$$
(2.48)





Case	Initial and boundary conditions	Solution
2-1	Continuous input with step function $C_0 = C_0(t)$	$C(x,t) = C_0 \left[1 - erf\left(\frac{x}{\sqrt{4Dt}}\right) \right] = C_0 erfc\left(\frac{x}{\sqrt{4Dt}}\right)$
2-2	$C_0(\tau)$ as a time variable concentration at $x = 0$	$C(x,t) = \int_{-\infty}^{t} \frac{\partial C_0}{\partial \tau} erfc \left(\frac{x}{\sqrt{4D(t-\tau)}}\right) d\tau$
2-3	Continuous injection of mass at the rate \dot{M} , $-\infty < t < \infty$	$C(x,t) = \int_{-\infty}^{t} \frac{\dot{M}(\tau)}{\sqrt{4\pi D(t-\tau)}} \exp\left[-\frac{x^2}{4D(t-\tau)}\right] d\tau$
2-4	Continuous injection of mass of constant strength \dot{M} , $t > 0$	$C(x,t) = \frac{\dot{M}x}{4D\sqrt{\pi}} \int_0^{\frac{4Dt}{x^2}} u^{-\frac{1}{2}} \exp(-\frac{1}{u}) du$
2-5	Continuous injection of distributed source of mass $m(x, t)$	$C(x,t) = \int_{-\infty}^{t} \int_{-\infty}^{\infty} \frac{m(\xi,\tau)}{\sqrt{4\pi D(t-\tau)}} \exp\left[-\frac{(x-\xi)^2}{4D(t-\tau)}\right] d\xi d\tau$

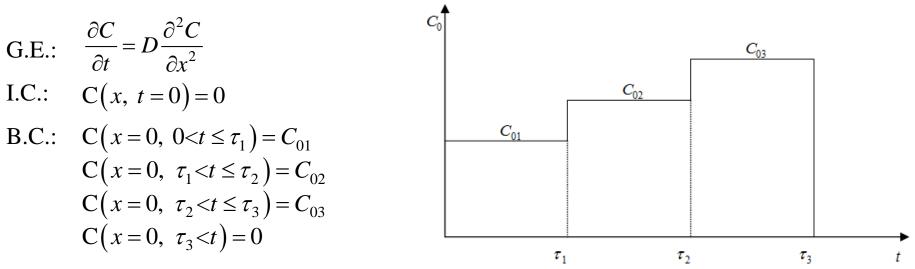
Summary of solutions for continuous inputs (Series 2)



Homework # 2

Due: 1 week from today

Consider pulse input of concentration specified as a step function



- a) Derive analytical solution using Laplace transformation.
- b) Plot C vs x for various time t with assumed C_0s ,

for example, $C_{01} = C_0/2$; $C_{02} = C_0$; $C_{03} = 3/2C_0$.

c) Plot *C* vs *t* for various distance *x*.





2.3.6 Solution Accounting for Boundaries

- Consider spreading restricted by the presence of boundaries
- Principle of superposition
- → If the equation and boundary conditions are <u>linear</u> it is possible <u>to superimpose</u> <u>any number of individual solutions</u> of the equation to obtain a new solution.
 The method of superposition for matching the <u>boundary condition of zero transport</u> through the walls (single boundary)
- (1) Mass input at x = 0 with <u>non-diffusive</u> boundary at $x = -L \rightarrow$ <u>Problem 3-1</u>
- I.C.: unit mass of solute at x = 0 at t = 0
- B.C.: wall through which concentration cannot diffuse located at x = -L



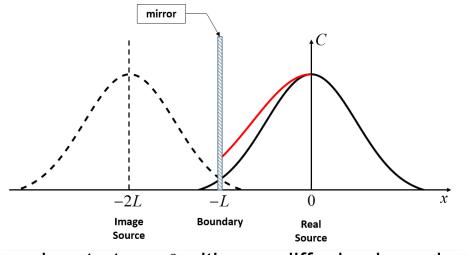


→ Fick's law for the boundary condition of no transport through the wall is

$$q\Big|_{x=-L} = -D \frac{\partial c}{\partial x}\Big|_{x=-L} = 0$$
 \rightarrow Neumann type B.C.

→ Concentration gradient must be zero at the wall.

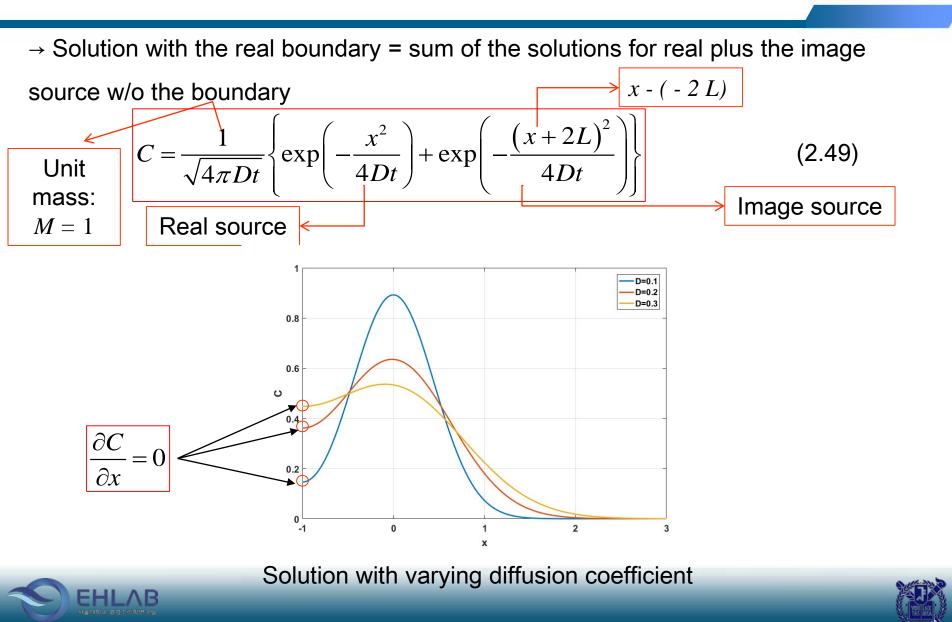
→ This condition would be met if an <u>additional unit mass of solute</u> (<u>image source</u>) was concentrated at the point x = -2L, and if the wall was removed so that <u>both slugs</u> <u>could diffuse to infinity in both directions</u>.



Mass input at x = 0 with non-diffusive boundary

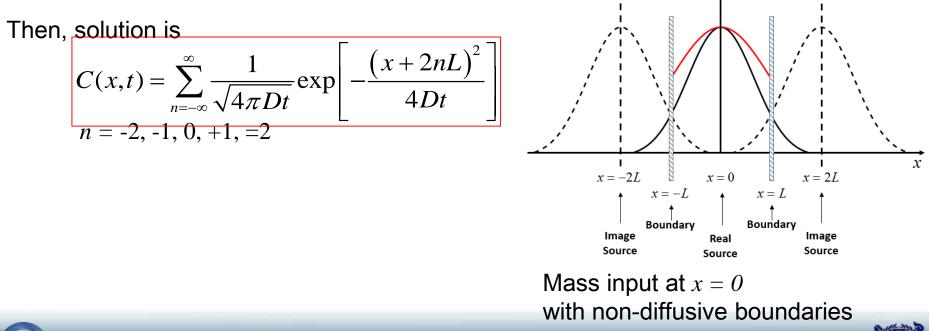




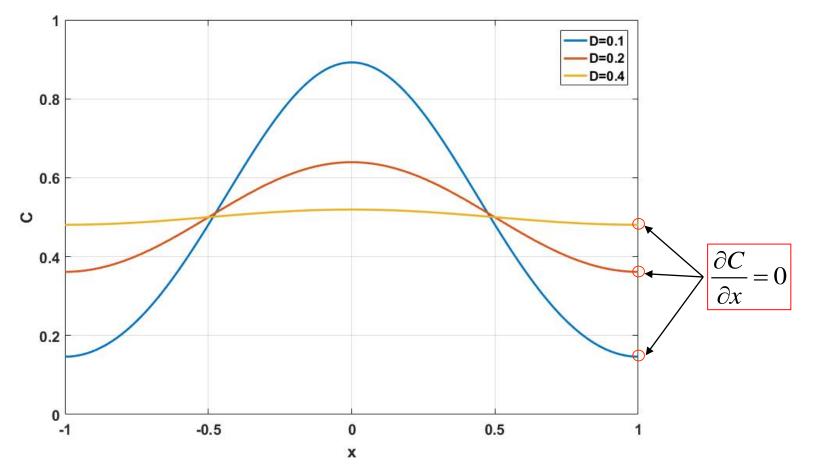


- (2) Unit mass input x = 0 with non-diffusive boundaries at x = -L and at x = +L
- \rightarrow Problem 3-2
- \rightarrow put image slugs *at* -2L, +2L, 4L, -6L, 8L,

(: slug at x = -2L causes a positive gradient at the boundary at +L, which must be counteracted by another slug located at x = +4L, and so on)







Solution for mass input at x = 0 with non-diffusive boundaries





- (3) Zero concentration at $x = \pm L$ (absorbing boundary) \rightarrow **Problem 3-3**
 - \rightarrow $C(x = \pm L, t) = 0$ \rightarrow Dirichlet type B.C.

→ $\int_{-\infty}^{\infty}$ negative image slugs at $x = \pm 2L$ positive image slugs at $x = \pm 4L$ etc.

$$C(x,t) = \frac{1}{\sqrt{4\pi Dt}} \sum_{n=-\infty}^{\infty} \left\{ \exp\left[\frac{-\left(x+4nL\right)^2}{4Dt}\right] - \exp\left[\frac{-\left[x+\left(4n-2\right)L\right]^2}{4Dt}\right] \right\}$$

(4) Mass input x = 0 with non-diffusive boundaries at $x = 0 \rightarrow$ **Problem 3-4**

 \rightarrow Solution for negative x is reflected in the plane x = 0 and superposed on the original distribution in the region x > 0.

 \rightarrow reflection at a boundary x = 0 means the adding of two solutions of the diffusion

equation

$$C = \frac{1}{\sqrt{4\pi Dt}} \left\{ \exp\left(-\frac{x^2}{4Dt}\right) + \exp\left(-\frac{(x+0)^2}{4Dt}\right) \right\} = \frac{1}{\sqrt{\pi Dt}} \exp\left(-\frac{x^2}{4Dt}\right)$$
EHLAB



Case	Initial and boundary conditions	Solution
3-1	Mass input at $x = 0$ with non- diffusive boundary at $x = -L$	$C(x,t) = \frac{1}{\sqrt{4\pi Dt}} \left\{ \exp\left(-\frac{x^2}{4Dt}\right) + \exp\left(-\frac{(x+2L)^2}{4Dt}\right) \right\}$
3-2	Mass input $x = 0$ with non- diffusive boundaries at $x = \pm L$	$C(x,t) = \sum_{n=-\infty}^{\infty} \frac{1}{\sqrt{4\pi Dt}} \exp\left[\frac{-(x+2nL)^2}{4Dt}\right]$
3-3	Zero concentration at $x = \pm L$	$C(x,t) = \frac{1}{\sqrt{4\pi Dt}} \sum_{n=-\infty}^{\infty} \begin{cases} \exp\left[\frac{-(x+4nL)^2}{4Dt}\right] \\ -\exp\left[\frac{-[x+(4n-2)L]^2}{4Dt}\right] \end{cases}$
3-4	Mass input $x = 0$ with non- diffusive boundaries at $x = 0$	$C(x,t) = \frac{1}{\sqrt{\pi Dt}} \exp\left(-\frac{x^2}{4Dt}\right)$





2.3.7 Solutions in Two and Three Dimensions

(1) 2D Fluid

- A mass *M* [*mass/L*] deposited at t = 0 at x = 0, $y = 0 \rightarrow$ **Problem 4-1**

G. E.:
$$\frac{\partial C}{\partial t} = D_x \frac{\partial^2 C}{\partial x^2} + D_y \frac{\partial^2 C}{\partial y^2}$$
 (2.50)
I.C.: $C(x, y, 0) = M \delta(x) \delta(y)$

For molecular diffusion, $D_x = D_y = D$

Use Product rule

where
$$C(x, y, t) = C_1(x, t)C_2(y, t)$$

 $C_1 \neq f(y), \quad C_2 \neq f(x)$
 $\frac{\partial C}{\partial t} = \frac{\partial}{\partial t}(C_1C_2) = C_1\frac{\partial C_2}{\partial t} + C_2\frac{\partial C_1}{\partial t}; \quad \frac{\partial^2 C}{\partial x^2} = \frac{\partial^2}{\partial x^2}(C_1C_2) = C_2\frac{\partial^2 C_1}{\partial x^2}$
 $\frac{\partial^2 C}{\partial y^2} = \frac{\partial^2}{\partial y^2}(C_1C_2) = C_1\frac{\partial^2 C_2}{\partial y^2}$



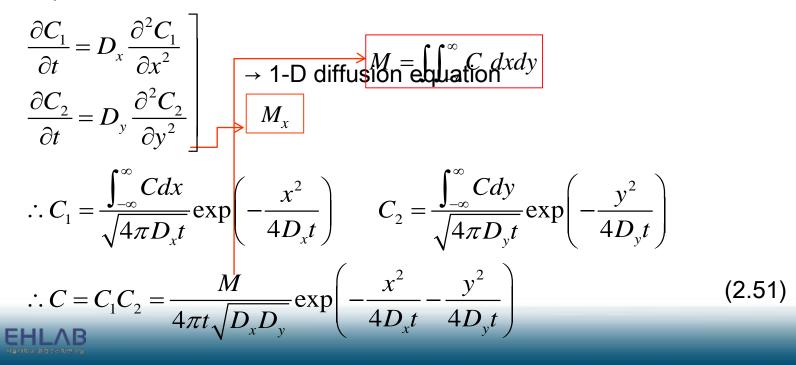
Eq. (2.50) becomes

$$C_1 \frac{\partial C_2}{\partial t} + C_2 \frac{\partial C_1}{\partial t} = D_x C_2 \frac{\partial^2 C_1}{\partial x^2} + D_y C_1 \frac{\partial^2 C_2}{\partial y^2}$$

Rearrange

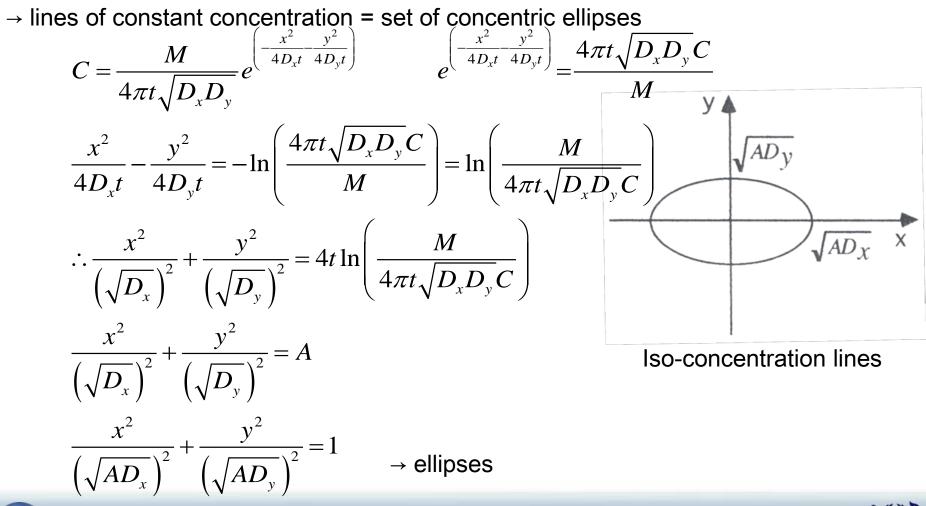
$$C_{2}\left[\frac{\partial C_{1}}{\partial t} - D_{x}\frac{\partial^{2}C_{1}}{\partial x^{2}}\right] + C_{1}\left[\frac{\partial C_{2}}{\partial t} - D_{y}\frac{\partial^{2}C_{2}}{\partial y^{2}}\right] = 0$$

Whole equation = 0 if





- Iso-concentration lines



If $D_x = D_y$ Then, $x^2 + y^2 = R^2 \rightarrow \text{circle}$

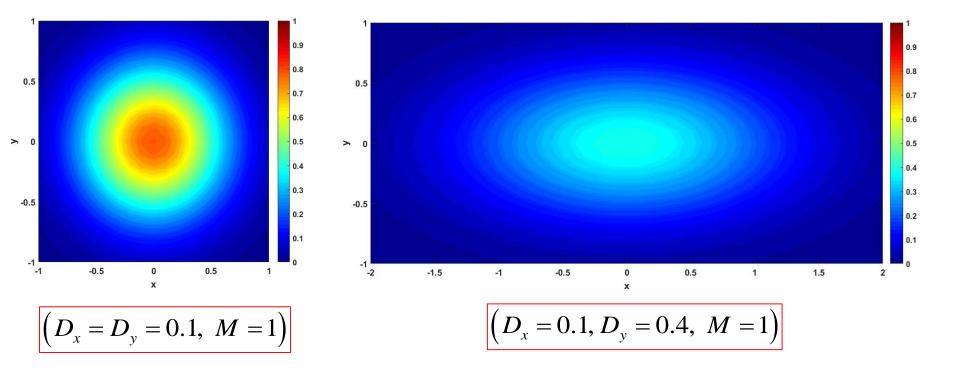


Two-dimensional advection and diffusion in open channels





-Contour Graphics-
$$C = \frac{M}{\sqrt{4\pi Dt}} \bigg\{ \exp \bigg(-\frac{x^2}{4D_x t} - \frac{y^2}{4D_y} \bigg) \bigg\}$$



Contour graphics for different cases of D_x and D_y





0.9

0.8

0.7

0.6

0.5

0.4

0.3

0.2

0.1

0

2.3 Mathematics of Diffusion Equation

3D graphics of concentration distributions



 v_{y} only



(2) 3D fluid

- A mass *M* [M] deposited at t = 0 at x = 0, y = 0, $z = 0 \rightarrow$ **Problem 4-2**

G. E.:
$$\frac{\partial C}{\partial t} = D_x \frac{\partial^2 C}{\partial x^2} + D_y \frac{\partial^2 C}{\partial y^2} + D_z \frac{\partial^2 C}{\partial z^2}$$
 (b)
I.C.: $C(x, y, z, 0) = M \delta(x) \delta(y) \delta(z) \rightarrow \text{point source}$

Use product rule

$$C(x, y, z, t) = C_1(x, t)C_2(y, t)C_3(z, t)$$

$$\frac{\partial C}{\partial t} = \frac{\partial}{\partial t}(C_1C_2C_3) = C_1\frac{\partial(C_2C_3)}{\partial t} + C_2C_3\frac{\partial C_1}{\partial t}$$

$$= C_1C_2\frac{\partial C_3}{\partial t} + C_1C_3\frac{\partial C_2}{\partial t} + C_2C_3\frac{\partial C_1}{\partial t}$$





$$\frac{\partial^2 C}{\partial x^2} = \frac{\partial^2}{\partial x^2} (C_1 C_2 C_3) = C_2 C_3 \frac{\partial^2 C_1}{\partial x^2}$$
$$\frac{\partial^2 C}{\partial y^2} = \frac{\partial^2}{\partial y^2} (C_1 C_2 C_3) = C_1 C_3 \frac{\partial^2 C_2}{\partial y^2}$$
$$\frac{\partial^2 C}{\partial z^2} = \frac{\partial^2}{\partial z^2} (C_1 C_2 C_3) = C_1 C_2 \frac{\partial^2 C_3}{\partial z^2}$$

Substituting these relations into (b) yields

$$C_{1}C_{2}\frac{\partial C_{3}}{\partial t} + C_{1}C_{3}\frac{\partial C_{2}}{\partial t} + C_{2}C_{3}\frac{\partial C_{1}}{\partial t} = D_{x}C_{2}C_{3}\frac{\partial^{2}C_{1}}{\partial x^{2}} + D_{y}C_{1}C_{3}\frac{\partial^{2}C_{2}}{\partial y^{2}} + D_{z}C_{1}C_{2}\frac{\partial^{2}C_{3}}{\partial z^{2}}$$
$$C_{1}C_{2}\left[\frac{\partial C_{3}}{\partial t} - D_{z}\frac{\partial^{2}C_{3}}{\partial z^{2}}\right] + C_{1}C_{3}\left[\frac{\partial C_{2}}{\partial t} - D_{y}\frac{\partial^{2}C_{2}}{\partial y^{2}}\right] + C_{2}C_{3}\left[\frac{\partial C_{1}}{\partial t} - D_{x}\frac{\partial^{2}C_{1}}{\partial x^{2}}\right] = 0$$





$$C_{1} = \frac{\int Cdx}{\sqrt{4\pi D_{x}t}} \exp\left(-\frac{x^{2}}{4D_{x}t}\right)$$

$$C_{2} = \frac{\int Cdy}{\sqrt{4\pi D_{y}t}} \exp\left(-\frac{y^{2}}{4D_{y}t}\right)$$

$$C_{3} = \frac{\int Cdz}{\sqrt{4\pi D_{z}t}} \exp\left(-\frac{z^{2}}{4D_{z}t}\right)$$

$$C = C_{1}C_{2}C_{3} = \frac{M}{(4\pi t)^{\frac{3}{2}}(D_{x}D_{y}D_{z})^{\frac{1}{2}}} \exp\left(-\frac{x^{2}}{4D_{x}t} - \frac{y^{2}}{4D_{y}t} - \frac{z^{2}}{4D_{z}t}\right)$$

$$M = \iiint C dx dy dz$$





2.3.8 Advective Diffusion

1D Advection-Diffusion Equation is

$$\frac{\partial C}{\partial t} + \frac{\partial}{\partial x}(uC) = D\frac{\partial^2 C}{\partial x^2}$$
(2.52)

1) Instantaneous mass input in 1D uniform flow \rightarrow **Problem 5-1**

Assume that *u* is constant and gradient in *y*-direction is small

I.C.:
$$C(x,0) = M\delta(x)$$

$$\mathsf{B.C.:} \quad C(\pm\infty,t) = 0$$

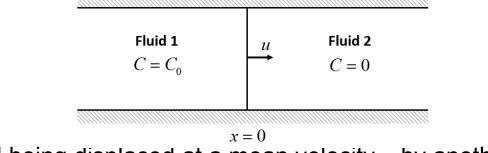
$$C(x,t) = \frac{M}{\sqrt{4\pi D t}} \exp\left(-\frac{\left(x - ut\right)^2}{4Dt}\right)$$





- 2) Instantaneous concentration input over $x < 0 \rightarrow$ <u>Problem 5-2</u>
- Problem of pipe filled with one fluid being displaced at a mean velocity u by another fluid with a tracer in concentration C_0

I.C.:
$$C(x,0) = 0$$
, $x > 0$; $C(x,0) = C_0$, $x < 0$



Fluid being displaced at a mean velocity *u* by another fluid

Transform coordinate system whose origin moves at velocity *u*

Let
$$x' = x - ut, t = t$$
 $\rightarrow \frac{\partial x'}{\partial x} = 1, \frac{\partial x'}{\partial t} = -u$
 $\frac{\partial t}{\partial x} = 0, \frac{\partial t}{\partial t} = 1$





(a)

Use chain rule

$$\frac{\partial}{\partial x} = \frac{\partial x'}{\partial x} \frac{\partial}{\partial x'} + \frac{\partial t}{\partial x} \frac{\partial}{\partial t} = \frac{\partial}{\partial x'}$$
$$\frac{\partial}{\partial t} = \frac{\partial x'}{\partial t} \frac{\partial}{\partial x'} + \frac{\partial t}{\partial t} \frac{\partial}{\partial t} = -u \frac{\partial}{\partial x'} + \frac{\partial}{\partial t}$$

Substitute this into G.E.

$$\frac{\partial C}{\partial t} = -u \frac{\partial C}{\partial x'} + \frac{\partial C}{\partial t}$$
$$u \frac{\partial C}{\partial x} = u \frac{\partial C}{\partial x'}$$
$$D \frac{\partial^2 C}{\partial x^2} = D \frac{\partial^2 C}{\partial x'^2}$$

Then G.E. becomes

$$\frac{\partial C}{\partial t} = D \frac{\partial^2 C}{\partial x'^2}$$

 \rightarrow This problem is identical to diffusion of distributed source with step function

 C_0 for x < 0 in a stagnant fluid (Problem 1-5)

There, solution is

$$C(x',t) = \frac{C_0}{2} \left[1 - erf\left(\frac{x'}{\sqrt{4Dt}}\right) \right]$$

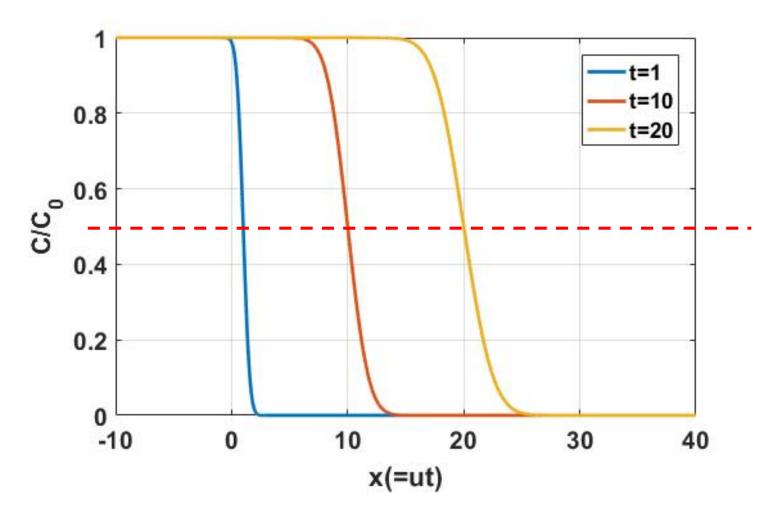
Adjust for the moving coordinates

$$C(x,t) = \frac{C_0}{2} \left[1 - erf\left(\frac{x - ut}{\sqrt{4Dt}}\right) \right]$$

(2.53)







Solution of instantaneous concentration input over x < 0

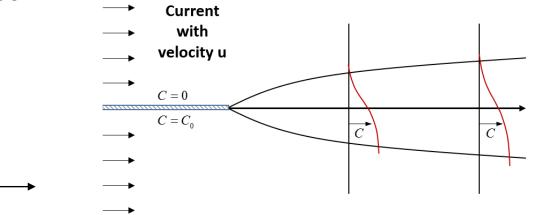




3) Lateral (transverse) diffusion \rightarrow **Problem 5-3**

- transverse mixing of two streams of different uniform concentrations flowing

side by side



Transverse mixing of two streams

Start with 2-D advection-diffusion equation

$$\frac{\partial C}{\partial t} + u \frac{\partial C}{\partial x} + v \frac{\partial C}{\partial y} = D \left[\frac{\partial^2 C}{\partial x^2} + \frac{\partial^2 C}{\partial y^2} \right]$$





Assumptions:

i) continuous input: $\frac{\partial C}{\partial t} \to 0$ ii) velocity in transverse direction is small: $v \frac{\partial C}{\partial y} \to 0$ iii) advection in *x*-direction is bigger than diffusion: $D \frac{\partial^2 C}{\partial x^2} \to 0$

Then, G.E. becomes

$$u\frac{\partial C}{\partial x} = D\frac{\partial^2 C}{\partial y^2}$$

 \rightarrow similar to 1-D diffusion equation

B. C.: C(0, y) = 0 y > 0 ; $C(0, y) = C_0$, y < 0

 \rightarrow Now, this problem is similar to <u>Problem 1-5</u> with t = x/u; x' = y

Solution is

$$\therefore C = \frac{C_0}{2} \left[1 - erf\left(\frac{x}{\sqrt{4Dt}}\right) \right]$$

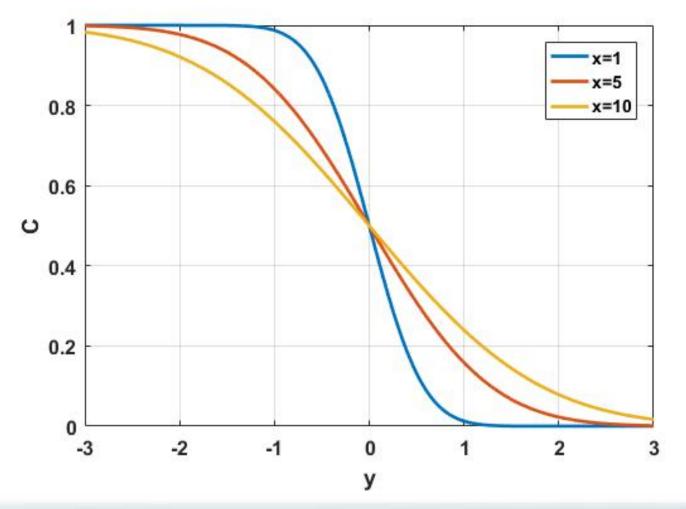
Convert to *x-y* coordinates

$$C = \frac{C_0}{2} \left[1 - erf\left(\frac{y}{\sqrt{4Dx/u}}\right) \right]$$

EHLAB

(2.54)









4) Continuous plane source
$$\rightarrow \underline{\text{Problem 5-4}}$$

G.E.: $\frac{\partial C}{\partial t} + u \frac{\partial C}{\partial x} = D \frac{\partial^2 C}{\partial x^2}$
B.C.: $C(0,t) = C_0$ $0 < t < \infty$ \rightarrow steady continuous input
 $C(x,0) = 0$ $0 < x < \infty$

→ identical to continuous input with step function $C_0 = C_0(t)$ (Problem 2-1). The solution is

$$C(x,t) = \frac{C_0}{2} \left[erfc\left(\frac{x-ut}{\sqrt{4Dt}}\right) + erfc\left(\frac{x+ut}{\sqrt{4Dt}}\right) \exp\left(\frac{ux}{D}\right) \right]$$
(2.55)

Set

$$P_{e} = Peclet number = \frac{ux}{D}$$
$$t_{R} = \frac{ut}{x} = \frac{t}{x/u}$$





Then,

$$\frac{C(x,t)}{C_0} = \frac{1}{2} \operatorname{erfc} \left[\left(\frac{P_e}{4t_R} \right)^{\frac{1}{2}} (1 - t_R) \right] + \frac{1}{2} \operatorname{erfc} \left[\left(\frac{P_e}{4t_R} \right)^{\frac{1}{2}} (1 + t_R) \right] \exp(P_e)$$

For <u>advection-dominated</u> case (large *u*)

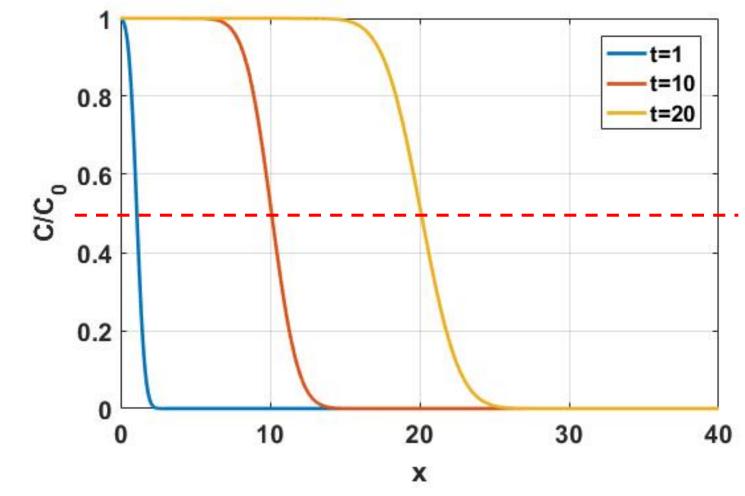
$$P_e > 500$$
; $\frac{C}{C_0} \approx \frac{1}{2} \operatorname{erfc}\left(\frac{x - ut}{\sqrt{4Dt}}\right)$

Diffusion problem (u = 0)

$$\frac{C}{C_0} = erfc\left(\frac{x}{\sqrt{4Dt}}\right)$$







Solution for continuous plane source with elapsed time





Case	e Initial and boundary conditions	Solution
5-1	Instantaneous mass input in 1D uniform flow	$C(x,t) = \frac{M}{\sqrt{4\pi Dt}} \exp\left(-\frac{(x-ut)^2}{4Dt}\right)$
5-2	Instantaneous concentration input over x < 0	$C(x,t) = \frac{C_0}{2} \left[1 - erf\left(\frac{x - ut}{\sqrt{4Dt}}\right) \right]$
5-3	Transverse mixing of two streams of different uniform concentrations flowing side by side	$C = \frac{C_0}{2} \left[1 - erf\left(\frac{y}{\sqrt{4Dx/u}}\right) \right]$
5-4	Continuous plane source in 1D uniform flow	$C(x,t) = \frac{C_0}{2} \left[erfc\left(\frac{x-ut}{\sqrt{4Dt}}\right) + erfc\left(\frac{x+ut}{\sqrt{4Dt}}\right) \exp\left(\frac{ux}{D}\right) \right]$

Summary of solutions for advective diffusion (Series 5)



Homework Assignment #3

Due: Two weeks from today

a) Derive analytical solution for 1-D dispersion equation with continuous plane source condition which is given as

$$C(0,t) = C_0, \qquad 0 < t < \infty$$

$$C(x,t=0) = 0, \qquad 0 < x < \infty$$

$$C(x = \pm \infty, t) = 0, \qquad 0 < t < \infty$$

$$C(x,t) = \frac{C_0}{2} \left[erfc\left(\frac{x-ut}{\sqrt{4Dt}}\right) + erfc\left(\frac{x+ut}{\sqrt{4Dt}}\right) exp\left(\frac{ux}{D}\right) \right]$$

b) Plot C vs. x for various values P_e of and t.

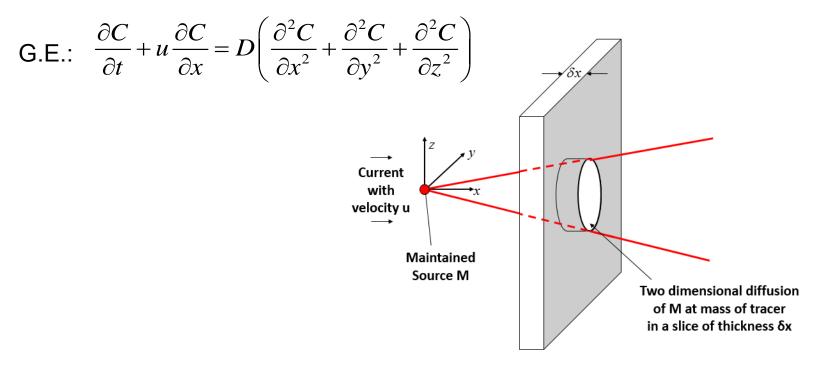




2.3.9 Maintained point source

(1) Constant point source in $3D \rightarrow Problem 6-1$

- Mass input at the rate \dot{M} at the origin (x, y, z) in three-dimensional flow



Constant point source in 3D flows





- Reduction of a three-dimensional problem to two dimensions by considering <u>diffusion in a moving slice</u>
- → visualize the flow as consisting of a series of parallel slices of thickness δx bounded by infinite parallel *y*-*z* planes
- → slices are being advected past the source with velocity *u*, and during the passage each one receives a slug of mass of amount $\dot{M}\delta t$
- time taken for slice to pass source; $\delta t = \frac{\delta x}{u}$ - mass collected by slice at it passes source = $\dot{M}\delta t = \dot{M}\frac{\delta x}{u}$ \rightarrow This is identical to 2-D solution of Eq. (2.51). $C = \frac{mass/l}{4\pi t\sqrt{D_y D_z}} \exp\left(-\frac{y^2}{4D_y t} - \frac{z^2}{4D_z t}\right)$; $C = \frac{\left(\dot{M}\frac{\delta x}{u}\right)}{4\pi D t} \exp\left(-\frac{(y+z)^2}{4D t}\right)$





Substitute
$$t = \frac{x}{u}$$

$$C(x, y, z) = \frac{\dot{M}}{4\pi Dx} \exp\left(-\frac{(y^2 + z^2)u}{4Dx}\right)$$

Eq. (2.56) was derived by neglecting diffusion in the direction of flow.

$$\rightarrow \qquad ut \gg \sqrt{2Dt} \quad or \quad t \gg 2D/u^2$$

(2) Maintained point source in 2D flow \rightarrow Problem 6-2 $\dot{M}\delta x/u$ (y^2)

$$C_{1} = \frac{1}{\sqrt{4\pi Dt}} \exp\left(-\frac{1}{4Dt}\right)$$

ubstitute $t = \frac{x}{u}$
$$C(x, y) = \frac{\dot{M}}{u\sqrt{4\pi Dx/u}} \exp\left(-\frac{y^{2}u}{4Dx}\right)$$

(2.57)

(2.55)

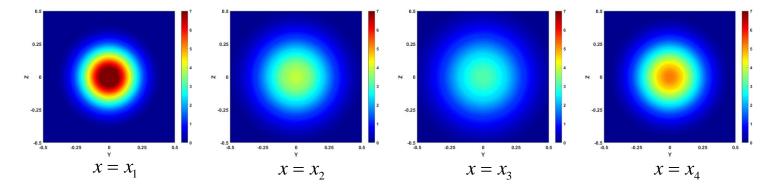
M = strength of a line source in units of mass per unit length per unit time



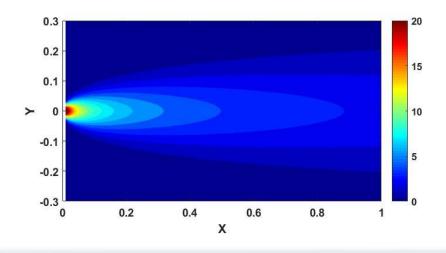
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-Constant point source in $3D \rightarrow Problem 6-1$



-Maintained point source in 2D flow \rightarrow **Problem 6-2**





 \dot{M}



Case	Initial and boundary conditions	Solution
6-1	Mass input at the rate \dot{M} at the origin (<i>x</i> , <i>y</i> , <i>z</i>) in 3D flow	$C(x, y, z) = \frac{\dot{M}}{4\pi Dx} \exp\left(-\frac{\left(y^2 + z^2\right)u}{4Dx}\right)$
6-2	Maintained point source in 2D flow	$C(x, y) = \frac{\dot{M}}{u\sqrt{4\pi Dx/u}} \exp\left(-\frac{y^2 u}{4Dx}\right)$

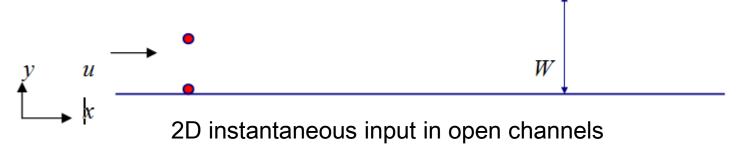
Solutions for maintained point discharges in 2D & 3D flows (Series 6)





2.3.10 Solutions for Pollutant Mixing in Rivers

(1) 2D Instantaneous Input



Assume rapid vertical mixing

G.E.:
$$\frac{\partial C}{\partial t} + u \frac{\partial C}{\partial x} = D_x \frac{\partial^2 C}{\partial x^2} + D_y \frac{\partial^2 C}{\partial y^2}$$

B.C.: $\left. \frac{\partial C}{\partial y} \right|_{y=0,w} = 0$ \rightarrow impermeable, non-diffusion boundary

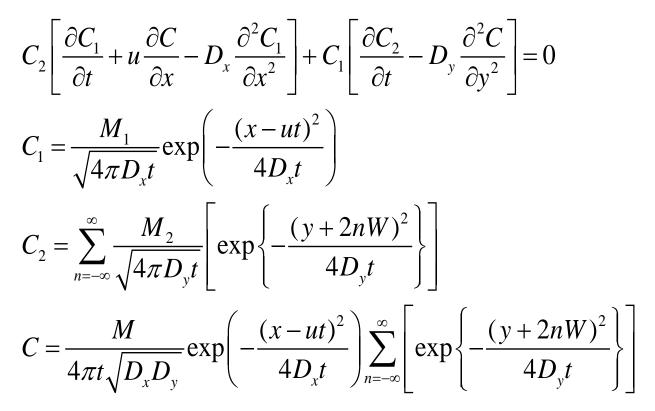
I.C.: $C(x, y, 0) = M\delta(x)\delta(y)$





i) Case A: Right-bank input

Use product rule $C = C_1(x,t)C_2(y,t)$







ii) Case B: Centerline input

a) For axis at right bank

$$C_{1} = \frac{M_{1}}{\sqrt{4\pi D_{x}t}} \exp\left(-\frac{(x-ut)^{2}}{4D_{x}t}\right) \qquad C_{2} = \sum_{n=-\infty}^{\infty} \frac{M_{2}}{\sqrt{4\pi D_{y}t}} \exp\left[-\frac{\left\{y+(2n-1)\frac{W}{2}\right\}^{2}}{4D_{y}t}\right]$$

$$C = \frac{M}{4\pi t \sqrt{D_{x}D_{y}}} \exp\left(-\frac{(x-ut)^{2}}{4D_{x}t}\right) \sum_{n=-\infty}^{\infty} \exp\left[-\frac{\left\{y+(2n-1)\frac{W}{2}\right\}^{2}}{4D_{y}t}\right]$$

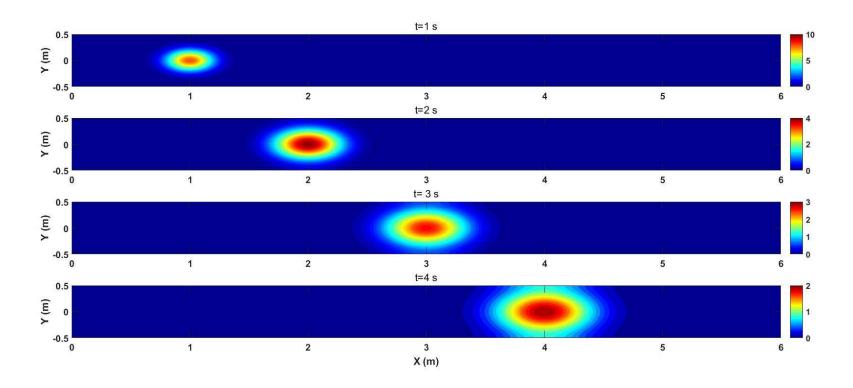
b) For axis at centerline

$$C_{1} = \frac{M_{1}}{\sqrt{4\pi D_{x}t}} \exp\left(-\frac{(x-ut)^{2}}{4D_{x}t}\right) \qquad C_{2} = \sum_{n=-\infty}^{\infty} \frac{M_{2}}{\sqrt{4\pi D_{y}t}} \left[\exp\left\{-\frac{y+nW^{2}}{4D_{y}t}\right\}\right]$$
$$C = \frac{M}{4\pi t \sqrt{D_{x}D_{y}}} \exp\left(-\frac{(x-ut)^{2}}{4D_{x}t}\right) \sum_{n=-\infty}^{\infty} \left[\exp\left\{-\frac{y+nW^{2}}{4D_{y}t}\right\}\right]$$





- ii) Case B: Centerline input
- b) For axis at centerline

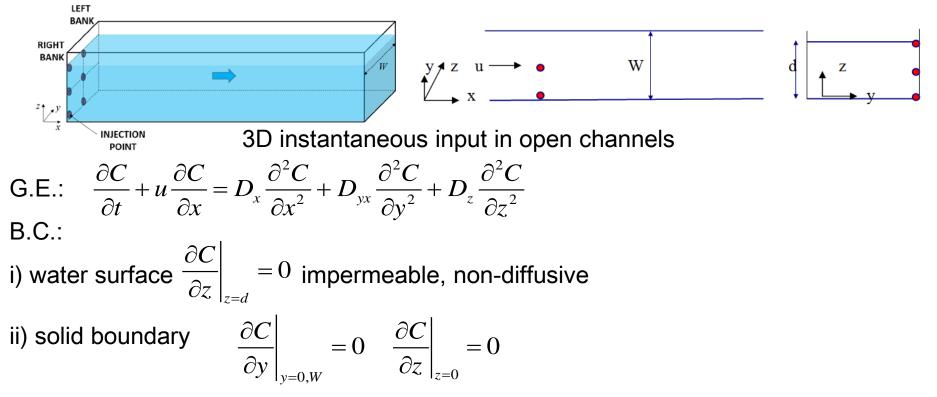






(2) 3D Instantaneous Input

Fig. 2.40 3D instantaneous input in open channels



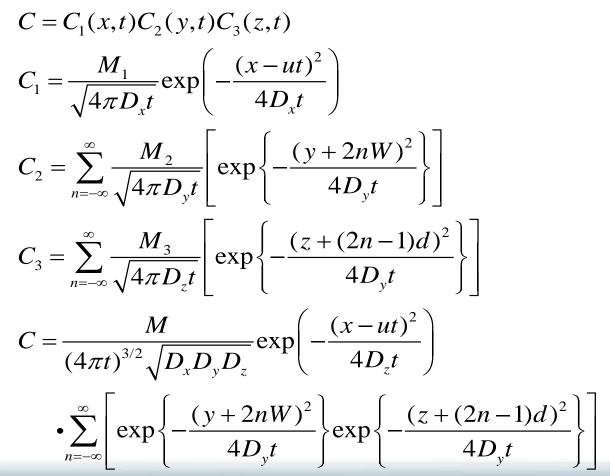
I.C.:
$$C(x, y, z, 0) = M\delta(x)\delta(y)\delta(z)$$





i) Case A: Right-bank input – surface input

Use product rule







145/149

2.3 Mathematics of Diffusion Equation

i) Case B: Right-bank input – mid-depth input

$$C_{3} = \sum_{n=-\infty}^{\infty} \frac{M_{3}}{\sqrt{4\pi D_{z}t}} \left[\exp\left\{-\frac{(z+(2n-1)\frac{d}{2})^{2}}{4D_{z}t}\right\} \right]$$

$$C = \frac{M}{(4\pi t)^{3/2}\sqrt{D_{x}D_{y}D_{z}}} \exp\left(-\frac{(x-ut)^{2}}{4D_{x}t}\right)$$

$$\cdot \sum_{n=-\infty}^{\infty} \left[\exp\left\{-\frac{(y+2nW)^{2}}{4D_{y}t}\right\} \exp\left\{-\frac{(z+(2n-1)\frac{d}{2})^{2}}{4D_{y}t}\right\} \right]$$

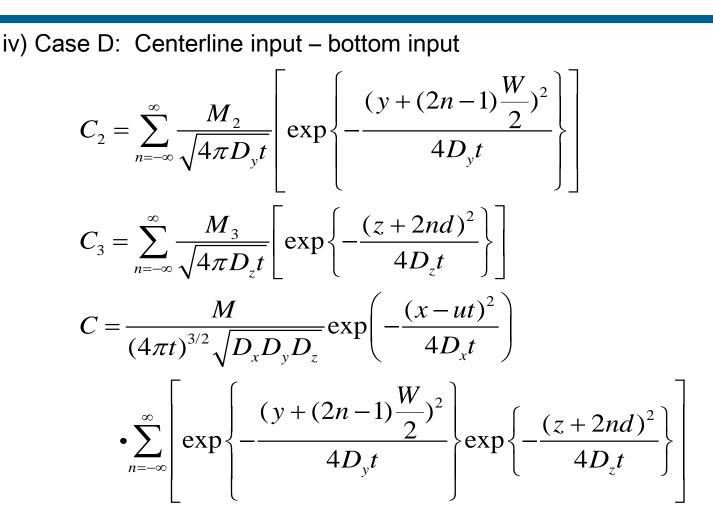
iii) Case C: Right-bank input – bottom input

$$C_{3} = \sum_{n=-\infty}^{\infty} \frac{M_{3}}{\sqrt{4\pi D_{z}t}} \left[\exp\left\{-\frac{(z+2nd)^{2}}{4D_{z}t}\right\} \right]$$

$$C = \frac{M}{(4\pi t)^{3/2}} \sqrt{D_{x}D_{y}D_{z}}} \exp\left(-\frac{(x-ut)^{2}}{4D_{x}t}\right)$$

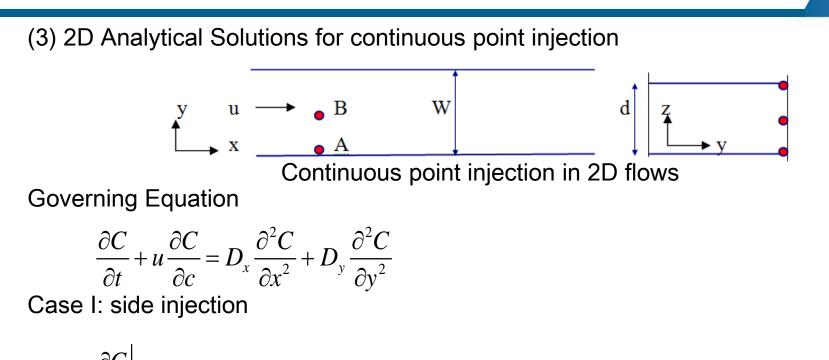
$$\sum_{n=-\infty}^{\infty} \left[\exp\left\{-\frac{(y+2nW)^{2}}{4D_{y}t}\right\} \exp\left\{-\frac{(z+2nd)^{2}}{4D_{z}t}\right\} \right]$$
EFICE PROPERTY











$$\frac{\partial C}{\partial y}\Big|_{y=0,w} = 0 \qquad C(0,0,t) = C_0 \qquad C(x,y,0) = 0$$

Case II: centerline injection

$$\frac{\partial C}{\partial y}\Big|_{y=0,w} = 0 \qquad C(0, w/2, t) = C_0 \qquad C(x, y, 0) = 0$$





Product Rule

$$C = C_1(x,t)C_2(y,t)$$

Then, the governing equation will be modified as

$$C_{2}\frac{\partial C_{1}}{\partial t} + C_{1}\frac{\partial C_{2}}{\partial t} + uC_{2}\frac{\partial C_{1}}{\partial x} = D_{x}C_{2}\frac{\partial^{2}C_{1}}{\partial x^{2}} + D_{y}C_{1}\frac{\partial^{2}C_{2}}{\partial y^{2}}$$
$$\rightarrow C_{2}\left[\frac{\partial C_{1}}{\partial t} + u\frac{\partial C_{1}}{\partial t} + D\frac{\partial^{2}C_{1}}{\partial x^{2}}\right] + C_{1}\left[\frac{\partial C_{2}}{\partial t} + D_{y}\frac{\partial^{2}C_{2}}{\partial y^{2}}\right] = 0$$

After that, we must to solve two equations

$$\frac{\partial C_1}{\partial t} + u \frac{\partial C_1}{\partial t} - D \frac{\partial^2 C_1}{\partial x^2} = 0$$
(A)

and

$$\frac{\partial C_2}{\partial t} - D_y \frac{\partial^2 C_2}{\partial y^2} = 0$$





(B)

i) Case I:
(A)
$$C_{1} = \frac{C_{1o}}{2} \left\{ erfc\left(\frac{x-ut}{\sqrt{4D_{x}t}}\right) + exp\left(\frac{ux}{D_{x}}\right) erfc\left(\frac{x+ut}{\sqrt{4D_{x}t}}\right) \right\}$$
(B)
$$C_{2} = C_{2o} \left\{ erfc\left(\frac{y}{\sqrt{4D_{y}t}}\right) + \sum_{n=1}^{\infty} erfc\left(\frac{y+2nw}{\sqrt{4D_{y}t}}\right) + \sum_{n=1}^{\infty} erfc\left(\frac{-(y-2nw)}{\sqrt{4D_{y}t}}\right) \right\}$$

$$\therefore C = \left[\frac{C_{1o}}{2} \left\{ erfc\left(\frac{x-ut}{\sqrt{4D_{x}t}}\right) + exp\left(\frac{ux}{D_{x}}\right) erfc\left(\frac{x+ut}{\sqrt{4D_{x}t}}\right) \right\} \right]$$

$$\left[C_{2o} \left\{ erfc\left(\frac{y}{\sqrt{4D_{y}t}}\right) + \sum_{n=1}^{\infty} erfc\left(\frac{y+2nw}{\sqrt{4D_{y}t}}\right) + \sum_{n=1}^{\infty} erfc\left(\frac{-(y-2nw)}{\sqrt{4D_{y}t}}\right) \right\} \right]$$

$$= \frac{C_{o}}{2} \left[erfc\left(\frac{x-ut}{\sqrt{4D_{x}t}}\right) + exp\left(\frac{ux}{D_{x}}\right) erfc\left(\frac{x+ut}{\sqrt{4D_{x}t}}\right) \right]$$

$$\left[erfc\left(\frac{y}{\sqrt{4D_{y}t}}\right) + \sum_{n=1}^{\infty} erfc\left(\frac{y+2nw}{\sqrt{4D_{y}t}}\right) + \sum_{n=1}^{\infty} erfc\left(\frac{-(y-2nw)}{\sqrt{4D_{y}t}}\right) \right]$$



ii) Case II:
(A)
$$C_1 = \frac{C_{1o}}{2} \left\{ erfc\left(\frac{x-ut}{\sqrt{4D_x t}}\right) + \exp\left(\frac{ux}{D_x}\right) erfc\left(\frac{x+ut}{\sqrt{4D_x t}}\right) \right\}$$

(B) $C_2 = \sum_{n=-\infty}^{\infty} C_{2o} erfc\left(\frac{y+2nw}{\sqrt{4D_y t}}\right)$
 $\therefore C = \left[\frac{C_{1o}}{2} \left\{ erfc\left(\frac{x-ut}{\sqrt{4D_x t}}\right) + \exp\left(\frac{ux}{D_x}\right) erfc\left(\frac{x+ut}{\sqrt{4D_x t}}\right) \right\} \right] \left[\sum_{n=-\infty}^{\infty} C_{2o}\left(\frac{y+2nw}{\sqrt{4D_y t}}\right) \right]$
 $= \frac{C_o}{2} \left[erfc\left(\frac{x-ut}{\sqrt{4D_x t}}\right) + \exp\left(\frac{ux}{D_x}\right) erfc\left(\frac{x+ut}{\sqrt{4D_x t}}\right) \right] \left[\sum_{n=-\infty}^{\infty} erfc\left(\frac{y+2nw}{\sqrt{4D_y t}}\right) \right]$

[Re] Decaying substance in 2D flow

G.E.:
$$\frac{\partial C}{\partial t} + u \frac{\partial C}{\partial x} = D_x \frac{\partial^2 C}{\partial x^2} + D_y \frac{\partial^2 C}{\partial y^2} - kC$$

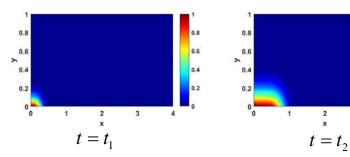
$$C(x, y, t) = C(k = 0) \exp(-kt)$$

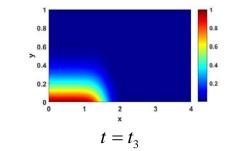


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2.3 Mathematics of Diffusion Equation

Case I: side injection





0.8

0.6

0.4

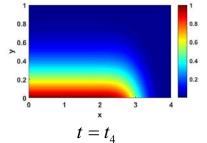
0.2

4

3

2

x



[Re] Decaying substance in 2D flow

