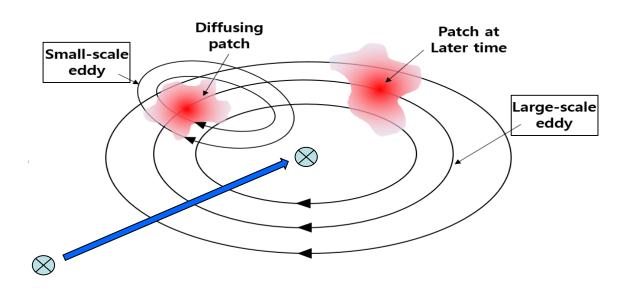
Chapter 3

Fluid Transport







Chapter 3 Fluid Transport

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- 3.2 Transport Analogies
- 3.3 Mass Transport
- 3.4 Heat Transport
- 3.5 Momentum Transport

Objectives

- Introduce the concept of fluid transport
- Study analogy between mass, heat, and momentum transport
- Derive a general equation of fluid transport





3.1 Introduction

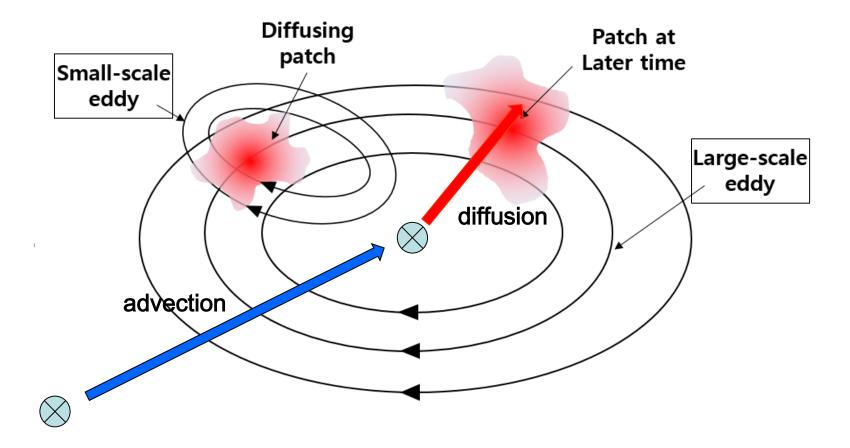
Fluid transport phenomena

- Transport
 - = ability of fluids in motion to <u>convey materials and properties from place</u> to <u>place</u>
 - = mechanism by which materials and properties are <u>diffused and</u> <u>transmitted through the fluid medium</u>
 - = advection + diffusion <
 - Advection = transport by imposed current (velocity)
 - Diffusion = movement of mass or heat or momentum in the direction of decreasing concentration of mass, temperature, or momentum





Introduction





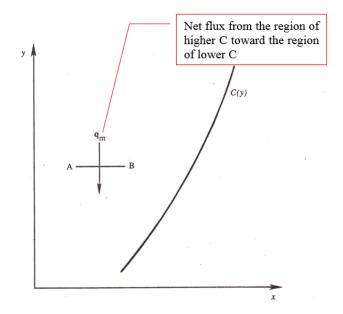


Introduction

Diffusion

$$q = \left\{ \frac{dM / dt}{area} \right\} \propto \left\{ \frac{d \left(M / vol \right)}{ds} \right\}$$

Flux = quantity per unit time per area Transport of materials and properties in the <u>direction of decreasing</u> mass, temperature, momentum





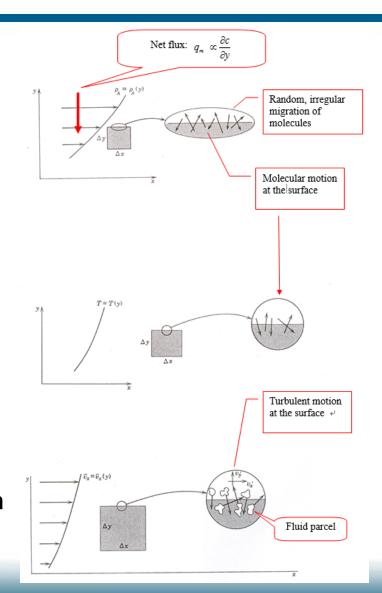


Introduction

Mass diffusion

Heat diffusion

Momentum diffusion







Diffusion: driving force = gradient

$$flux = \left\{ \frac{dM / dt}{area} \right\} \propto \left\{ \frac{d \left(M / vol \right)}{ds} \right\}$$

$$\frac{dM / dt}{A} = K \frac{d(M / vol)}{ds}$$

unit area normal to transport direction

Flux = Time rate of transport of M per

mass, heat,

Gradient of *M* per unit volume of fluid in the transport direction

(3.3)





where $K = \underline{\text{diffusivity constant}} \left(m^2 / S \right) \left[L^2 / t \right]$

K = f (modes of fluid motion, i.e., laminar and turbulent flow)

molecular diffusivity for laminar flow turbulent diffusivity for turbulent flow





1) Momentum transport

Set $M = \text{momentum} = \Delta mu$

$$\therefore \frac{d(\Delta mu)}{dt} \frac{1}{\Delta x \Delta z} = K \frac{d}{dy} \left(\frac{\Delta mu}{\Delta vol} \right)$$

Now, apply Newton's 2nd law to LHS

$$\frac{d}{dt}(mu) = m\frac{du}{dt} = ma = F$$

$$\therefore \frac{d(\Delta mu)}{dt} = \Delta F_x$$

$$\frac{d(\Delta mu)}{dt} = \frac{d(\Delta mu)}{\Delta x \Delta z} = \frac{\Delta F_x}{\Delta x \Delta z} = \tau_{yx}$$
(i)





 τ_{yx} = shear stress parallel to the x-direction acting on a plane whose normal is parallel to *y*-direction

RHS:

$$\frac{\Delta m}{\Delta vol} = \rho$$

$$\therefore RHS = K \frac{d}{dv} \left(\frac{\Delta mu}{\Delta vol} \right) = K \frac{d(\rho u)}{dv}$$
 (ii)

Combine (i) and (ii)

$$\tau_{yx} = K \frac{d(\rho u)}{dv} \tag{3.4}$$





If ρ = constant

$$\tau_{yx} = \rho K \frac{du}{dy} \tag{3.5}$$

 $K = \text{molecular diffusivity constant } (\text{m}^2/\text{s})$

If
$$K \equiv v = \frac{\mu}{\rho} = \text{kinematic viscosity}$$

Then,

$$\tau_{yx} = \rho v \frac{du}{dy} = \mu \frac{du}{dy} \tag{3.6}$$





2) Heat transport

upper plate ~ high temperature

lower plate ~ low temperature

Set

$$M = \text{heat} = Q = \Delta m C_p T \tag{3.7}$$

where C_p = specific heat at constant pressure

Then, Eq. (3.3) becomes

$$\frac{dQ}{dt}\frac{1}{\Delta x \Delta z} = q_{H_y} = -K\frac{d}{dy} \left[\frac{\Delta m C_p T}{\Delta vol} \right]$$
 (3.8)





 q_H = time rate of heat transfer per unit area normal to the direction of transport $(j/\text{sec}-\text{m}^2)$

$$K = \alpha = \text{thermal diffusivity } (\text{m}^2/\text{sec})$$

If
$$\rho (= \frac{\Delta m}{\Delta vol})$$
 and $C_p = \text{const.}$

$$\therefore q_{Hy} = -\rho C_p K \frac{dT}{dy} = -k \frac{dT}{dy}$$
 (3.9)

where $k = \rho C_p K = \underline{\text{thermal conductivity}} (j / \sec - m - K)$





3) Mass transport

$$M = \text{dissolved mass of substancs} = \Delta m_f C_M$$

(3.10)

where $\Delta m_f = {
m mass}$ of fluid

 $C_{\scriptscriptstyle M} = {\rm concentration}$

≡ mass of dissolved substance /unit mass of fluid

[Cf]
$$C_s = \frac{\Delta m_s}{\Delta vol_f} \quad (\text{mg/}l, ppm)$$





Then, Eq. (3.3) becomes

$$\frac{d\left(\Delta m_f C_M\right)}{dt} \frac{1}{\Delta x \Delta z} = j_{M_y} = -K \frac{d}{dy} \left[\frac{\Delta m_f C_M}{\Delta vol} \right]$$
(3.11)

 $j_{\it M}=$ time rate or mass transfer per unit area normal to the direction of transport $\,$ kg/m $^2\cdot$ s

If
$$\rho = \frac{\Delta m}{\Delta vol} = \text{const.} = \frac{\Delta m_f}{\Delta vol_f}$$

$$j_{M_y} = -\rho K \frac{dC_M}{dv}$$
(3.12)





$$= -K \frac{dC_M \cdot \rho}{dy} = -K \frac{d\left(\frac{\Delta m_s}{\Delta m_f} \cdot \frac{\Delta m_f}{\Delta vol_f}\right)}{dy} = -K \frac{d\left(\frac{\Delta m_s}{\Delta vol_f}\right)}{dy} = -K \frac{dC_s}{dy}$$

Set $K = D = \text{molecular diffusion coefficient } (\text{m}^2/\text{sec})$

$$j_{M_y} = -\rho K \frac{dC_M}{dy} = -D \frac{dC_s}{dy}$$

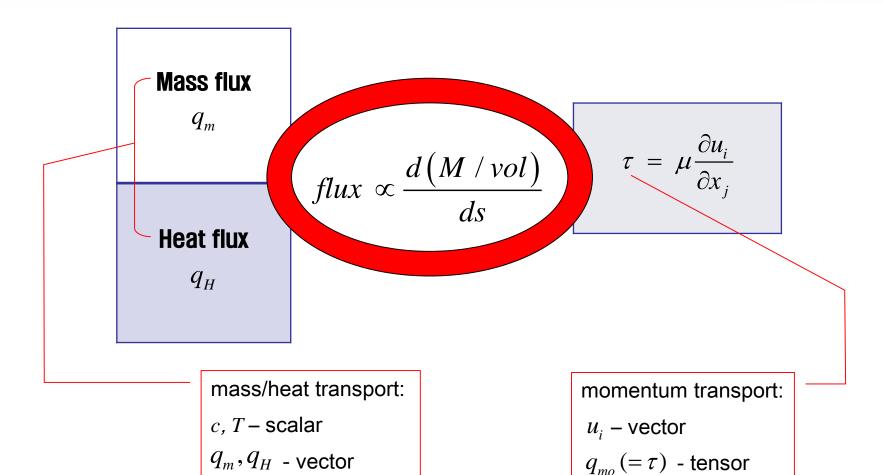




Flux	Driving force	Law	Relation
Mass flux $q_{\scriptscriptstyle m}$	Concentration gradient $\frac{\partial c}{\partial x_j}$	Fick's law	$q_m = -D\frac{\partial c}{\partial x_j} = -D\nabla c$
Heat flux $q_{\scriptscriptstyle H}$	Temperature gradient $\frac{\partial T}{\partial x_j}$	Fourier's law	$q_{H} = -k \frac{\partial T}{\partial x_{j}} = -k \nabla T$
Momentum Flux, ${\it q}_{\it mo}$	Velocity gradient $\frac{\partial u_i}{\partial x_j}$	Newton's law	$\tau = \mu \frac{\partial u_i}{\partial x_j}$











Transport process	Kinematic fluid property (m^2/s)
Momentum	u (kinematic viscosity)
Heat	lpha (thermal diffusivity)
Mass	D (diffusion coefficient)





3.3 Mass Transport

All fluid motions must satisfy the principle of conservation of matter.

- homogeneous fluid — single phase
- non-homogeneous fluid — multi-phase: air-liquid, liquid-solid
- multi-species: fresh water - salt water

Continuity equation: relation for temporal and spatial variation of velocity and density

$$\frac{\partial \rho}{\partial t} + \nabla \cdot (\rho \vec{q}) = 0$$





Mass Transport

Homogeneous fluid	Non-homogenous fluid	
single phase	multi phase	
single species	single phase & multi species	
Continuity Equation [Ch. 4]	mass transport due to local velocity + mass transport due to diffusion → Advection-Diffusion Equation [Advanced Environmental Hydraulics I] [Ch. 16]	

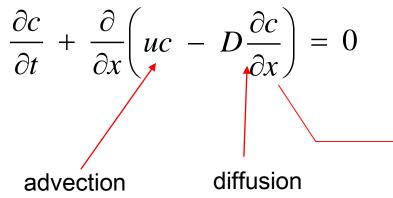


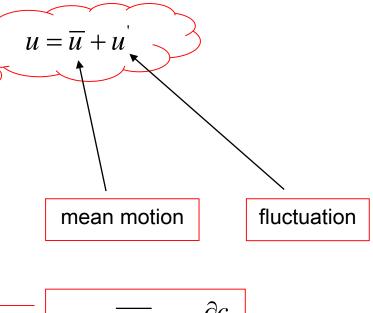


Mass Transport

Advection-Diffusion Equation

= mass conservation + Fick's law





$$q_d = \overline{u'c'} = D \frac{\partial c}{\partial x}$$





thermodynamics ~ <u>non-flow processes</u>

equilibrium states of matter

fluid dynamics ~ <u>transport of heat (scalar) by fluid motion</u>

- Apply conservation of energy to flow process (= 1st law of thermodynamics)
- ~ relation between pressure, density, temperature, velocity, elevation, mechanical work, and heat input (or output).
- ~ since <u>heat capacity of fluid</u> is large compared to its kinetic energy, <u>temperature and density remain constant</u> even though large amounts of kinetic energy are dissipated by friction.
- → simplified energy equation

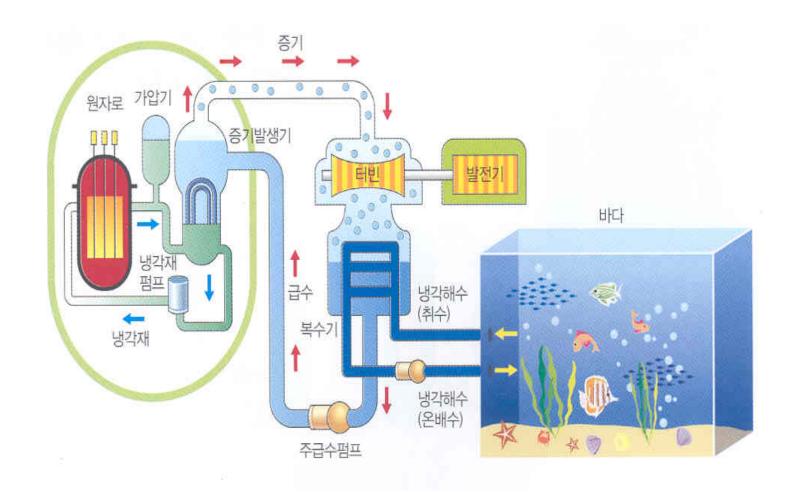




- Heat transfer in flow process
 - 1) convection: due to velocity of the flow → advection
 - 2) conduction: analogous to diffusion, tendency for heat to move in the direction of decreasing temperature
- Application
 - 1) Fluid machine (compressors, pumps, turbines): energy transfer in flow processes
 - 2) Heat pollution: discharge of heated water for nuclear power plant discharge of cooled water for LNG plant

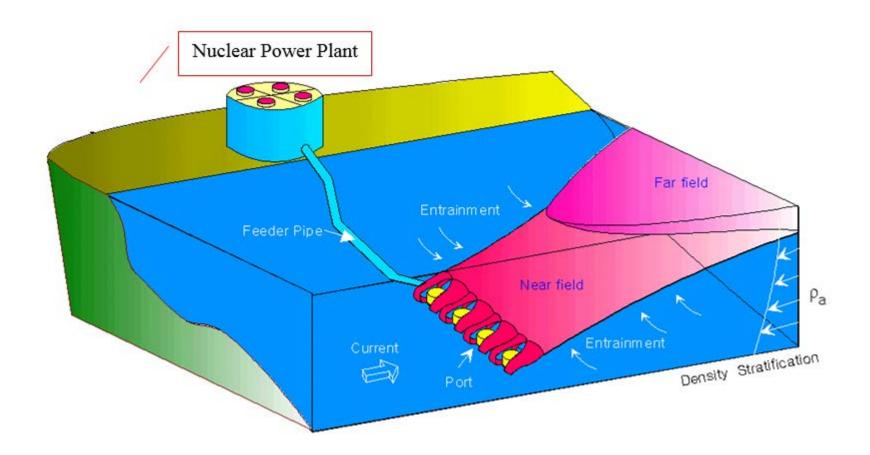






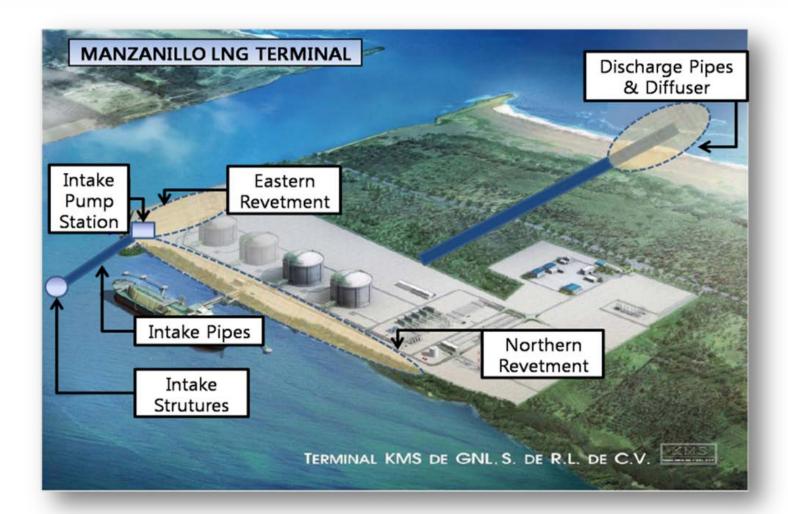
















Momentum transport phenomena

~ encompass the mechanisms of <u>fluid resistance</u>, boundary and internal <u>shear stresses</u>, and propulsion and forces on immersed bodies.

Momentum = mass · velocity vector =
$$\vec{mu}$$

Adopt Newton's 2nd law
$$\sum \vec{F} = m\vec{a} = m\frac{d\vec{u}}{dt} = \frac{d}{dt}(m\vec{u})$$
(3.2)

→ Equation of motion





- Effect of velocity gradient $\frac{\partial u}{\partial y}$
- macroscopic fluid velocity tends to <u>become uniform due to the random</u> <u>motion of molecule</u>s because of intermolecular collisions and the consequent <u>exchange of molecular momentum</u>
- → the velocity distribution tends toward the dashed line
- → momentum flux is equivalent to the existence of the shear stress

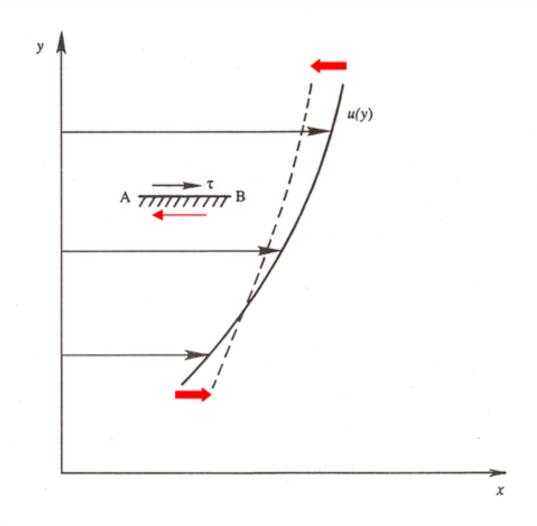
$$\tau \propto \frac{\partial u}{\partial y}$$

$$\tau = \mu \frac{\partial u}{\partial v}$$

→ Newton's law of friction











Momentum transport for Couette flow

Couette flow – laminar flow between two plates

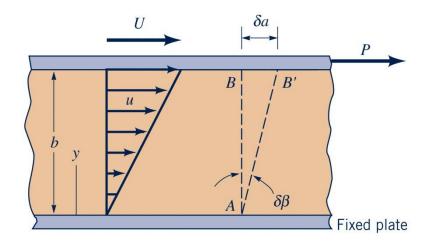
transverse transport of longitudinal momentum (mv)

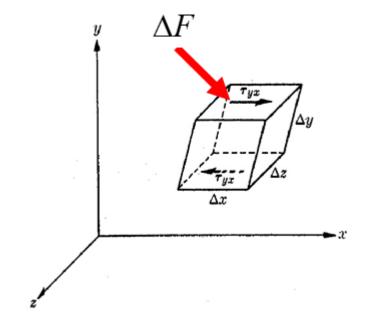
 ∞ transverse gradient of longitudinal velocity $\left(\frac{dv}{dy}\right)$

in the direction of decreasing velocity (longitudinal momentum)













velocity gradient of Couette flow - linear

$$\frac{dv}{dy} = \frac{U}{b}$$

$$\tau = \mu \frac{U}{b}$$

$$\beta a$$

$$\beta a$$

$$\delta a$$

$$\delta a$$

$$\delta A$$

$$\delta \beta$$
Fixed plate

(b)

(a)





Homework Assignment No. 3

 Derive an one-dimensional advection-diffusion equation given below by <u>combining the conservation of mass and</u> <u>Fick's law</u> for molecular diffusion.

$$\frac{\partial c}{\partial t} + \frac{\partial}{\partial x} \left(uc - D \frac{\partial c}{\partial x} \right) = 0$$



