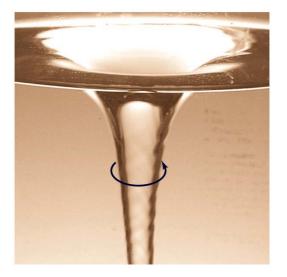
Chapter 6 Equations of Continuity and Motion

Session 6-3 Motions of viscous and inviscid fluids







Contents

- 6.1 Continuity Equation
- 6.2 Stream Function in 2-D, Incompressible Flows
- 6.3 Rotational and Irrotational Motion
- 6.4 Equations of Motion

6.5 Examples of Laminar Motion

6.6 Irrotational Motion

6.7 Frictionless Flow

6.8 Vortex Motion





- In Ch. 4, 1st law of thermodynamics
- → <u>1D Energy eq</u>.
- → Bernoulli eq. for steady flow of an incompressible fluid with zero friction (ideal fluid)
- In Ch. 6,

Newton's 2nd law \rightarrow Momentum eq. \rightarrow Eq. of motion (6.4) \rightarrow Bernoulli eq.

Integration assuming irrotational flow (6.3)

Irrotational flow = Potential flow





6.6.1 Velocity potential and stream function

If $\phi(x, y, z, t)$ is any scalar quantity having continuous first and second derivatives, then by a fundamental vector identity

$$\rightarrow curl(grad \ \phi) \equiv \nabla \times (\nabla \phi) \equiv 0 \tag{6.46}$$

[Detail] vector identity

$$\nabla \phi = grad \ \phi = \frac{\partial \phi}{\partial x}\vec{i} + \frac{\partial \phi}{\partial y}\vec{j} + \frac{\partial \phi}{\partial z}\vec{k}$$





$$curl(grad \phi) = \begin{vmatrix} \vec{i} & \vec{j} & \vec{k} \\ \frac{\partial}{\partial x} & \frac{\partial}{\partial y} & \frac{\partial}{\partial z} \\ \frac{\partial\phi}{\partial x} & \frac{\partial\phi}{\partial y} & \frac{\partial\phi}{\partial z} \end{vmatrix}$$
$$= \vec{i} \left(\frac{\partial\phi^2}{\partial y \partial z} - \frac{\partial\phi^2}{\partial y \partial z} \right) + \vec{j} \left(\frac{\partial\phi^2}{\partial z \partial x} - \frac{\partial\phi^2}{\partial z \partial x} \right) + \vec{k} \left(\frac{\partial\phi^2}{\partial x \partial y} - \frac{\partial\phi^2}{\partial x \partial y} \right) \Rightarrow 0$$





By the way, for <u>irrotational flow</u> Eq.(6.17): $\nabla \times \vec{q} = 0$

(A)

Thus, from (6.46) and (A), we can say that for <u>irrotational flow</u> there must exist a <u>scalar function</u> ϕ whose gradient is equal to the velocity vector \vec{q} .

$$grad \phi = \vec{q}$$
 (B)

Now, let's define the positive direction of flow is the direction in which ϕ is decreasing, then

$$\vec{q} = -grad \ \phi(x, y, z, t) = -\nabla\phi \tag{6.47}$$



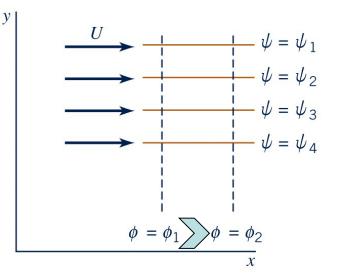


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where ϕ = velocity potential

$$u = -\frac{\partial \phi}{\partial x}, \ v = -\frac{\partial \phi}{\partial y}, \ w = -\frac{\partial \phi}{\partial z}$$

- → Velocity potential exists only for
 irrotational flows; however stream function
 is not subject to this restriction.
- \rightarrow irrotational flow = potential flow for both compressible and incompressible fluids







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(1) Continuity equation for <u>incompressible</u> fluid Eq. (6.5): $\nabla \cdot \vec{q} = 0$

Substitute (6.47) into (C)

$$\therefore \nabla \cdot (-\nabla \phi) = -\nabla^2 \phi = 0 \quad \rightarrow \text{Laplace Eq.}$$
(6.48)

$$\nabla^2 \phi = \frac{\partial^2 \phi}{\partial x^2} + \frac{\partial^2 \phi}{\partial y^2} + \frac{\partial^2 \phi}{\partial z^2} = 0 \quad \leftarrow \text{Cartesian coordinates}$$
(6.49)

$$\nabla^2 \phi = \frac{1}{r} \frac{\partial}{\partial r} \left(r \frac{\partial \phi}{\partial r} \right) + \frac{1}{r^2} \frac{\partial^2 \phi}{\partial \theta^2} + \frac{\partial^2 \phi}{\partial z^2} = 0 \quad \leftarrow \text{ Cylindrical coordinates} \quad (6.50)$$





(C)

[Detail] velocity potential in cylindrical coordinates

$$v_r = -\frac{\partial \phi}{\partial r}, \ v_{\theta} = -\frac{\partial \phi}{r \partial \theta}, \ v_z = -\frac{\partial \phi}{\partial z}$$

(2) For 2-D incompressible irrotational motion

Velocity potential

$$u = -\frac{\partial \phi}{\partial x}$$
$$v = -\frac{\partial \phi}{\partial y}$$

(6.51)



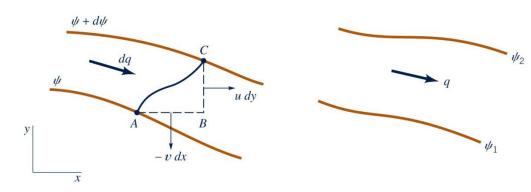


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6.6 Irrotational Motion

• Stream function: Eq. (6.8)

 $u = -\frac{\partial \psi}{\partial y}$ $v = \frac{\partial \psi}{\partial x}$ (6.52)



$$\left. \begin{array}{c} \frac{\partial \psi}{\partial y} = \frac{\partial \phi}{\partial x} \\ \therefore \\ \frac{\partial \psi}{\partial x} = -\frac{\partial \phi}{\partial y} \end{array} \right\} \rightarrow \text{Cauchy-Riemann equation} \quad (6.53)$$





Now, substitute stream function, (6.8) into irrotational flow, (6.17)

Eq. (6.17):
$$\frac{\partial u}{\partial y} = \frac{\partial v}{\partial x} \leftarrow [rotation = 0 \quad \nabla \times \vec{q} = 0]$$

 $\therefore -\frac{\partial^2 \psi}{\partial y^2} = \frac{\partial^2 \psi}{\partial x^2} \rightarrow \frac{\partial^2 \psi}{\partial x^2} + \frac{\partial^2 \psi}{\partial y^2} = 0 \rightarrow \text{Laplace eq.}$ (D)

Also, for 2-D incompressible flow, velocity potential satisfies the Laplace eq.

$$\frac{\partial^2 \phi}{\partial x^2} + \frac{\partial^2 \phi}{\partial y^2} = 0 \tag{E}$$





→ Both ϕ and ψ satisfy the Laplace eq. for 2-D <u>incompressible</u> <u>irrotational motion</u>.

- $\rightarrow \phi$ and ψ may be <u>interchanged</u>.
- \rightarrow Lines of constant ϕ and ψ must form an orthogonal mesh system
- \rightarrow Flow net
- Flow net analysis

Along a streamline, $\psi = \text{constant}$.

Eq. for a streamline, Eq. (2.10)

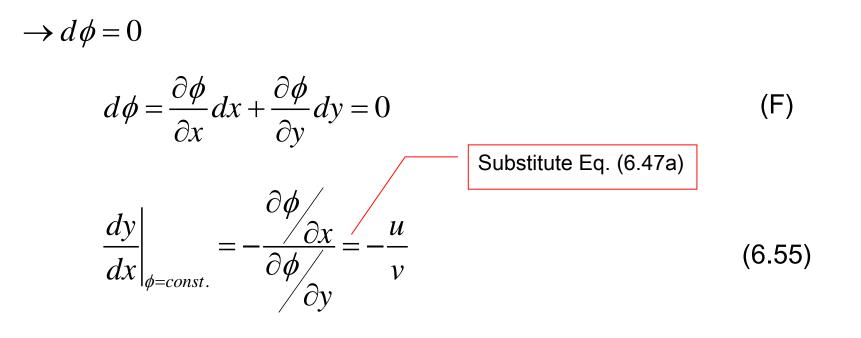
$$\left. \frac{dy}{dx} \right|_{\psi = const.} = \frac{v}{u}$$

(6.54)





BTW along lines of constant velocity potential

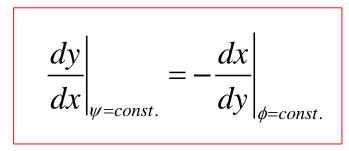






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From Eqs. (6.54) and (6.55)

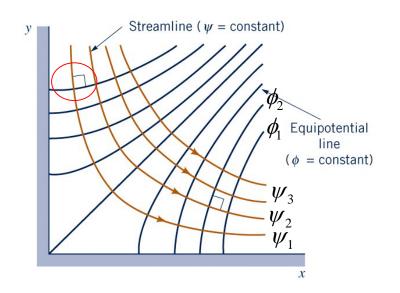


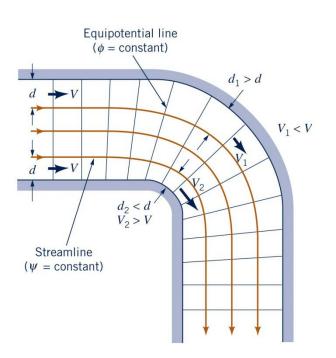


- \rightarrow Slopes are the <u>negative reciprocal</u> of each other.
- \rightarrow Flow net analysis (graphical method) can be used when a solution of the Laplace equation is difficult for complex boundaries.









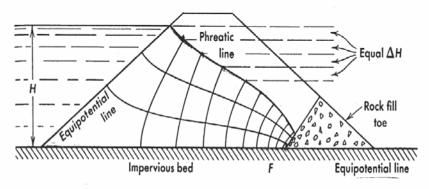


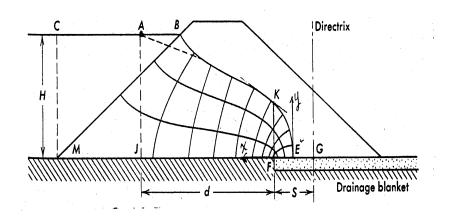


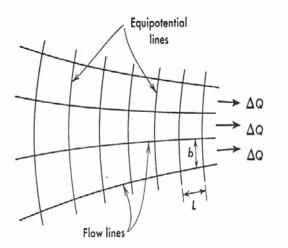
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6.6 Irrotational Motion

Seepage of earth dam







$$Q = \sum \Delta Q = n_f K \Delta H = \frac{n_f}{n_d} K H$$

 n_f = number of flowlines;

- n_d = number of equipotential lines;
- K = permeability coefficient (m/s)

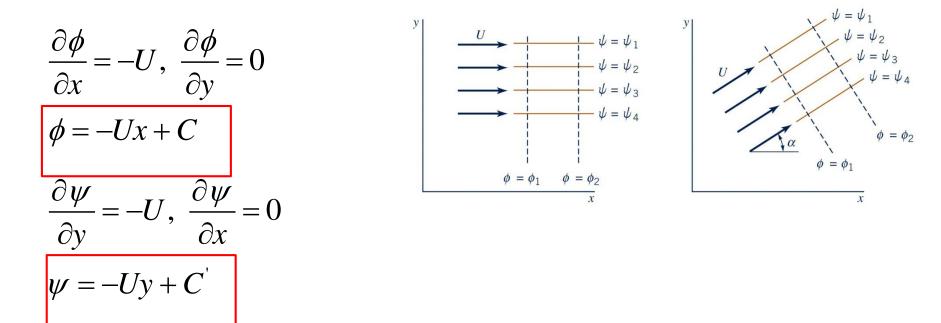




Potential flows

1. Uniform flow

 \rightarrow streamlines are all straight and parallel, and the magnitude of the velocity is constant







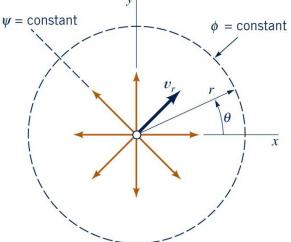
- 2. Source and Sink
- Fluid <u>flowing radially outward</u> from a line through the origin perpendicular to the *x-y* plane
- Let *m* be the volume rate of flow emanating from the line (per unit length)

$$(2\pi r)v_r = m$$

$$v_r = \frac{m}{2\pi r}$$

The streamlines are radial lines,

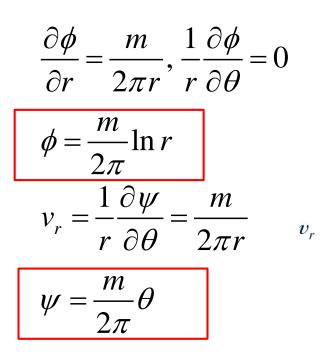
and equipotential lines are concentric circles.

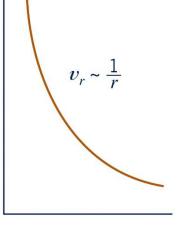




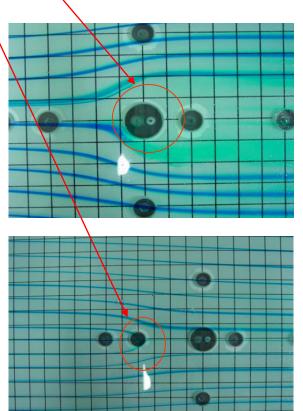


If *m* is positive, the flow is radially outward \rightarrow source If *m* is negative, the flow is radially inward \rightarrow sink





r







3. Vortex (Sec. 6.8)

Flow field in which the streamlines are concentric circles

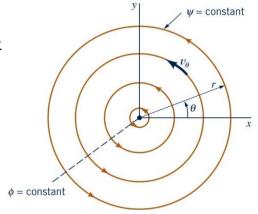
In cylindrical coordinate

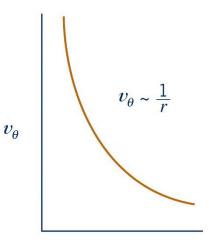
$$\phi = K\theta$$

$$\psi = -K\ln r$$

$$v_{\theta} = \frac{1}{r} \frac{\partial \phi}{\partial \theta} = -\frac{\partial \psi}{\partial r} = \frac{K}{r}$$

The tangential velocity <u>varies inversely with</u> <u>distance</u> from the origin. \rightarrow <u>free vortex</u>

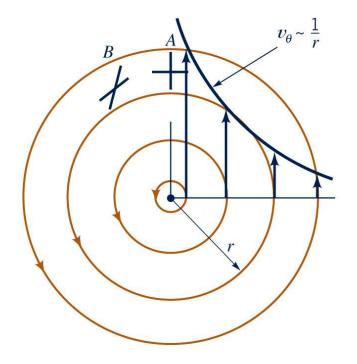




r



X



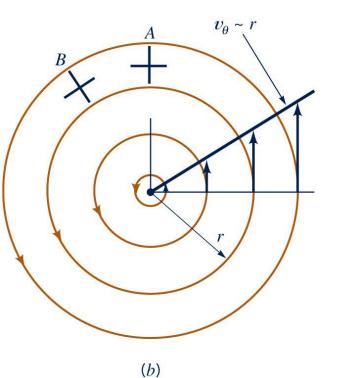
(*a*)

Free vortex → irrotational flow

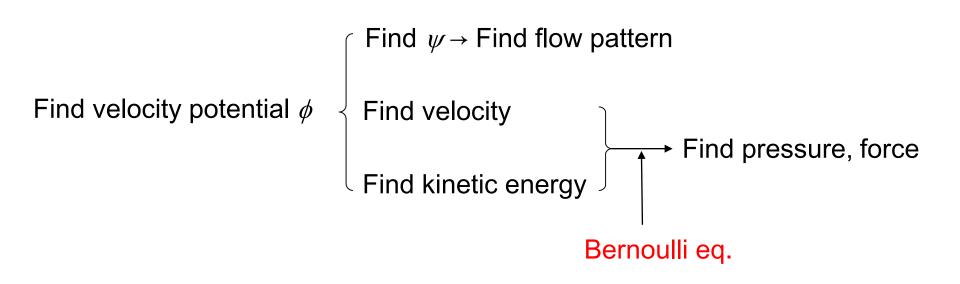
Forced vortex \rightarrow rotational flow







[Appendix II] Potential flow problem







6.6.2 The Bernoulli equation for irrotational incompressible fluids

(1) Find the solution of N-S equation for <u>irrotational incompressible</u> fluids Substitute Eq. (6.17) into Eq. (6.28)

Eq. (6.17) :
$$\nabla \times \vec{q} = 0$$

$$\frac{\partial w}{\partial y} = \frac{\partial v}{\partial z}$$

$$\frac{\partial u}{\partial z} = \frac{\partial w}{\partial x}$$

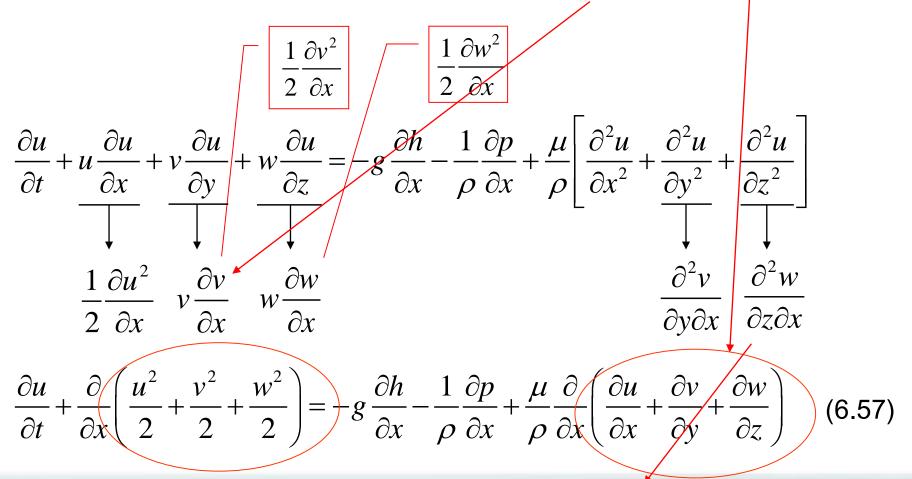
$$\frac{\partial v}{\partial x} = \frac{\partial u}{\partial y}$$

irrotational flow





Eq. (6.28): Navier-Stokes eq. (x-comp.) for irrotational incompressible fluid







Substitute $q^2 = u^2 + v^2 + w^2$ and <u>continuity eq. for incompressible fluid into</u> Eq. (6.57) Continuity eq., Eq. (6.5): $\nabla \cdot \vec{a} = \frac{\partial u}{\partial u} + \frac{\partial u}{\partial u} = 0$

Continuity eq., Eq. (6.5):
$$\nabla \cdot \vec{q} = \frac{\partial u}{\partial x} + \frac{\partial u}{\partial y} + \frac{\partial u}{\partial z} = 0$$

Then, viscous force term can be dropped.

$$\frac{\partial u}{\partial t} + \frac{\partial}{\partial x} \left(\frac{q^2}{2} \right) = -g \frac{\partial h}{\partial x} - \frac{1}{\rho} \frac{\partial p}{\partial x} \rightarrow x - \text{Eq.}$$
$$\frac{\partial u}{\partial t} + \frac{\partial}{\partial x} \left[\frac{q^2}{2} + gh + \frac{p}{\rho} \right] = 0$$





$$y - Eq. \quad \frac{\partial v}{\partial t} + \frac{\partial}{\partial y} \left[\frac{q^2}{2} + gh + \frac{p}{\rho} \right] = 0$$

$$z - Eq. \quad \frac{\partial w}{\partial t} + \frac{\partial}{\partial z} \left[\frac{q^2}{2} + gh + \frac{p}{\rho} \right] = 0$$
(6.58)
(6.59)

Introduce velocity potential ϕ

$$u = -\frac{\partial \phi}{\partial x}, v = -\frac{\partial \phi}{\partial y}, w = -\frac{\partial \phi}{\partial z}$$

$$\frac{\partial u}{\partial t} = -\frac{\partial^2 \phi}{\partial t \partial x}, \quad \frac{\partial v}{\partial t} = -\frac{\partial^2 \phi}{\partial t \partial y}, \quad \frac{\partial w}{\partial t} = -\frac{\partial^2 \phi}{\partial t \partial z}$$
(A)





Substituting (A) into (6.59) yields

$$\frac{\partial}{\partial x} \left[-\frac{\partial \phi}{\partial t} + \frac{q^2}{2} + gh + \frac{p}{\rho} \right] = 0 \qquad x - Eq.$$
$$\frac{\partial}{\partial y} \left[-\frac{\partial \phi}{\partial t} + \frac{q^2}{2} + gh + \frac{p}{\rho} \right] = 0 \qquad y - Eq.$$

$$\frac{\partial}{\partial z} \left[-\frac{\partial \phi}{\partial t} + \frac{q^2}{2} + gh + \frac{p}{\rho} \right] = 0$$

$$z - Eq.$$
 (B)





-

Integrating (B) leads to Bernoulli eq.

$$-\frac{\partial\phi}{\partial t} + \frac{q^2}{2} + gh + \frac{p}{\rho} = F(t)$$
(6.60)

~ valid throughout the entire field of irrotational motion

For a steady flow;
$$\frac{\partial \phi}{\partial t} = 0$$
; $F(t) = C$

$$\frac{q^2}{2} + gh + \frac{p}{\rho} = const.$$

(6.61)

→ Bernoulli eq. for a steady, irrotational flow of an incompressible fluid

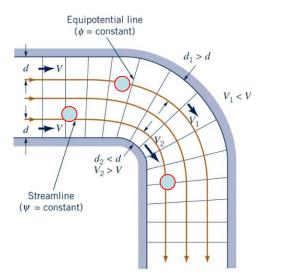




Dividing (6.61) by g (acceleration of gravity) gives the <u>head</u> terms

$$\frac{q^{2}}{2g} + h + \frac{p}{\gamma} = const.$$

$$\frac{q_{1}^{2}}{2g} + h_{1} + \frac{p_{1}}{\gamma} = \frac{q_{2}^{2}}{2g} + h_{2} + \frac{p_{2}}{\gamma} = H \qquad (6.62)$$



H = total head at a point; constant <u>for entire flow field</u> of <u>irrotational motion</u>

(for both along and normal to any streamline)

 \rightarrow point form of 1- D Bernoulli Eq.

p, *H*, *q* = values at particular point \rightarrow point values in flow field





[Cf] Eq. (4.26)

$$\frac{p_1}{\gamma} + h_1 + \frac{V_1^2}{2g} = \frac{p_2}{\gamma} + h_2 + \frac{V_2^2}{2g} = H$$

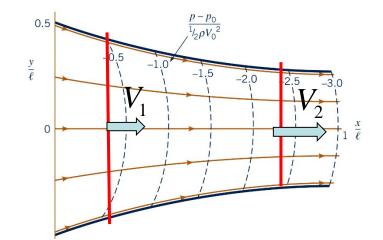
H = constant <u>along a stream tube</u>

 \rightarrow 1-D form of 1-D Bernoulli eq.

p, *h*, *V* = cross-sectional average values at each section \rightarrow <u>average values</u>

- Assumptions made in deriving Eq. (6.62)
- → incompressibility + steadiness + irrotational motion+ constant viscosity (Newtonian fluid)







In Eq. (6.57), viscosity term dropped out because $\nabla \cdot \vec{q} = 0$ (continuity Eq.).

- \rightarrow Thus, Eq. (6.62) can be applied to either a <u>viscous or inviscid fluid</u>.
- Viscous flow

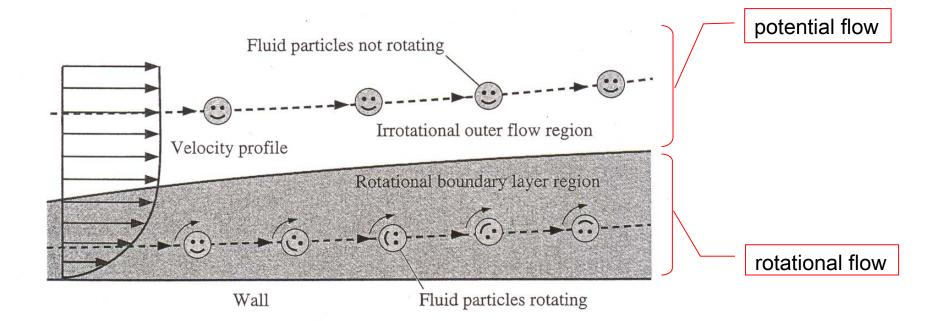
Velocity gradients result in viscous shear.

- \rightarrow Viscosity causes a <u>spread of vorticity</u> (forced vortex).
- \rightarrow Flow becomes rotational.
- \rightarrow H in Eq. (6.62) varies throughout the fluid field.
- \rightarrow Irrotational motion takes place only in a few special cases (irrotational vortex).





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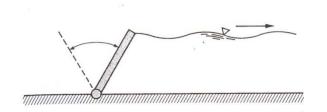


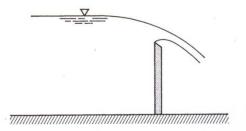
- Boundary layer flow (Ch. 8)
- i) Flow within thin boundary layer viscous flow- rotational flow
- → use boundary layer theory
- ii) Flow outside the boundary layer irrotational (potential) flow
 → use potential flow theory





- Irrotational motion can never become rotational as long as only gravitational and pressure force acts on the fluid particles (without shear forces).
- \rightarrow In real fluids, nearly irrotational flows may be generated if the motion is primarily a result of pressure and gravity forces.
- [Ex] <u>free surface wave</u> motion generated by pressure forces (Fig. 6.8) <u>flow over a weir</u> under gravity forces (Fig. 6.9)









- Vortex motion
- i) Forced vortex rotational flow
- ~ generated by the transmission of tangential
- shear stresses
- \rightarrow rotating cylinder
- ii) Free vortex irrotational flow
- ~ generated by the gravity and pressure
- \rightarrow drain in the tank bottom, tornado, hurricane

