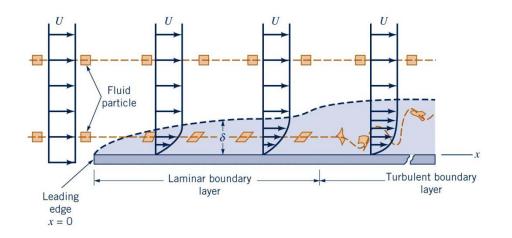
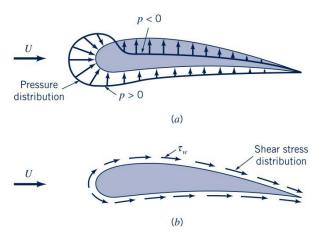


Specialized Equations in Fluid Dynamics









Contents

7.1 Flow Classifications

7.2 Equations for Creeping Motion and 2-D Boundary Layers

7.3 The Notion of Resistance, Drag, and Lift

Objectives

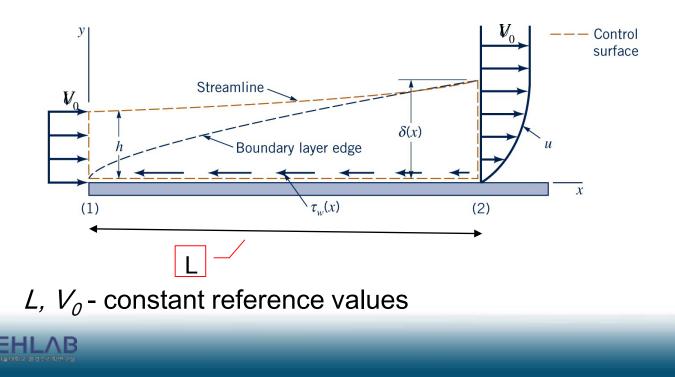
- Discuss special cases of flow motion
- Derive equations for creeping motion
- Derive equation for 2-D boundary layers and integral equation
- Study flow resistance and drag force





7.2.2 Equations for 2-D boundary layers

- (1) Two-dimensional boundary layer equations: Prandtl
- → simplification of the N-S Eq. using order-of-magnitude arguments
- → <u>2D dimensionless N-S eq</u>. for incompressible fluid (omit gravity)





Within thin and small curvature boundary layer

$$u \gg v, \qquad x \gg y$$
$$\frac{\partial u}{\partial y} \gg \frac{\partial u}{\partial x}$$
$$\frac{\partial p}{\partial y} \text{ is small} \sim may \text{ be neglected}$$

dimensionless boundary-layer thickness δ°

$$\delta^{\circ} = \frac{\delta}{L} \to \delta^{\circ} \ll 1$$

 \therefore scale for decreasing order

$$\frac{1}{\delta^{\circ^2}} > \frac{1}{\delta^{\circ}} > 1 > \delta^{\circ} > \delta^{\circ^2}$$





Order of magnitude

| | r |
|--|------------------------------------|
| $x^{\circ} \sim O(1)$ | $x^{\circ} = \frac{x}{L}$ |
| $y^{\circ} \sim O(\delta^{\circ})$ | $y^{\circ} = \frac{y}{L}$ |
| $u^{\circ} \sim O(1)$ | $u^{\circ} = \frac{u}{V_0}$ |
| $v^{\circ} \sim O(\delta^{\circ})$ | V_0 |
| $\frac{\partial u^{\circ}}{\partial x^{\circ}} \sim O(1)$ | $v^{\circ} = \frac{v}{V_0}$ |
| $\frac{\partial v^{\circ}}{\partial y^{\circ}} \sim O(1) \leftarrow continuity\left(\frac{\partial v^{\circ}}{\partial y^{\circ}} = -\frac{\partial u^{\circ}}{\partial x^{\circ}}\right)$ | $p^{\circ} = \frac{p}{\rho V_0^2}$ |
| $\frac{\partial u^{\circ}}{\partial y^{\circ}} \sim O\left(\frac{1}{\delta^{\circ}}\right)$ | |
| $\frac{\partial v^{\circ}}{\partial x^{\circ}} \sim O\left(\delta^{\circ}\right)$ | |





$$\frac{\partial^2 u^{\circ}}{\partial (x^{\circ})^2} = \frac{\partial}{\partial x^{\circ}} \left(\frac{\partial u^{\circ}}{\partial x^{\circ}} \right) \sim O(1)$$

$$\frac{\partial^2 v^{\circ}}{\partial (y^{\circ})^2} = \frac{\partial}{\partial y^{\circ}} \left(\frac{\partial v^{\circ}}{\partial y^{\circ}} \right) \sim O(\frac{1}{\delta^{\circ}})$$

$$\frac{\partial u^{\circ}}{\partial t^{\circ}} = \frac{\partial u^{\circ}}{\partial x^{\circ}} \frac{\partial x^{\circ}}{\partial t^{\circ}} = u^{\circ} \frac{\partial u^{\circ}}{\partial x^{\circ}} \sim O(1)$$

$$\frac{\partial v^{\circ}}{\partial t^{\circ}} = \frac{\partial v^{\circ}}{\partial x^{\circ}} \frac{\partial x^{\circ}}{\partial t^{\circ}} = u^{\circ} \frac{\partial v^{\circ}}{\partial x^{\circ}} \sim O(\delta^{\circ})$$

$$\operatorname{Re} = \frac{\rho v y}{\mu} \sim O(\delta^{\circ^2})$$





$$x:\frac{\partial u^{\circ}}{\partial t^{\circ}} + u^{\circ}\frac{\partial u^{\circ}}{\partial x^{\circ}} + v^{\circ}\frac{\partial u^{\circ}}{\partial y^{\circ}} = -\frac{\partial p^{\circ}}{\partial x^{\circ}} + \frac{1}{\operatorname{Re}}\left(\frac{\partial^{2}u^{\circ}}{\partial x^{\circ^{2}}} + \frac{\partial^{2}u^{\circ}}{\partial y^{\circ^{2}}}\right)$$
(7.3)
$$1 \quad 1 \times 1 \quad \delta^{\circ} \times 1/\delta^{\circ} \qquad \delta^{\circ^{2}}(1+1/\delta^{\circ^{2}}) \to 1$$

$$y:\frac{\partial v^{\circ}}{\partial t^{\circ}} + u^{\circ}\frac{\partial v^{\circ}}{\partial x^{\circ}} + v^{\circ}\frac{\partial v^{\circ}}{\partial y^{\circ}} = -\frac{\partial p^{\circ}}{\partial y^{\circ}} + \frac{1}{\operatorname{Re}}\left(\frac{\partial^{2} v^{\circ}}{\partial x^{\circ^{2}}} + \frac{\partial^{2} v^{\circ}}{\partial y^{\circ^{2}}}\right)$$
$$\delta^{\circ} \quad 1 \times \delta^{\circ} \quad \delta^{\circ} \times 1 \qquad \delta^{\circ^{2}}(\delta^{\circ} + 1/\delta^{\circ}) \rightarrow \delta^{\circ}$$

Continuity:
$$\frac{\partial u^{\circ}}{\partial x^{\circ}} + \frac{\partial v^{\circ}}{\partial y^{\circ}} = 0$$

1 1





Therefore, eliminate all terms of order less than unity in Eq. (7.3) and revert to dimensional terms

$$\frac{\partial u}{\partial t} + u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} = -\frac{1}{\rho} \frac{\partial p}{\partial x} + \frac{\mu}{\rho} \frac{\partial^2 u}{\partial y^2}$$

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0$$
(7.7)

→ <u>Prandtl's 2-D boundary-layer equation</u>

BC: 1)
$$y = 0$$
; $u = 0, v = 0$

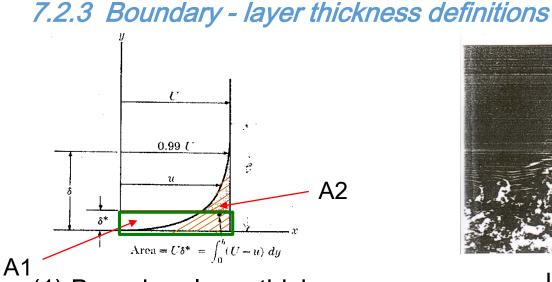
2)
$$y = \infty$$
; $u = U(x)$

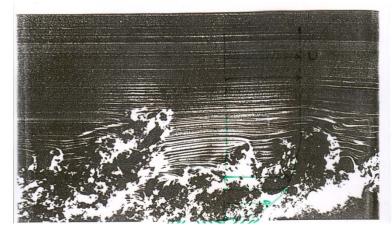
(7.8)

Unknowns: *u*, *v*, *p*; Eqs. = $2 \rightarrow$ needs assumptions for p









(1) Boundary-layer thickness,

Intermittent nature

- ~ The point separating the boundary layer from the <u>zone of negligible</u> <u>viscous influence</u> is not a sharp one. \rightarrow very intermittent
 - δ = distance to the point where the velocity is within 1% of the freestream velocity, U

$$@ y = \delta \rightarrow u_{\delta} = 0.99U$$



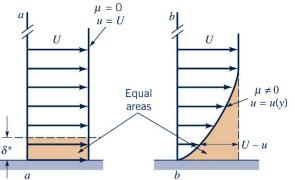
- (2) Mass displacement thickness, $\delta^*(\delta_l)$
- ~ is the thickness of an <u>imaginary</u> layer of fluid of velocity U.
- ~ is the thickness of mass flux rate equal to the amount of defect

$$A_1 = A_2$$

$$\rho U \delta^* = \frac{\rho \int_0^h (U - u) dy}{mass \ defect} \qquad h \ge \delta$$

$$\therefore \delta^* = \int_0^h (1 - \frac{u}{U}) dy \qquad (7.9)$$

$$y$$
 $u = 0.99 U$
 U U δ







[Re] mass flux = mass/time

$$= \rho Q = \rho U A = \rho U \delta^* \times 1$$

(3) Momentum thickness, $\theta(\delta_2)$

→ Velocity retardation within δ causes a <u>reduction in the rate of</u> <u>momentum flux</u>.

→ θ is the thickness of an imaginary layer of fluid of velocity U for which the <u>momentum flux rate</u> equals the reduction caused by the velocity profile.

$$\rho\theta U^2 = \rho \int_0^h (U-u)u dy = \rho \int_0^h (Uu-u^2) dy$$

$$\therefore \theta = \int_0^h \frac{u}{U} (1 - \frac{u}{U}) dy$$





[Re] momentum in θ = mass × velocity = $\rho \theta U \times U = \rho \theta U^2$

momentum in shaded area = $\int [\rho(U-u) \times u] dy$

 $\delta > \delta^* > \theta$

(4) Energy thickness, δ_3

$$\frac{1}{2}\rho U^{3}\delta_{3} = \frac{1}{2}\int_{0}^{h}\rho u(U^{2} - u^{2})dy$$
$$\therefore \delta_{3} = \int_{0}^{h}\frac{u}{U}(1 - \frac{u^{2}}{U^{2}})dy$$





[Re]

1) Batchelor (1985):

displacement thickness = distance through which streamlines just outside the boundary layer are displaced laterally by the <u>retardation</u> <u>of fluid</u> in the boundary layer.

2) Schlichting (1979):

displacement thickness = distance by which the external streamlines are shifted owing to the formation of the boundary layer.

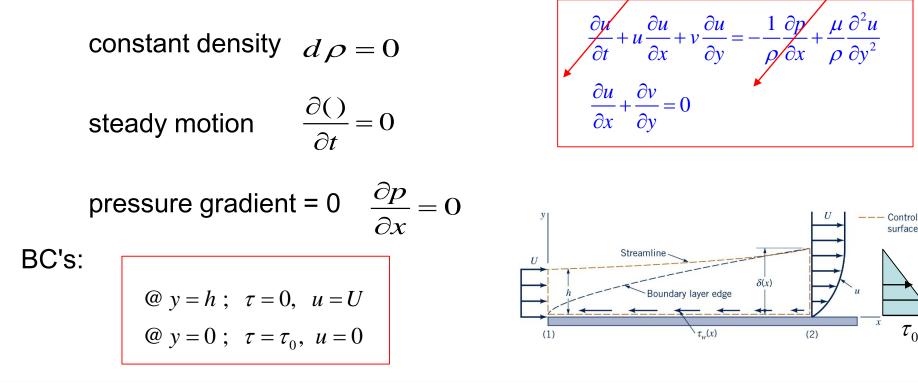




7.2.4 Integral momentum equation for 2-D boundary layers

Integrate Prandtl's 2-D boundary-layer equations

Assumptions:







Prandtl's 2-D boundary-layer equations become as follows:

$$u\frac{\partial u}{\partial x} + v\frac{\partial u}{\partial y} = \frac{\mu}{\rho}\frac{\partial^2 u}{\partial y^2}$$
(A)
$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0$$
(B)

Integrate Eq. (A) w.r.t. y

$$\int_{y=0}^{y=h\geq\delta} \left(\frac{u\frac{\partial u}{\partial x}}{\frac{1}{2}} + \frac{v\frac{\partial u}{\partial y}}{\frac{1}{2}} \right) dy = \frac{\mu}{\rho} \int_{y=0}^{y=h} \frac{\partial^2 u}{\partial y^2} dy$$
(C)
(1) (2) (3)





$$(3) = \mu \int_{0}^{h} \frac{\partial^{2} u}{\partial y^{2}} dy = \int_{0}^{h} \frac{\partial}{\partial y} \left(\mu \frac{\partial u}{\partial y} \right) dy = \int_{0}^{h} \frac{\partial \tau}{\partial y} dy = [\tau]_{0}^{h}$$
$$= \tau |_{y=h} - \tau |_{y=0} = 0 - \tau_{0} = -\tau_{0}$$
$$(2) = \int_{0}^{h} v \frac{\partial u}{\partial y} dy = \int_{0}^{h} \frac{\partial u v}{\partial y} dy + \int_{0}^{h} \frac{\partial v}{\partial y} dy$$
$$(5)$$
[Re] Integration by parts: $\int v u' dy = uv - \int uv' dy$

$$(4) = \int_0^h \frac{\partial uv}{\partial y} dy = [uv]_0^h = Uv_h - 0 = Uv$$





(D)

Continuity Eq.:
$$\frac{\partial v}{\partial y} = -\frac{\partial u}{\partial x}$$

 $\rightarrow v = -\int_0^h \frac{\partial u}{\partial x} dy$

(i)

Substitute (i) into (5)

$$(5) = \int_0^h u \left(-\frac{\partial u}{\partial x} \right) dy = -\int_0^h u \frac{\partial u}{\partial x} dy$$
(ii)

Substitute (i) into ④

$$(4) = Uv = -U \int_0^h \frac{\partial u}{\partial x} dy$$





Eq. (D) becomes

$$\int_{0}^{h} v \frac{\partial u}{\partial y} dy = -U \int_{0}^{h} \frac{\partial u}{\partial x} dy + \int_{0}^{h} u \frac{\partial u}{\partial x} dy$$

Then, (C) becomes

$$\int_{0}^{h} u \frac{\partial u}{\partial x} dy - U \int_{0}^{h} \frac{\partial u}{\partial x} dy + \int_{0}^{h} u \frac{\partial u}{\partial x} dy = -\frac{\tau_{0}}{\rho}$$
(F)

For steady motion with and U = const., (F) becomes

$$\frac{\tau_0}{\rho} = U \int_0^h \frac{\partial u}{\partial x} dy - 2 \int_0^h u \frac{\partial u}{\partial x} dy = \int_0^h \frac{\partial U u}{\partial x} dy - \int_0^h \frac{\partial u^2}{\partial x} dy$$
$$= \int_0^h \frac{\partial}{\partial x} [u(U-u)] dy = \frac{\partial}{\partial x} \int_0^h u(U-u) dy = \frac{\partial}{\partial x} (\theta U^2)$$
$$\theta U^2$$





18/32

(E)

where θ = momentum thickness

$$\frac{\tau_0}{\rho} = \frac{\partial}{\partial x} (U^2 \theta) = U^2 \frac{\partial \theta}{\partial x}$$
$$\frac{\partial \theta}{\partial x} = \frac{\tau_0}{\rho U^2} = \left(\frac{u^*}{U}\right)^2$$

Introduce local surface (frictional) resistance coefficient C_f

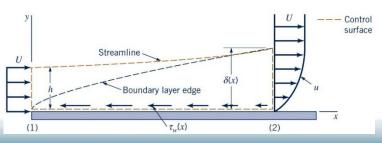
$$C_{f} = \frac{D_{f}}{\frac{\rho}{2}u^{2}A_{f}} = \frac{\tau_{0}}{\frac{\rho}{2}U^{2}}$$

$$D_{f} = \frac{\rho}{2}C_{f}A_{f}u^{2}$$

$$\tau_{0} = \frac{\rho}{2}C_{f}U^{2}$$
(7.19)

Combine (7.18) with (7.19)

$$C_f = 2\frac{\partial\theta}{\partial x} \qquad (7.20)$$





(7.18)

[Re] Integral momentum equation for unsteady motion

→ unsteady motion:
$$\frac{\partial ()}{\partial t} \neq 0$$

→ pressure gradient, $\frac{\partial p}{\partial x} \neq 0$

First, simplify Eq. (7.7) for external flow where viscous influence is negligible. $\partial U = \partial U = \partial U + \frac{1}{2} \partial p + \frac{1}{2} \partial p$

$$\frac{\partial U}{\partial t} + U \frac{\partial U}{\partial x} + v \frac{\partial U}{\partial y} = -\frac{1}{\rho} \frac{\partial p}{\partial x} + \frac{\mu}{\rho} \frac{\partial^2 U}{\partial y^2}$$

$$\rho \frac{\partial U}{\partial t} + \rho U \frac{\partial U}{\partial x} = -\frac{\partial p}{\partial x}$$
(A)





Substitute (A) into (7.7)

$$\frac{\partial u}{\partial t} + u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} = \frac{\partial U}{\partial t} + U \frac{\partial U}{\partial x} + \frac{\mu}{\rho} \frac{\partial^2 u}{\partial y^2}$$
$$-\frac{1}{\rho} \frac{\partial p}{\partial x}$$

$$\int_{0}^{h} \frac{\mu}{\rho} \frac{\partial^{2} u}{\partial y^{2}} dy = \int_{0}^{h} \left\{ \frac{\partial u}{\partial t} - \frac{\partial U}{\partial t} + \frac{u}{\partial x} \frac{\partial u}{\partial x} - U \frac{\partial U}{\partial x} + \frac{u}{\partial y} \right\} dy$$
(B)

$$(1) \qquad (2) \qquad (3) \qquad (4)$$

$$(1): \int_0^h \frac{\mu}{\rho} \frac{\partial^2 u}{\partial y^2} \, dy = -\frac{\tau_0}{\rho}$$

$$(2): \int_0^h \left(\frac{\partial u}{\partial t} - \frac{\partial U}{\partial t}\right) dy = \int_0^h \frac{\partial}{\partial t} (u - U) dy = \frac{\partial}{\partial t} \int_0^h (u - U) dy = -\frac{\partial}{\partial t} U \delta$$

 $-U\delta^*$



Integrate



$$(3) = \frac{\int_{0}^{h} \left(u \frac{\partial u}{\partial x} - u \frac{\partial U}{\partial x} \right) dy}{(3) - 1} dy + \frac{\int \left(u \frac{\partial U}{\partial x} - U \frac{\partial U}{\partial x} \right) dy}{(3) - 2}$$

$$(3-1= \int_0^h \left\{ u \frac{\partial}{\partial x} (u-U) \right\} dy$$

$$(3-2= \int_0^h \left\{ (u-U)\frac{\partial U}{\partial x} \right\} dy = \frac{\partial U}{\partial x} \int_0^h (u-U)dy = \frac{\partial U}{\partial x} (-U\delta^*)$$

$$() = \int_{0}^{h} v \frac{\partial u}{\partial y} dy = -U \int_{0}^{h} \frac{\partial u}{\partial x} dy + \int u \frac{\partial u}{\partial x} dy = \int_{0}^{h} (u - U) \frac{\partial u}{\partial x} dy$$

$$Eq.(E)$$





Combine ③-1 and ④

$$\int_{0}^{h} u \frac{\partial}{\partial x} (u - U) dy + \int_{0}^{h} (u - U) \frac{\partial u}{\partial x} dy = \int_{0}^{h} \left[u \frac{\partial}{\partial x} (u - U) + (u - U) \frac{\partial u}{\partial x} \right] dy$$

$$= \int_{0}^{h} \frac{\partial}{\partial x} \left\{ u(u - U) \right\} dy = \frac{\partial}{\partial x} \int_{0}^{h} u(u - U) dy = \frac{\partial}{\partial x} (-\theta U^{2})$$
Substituting all these into (B) yields

$$-\frac{\tau_0}{\rho} = -\frac{\partial}{\partial t} (U\delta^*) - U\frac{\partial U}{\partial x}\delta^* - \frac{\partial}{\partial x} (\theta U^2)$$
$$\frac{\tau_0}{\rho} = \frac{\partial}{\partial x} (U^2\theta) + U\frac{\partial U}{\partial x}\delta^* + \frac{\partial}{\partial t} (U\delta^*)$$

(7.21)

 \rightarrow Karman's integral momentum eq.

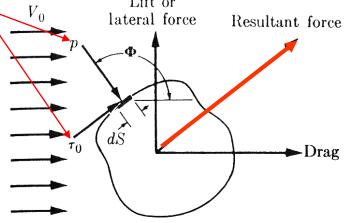




→ Study Ch.15 (D&H)

Resistance to motion = <u>drag of a fluid on an immersed body</u> in the direction of flow

- ◆ Dynamic (surface) force exerted on the rigid boundary by moving fluid are
- 1) Tangential force caused by <u>shear stresses</u> due to <u>viscosity and velocity</u> <u>gradients</u> at the boundary surfaces
- 2) Normal force caused by pressure intensities which vary along the surface due to dynamic effects









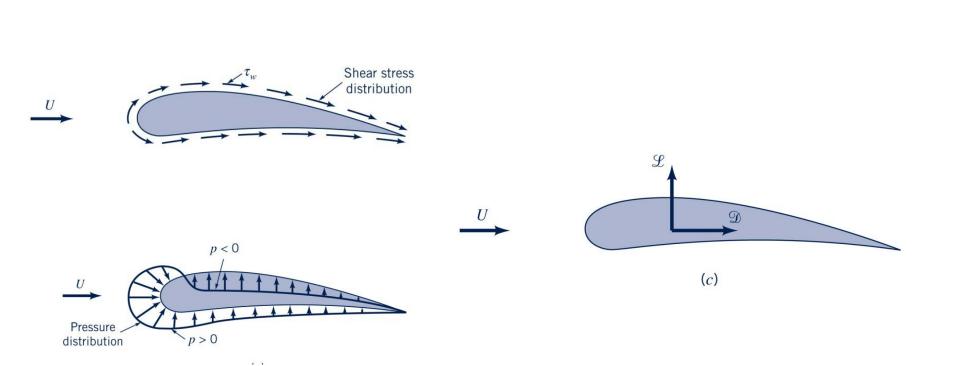
Resultant force = <u>vector sum of the normal and tangential surface</u>

forces integrated over the complete surface

- ~ resultant force is <u>divided into two components</u>:
 - 1) **Drag force** = component of the resultant force in the direction of relative velocity $V_{\underline{0}}$
 - 2) Lift force = component of the resultant force <u>normal to the relative</u> <u>velocity $V_{\underline{0}}$ </u>
- ~ Both drag and lift include frictional and pressure components.





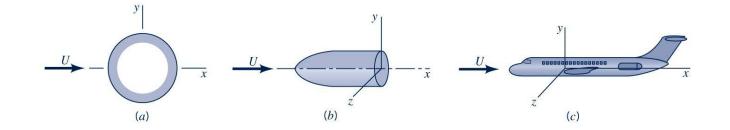






- ① Frictional drag = surface resistance = skin drag
- ② Pressure drag = form drag
- ~ depends largely on shape or form of the body

For airfoil, hydrofoil, and slim ships: surface drag > form drag For bluff objects like spheres, bridge piers: surface drag < form drag

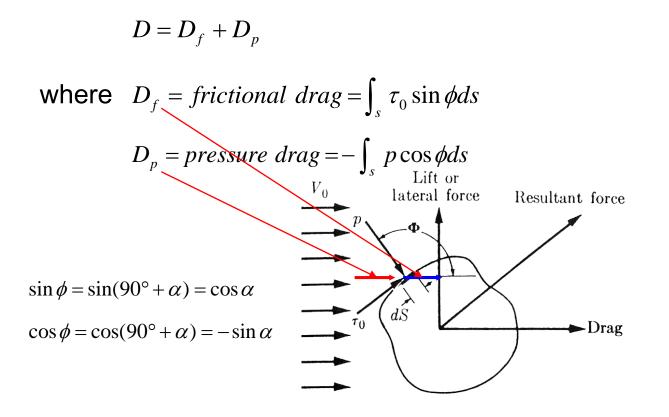






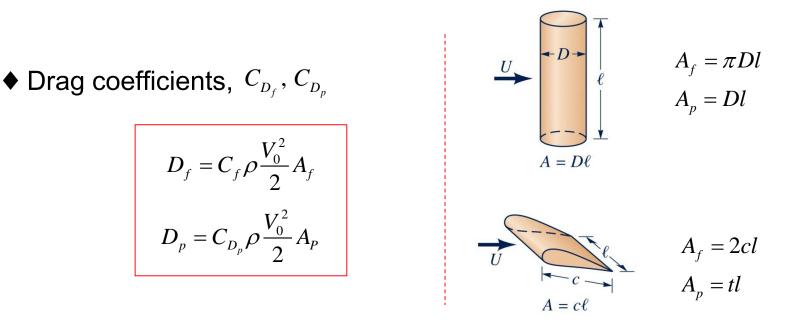
7.3.1 Drag force

♦ Total drag, D









Where $A_f = actual area over which shear stresses act to produce <math>D_f$ $A_p = frontal (projected) area normal to the velocity$





• Total drag coefficient C_D

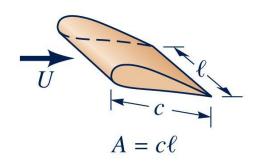
$$D = C_D \rho \frac{V_0^2}{2} A$$

where $A = \text{frontal area normal to } V_O$

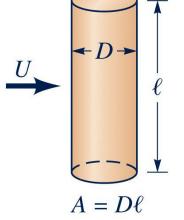
$$C_D = C_{D_f} + C_{D_p}$$
$$C_D = C_D(geometry, \text{Re})$$

[Re] Dimensional Analysis
$$\rightarrow$$
 Ch. 15

$$D = f_1(\rho, \mu, V, L)$$
$$\frac{D}{\rho L^2 V^2} = f_2 \left(\frac{\rho V L}{\mu}\right) = f_2(\text{Re}) = C_D$$
$$\therefore D = C_D \frac{\rho}{2} A V^2$$





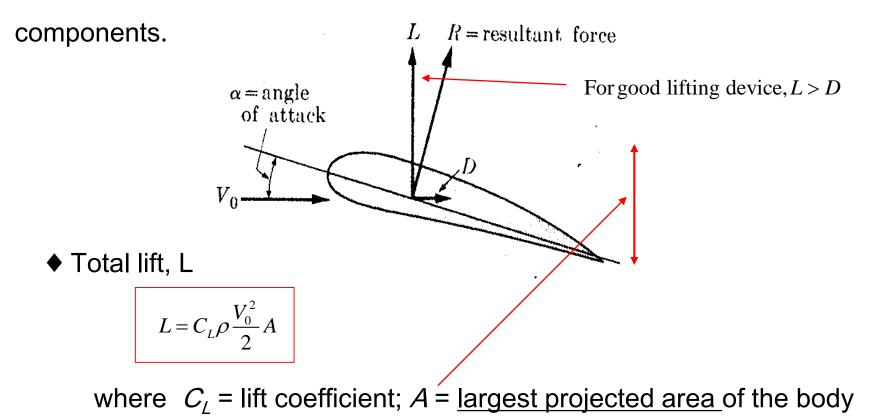


 $Cf = C_{D_f} \left(\frac{A_p}{A_r} \right)$



7.3.1 Lift force

For lift forces, it is not customary to separate the frictional and pressure







32/32

Homework Assignment # 7

Due: 1 week from today

1. Derive the equation of falling velocity of the sediment particle in the still water. Use Stokes law.

 $\downarrow W_s$



