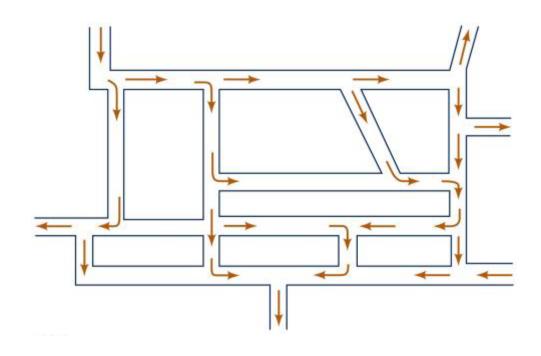


Ch. 5 Pipe Problems 5-2 Multiple pipes





Contents

- 5.4 Multiple Pipes
- 5.5 Three Reservoir Problems
- 5.6 Pipe Networks





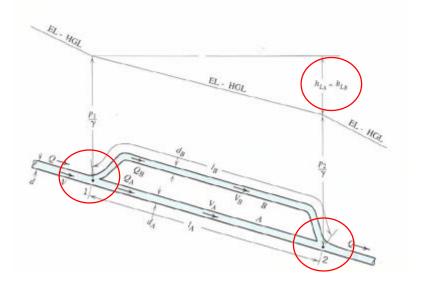
Objectives of class

- Solve problems of multiple pipes
- Learn methods to solve pipe network problems



5.4 Multiple Pipes

- In real world, pipe is not single but connected with others.
- Sometimes, there are connections among hundred pipes.
- Even though there are many pipes, still basic principles are the same.



- Make problem simple, local loss and velocity head are neglected in the Bernoulli eq. with the EL-HGL considered coincident.
- As a consequence, the <u>EL-HGLs of the pipes form a continuous</u> <u>network</u> above the pipes, joining at the <u>pipe junctions</u>.

 \rightarrow The head loss through <u>both branches of the loop must be the same</u>.

 The flowrate in the main pipe is equal to the sum of the flowrates in the branches.→ Continuity equation

$$h_{L_A} = h_{L_B}$$
$$Q = Q_A + Q_B$$

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 $2 \, equations - 4 \, unknowns$

 Head losses are expressed in terms of flowrate through the Darcy-Weisbach equation

$$h_{L} = f \frac{l}{d} \frac{V^{2}}{2g_{n}} = \frac{fl}{2g_{n}d} \frac{16Q^{2}}{\pi^{2}d^{4}} = \left(\frac{16fl}{2\pi^{2}g_{n}d^{5}}\right)Q^{2}$$

This equation may be generalized by writing it as

$$h_L = KQ^n \quad \leftarrow \text{usually n=2}$$



 $h_{L_{\Lambda}}; Q_{L_{\Lambda}}$



The general description of head loss can be plugged in the relationship,

$$K_A Q_A^n = K_B Q_B^n$$
$$Q = Q_A + Q_B$$

2 equations - 2 unknowns

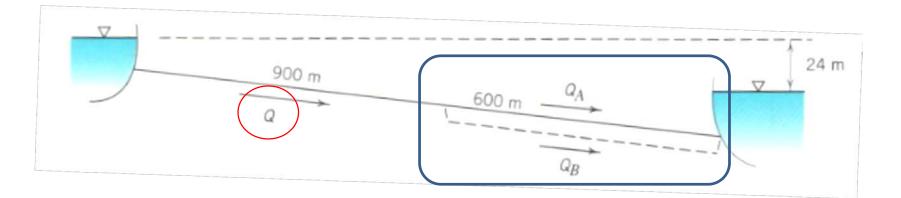
- Solution of these simultaneous equations allows prediction of the division of a flowrate Q into <u>flowrates of two diverged pipes</u>.
- Application of these equations also allows prediction of the increased flowrate obtainable by looping an existing pipeline.





I.P. 9.20 (p. 382)

A 300 mm pipe 1,500 m long is laid between two reservoirs having a difference in surface elevation of 24 m. The maximum flowrate obtainable through this line (with all valves wide open) is 0.15 m³/s. When this pipe is looped with a 600 m pipe of the same size and material laid parallel and connected to it, what percent increase in maximum flowrate may be expected?





Solution:



(I) Before looped; $h_L = KQ^n$

For original 1,500 m line, $K_{1500} = \frac{h_L}{Q_{old}^2} = \frac{24m}{\left(0.15m^3/s\right)^2} = 1,067$

• In equation of $K = \frac{16 fl}{2\pi^2 g_n d^5}$

We may know that <u>*K* is linear with length if the size and</u> material of the pipe are the same, then

$$K_{600} = K_{1500} \frac{600}{1500} = 427 \text{ for looped section}$$
$$K_{900} = K_{1500} \frac{900}{1500} = 640 \text{ for unlooped portion}$$



(II) After looped

24 m

1) For the <u>original pipeline (red pipe)</u>, the head loss in the unlooped (900 m) plus pipe A (600 m)gives

$$h_{L,ori} = 24m = K_{900}Q_{new}^{2} + K_{600}Q_{A}^{2} = 640Q_{new}^{2} + 427Q_{A}^{2}$$
(1)

2) For looped pipe(red+blue), the head loss in the unlooped (900 m) plus the head loss in the pipe B in the looped portion is

$$h_{L,new} = 24m = K_{900}Q_{new}^{2} + K_{600}Q_{B}^{2} = 640Q_{new}^{2} + 427Q_{B}^{2}$$
(2)

- Eliminating Q_{new} shows that $Q_A = Q_B$. Then $Q_A = Q_{new}/2$. From (1) $Q_{new} = 0.18m^3 / s$
- Thus, the gain in capacity is 0.03m³/s.

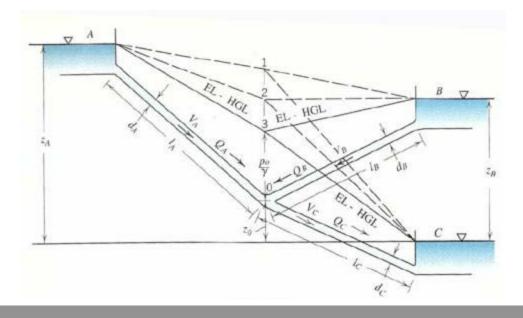
$$\frac{0.03}{0.15} \times 100 = 20\%$$





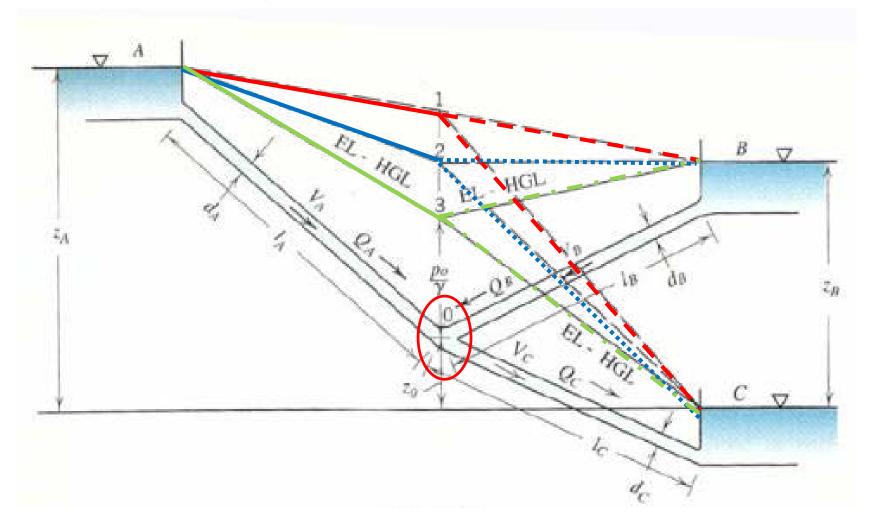
5.5 Three Reservoir Problems

- Three-reservoir problem: Flow may take place
 - 1) From reservoir A to reservoirs <u>B and C</u>
 - 2) From reservoir A to C without inflow or outflow from reservoir B
 - 3) From reservoirs <u>A and B into reservoir C</u>
- Solve by use of the energy line











1) Situation 1: flow may take place from reservoir A to B and C

$$h_{L_{A-B}} = K_A Q_A^2 + K_B Q_B^2$$

$$h_{L_{A-C}} = K_A Q_A^2 + K_C Q_C^2$$

$$z_A - K_A Q_A^n - K_B Q_B^n = z_B$$

$$z_A - K_A Q_A^n - K_C Q_C^n = 0$$

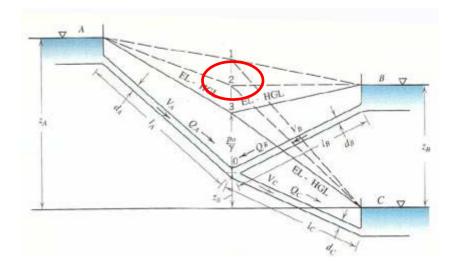
$$Q_A = Q_B + Q_C$$
(since $z_C = 0$)
$$Q_A = Q_B + Q_C$$





2) Situation 2: flow may take place from reservoir A to C without flowing to $B(Q_B=0)$

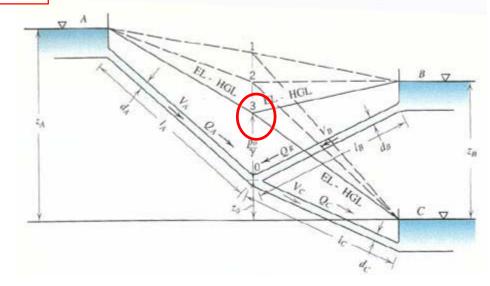
$$z_A - K_A Q_A^n - K_C Q_C^n = 0$$
$$z_A - K_A Q_A^n = z_B$$
$$Q_A = Q_C$$





3) Situation 3: Flow may take place from reservoir A and B to C,

$$z_A - K_A Q_A^n - K_C Q_C^n = 0 \quad (\text{since } z_C = 0)$$
$$z_A - K_A Q_A^n = z_0 = z_B - K_B Q_B^n$$
$$Q_A + Q_B = Q_C$$



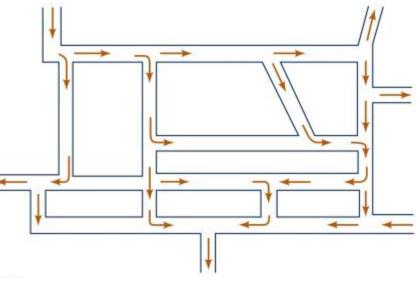




5.6 Pipe Networks

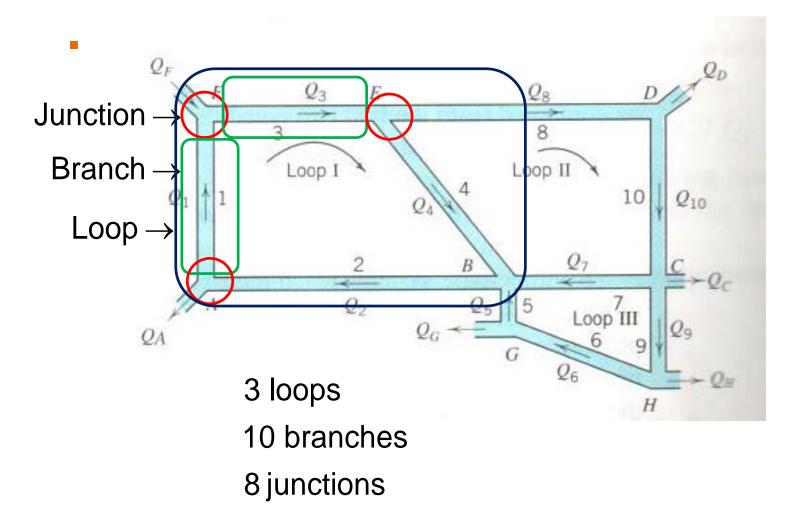
- A pipe network of a water system is the aggregation of connected pipes used to <u>distribute water to users</u> in a specific area, such as a city or subdivision.
- The network consists of pipes of various sizes, geometric orientations, and hydraulic characteristics plus pumps, valves, and fittings and so forth.







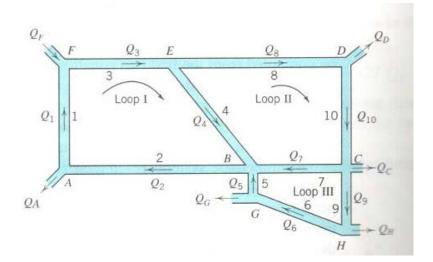






Networks

- Pipe junction: A~H
- Branch pipe: 1~10
- Loop (closed circuit of pipes): I~III



1) The continuity principle states that the <u>net flowrate into any pipe</u> junction must be zero.

2) The work-energy principle requires that at any junction there be only one position of the EL-HGL.

 \rightarrow Net head loss around any single loop of the network must be zero.

3) Clockwise is positive, and opposite is negative.

• For example, pipe 4 for Loop II is negative and positive for Loop I.

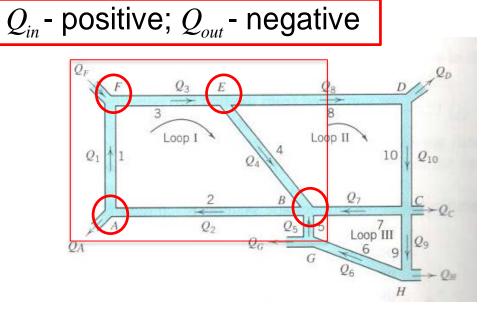


The equations for Loop I,

$$\sum_{A} Q = -Q_{A} + Q_{2} - Q_{1} = 0$$
$$\sum_{F} Q = Q_{1} + Q_{F} - Q_{3} = 0$$

$$\sum_{E} Q = Q_3 - Q_4 - Q_8 = 0$$

 $\sum Q = -Q_2 + Q_4 + Q_7 + Q_5 = 0$



$$\sum_{I}^{B} h_{L} = K_{1}Q_{1}^{n} + K_{3}Q_{3}^{n} + K_{4}Q_{4}^{n} + K_{2}Q_{2}^{n} = 0$$
$$K_{1}Q_{1}^{n} + K_{3}Q_{3}^{n} + K_{4}Q_{4}^{n} = -K_{2}Q_{2}^{n}$$

 To construct flownet, we need to assume the flow direction of each pipe.



The equations for Loop II,

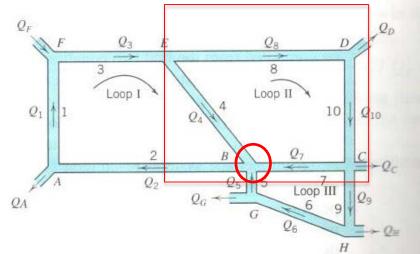
$$\sum_{B} Q = -Q_{2} + Q_{4} + Q_{5} + Q_{7} = 0$$

$$\sum_{E} Q = Q_{3} - Q_{4} - Q_{8} = 0$$

$$\sum_{D} Q = -Q_{D} + Q_{8} - Q_{10} = 0$$

$$\sum_{C} Q = -Q_{C} - Q_{7} - Q_{9} + Q_{10} = 0$$

$$\sum_{H} h_{L} = -K_{4}Q_{4}^{n} + K_{8}Q_{8}^{n} + K_{10}Q_{10}^{n} + K_{7}Q_{7}^{n} = 0$$





The equations for Loop III,

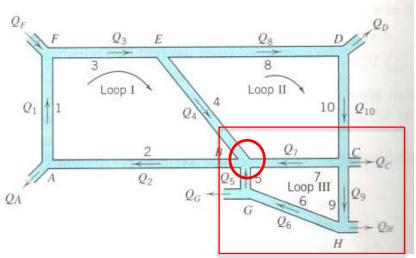
$$\sum_{B} Q = -Q_{2} + Q_{4} + Q_{5} + Q_{7} = 0$$

$$\sum_{C} Q = -Q_{7} + Q_{10} - Q_{C} - Q_{9} = 0$$

$$\sum_{C} Q = -Q_{6} + Q_{9} - Q_{H} = 0$$

$$\sum_{H} Q = -Q_{6} - Q_{5} + Q_{6} = 0$$

$$\sum_{H} h_{L} = K_{5}Q_{5}^{n} - K_{7}Q_{7}^{n} + K_{9}Q_{9}^{n} + K_{6}Q_{6}^{n} = 0$$







- Flow directions of each pipe have been assumed.
- The <u>pipe size</u>, <u>length</u>, <u>and hydraulic characteristics are known</u> as well as network inflows and outflows.
- Pump locations and pump characteristics, network layout and elevations are also given.
- Now we have the <u>10 unknown flowrate</u> Q_i, for i=1, 10, when Q_A, Q_F, Q_D, Q_C, Q_H, Q_G are given.
- The solution for the ten unknown flowrates is obtained by a <u>trial-and-</u> <u>correction method</u> or iteration process.





Hardy Cross Method (1936)

- The most simple and easy one may be the **Hardy Cross method**.
 - The essence of the method is to start with a best estimate of a set of initial values, Q_{0i} that satisfy continuity at each junction
 - And then to systematically <u>adjust these values keeping continuity</u> <u>satisfied until the head loss equations around each loop are satisfied</u> to a desired level of accuracy
 - All the equations of continuity at the pipe junctions are automatically and continuously satisfied by this approach.
 - Hence, only the head loss equations remain and the number of simultaneous equations to be solved is <u>reduced to the number of</u> <u>loops.</u>

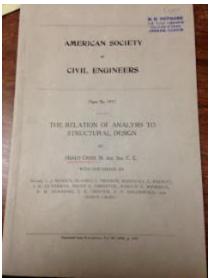


Hardy Cross (1885 - 1959)

Hardy Cross was an <u>American structural</u> <u>engineer</u> and the developer of the <u>moment</u> <u>distribution method</u> for <u>structural analysis</u> of <u>statically indeterminate</u> structures.

Another <u>Hardy Cross method</u> is also famous for modeling flows in complex <u>water supply</u> networks.







 If the first estimates are reasonably accurate, the <u>true flowrate</u> should only be a <u>small increment</u> different from the original (initial) flowrate in each loop.

$$Q_{i} = Q_{0i} \pm \Delta_{L} \quad (\Delta_{L} \text{ is loop correction})$$
(1)
$$Q_{0i} = \text{initial guess for pipe } i$$

For example

$$Q_3 = Q_{03} + \Delta_I$$
 (Loop I correction)
 $Q_8 = Q_{08} + \Delta_{II}$ (Loop II correction)

But for <u>pipe 4</u>,

$$Q_4 = Q_{04} + \Delta_I - \Delta_{II}$$

• For general <u>head loss equations</u> $\sum_{L} h_{Li} = \sum_{L} \pm K_i Q_i^n = 0$

(2)



Example for the head loss

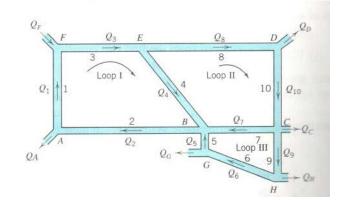
$$\sum_{I} h_{L} = K_{1}Q_{1}^{n} + K_{3}Q_{3}^{n} + K_{4}Q_{4}^{n} + K_{2}Q_{2}^{n} = 0$$

$$\sum_{II} h_{L} = -K_{4}Q_{4}^{n} + K_{8}Q_{8}^{n} + K_{10}Q_{10}^{n} + K_{7}Q_{7}^{n} = 0$$

$$\sum_{III} h_{L} = K_{5}Q_{5}^{n} - K_{7}Q_{7}^{n} + K_{9}Q_{9}^{n} + K_{6}Q_{6}^{n} = 0$$

Substitute (1) into (2)

$$\sum_{L} h_{Li} = \sum_{L} \pm K_i \left(Q_{0i} \pm \Delta_L \right)^n = 0$$



(3)



• Expanding Eq. (3) by the <u>binomial theorem</u> and neglecting all terms higher order of containing small increments, Δ_L^2, Δ_L^3 ,

$$\sum_{L} h_{Li} = \sum_{L} \pm K_i \left(Q_{0i} \pm \Delta_L \right)^n = \sum_{L} \pm K_i \left(Q_{0i}^n \pm n Q_{0i}^{n-1} \Delta_L + \cdots O(\Delta_L^r) \right) = 0$$

$$\Delta_L = -\frac{\sum_{L} \pm K_i Q_{0i}^n}{\sum_{L} \left| K_i n Q_{0i}^{n-1} \right|} \quad (n = 2)$$
(9.54)

 Several pipes share loop and we neglect the higher order flow increment. Therefore, the above one is quite not right to satisfy the head loss equations. Therefore, we need to iterate to find final values. So,

$$\Delta_{L}^{(j+1)} = \underbrace{\sum_{L} \pm K_{i} \left(Q_{0i}^{(j)} \right)^{n}}_{\sum_{L} \left| K_{i} n \left(Q_{0i}^{(j)} \right)^{n-1} \right|}$$

j - jth trial-and-correction for loop L





Pump in pipe network

- To add a pump to a pipe in the network, an expression representing the head increase versus the capacity curve is required.
- One method to accomplish this is to a fit a <u>polynomial curve</u> to the pump characteristics to form an equation of the form

$$E_{pi} = a_0 + a_1 Q_i + a_2 Q_i^2 + a_3 Q_i^3 + \cdots$$

 If a pump (head increase) is added to the line 8 in loop II, the head loss equation for loop II becomes

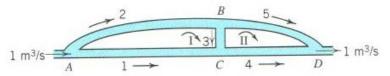
$$-K_{4}Q_{4}^{n} + K_{8}Q_{8}^{n} - a_{0} + a_{1}Q_{8} + a_{2}Q_{8}^{2} + \cdots + K_{10}Q_{10}^{n} + K_{7}Q_{7}^{n} = 0$$





I.P. 9.21 (p. 387~388)

- A parallel commercial steel pipe network was build in two parts. As shown below, section ACD is the original line the parallel section ABC was then added; then section BD was added to complete the job. By accident, a <u>valve is left open in the short pipe BC</u>. What are the resulting flowrates in all the pipes, neglecting local losses and assuming the <u>flows are wholly</u> <u>rough.</u>
- The pipe table below constructed using the Darcy-Weisbach equation gives all the pertinent pipe characteristics.



Pipe No.	Length (m)	Diameter (m)	e/d	f	<i>K_i</i> (Eq. 9.50)
1	1 000	0.5	9×10^{-5}	0.012	31.7
2	1 000	0.4	1×10^{-4}	0.012	96.8
3	100	0.4	1×10^{-4}	0.012	9.7
4	1 000	0.5	9×10^{-5}	0.012	31.7
5	1 000	0.3	1.4×10^{-4}	0.013	442.0



Solution:

 We begin the analysis by writing out the equations for increment for each loop.

$$\Delta_{L} = -\frac{\sum_{L} \pm K_{i} Q_{0i}^{n}}{\sum_{L} \left| K_{i} n Q_{0i}^{n-1} \right|} \quad (n = 2)$$
zero subscript for first iteration
$$\Delta_{I} = -\frac{-K_{1} Q_{01}^{2} + K_{2} Q_{02}^{2} + K_{3} Q_{03}^{2}}{2\left(\left| K_{1} Q_{01} \right| + \left| K_{2} Q_{02} \right| + \left| K_{3} Q_{03} \right| \right)}$$

$$\Delta_{II} = -\frac{-K_{3} Q_{03}^{2} + K_{5} Q_{05}^{2} - K_{4} Q_{04}^{2}}{2\left(\left| K_{3} Q_{03} \right| + \left| K_{5} Q_{05} \right| + \left| K_{4} Q_{04} \right| \right)}$$

$$\sum_{l m^{3}/s} \frac{1}{A} = -\frac{-K_{1} Q_{01}^{2} + K_{5} Q_{02}^{2} - K_{4} Q_{04}^{2}}{2\left(\left| K_{3} Q_{03} \right| + \left| K_{5} Q_{05} \right| + \left| K_{4} Q_{04} \right| \right)}$$



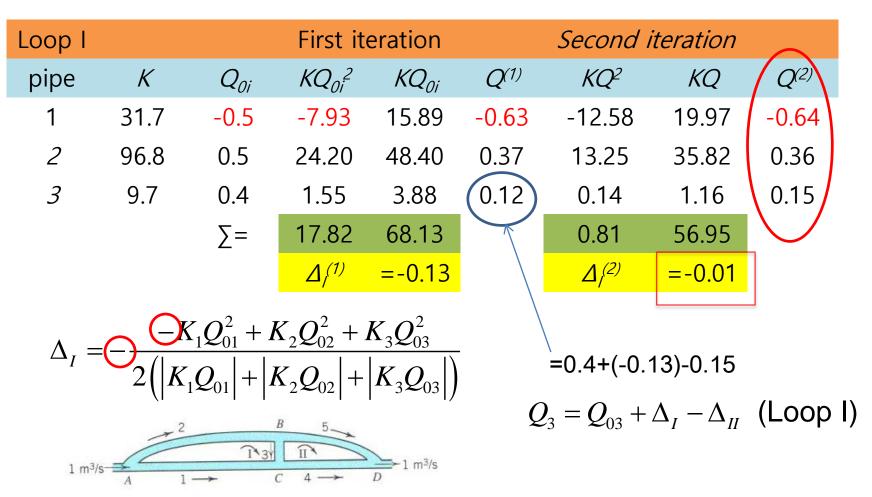
Solution:

 $1 \text{ m}^{3/\text{s}} \xrightarrow{A} 1 \xrightarrow{D} C \xrightarrow{A} D \xrightarrow{A} D \xrightarrow{A} C \xrightarrow{A} D \oplus{A} D \xrightarrow{A} D \oplus{A} D \oplus{A}$

Initial Subsequent calculation calculations $Q_1^{(j+1)} = Q_1^{(j)} + \Delta_I^{(j)}$ $Q_1 = Q_{01} + \Delta_I$ $Q_2^{(j+1)} = Q_2^{(j)} + \Delta_I^{(j)}$ $Q_2 = Q_{02} + \Delta_I$ $Q_3^{(j+1)} = Q_1^{(j)} + \Delta_I^{(j)} - \Delta_H^{(j)}$ (Loop I) $Q_3 = Q_{03} + \Delta_I - \Delta_{II}$ $Q_3 = Q_{03} - \Delta_I + \Delta_{II}$ $Q_3^{(j+1)} = Q_1^{(j)} - \Delta_I^{(j)} + \Delta_{II}^{(j)}$ (Loop II) $Q_{A}^{(j+1)} = Q_{A}^{(j)} + \Delta_{II}^{(j)}$ $Q_A = Q_{0A} + \Delta_H$ $Q_5^{(j+1)} = Q_5^{(j)} + \Delta_{II}^{(j)}$ $Q_5 = Q_{05} + \Delta_{II}$



 The iteration is carried out by setting up a table for systematically calculating the increment and correcting the flowrates in all pipes. The following table illustrates for the first two iterations.

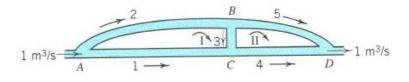




 $Q_3 = Q_{03} - \Delta_I + \Delta_{II}$ (Loop II) =-0.4-(-0.13)+0.15

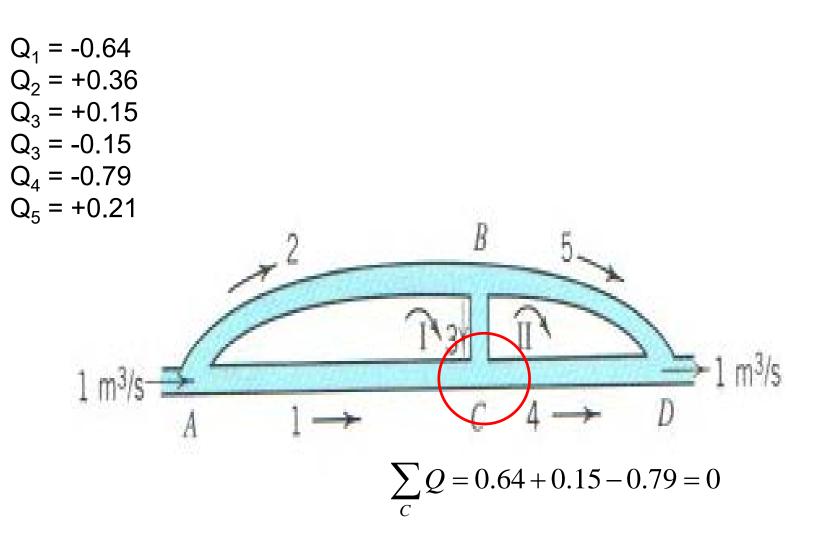
Loop II			First ite	eration		Second	iteration	\frown
pipe	K	Q_{0}	KQ_2 ²	KQ ₀	Q ⁽¹⁾	KQ ²	KQ	$Q^{(2)}$
3	9.7	-0.4	-1.55	3.88	-0.12	-0.14	1.16	-0.15
4	31.7	-0.9	-25.68	28.53	-0.75	-17.83	23.78	-0.79
5	442.0	0.1	4.42	44.20	0.25	27.63	110.50	0.21
			-22.81	76.61		9.66	135.44	\bigcirc
			$\Delta_{\prime\prime}^{(1)}$	0.15		$\Delta_{\prime\prime}^{(2)}$	=-0.04	

$$\Delta_{II} = -\frac{-K_3 Q_{03}^2 + K_5 Q_{05}^2 - K_4 Q_{04}^2}{2\left(\left|K_3 Q_{03}\right| + \left|K_5 Q_{05}\right| + \left|K_4 Q_{04}\right|\right)}$$





Check continuity eq.



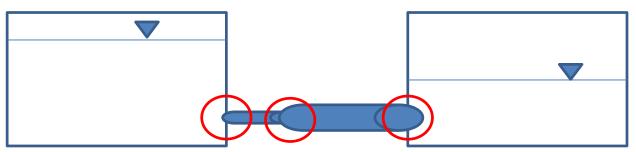




Homework Assignment No. 4 Due: 1 week from today Answer questions in Korean or English

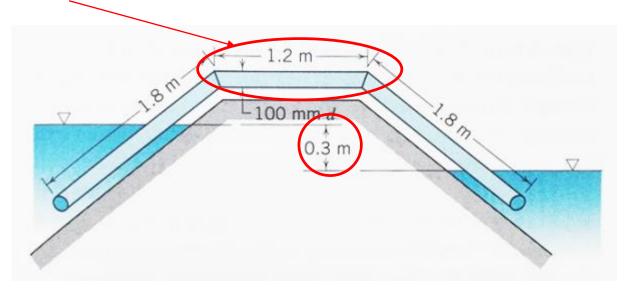
1.(9-111) A horizontal 50 mm PVC (smooth) pipeline leaves (squareedged entrance) a water tank 3 m below its free surface. At 15 mfrom the tank, it <u>enlarges abruptly</u> to a 100 mm pipe which runs 30 mhorizontally to another tank, entering it 0.6 m below its surface. <u>Calculate the flowrate through the line (water temperature 20 °C)</u>,

<u>including all head losses</u>.→ Type 2



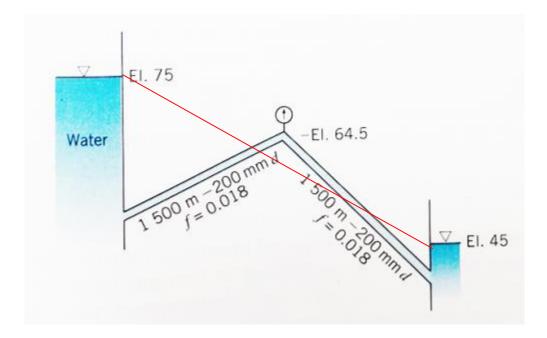


2. (9-123) <u>An irrigation siphon has the dimensions shown and is</u> placed over a dike. <u>Estimate the flowrate to be expected under a</u> head of 0.3 *m*. Assume a re-entrant entrance, a friction factor of 0.020, and <u>bend loss coefficients of 0.20</u>.



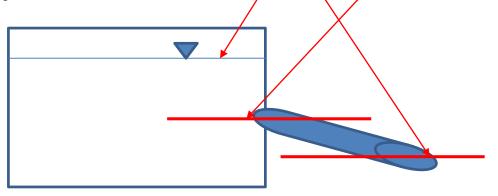


3. (9-124) <u>Calculate the flowrate and the gage reading</u>, <u>neglecting</u> <u>local losses and velocity heads</u>.



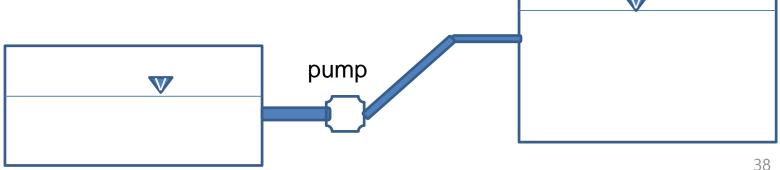
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4. (9-132) A 0.3 *m* pipeline 450 *m* long leaves (square-edged entrance) a reservoir of surface elevation 150 at elevation 138 and runs to elevation 117, where it discharges into the atmosphere. <u>Calculate the flowrate</u> and sketch the energy and hydraulic grade lines (assuming that f = 0.022) (a) for these conditions, and (b) when a <u>75 *mm* nozzle is attached to the end of the line, assuming the lost</u> head caused by the nozzle to be 1.5 *m*. How much power is available in the jet?



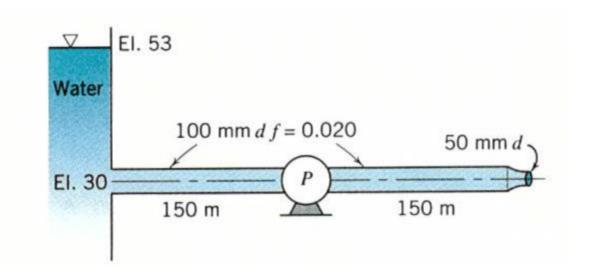


5. (9-138) The horizontal 200 *mm* suction pipe of a pump is 150 *m* long and is connected to a reservoir of surface elevation 90 m, 3 m below the water surface. From the pump, the <u>150 *mm* discharge pipe</u> runs 600 *m* to a reservoir of surface elevation 126, which it enters 10 *m* below the water surface. Taking *f* to be 0.020 for both pipes, calculate the power required to pump 0.085 m^3/s from the lower reservoir. What is the maximum dependable flowrate that may be pumped through this system (a) with the 200 *mm* suction pipe, and (b) with a 150 *mm* suction pipe?



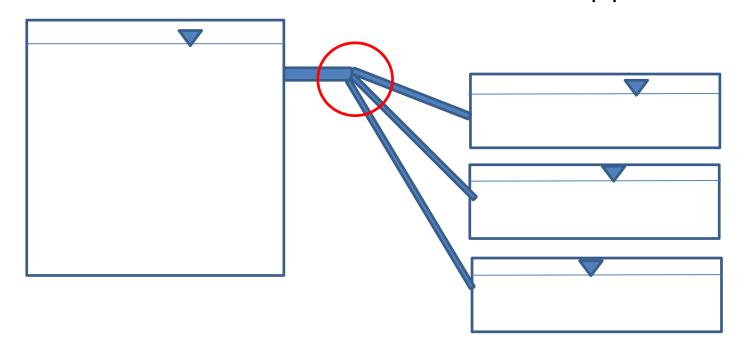


6. (9-143) The pump is required to maintain the flowrate which would have occurred <u>without any friction</u>. What power pump is needed? Neglect local losses.





7. (9-166) A 0.9 *m* pipe divides into three 0.45 *m* pipes at elevation 120. The 0.45 *m* pipes run to reservoirs which have surface elevations 90, 60, and 30, these pipes having respective lengths of 3.2, 4.8, and 6.8 kilometers. When 1.4 m^3/s flows in the 0.9 *m* line, how will the flow divide? Assume that *f* = 0.017 for all pipes.





8. (9-175) Calculate The flowrates on the pipes of this loop if all friction factors are 0.020.

