Chemical transformations

Types of reactions

• Oxidation/reduction $2H_2 + O_2 \leftrightarrow 2H_2O$

$$2H_2 + O_2 \leftrightarrow 2H_2O$$

Acid/base

$$HCOOH \leftrightarrow H^+ + HCOO^-$$

Substitution

$$CH_3Br + HS^- \leftrightarrow CH_3SH + Br^-$$

Hydrolysis

$$CH_3Br + H_2O \leftrightarrow CH_3OH + H^+ + Br^-$$

Elimination

$$Cl_2HC - CHCl_2 + OH^- \leftrightarrow ClHC = CCl_2 + Cl^- + H_2O$$

Concepts & definitions

- Conservative: does not chemically transform; does not partition from water
- Reactive: undergoes chemical transformations
- Persistent: does not (readily) undergo transformations
 - POPs: persistent, bioaccumulative, toxic
- Xenobiotic: man-made
- Transformation: change in chemical structure, still an organic molecule
- Mineralization: products are stable, inorganic molecules/ions (H₂O, CO₂, Cl⁻, ...)

Factors affecting compound degradability

Biotic

- Enzyme compatibility
 - Anthropogenic compounds may have unusual structures
- Energy available from transformation
- Toxicity
 - of compound
 - of metabolic byproducts
- Microbial community
- Environmental conditions
 - Suitable electron donors/acceptors
 - Energy source

Abiotic

- Suitable minerals, organics (i.e., humics), chemicals
- Light
- Heat
- Redox conditions

Reaction kinetics

$$aA+bB$$
 \xrightarrow{k} $cC+dD$
$$R=-\frac{d[A]}{dt}=k[A]^{\alpha}[B]^{\beta} \qquad k=\text{rate constant}$$
 $\text{overall reaction order}=\alpha+\beta$ $\alpha^{th} \text{ order with respect to A, } \beta^{th} \text{ order with respect to B}$ $\alpha \text{ and } \beta \text{ not necessarily be a and b, respectively}$

Types of rate expressions

$$R = k$$
 zero order

 $R = k[A]$ first order

 $R = k[A]^2$ second order (both overall and w.r.t. A)

 $R = k[A][B]$ second order (overall; 1st w.r.t. A or B)

 $R = \frac{k[A]}{K + [A]}$ saturation-type or mixed-order

Reaction kinetics

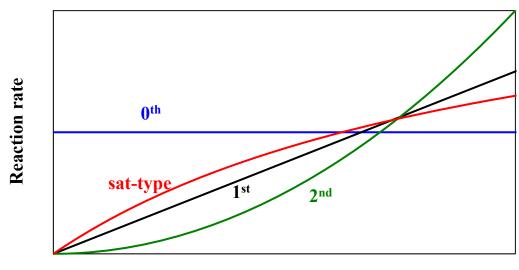
$$aA + bB \xrightarrow{k} cC + dD$$

$$R = -\frac{d[A]}{dt} = k[A]^{\alpha}[B]^{\beta} \qquad k = \text{rate constant}$$
 overall reaction order = $\alpha + \beta$
$$\alpha^{th} \text{ order with respect to A, } \beta^{th} \text{ order with respect to B}$$
 $\alpha \text{ and } \beta \text{ not necessarily be a and b, respectively}$

Types of rate expressions

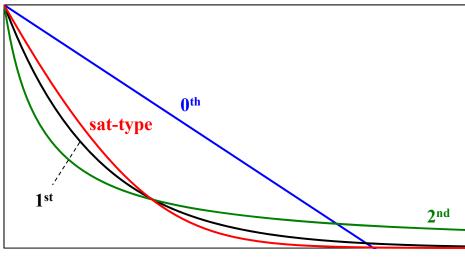
$$R=k$$
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Reaction kinetics



Concentration

Concentration



 2^{nd} : $R = k[A]^2$

Time

7

Reaction kinetics – irreversible, single step

For an <u>irreversible</u>, <u>single step</u> reaction

$$A + B \longrightarrow P$$

The reaction rate will be described as

$$R = -\frac{d[A]}{dt} = k[A][B]$$

Since the rate that the reaction will proceed is proportional to the chance that the two reactants collide to each other

Reaction kinetics - general

However, the reaction rate expression for a generic reaction is usually not determined this way because:

- Reactions we observe may involve multiple steps, multiple pathways
 - Different relative rates for each step
 - Some may involve species other than reactants (e.g., catalysts)
- For reversible reactions, backward reactions also occur
 - As reactants accumulates, the reaction rate slows down
 - For multiple-step reactions, some steps may be reversible while others irreversible
- Inhibition by products, intermediates, or reactants
- Relative abundance of reactants
 - pseudo-1st order, pseudo-2nd order

→ Rate expressions should be determined by experiments!

Pseudo nth order reactions

Consider a 2nd order reaction as an example

$$aA + bB \longrightarrow cC + dD$$

$$R = -\frac{d[A]}{dt} = k[A][B]$$

when $[A]_0 \ll [B]_0$, [B] changes little while [A] reacts completely, so:

$$[B] \approx [B]_0 = const.$$

 $[A]_0 \& [B]_0$ = initial concentrations of A & B

$$R = -\frac{d[A]}{dt} \approx k[A][B]_0 = k'[A]$$

 $k_1' = k[B]_0 = pseudo 1^{st}$ order rate constant

Irreversible 1st order reactions in series

$$A \xrightarrow{k_1} B \xrightarrow{k_2} C$$
 Assume 1st order

$$r_A = \frac{dC_A}{dt} = -k_1 C_A \qquad r_B = \frac{dC_B}{dt} = k_1 C_A - k_2 C_B \qquad r_C = \frac{dC_C}{dt} = k_2 C_B$$

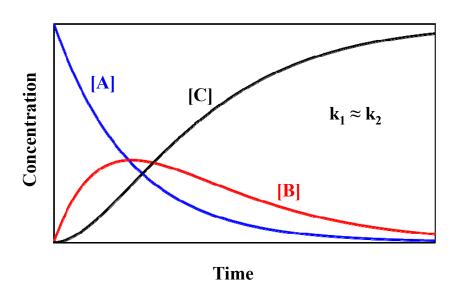
Solution (if $C_{BO} = C_{CO} = 0$):

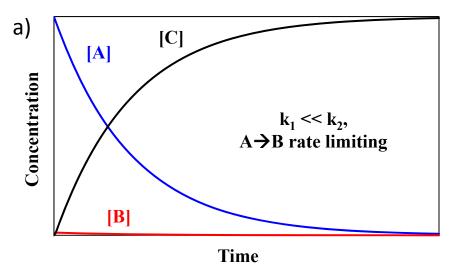
$$C_A = C_{A_0} e^{-k_1 t}$$

$$C_B = \frac{k_1}{k_2 - k_1} C_{A_0} (e^{-k_1 t} - e^{-k_2 t})$$

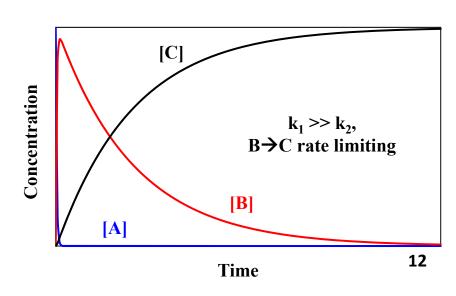
$$C_C = C_{A_0} + \frac{C_{A_0}}{k_2 - k_1} (k_1 e^{-k_2 t} - k_2 e^{-k_1 t})$$

Irreversible 1st order reactions in series

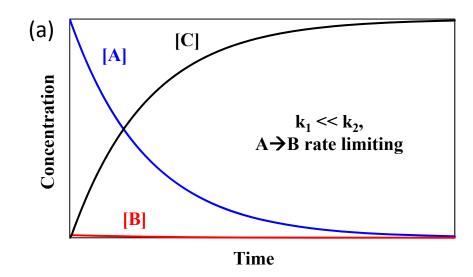


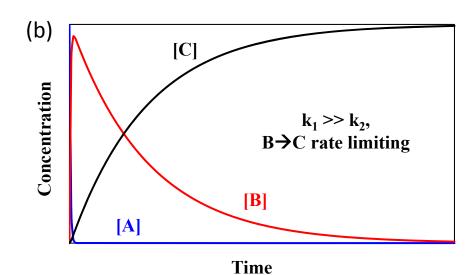


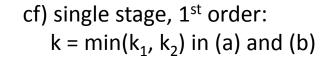
- Formation of "C" controlled by a rate limiting step
 - Often the reaction path involves several steps (which may be unknown) with one rate-limiting step
 - Overall expression is given as an apparent rate

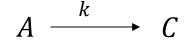


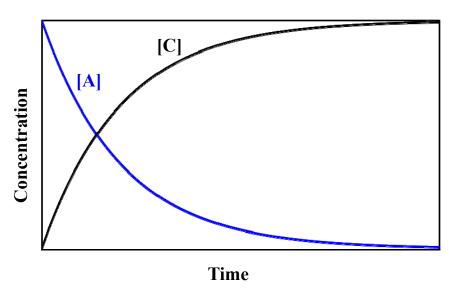
Irreversible 1st order reactions in series



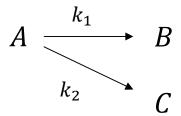








Irreversible 1st order reactions in parallel



$$r_A = \frac{dC_A}{dt} = -k_1C_A - k_2C_A$$

disappearance controlled by the path with larger k

ex) Abiotic vs. biological transformation:

 $Fe(II) \rightarrow Fe(III)$

Low pH: biological

ex) Acid mine drainage, pH < 3

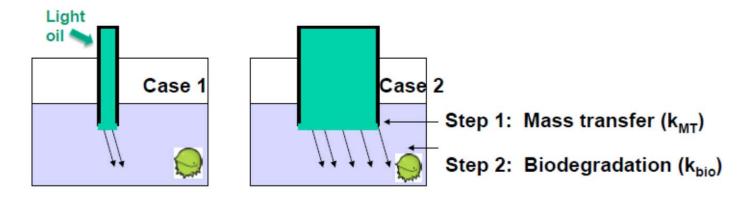
High pH: abiotic

ex) Pumped groundwater, neutral pH

Mass transfer + reaction in series

 Mass transfer should also be considered as a potential rate limiting step

 $k_{MT} = 1^{\text{st}}$ order mass transfer rate [T⁻¹]; $k_{bio} = 1^{\text{st}}$ order biodegradation rate [T⁻¹]



- → Here mass transfer supplies the reactant
- Damköhler #2 (Da_{II}) = (rate of reaction) / (rate of molecular diffusion) = k_{bio}/k_{MT}
 - If $Da_{II} > 1$, then mass transfer controls (mass transfer is a limiting step)
 - If $Da_{II} < 1$, then biodegradation controls (biodegradation is a limiting step)

Supplementary note: dimensionless

- Dimensionless numbers are often used to compare the relative significance of two processes involved in a phenomenon
- Examples

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- Reynolds # (Re) = (inertial force) / (viscous force) = \frac{d \times u \times \rho}{\mu}

d = characteristic length (e.g., diameter) [L]

u = flow velocity [L/T]

\rho = fluid density [M/L³]

\mu = dynamic viscosity [M/L/T]
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- Damköhler #1 (Da₁) = (rate of reaction) / (rate of advective transport) = HRT x k

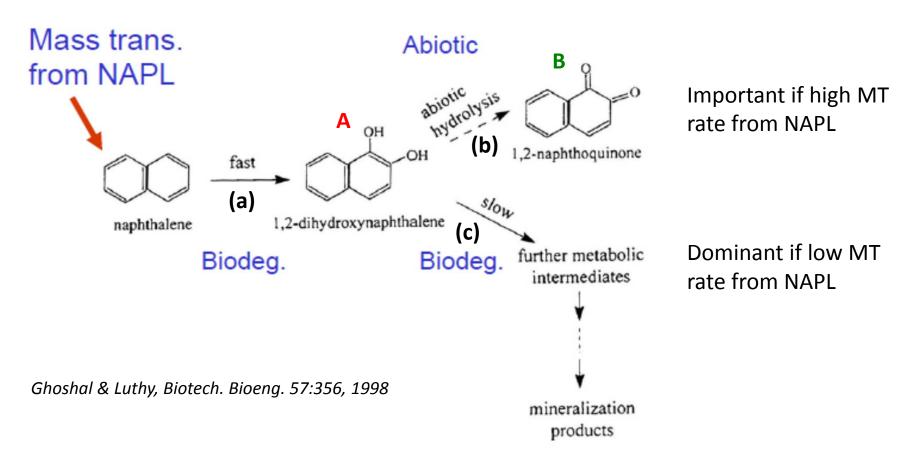
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HRT = V/Q = hydraulic retention time of a reactor [T]

k = 1^{st} order reaction rate constant [1/T]

V = volume of a reactor [L<sup>3</sup>]

Q = flowrate into and out of a reactor [L<sup>3</sup>/T]
```

{Reactions + MT} in series + parallel



- Reaction rate: (a) >> (c) >> (b) in the absence of inhibition
- But: inhibition of (c) by A and B
- Consequence: as mass transfer rate \uparrow , reaction (b) becomes more significant