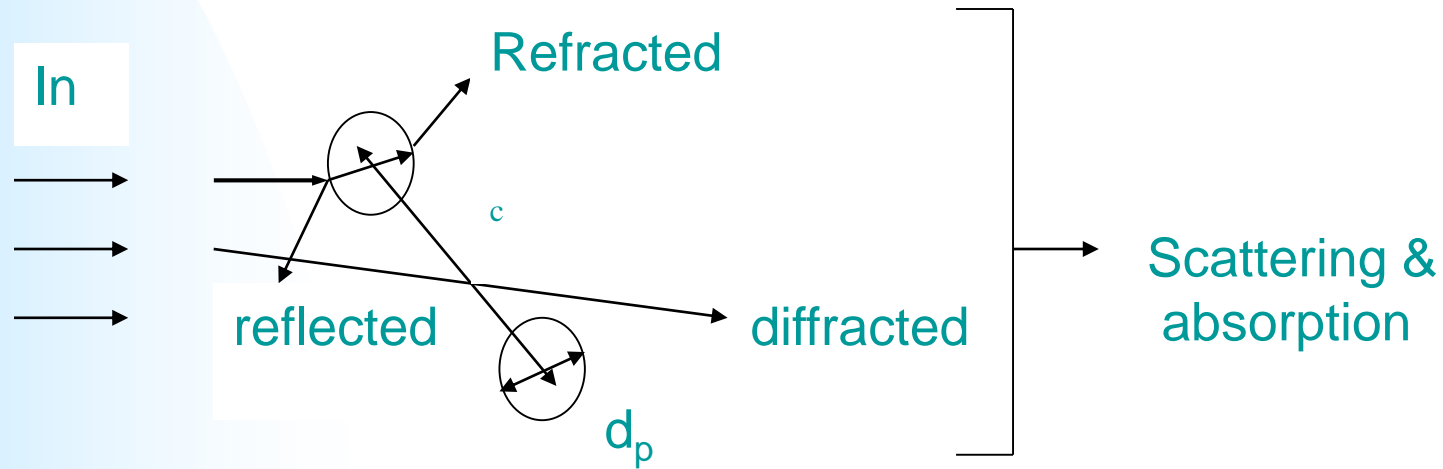


- * **Scattering of Light on Particulate media**
- * **elastic independent isotropic**
- * **inelastic dependent an isotropic**



- * **blue sky, red sunset, rainbow, etc**
- * **smog visibility**



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- function of particle shape, material of particle (complex index of refraction $m=n-ik$), relative size compared to wavelength of photons, clearance between particles

- → generally assume spherical particles

(Rayleigh and Mie Scattering), Rayleigh-Debye-Gans theory for non-spherical aggregate

- * independent scattering $c/d_p > 4$ or $f_v < 0.006$ (volume fraction)

- * Rayleigh scattering : small particle (Lord Rayleigh(1871))

$$\frac{\pi d_p}{\lambda} < 0.3$$

$$\frac{\pi d_p}{\lambda} \approx 1$$



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Mie Scattering (1908) (Gustav Mie : German physicist)

$$\text{Scattered Power} \approx \frac{1}{\lambda^4}$$

$$\text{Absorbed power} \approx \frac{1}{\lambda}$$

(shorter wavelength photons scattered dominantly)

Blue sky : blue (shorter scattered wavelength)

Scattered into all directions

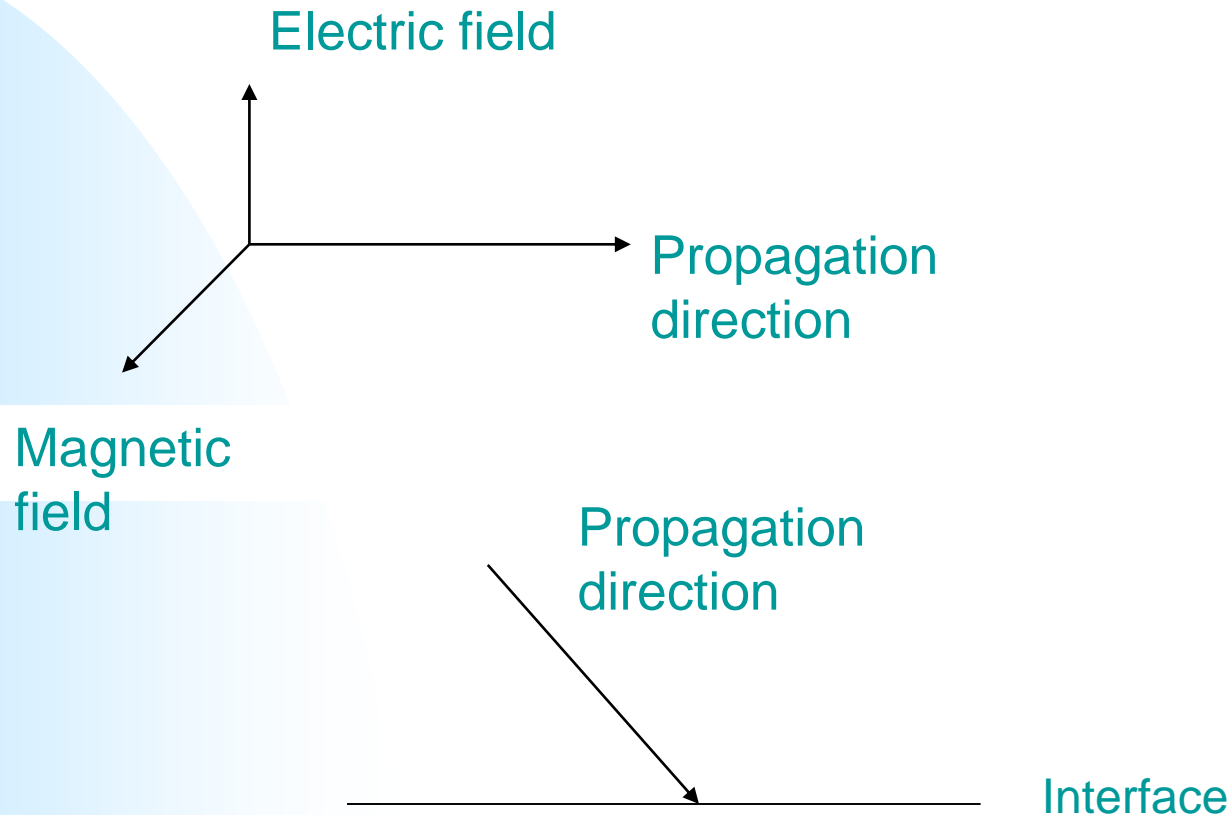
Red sunset : large wavelength red rays are able to penetrate the atmosphere without attenuation



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* Electro-magnetic wave propagation



***plane of incidence : plane containing both the normal to interface and incident direction**



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*polarization of light

: horizontally polarized (E-field vector is parallel to the plane of incidence)

: vertically polarized (E-field vector is perpendicular to the plane of incidence)

*Let's consider a single particle illuminated by radiation with incident power per unit area I_0 (W/m²)

Total scattered power $P_{\text{sca}} = C_{\text{sca}} I_0$

Total absorbed power $P_{\text{abs}} = C_{\text{abs}} I_0$

Where C_{sca} and C_{abs} are scattering and absorption cross sections, respectively.



$$P_{\text{extinction}} = P_{\text{sca}} + P_{\text{abs}}$$

$$C_{\text{ext}} = C_{\text{sca}} + C_{\text{abs}}$$

Power incident on the particle is $P_{\text{inc}} = AI_0$

Where A is the cross sectional area of particle

$$\therefore \frac{P_{\text{abs}}}{P_{\text{inc}}} = \frac{C_{\text{abs}}}{A} = Q_{\text{abs}} : \text{absorption efficiency factor}$$

$$\therefore \frac{P_{\text{sca}}}{P_{\text{inc}}} = \frac{C_{\text{sca}}}{A} = Q_{\text{sca}} : \text{scattering efficiency factor}$$



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**For an aerosol consisting of polydisperse particles
effective scattering area**

$$= dV \int_0^{\infty} C_{sca,\lambda}(d_p) dN(d_p)$$

$dN(d_p)$: #/cm³

between dp and $d_p+dd_p = n(d_p)dd_p$

effective scattering area per unit volume

= scattering coefficient [1/m]

$$\sigma_{s\lambda} = \int_0^{\infty} C_{sca,\lambda}(dp) dN(dp)$$

if monodisperse

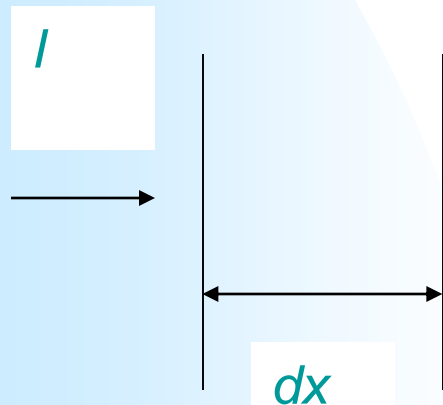
$$\sigma_{s\lambda} = C_{sca,\lambda} N$$



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$$I = I_0 \exp(-(\sigma_{s\lambda} + \alpha_\lambda)x)$$



$$dI = -I \frac{C_{sca}}{A}$$

$$I + dI \quad dI = -I \frac{\text{effective scattering area}}{A} = -I \frac{dV \sigma_{s\lambda}}{A}$$

$$= -I dx \sigma_{s\lambda}$$

$$\frac{dI}{I} = -\sigma_{s\lambda} dx$$

$$\therefore \frac{I}{I_0} = \exp(-\sigma_{s\lambda} x)$$



•Rayleigh scattering

$$x = \frac{\pi d_p}{\lambda} \rightarrow 0$$

$$Q_{sca} = \frac{\lambda}{3} \left| \frac{m^2 - 1}{m^2 + 2} \right|^2 x^4 \approx \frac{1}{\lambda^4}$$

$$Q_{ext} = -4x \operatorname{Im} \left\{ \frac{m^2 - 1}{m^2 + 2} \right\} \approx Q_{abs}$$

$$C_{ext} = \pi \frac{d_p^2}{4} Q_{ext} \quad \overline{C_{ext}} = \int C_{ext} p(d_p) dd_p$$

$$\sigma_{ext} = \int_0^\infty C_{ext} n(v) dv = -\frac{6\pi}{\lambda} f_v \operatorname{Im} \left\{ \frac{m^2 - 1}{m^2 + 2} \right\}$$

→ only depends on volume fraction not on particle size distribution

f_v = volume fraction

$$\frac{I_{ext}}{I_o} = \exp\left(-\int \sigma_{ext} ds\right)$$



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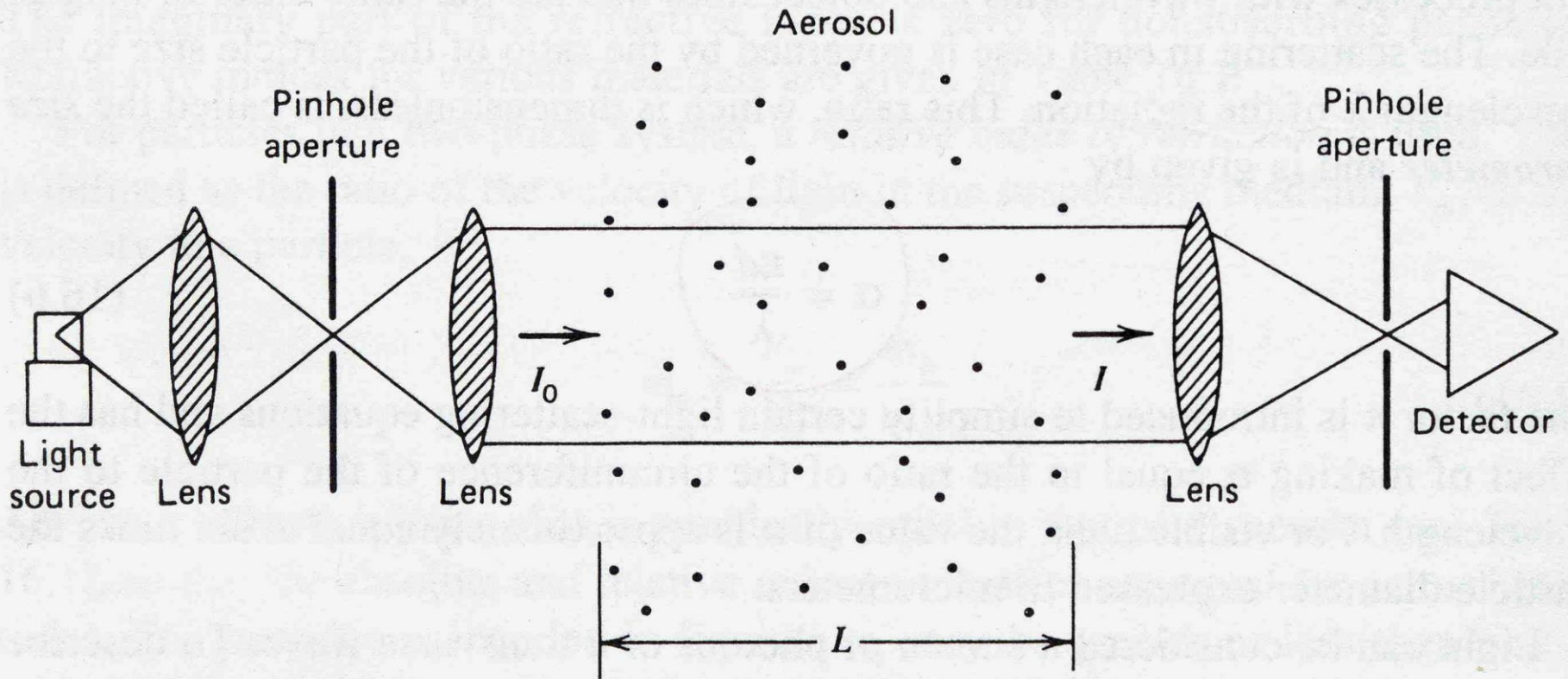


FIGURE 16.1 Schematic diagram of an extinction-measuring apparatus.



Extinction-Scattering method for small particles

Rayleigh scattering & extinction

$$C_{ext} = -4 \frac{2\pi^2 a^3}{\lambda} \operatorname{Im} \left\{ \frac{m^2 - 1}{m^2 + 2} \right\}$$

$$\begin{aligned} \overline{C}_{ext} &= \int_0^\infty \frac{\pi^2 d_p^3}{N\lambda} \frac{1}{\sqrt{2\pi \ln \sigma_g} d_p} \exp\left(-\frac{(\ln d_p / d_g)^2}{\ln \sigma_g}\right) dd_p \times \operatorname{Im} \left\{ \frac{m^2 - 1}{m^2 + 2} \right\} \\ &= \frac{\pi^2}{\lambda} d_m^3 E(\tilde{m}) \end{aligned}$$

d_m^- : diameter of average volume

$$\therefore d_m^3 = \frac{\lambda}{\pi^2} \frac{\overline{C}_{ext}}{E(\tilde{m})}$$



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$$f_v = \frac{1}{6} \pi d_m^3 N = \frac{\lambda}{6\pi} \frac{1}{E(\tilde{m})} \overline{C_{ext}} N$$

Since $\overline{C_{ext}} N = K_{ext}$ we can measure f_v from K_{ext}

Differential scattering cross-section for vertically polarized light

$$C_{vv}(\theta) \approx \frac{a^6}{\lambda^4} \left| \frac{m^2 - 1}{m^2 + 2} \right|^2$$

$$\overline{C(\theta)_{vv}} = \int_0^\infty C_{vv}(\theta) p(d_p) dd_p = \frac{1}{(2\pi/\lambda)^2} \left(\frac{\pi}{\lambda} \right)^6 \frac{M_6}{M_0} F(m) \sim d_p^6$$

$$\frac{M_6}{M_0} = \int_0^\infty d_p^6 p(d_p) dd_p$$

$$\overline{C_{ext}} = \frac{\pi^2}{\lambda} \frac{M_3}{M_0} E(m) \sim d_p^3$$



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$$\frac{\overline{C_{vv}}}{C_{ext}} = \frac{\pi^2 M_6 F(m)}{4\lambda^3 M_3 E(m)} \sim d_p^3$$

$$\therefore M_6/M_3 = \left(\frac{\lambda^3}{\pi^3}\right) \left\{4\pi \frac{\overline{C_{vv}}}{C_{ext}} \frac{E(m)}{F(m)}\right\}$$

$$\therefore \left(\frac{M_6}{M_3}\right)^{1/3} = \frac{\lambda}{\pi} \left\{4\pi \frac{\overline{C_{vv}}}{C_{ext}} \frac{E(m)}{F(m)}\right\}^{1/3}$$

$$d_{p63} = \left(\frac{M_6}{M_3}\right)^{1/3} \\ = \left(\frac{\int d_p^6 n(d_p) dd_p}{\int d_p^3 n(d_p) dd_p}\right)^{1/3}$$



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If we assume log-normal distribution,

$$\frac{M_0 M_6}{M_3^2} = \left\{ \frac{dp_{63}}{dp_{30}} \right\}^3 = \exp(9 \ln^2 \sigma_g)$$

If σ_g is known, then d_{p30} can be determined.

$\sigma_g = 1 \rightarrow$ monodisperse

$\sigma_g \approx 1.36 \rightarrow$ self-preserving

absorbing particle only : carbon soot particle



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* Mie Scattering

$$Q_{sca} = \frac{2}{x^2} \sum_{n=1}^{\infty} (2n+1)(|a_n|^2 + |b_n|^2)$$

$$Q_{ext} = \frac{2}{x^2} \sum_{n=1}^{\infty} (2n+1)R(a_n + b_n)$$

$$C_{sca} = \pi \frac{d_p^2}{4} Q_{sca} = \int_{4\pi} (\text{differential cross section}) d\Omega$$

Consider only vertically polarized comp. $\rightarrow C_{vv}(\theta, d_p, m)$

Scattering angle

$m=n-ik$



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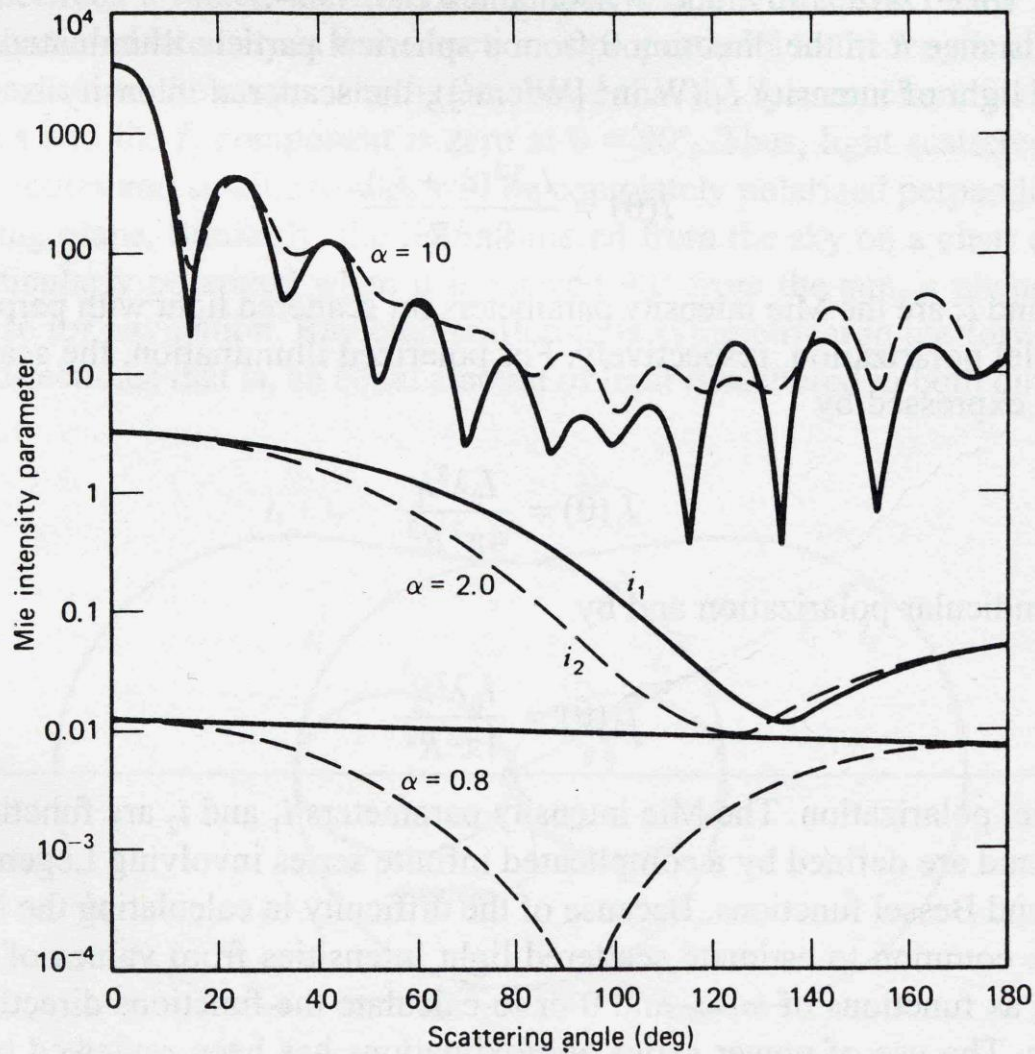


FIGURE 16.8 Mie intensity parameters versus scattering angle for water droplets ($m = 1.33$) having $\alpha = 0.8, 2.0,$ and 10.0 . Solid lines are i_1 and dashed lines are i_2 .



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We can determine particle size distribution by measuring scattered lights at different angles → angular dissymmetric light scattering method
differential scattering coefficient

$$\sigma_s(\theta) = \int_0^{\infty} C_{vv}(x, \theta, m)n(v)dv$$

Assume independent scattering → or single scattering



* Detected power of scattered light

$$S_{\nu\nu}(\theta) = \sigma_s(\theta)\eta\Delta V\Delta\Omega I_{0,\nu\nu}$$

$$= \sigma_s(\theta)SR(\theta)$$

$SR(\theta)$ = system response (independent of size distribution or material)

(Example)

$$n(\nu) = \frac{M_0}{3\sqrt{2\pi} \ln \sigma_g} \exp\left[-\frac{\ln^2\left(\frac{\nu}{\nu_g}\right)}{18\ln^2 \sigma_g}\right] \frac{1}{\nu}$$

M_0, ν_g, σ_g : 3 unknowns



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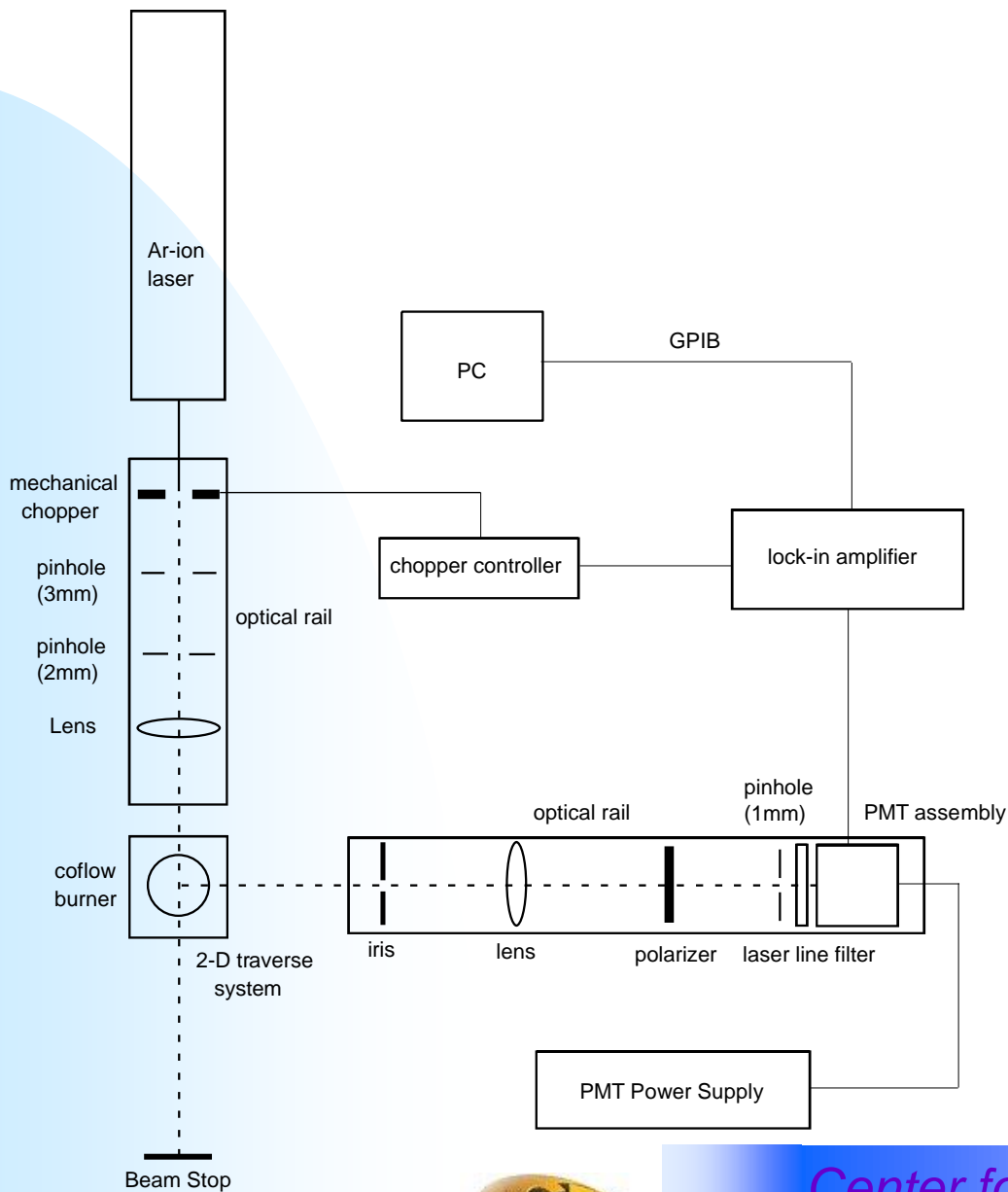
$$SR(\theta) \int_0^{\infty} C_{vv}(x, \theta) \frac{M_0}{3\sqrt{2\pi} \ln \sigma_g} \exp \left[-\frac{\ln^2(v/v_g)}{18 \ln^2 \sigma_g} \right] \frac{1}{v} dv$$

$$= S_{vv}(\theta)$$

$$\frac{S_{vv}(\theta_1)}{SR(\theta_1)} = \int_0^{\infty} C_{vv}(x, \theta_1) \frac{M_0}{3\sqrt{2\pi} \ln \sigma_g} \exp \left[-\frac{\ln^2(v/v_g)}{18 \ln^2 \sigma_g} \right] \frac{1}{v} dv$$

$$\frac{S_{vv}(\theta_2)}{SR(\theta_2)} = \int_0^{\infty} C_{vv}(x, \theta_2) \frac{M_0}{3\sqrt{2\pi} \ln \sigma_g} \exp \left[-\frac{\ln^2(v/v_g)}{18 \ln^2 \sigma_g} \right] \frac{1}{v} dv$$





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■ Optical Particle Counter (OPC):

- measures particle size distribution covering the size range 0.1-5 μm . The aerosol flow should be diluted to make sure that only one particle at a time is illuminated and scatters light to the detector. As each particle passes through the focused light beam, it scatters a pulse of light to the detector, which is converted to an electrical signal. Electronic pulse height (or area) analysis is used to interpret the pulse and direct a count to the proper size channel where the total count is obtained from the accumulated counts in each size channel.
- Optical particle counters are restricted by “coincidence errors” to the measurement of aerosols with relatively low number concentrations usually less than $10^4/\text{cc}$. Coincidence errors arise when two or more particles are in the measuring volume simultaneously and causing a spurious signal that leads to an underestimation of the particle number concentration and the overestimation of the particle size.



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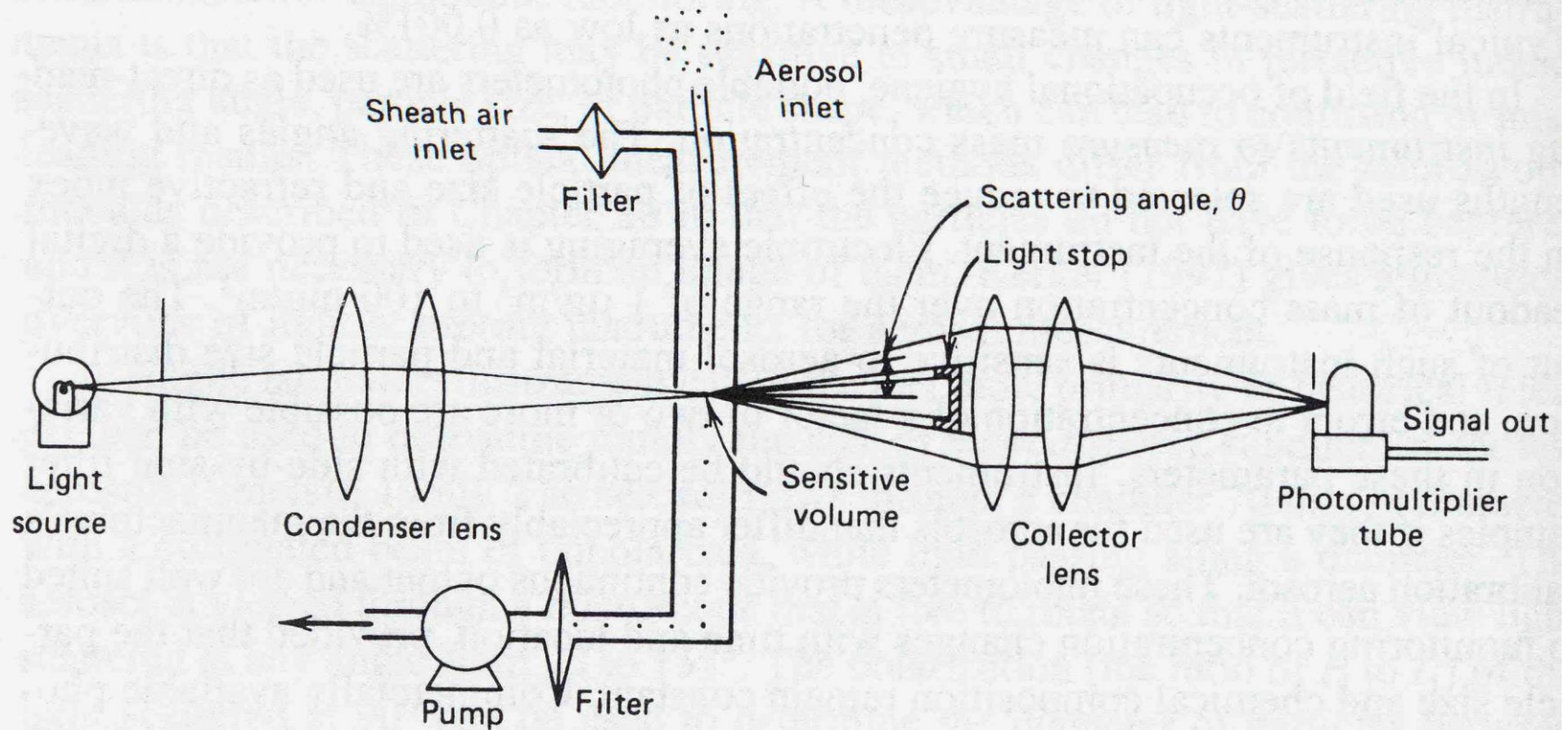


FIGURE 16.15 Diagram of a forward-scattering optical particle counter.



TABLE 16.3 Characteristics of Some Optical Particle Counters

Instrument	Particle Size Range (μm)	Number of Channels	Scattering Angle Range (deg)	Sample Flow Rate (cm^3/min)	Maximum Concentration ^a (cm^{-3})
Climet ^b					
208 ^c	0.3→20	16	15–105	28,000	90
7400	0.1→0.5	6	15–150	2800	14
7500	0.19→5.0	6	15–150	28,000	14
Hiac/Royco ^d					
236	0.12→6.0	16	35–120	280	3000
5100	0.25→10	6	60–120	28,000	7
PMS, Inc. ^e					
HS-LAS	0.065–1.0	32	35–120	2800	8000
LAS-X	0.09–3	16 ^f	35–120	60	17,000
LAS-X	0.12–7.5	16 ^f	35–120	280	3000
LPC-525	0.2→5.0	6	60–120	28,000	3.5

^aConcentration for 10 % coincidence error.

^bClimet Instruments Co., Redlands, CA.

^cWhite light illumination; all others use laser light.

^dHiac/Royco, Menlo Park, CA.

^eParticle Measuring Systems, Inc., Boulder, CO.

^fFour ranges with 16 channels each.



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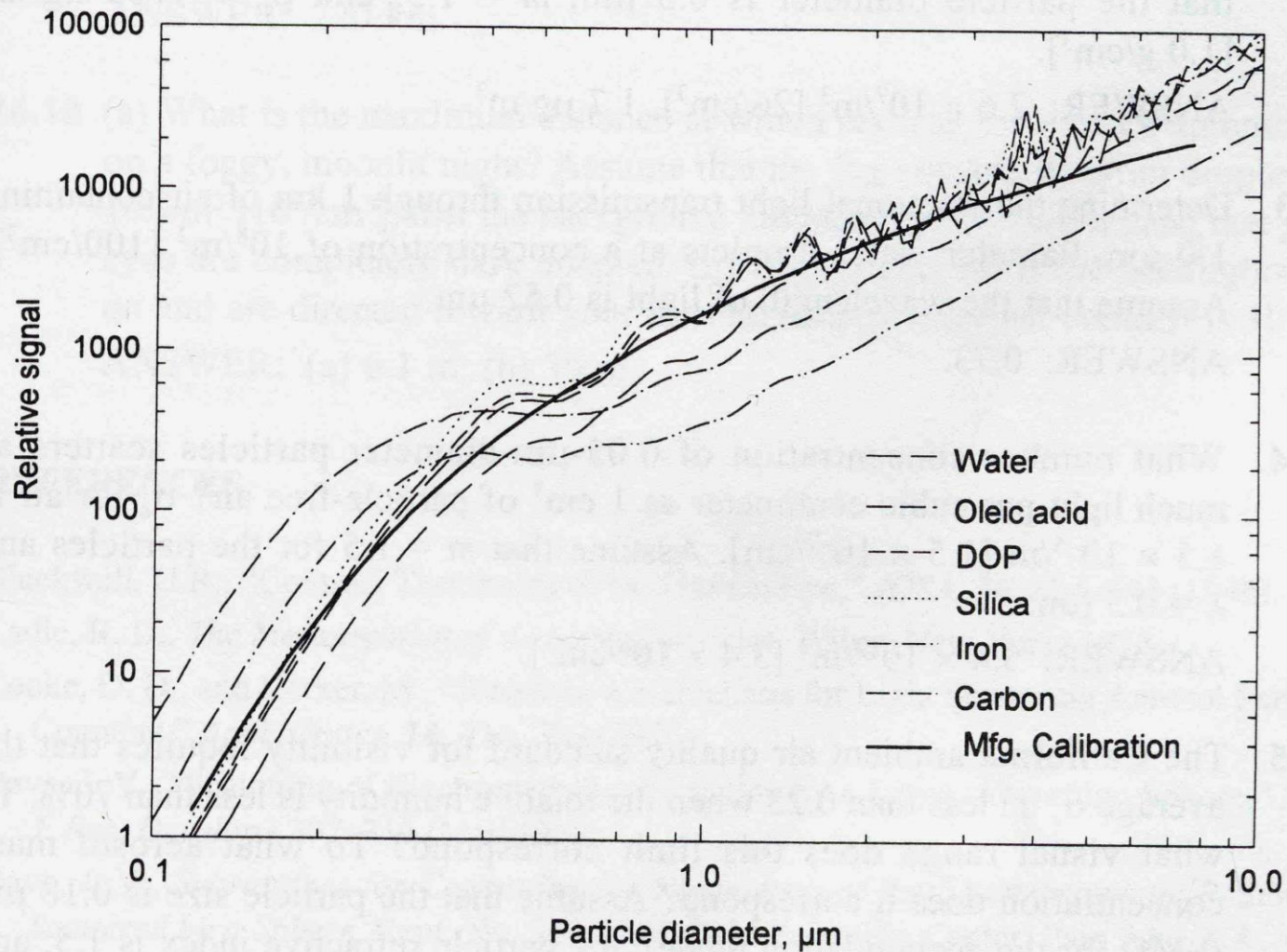


FIGURE 16.16 Calculated response curves for six materials and manufacturer's calibration curve for model LAS-X[®] (PMS, Inc., Boulder, CO) optical particle counter.



Evolution of size, morphology, and concentration of particles

- **Particle growth**

 - : size and morphology change, concentration change

 - : spherical, non-spherical

- **Evolution of size distribution of aerosol**

- **What makes the size distribution change?**



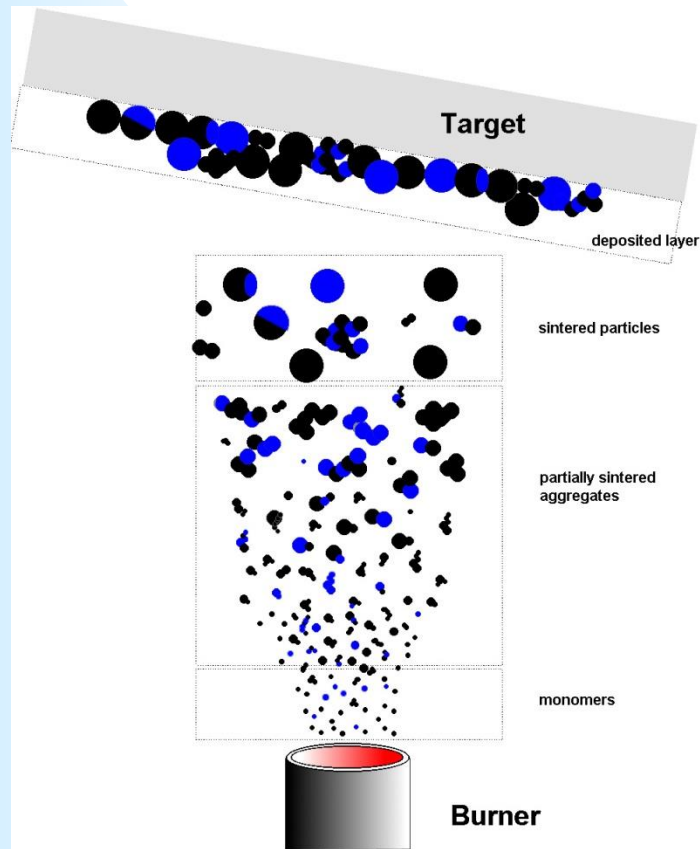
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- **Convection, diffusion, external force → aerosol transport and migration → concentration change, but size and morphology remain**
- **Collision of Particles**
 - : size, morphology and concentration changes
- **Condensation and Evaporation**
 - : size change
- **Coalescence of particles**
 - : morphology change
- **Nucleation**
 - : generation of particles



Nanoparticle synthesis-Flame Aerosol Synthesis



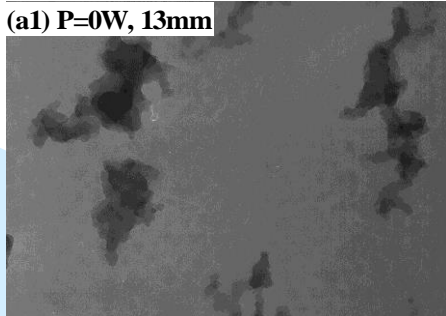
Pro : high purity nanoparticles at high concentrations

Con : difficulty in controlling the growth of nanoparticles : generation of aggregates when nanoparticles are synthesized at high concentrations.

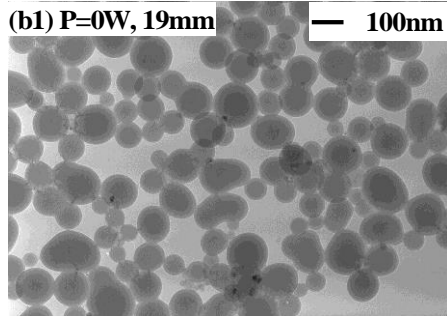
“How can we synthesize small and unagglomerate sphere nanoparticles at high concentrations?”



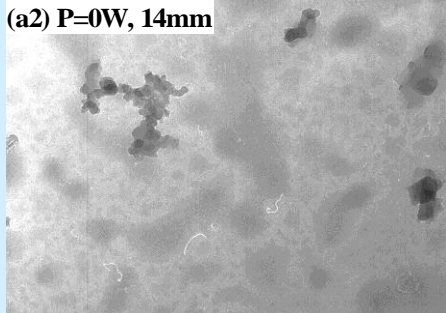
(a1) P=0W, 13mm



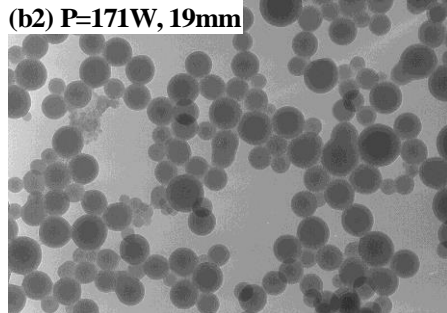
(b1) P=0W, 19mm



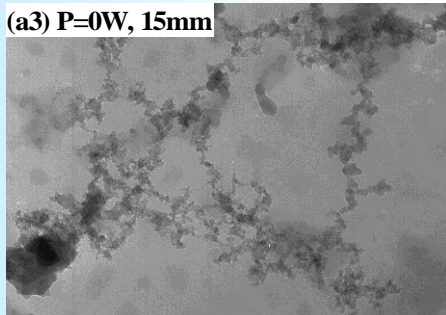
(a2) P=0W, 14mm



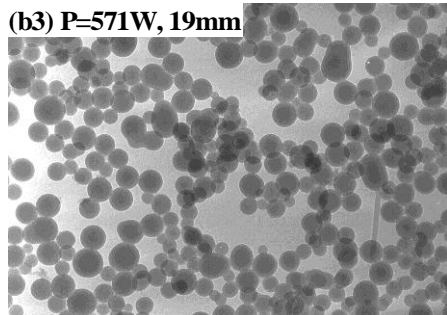
(b2) P=171W, 19mm



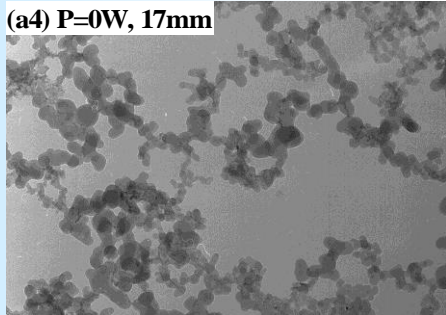
(a3) P=0W, 15mm



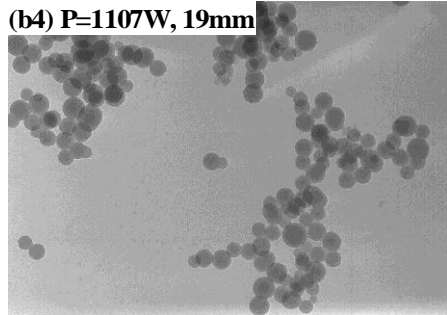
(b3) P=571W, 19mm



(a4) P=0W, 17mm



(b4) P=1107W, 19mm



Growth of SiO₂ Particles in a Flame



- **Generation of nanoparticles : Physical or chemical**
 - Homogeneous nucleation or chemical reactions
 - Temperature and concentration fields

- **Growth of nanoparticles :**
 - Collision and coalescence (+residence)
 - Temperature, concentration and fluid flow fields

- **Transport of nanoparticles :**
 - Diffusion, convection and thermophoresis
 - Temperature, concentration and fluid flow fields

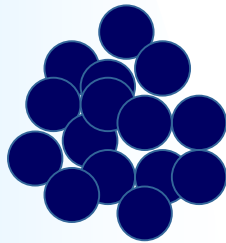
- **Deposition of nanoparticles :**
 - Diffusion and thermophoresis
 - Temperature and concentration gradients



Description the morphology of non-spherical particles;

$$n_p = k_f \left(\frac{R_g}{d_p} \right)^{D_f}$$

(i) Mass fractal dimension, D_f



$D_f=3$: Compact agglomerate structure



$D_f =1$: Chain-like



Fractal dimension

$$N_p = k_f \left(\frac{R_g}{r_p} \right)^{D_f}$$

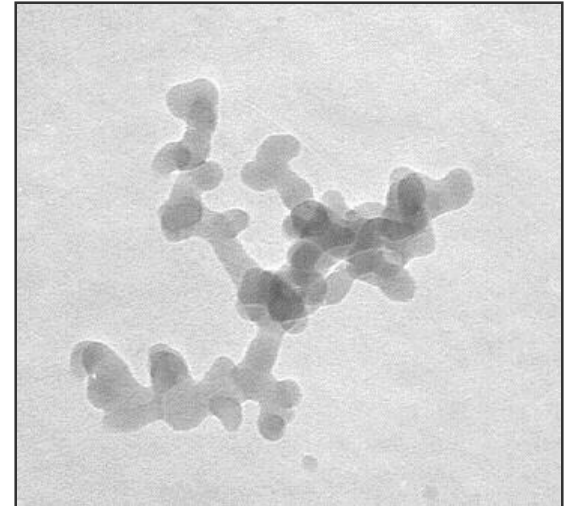
Image processing

N_p : primary particle number per aggregate

$$N_p = \left(\frac{A_a}{A_p} \right)^{1.1}$$

$$A_a = D_{binary}$$

$$A_p = \pi r_p^2$$



R_g : radius of gyration

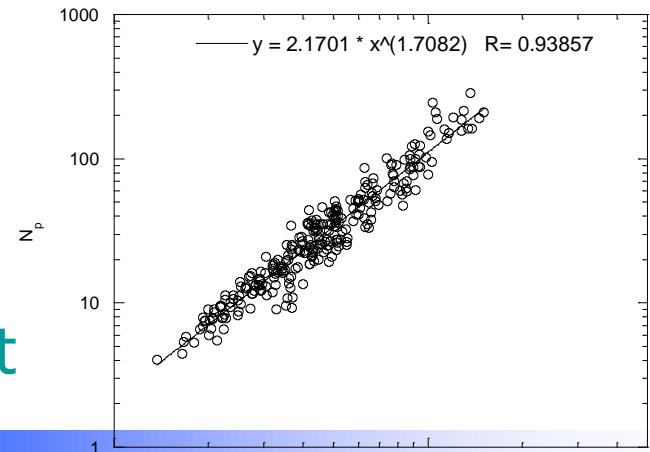
$$MR_g^2 = \sum_i m_i (\vec{r}_i - \vec{r}_{cm})^2$$

$$D_{binary} R_{g,2}^2 = \sum_i D_{binary,i} (\vec{r}_i - \vec{r}_{cm})^2$$

$$R_g \approx R_{g,2}$$

D_f : fractal dimension

Slope of $\ln(N_p) - \ln(R_g / r_p)$ plot



Determination of Size and Morphology

- **Competition between Collision and Coalescence of nanoparticles**
 - **If collision is faster than coalescence, aggregate form**
 - **If coalescence is faster than collision, spherical particle form**



Cho and Choi, 2000, J. Aerosol Sci., 31, 1077

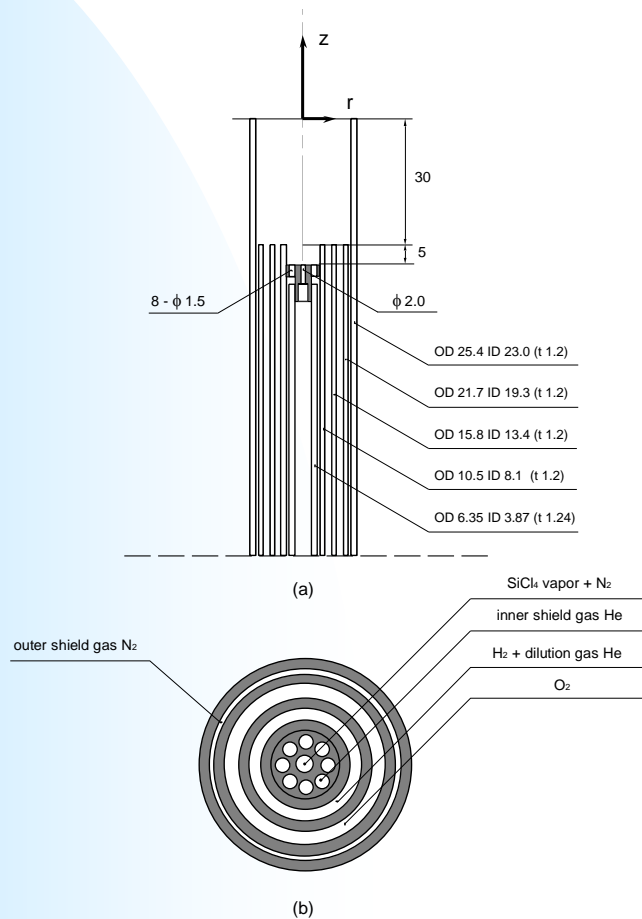
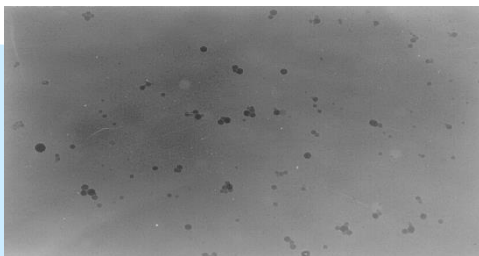


Fig.1 (a) Schematic of a coflow burner and coordinates (unit : mm)
(ID : inside diameter, OD : outside diameter, t : thickness)
(b) Burner exit configuration

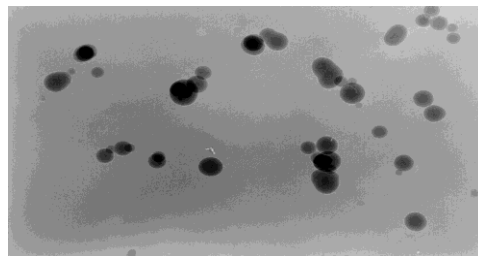


0.1 μm

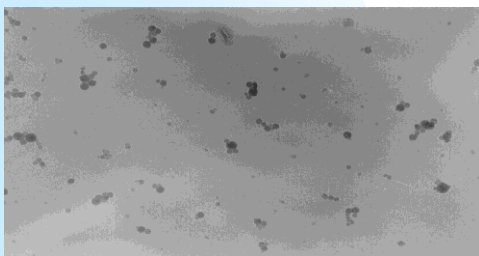


(a) 30 cc/min

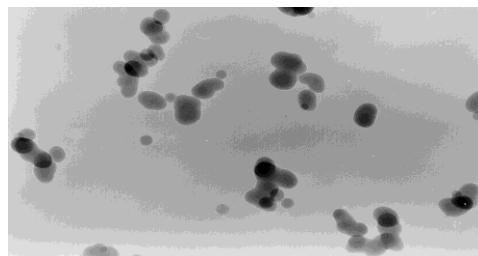
0.1 μm



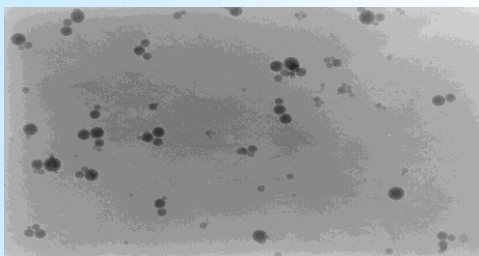
(e) 200 cc/min



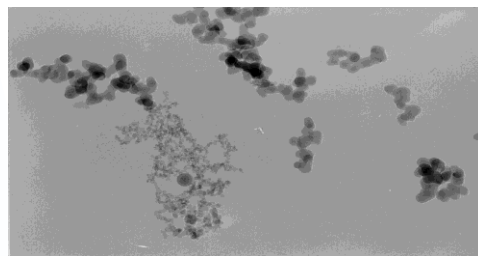
(b) 50 cc/min



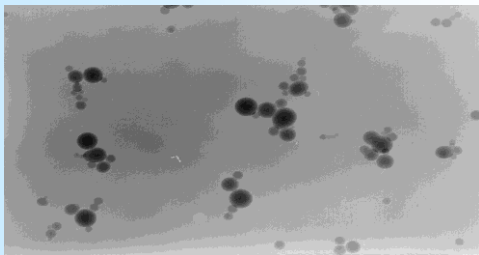
(f) 250 cc/min



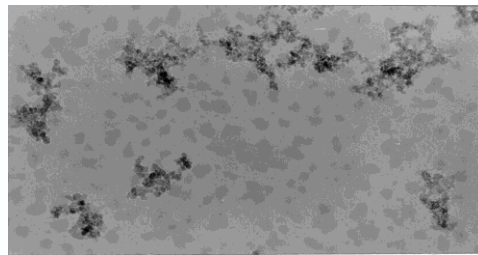
(c) 100 cc/min



(g) 300 cc/min



(d) 150 cc/min



(h) 350 cc/min

Effect of carrier gas flow rates on the morphology of SiO_2 particles in flames (inner shield He 3.0 l/min, H_2 4.0 l/min, dilution He 2.0 l/min, O_2 7.5 l/min, outer shield N_2 7.0 l/min, carrier gas N_2 for SiCl_4 , $r = 0$ mm, $z = 5$ mm)

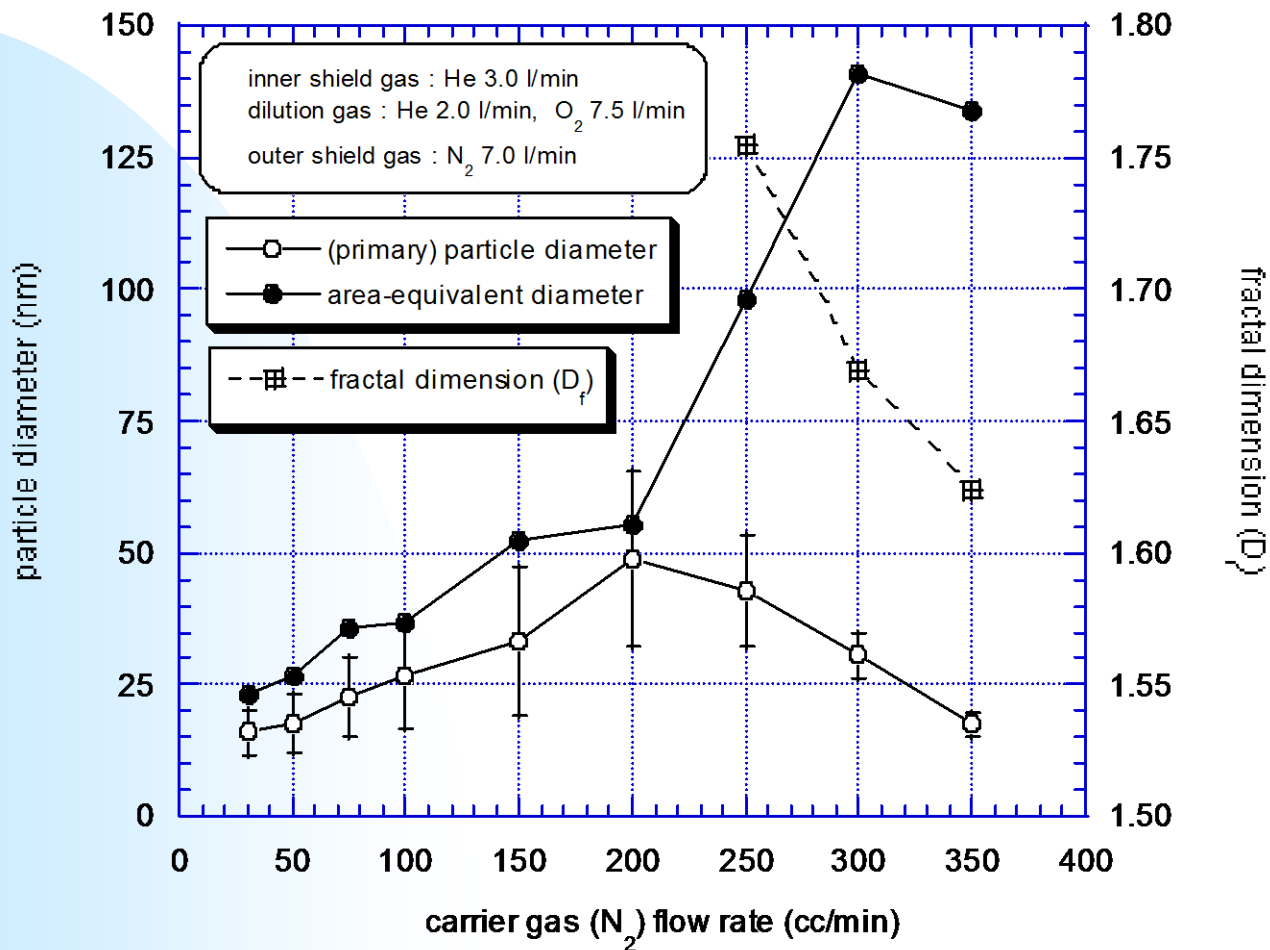
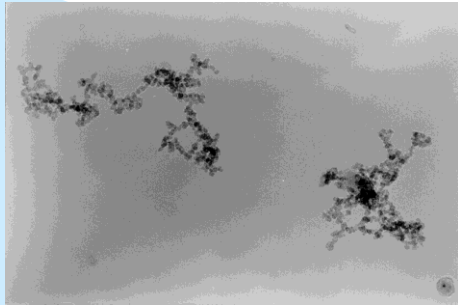


Fig.6 Effect of carrier gas flow rate on particle diameters and fractal dimensions

(H₂ 4.0 l/min, r = 0 mm, z = 5 mm, carrier gas N₂)

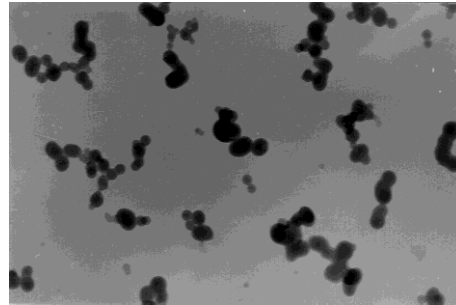


0.1 μm

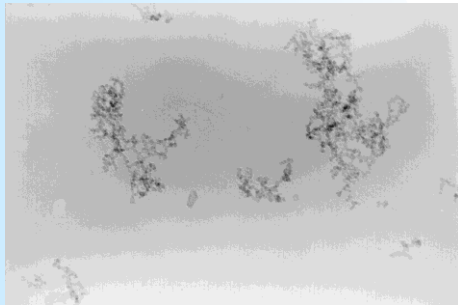


(a) H_2 1.5 l/min,
 $Q_{\text{vw}} = 1.048\text{E-}3 \pm 3.59\%$

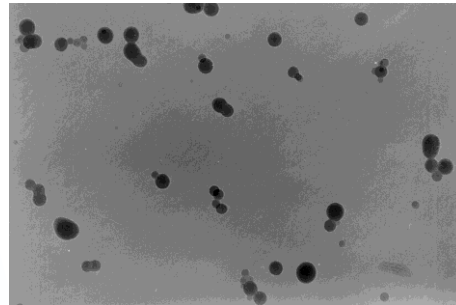
0.1 μm



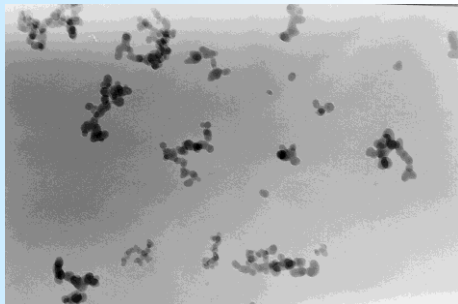
(d) H_2 3.0 l/min,
 $Q_{\text{vw}} = 3.395\text{E-}3 \pm 4.24\%$



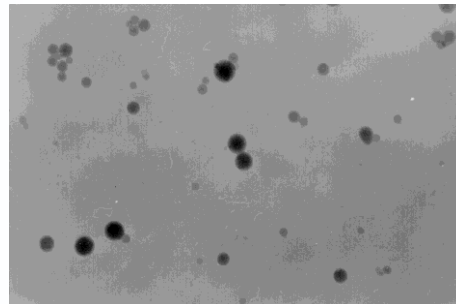
(b) H_2 2.0 l/min,
 $Q_{\text{vw}} = 8.281\text{E-}4 \pm 4.79\%$



(e) H_2 4.0 l/min,
 $Q_{\text{vw}} = 2.079\text{E-}3 \pm 5.63\%$



(c) H_2 2.5 l/min, $Q_{\text{sub vw}}$
 $Q_{\text{vw}} = 1.750\text{E-}3 \pm 5.15\%$



(f) H_2 5.0 l/min, $Q_{\text{sub vw}}$
 $Q_{\text{vw}} = 1.091\text{E-}3 \pm 7.18\%$

Effect of H_2 flow rates on the morphology of SiO_2 particles in flames (inner shield He 3.0 l/min, dilution He 2.0 l/min, O_2 7.5 l/min, outer shield N_2 7.0 l/min, carrier gas N_2 50 cc/min for SiCl_4 , $r = 0$ mm, $z = 30$ mm, unit of $Q_{\text{vw}} : [\text{cm}^{-1} \text{sr}^{-1}]$)

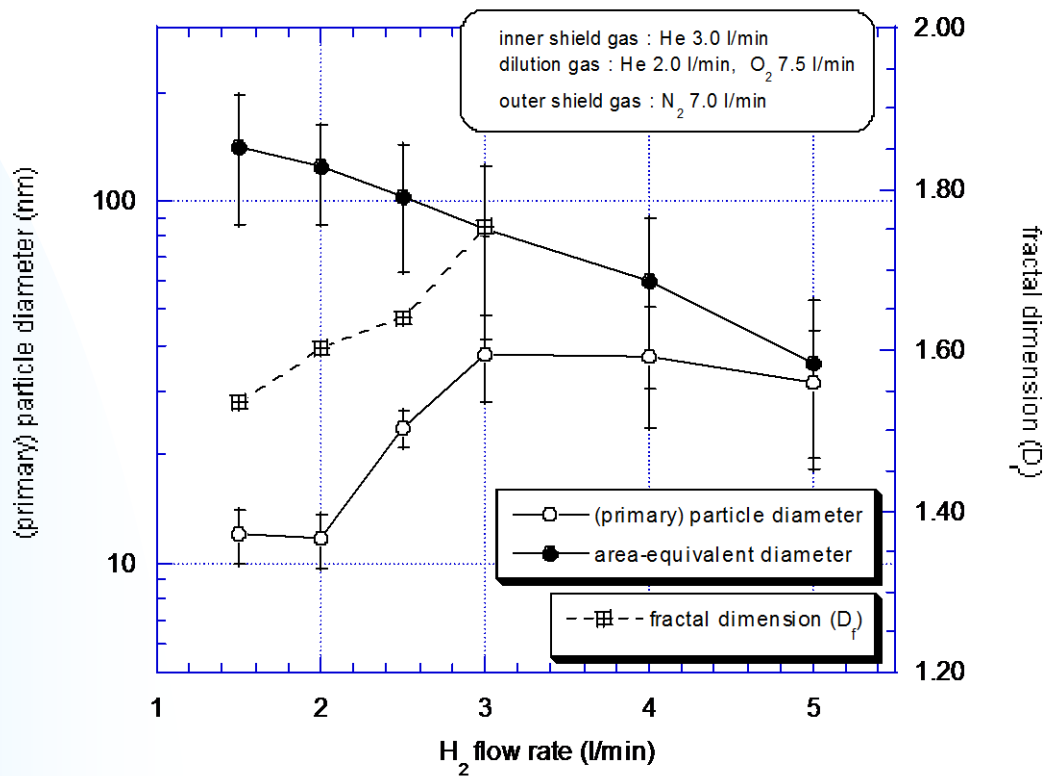
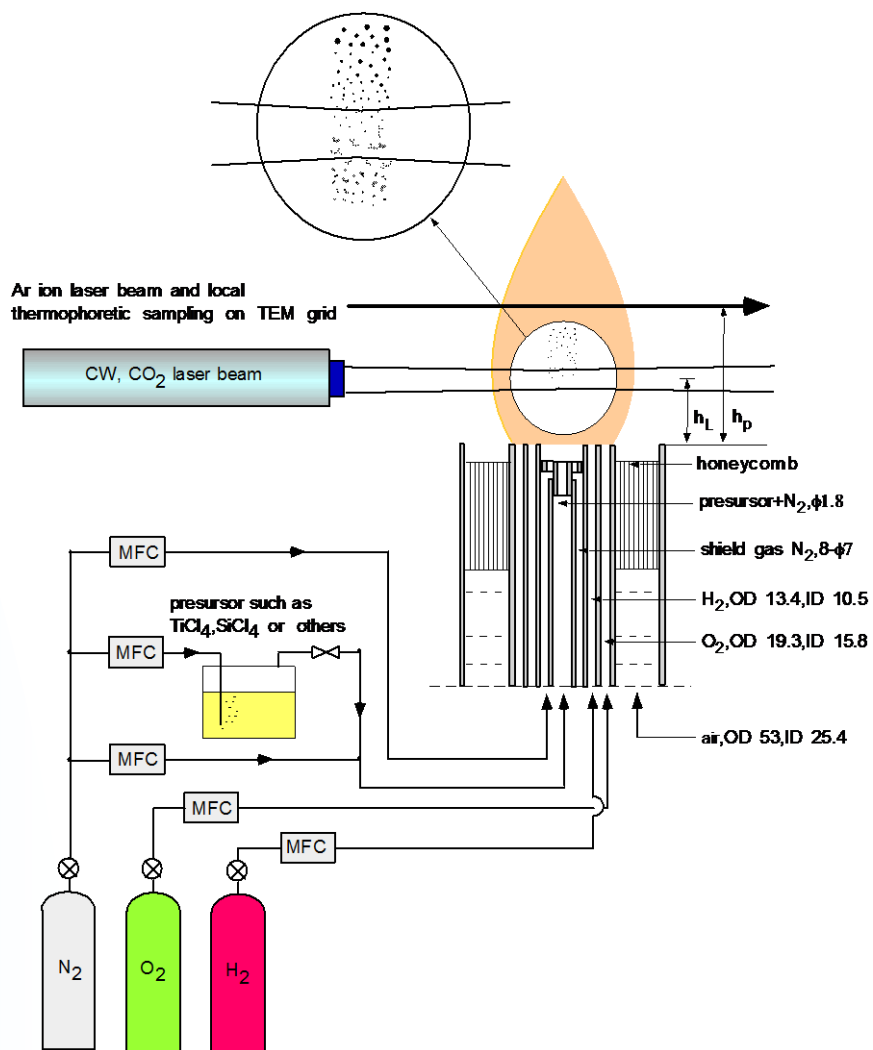


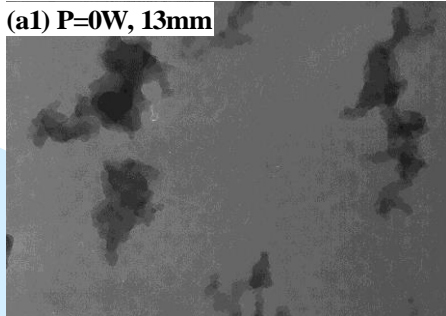
Fig.11 Effect of H₂ flow rates on particle diameters and fractal dimensions
 (carrier gas N₂ 50 cc/min for SiCl₄, r = 0 mm, z = 30 mm)



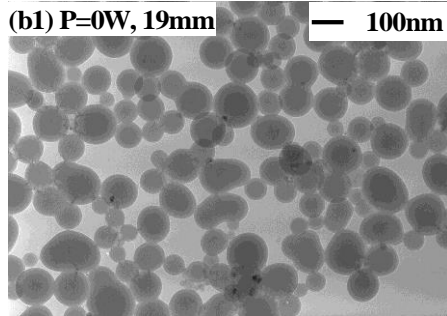
Present Control Principle



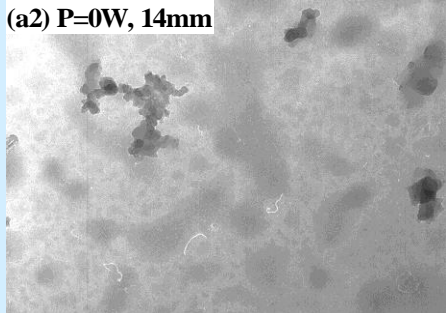
(a1) P=0W, 13mm



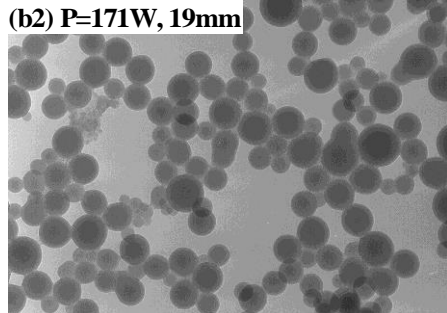
(b1) P=0W, 19mm



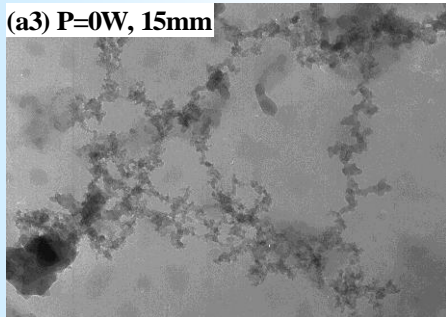
(a2) P=0W, 14mm



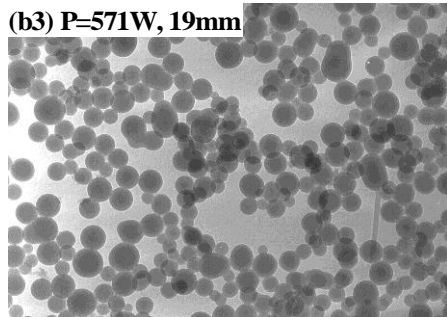
(b2) P=171W, 19mm



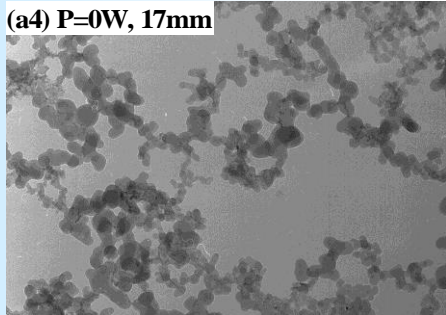
(a3) P=0W, 15mm



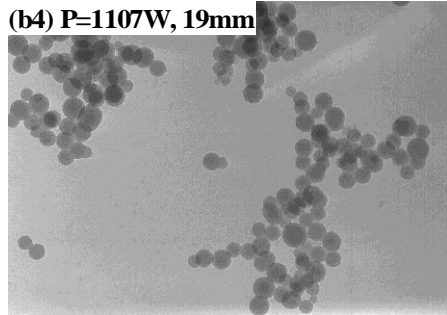
(b3) P=571W, 19mm



(a4) P=0W, 17mm



(b4) P=1107W, 19mm



Growth of SiO₂ Particles in a Flame



Aerosol Synthesis of Nanoparticles

- Nanoparticle grows by two processes : particle collision and coalescence.

1. If collision is faster than coalescence,



2. If coalescence is faster than collision,

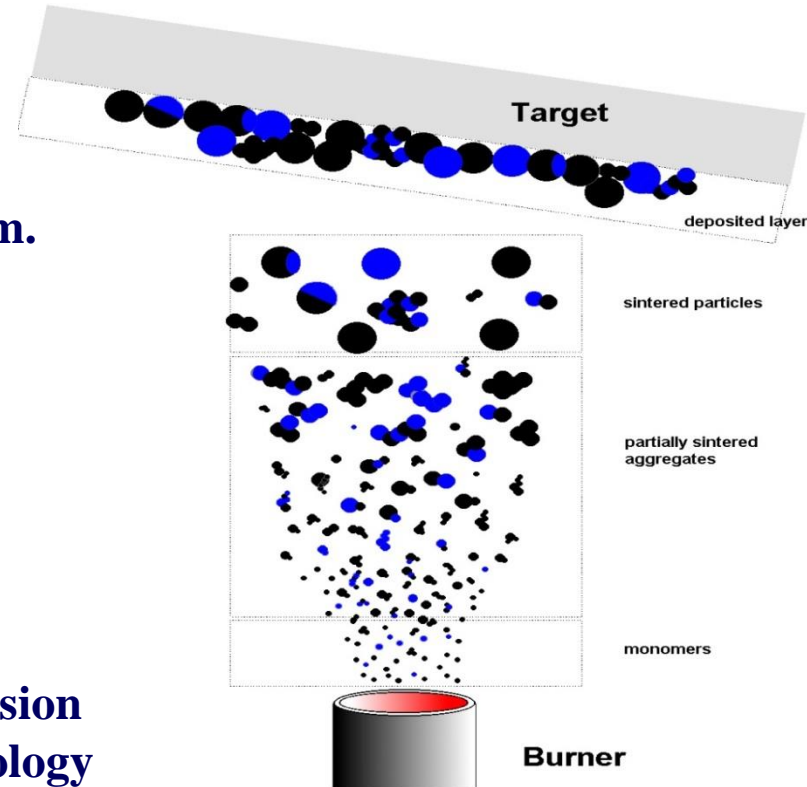


Collision characteristic time $\sim \frac{1}{\sqrt{T}}$

Coalescence characteristic time $\sim \exp\left(\frac{C}{T}\right)$

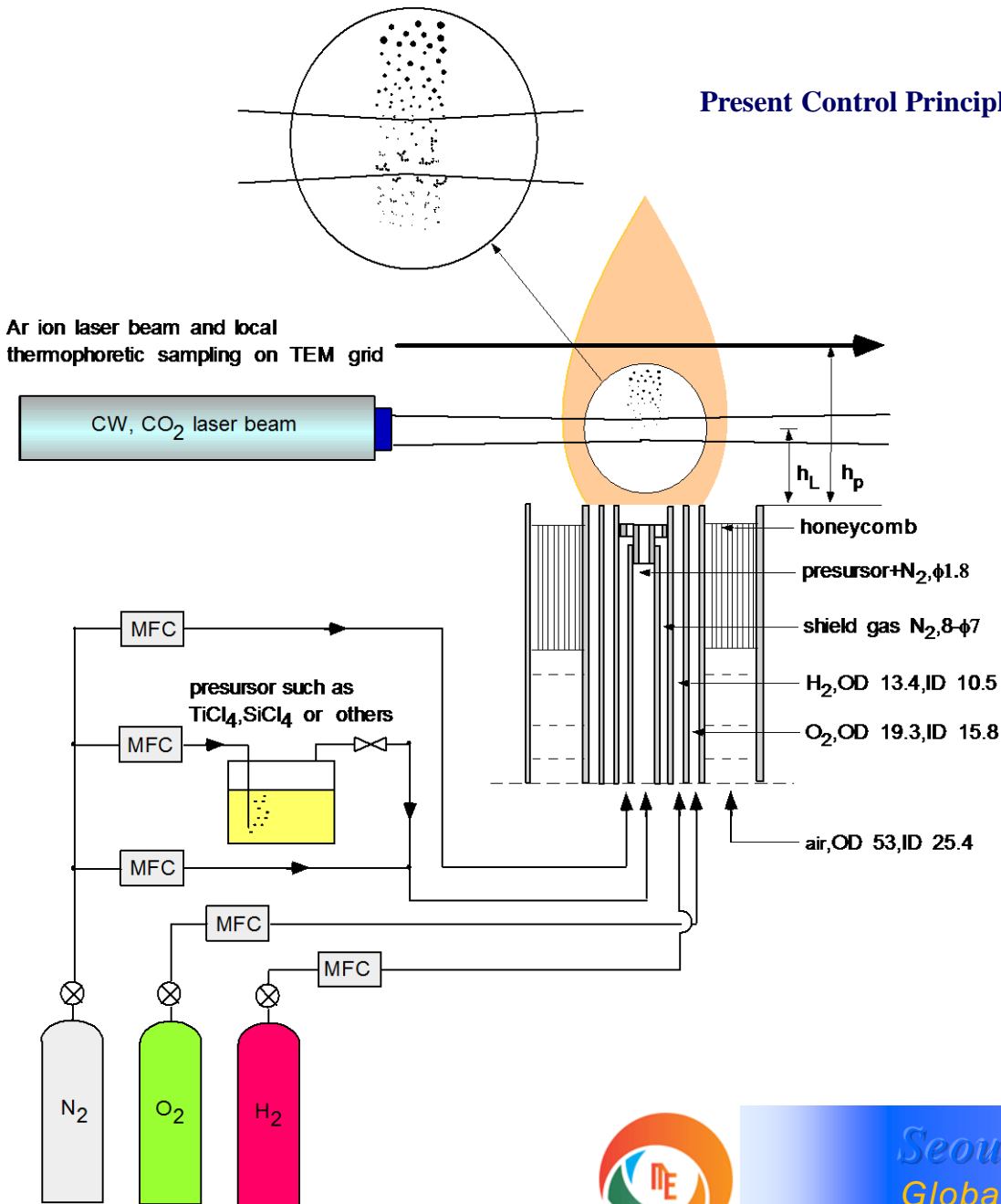
➡ Heat transfer can control the rates of collision and coalescence, then the size and morphology of nanoparticle can be controlled.

- Nanoparticle crystallinity can be also controlled by heat transfer.

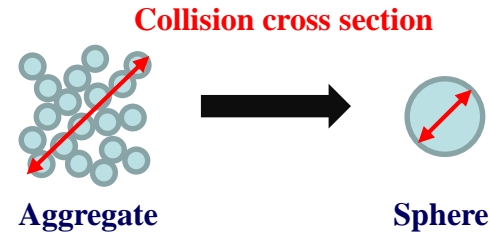


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Laser irradiation in a particle generating flame can enhance coalescence by increasing particle temperature.



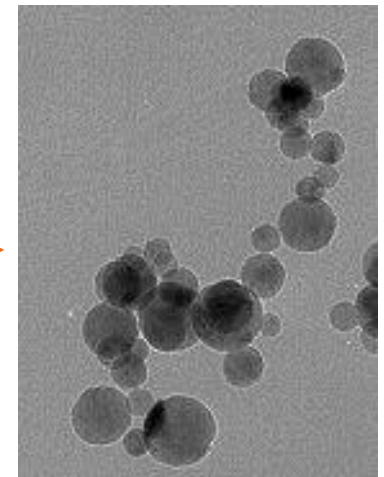
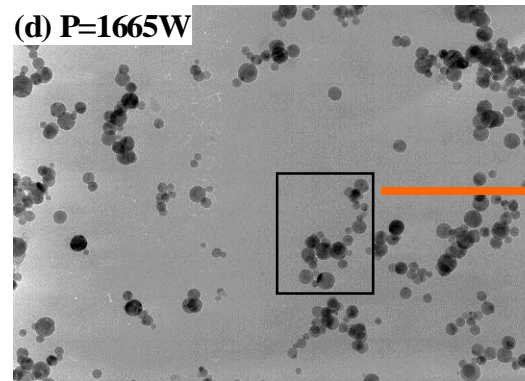
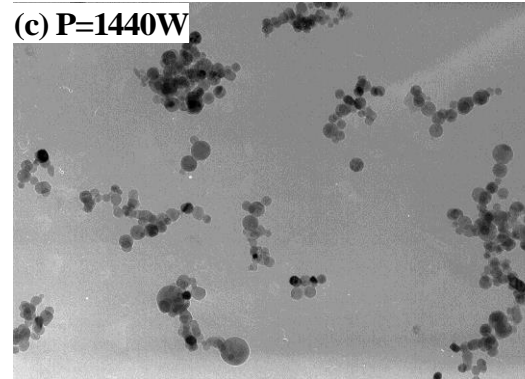
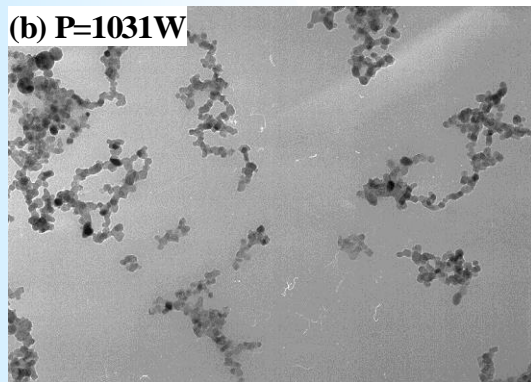
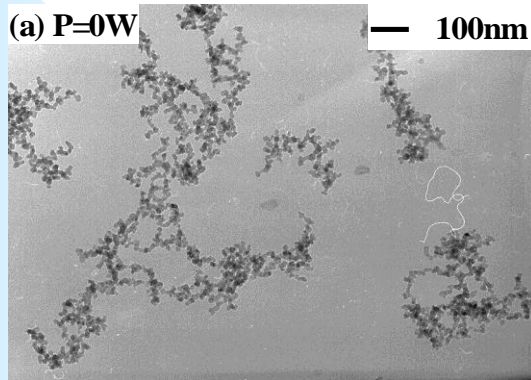
By enhancing coalescence, collision probability can be greatly reduced

➡ Much smaller and, at the same time, spherical nanoparticles at higher concentrations.



Apply the Method to Crystalline TiO₂

(Lee and Choi, 2002 J. Aerosol Science 33, 1-16)



$\text{TiCl}_4 = 9.6 \times 10^{-4} \text{ mol/min}$

$h_L = 13 \text{ mm}$

$h_P = 16 \text{ mm}$



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Variations of Size, Number Concentration and Volume Fraction

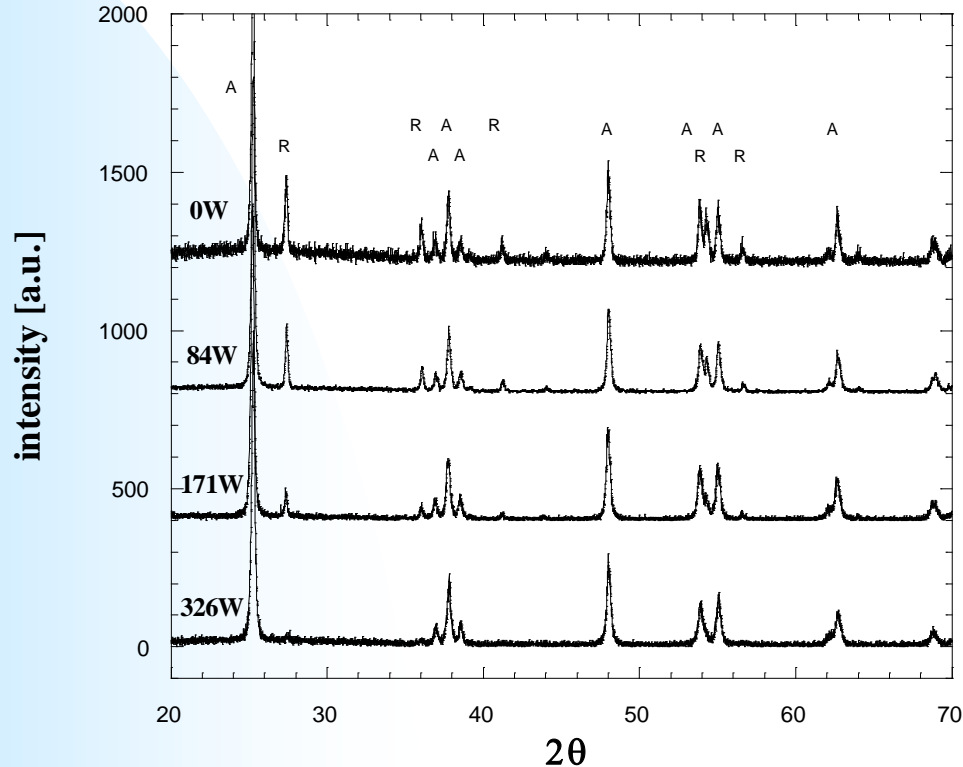
	P = 0 W	P = 2405 W	Note
d_a (nm)	109.6	20.3	
d_v (nm)	58.7	20.3	Particle volume reduction by 24 times
N (#/cm ³)	1.77×10^9	3.77×10^{10}	Particle number increase by 21 times
f_v	2.71×10^{-7}	2.49×10^{-7}	

d_a : projected area equivalent diameter

d_v : volume equivalent diameter



Transformation of Crystalline Phase



Variations of XRD profiles
; $h_L=25\text{mm}$, $h_p=65\text{mm}$

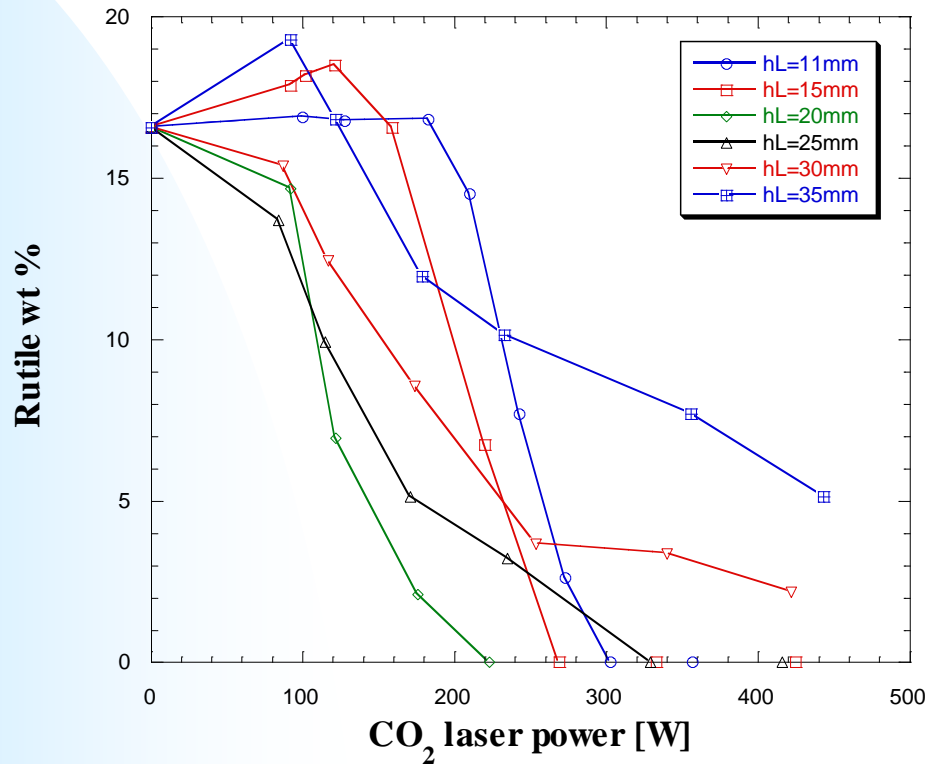
- **Surprising result : thermodynamically stable rutile has been transformed into metastable anatase.**



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Transformation of Crystalline Phase

(Lee and Choi, 2002 J. Aerosol Science 33, 1-16)



Variations of
rutile contents



Laser irradiation in an H₂/O₂ flame with C₂H₂ precursor for crystallinity control of carbon nanoparticles



without laser
irradiation



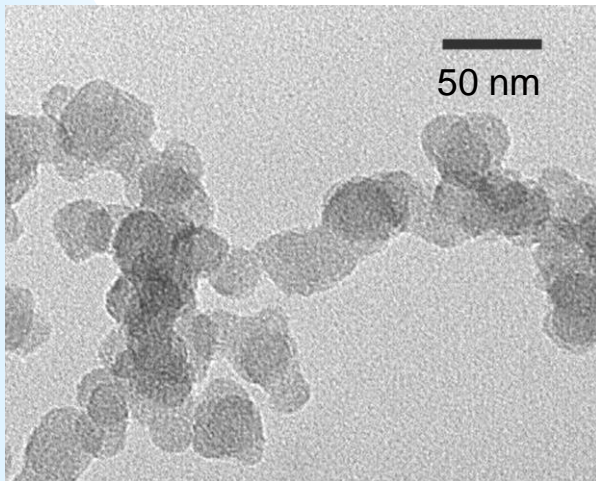
800 W



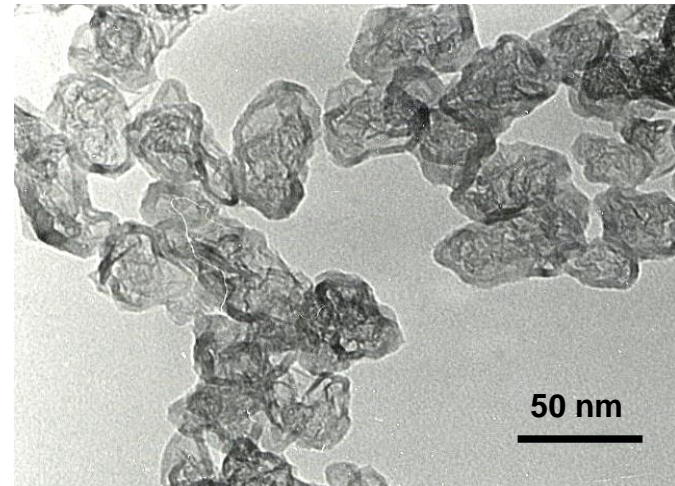
1500 W



TEM images of usual soot and shell shaped carbon particles after laser irradiation at 10 mm



Common Soot

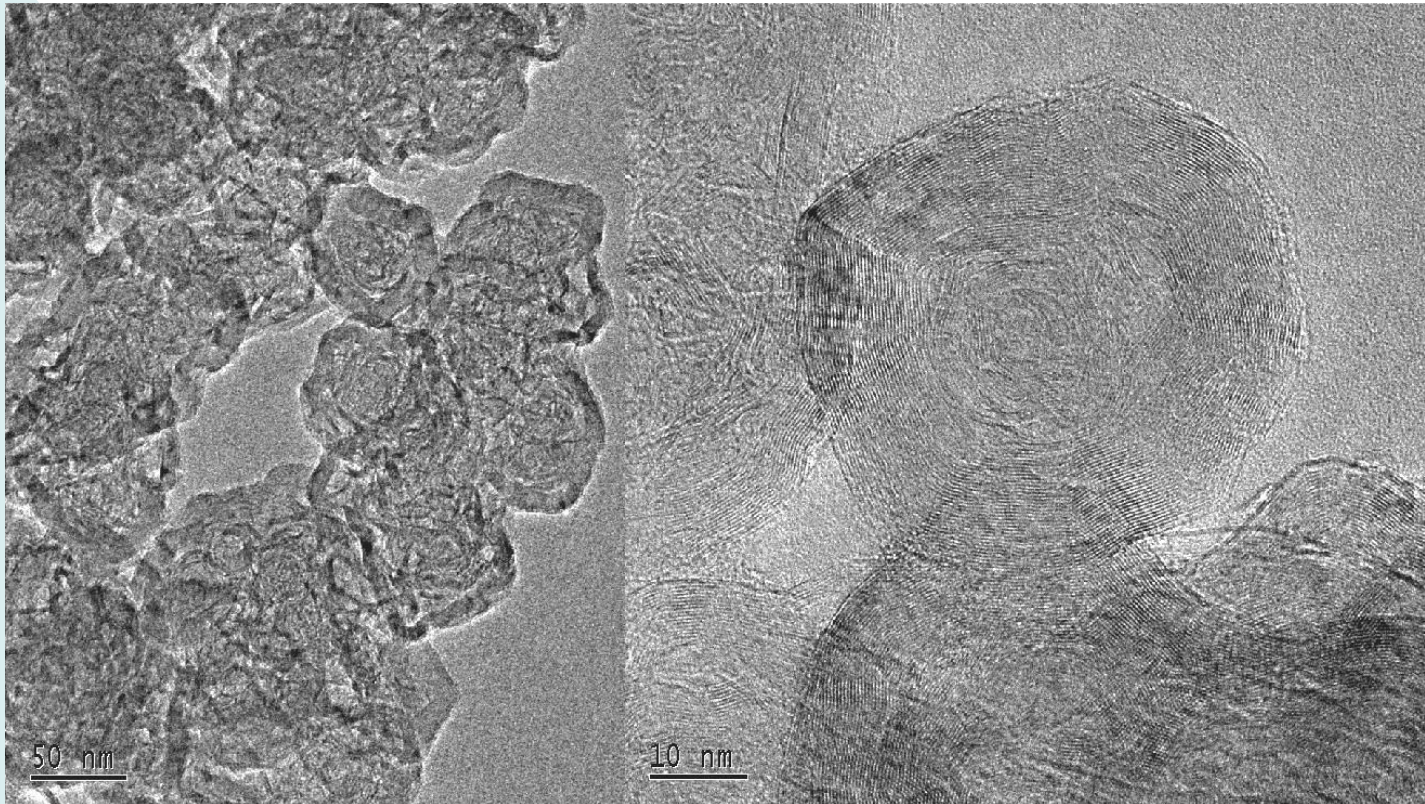


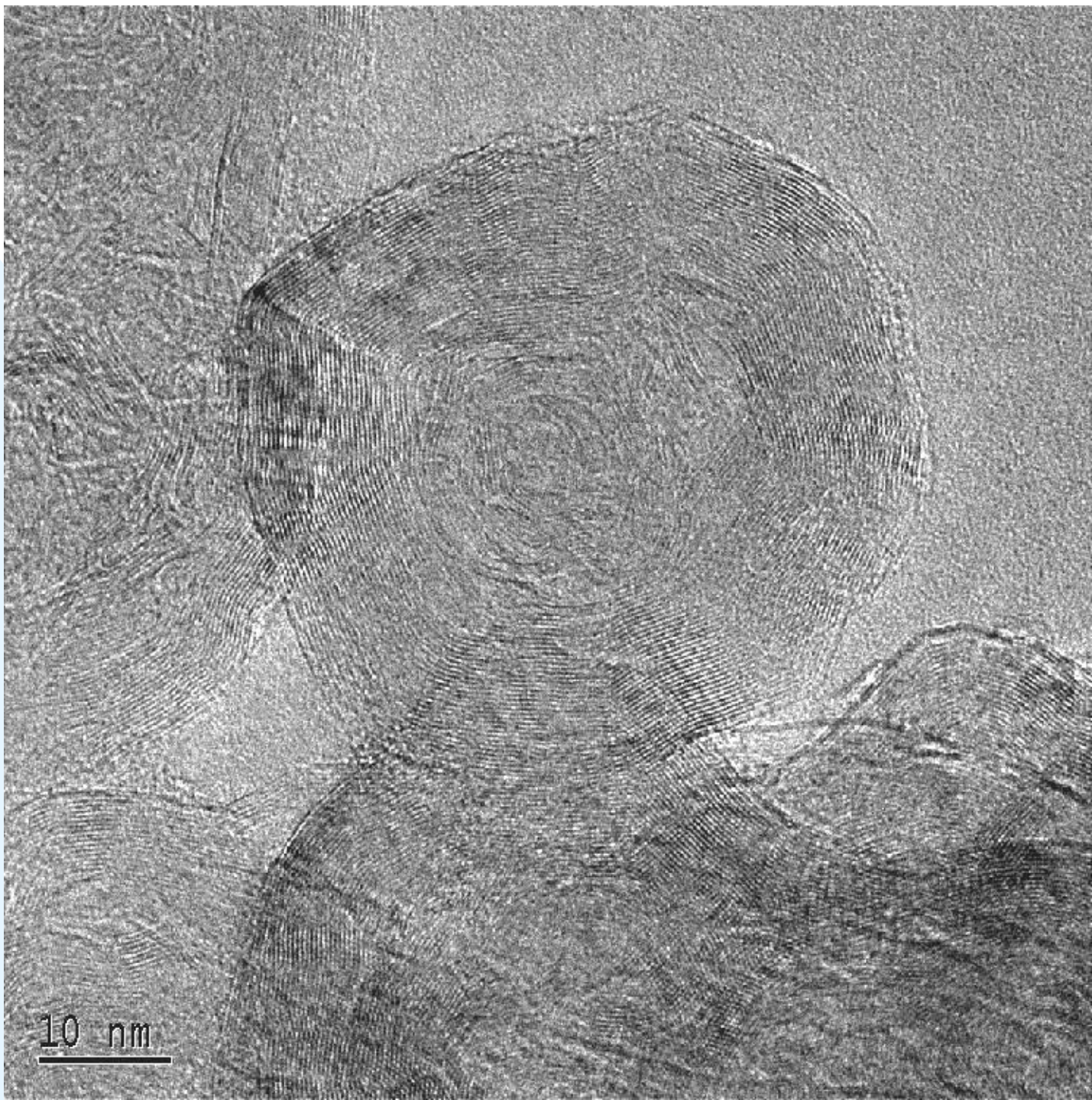
Shell-shaped carbon nanoparticles
(SCNP)



Synthesis of shell-shaped carbon nanoparticle(SCNP):

(Choi et al., Advanced Materials, 16, 1721, 2004)



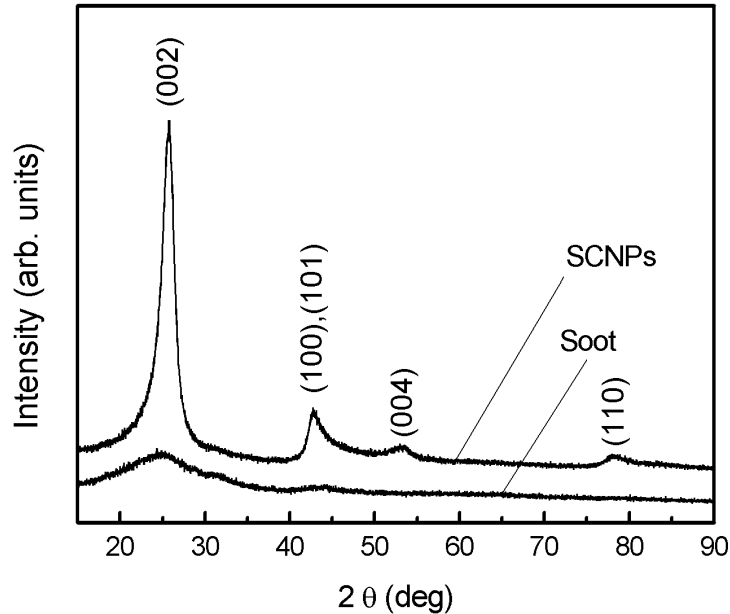


10 nm

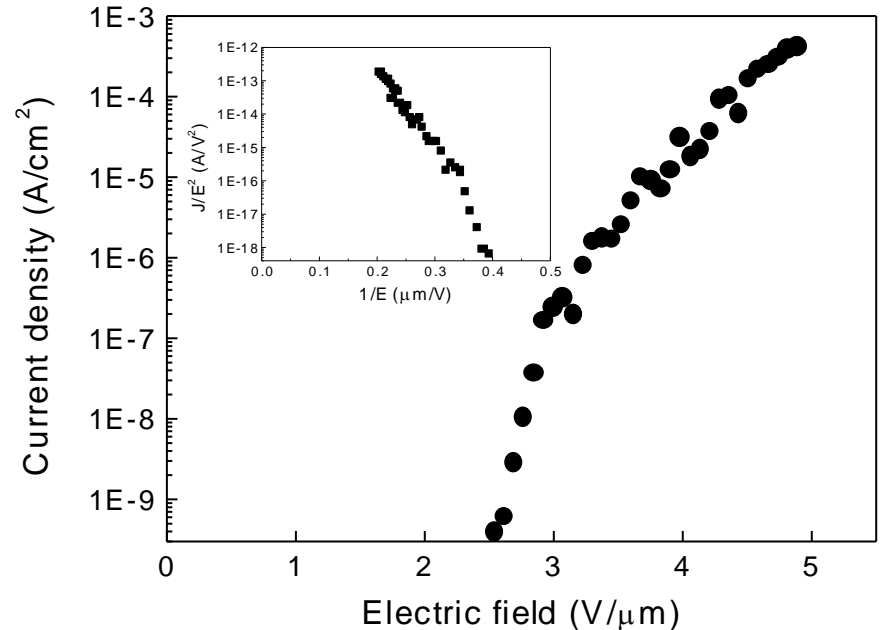
ol

Properties of SCNP

(Advanced Materials, 2004)



XRD



Field Emission Performance

: Comparable to that of Carbon Nanotubes
(Applied Physics Letters, 2004, and J. Applied
Physics, 2004)



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