

- Write CLEARLY and describe ALL details of your work.
- Answers can be written in English or Korean.
- Without a proof, you may use the information provided together.

1. (20 points) Explain the followings as much as you can.

- (a) (10 points) Boussinesq approximation  
 (b) (10 points) Rayleigh criterion for instability

2. (50 points) For a 2D flat-plate boundary-layer flow, by integrating the Prandtl's boundary-layer equation along the wall-normal direction ( $y$ ), one can derive the following equation, known as a general momentum integral (GMI). Here,  $\theta$  is momentum thickness,  $U_o$  is free-stream velocity,  $H$  is shape factor and  $c_f$  is wall-friction coefficient. Plate length is  $L$ .

$$\frac{d\theta}{dx} + (2 + H) \frac{\theta}{U_o} \frac{dU_o}{dx} = \frac{c_f}{2}$$

- (a) (10 points) Starting with the Navier-Stokes equation, derive the Prandtl's boundary-layer equation. You need to provide assumptions that you used.  
 (b) (10 points) Derive the GMI relation, given above.  
 (c) (30 points) for the following approximate flat-plate boundary-layer profile, determine the displacement thickness,  $\delta^*$ , momentum thickness,  $\theta$  and shape factor  $H$ . Use the zero-pressure gradient boundary-integral equation to find  $(\delta/x)\text{Re}_x^{1/2}$ ,  $(\delta^*/x)\text{Re}_x^{1/2}$ ,  $(\theta/x)\text{Re}_x^{1/2}$ ,  $c_f\text{Re}_x^{1/2}$ , and  $C_D\text{Re}_L^{1/2}$ . ( $C_D$  is the drag coefficient)

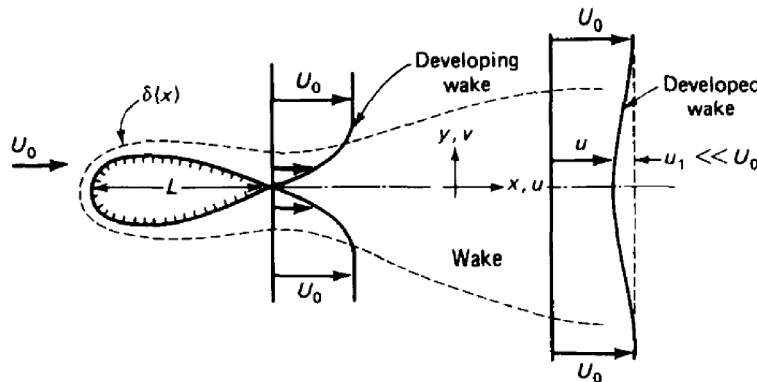
$$\frac{u}{u_\infty} = \begin{cases} \sin\left(\frac{\pi y}{2\delta}\right) & \text{for } 0 \leq y \leq \delta \\ 1 & \text{for } y > \delta \end{cases}$$

3. (30 points) Let's consider the 2D laminar wake behind a body (length of  $L$ ). Far downstream, the velocity defect ( $u_1$ ) becomes small and has a similarity solution (see the figure below) such that

$$\frac{u_1}{U_o} = 1 - \frac{u(x, y)}{U_o} \ll 1$$

- (a) (5 points) Obtain the governing equation and associated boundary conditions in terms of  $u_1$ .  
 (b) (5 points) Assuming the similarity solution ( $u_1$ ) as  $\frac{u_1}{U_o} = C \left(\frac{x}{L}\right)^{-\frac{1}{2}} g(\eta)$ , obtain the governing equation and boundary conditions for  $g(\eta)$ . If necessary, find the similarity variable  $\eta$ .

- (c) (5 points) Solve the equation in (b) to obtain  $g(\eta)$  (Hint: Try to integrate the governing equation). How does the velocity defect scale with  $y$ ?
- (d) (5 points) How can you determine the constant  $C$ ? (You don't need to calculate up to the final result.)
- (e) (10 points) If the body in consideration is a flat plate (wetted on both upper and lower sides) which has a drag coefficient of  $C_D = 2.7/\sqrt{\text{Re}_L}$ , where  $\text{Re}_L = U_0 L/\nu$ , what is the relationship between  $C_D$  and  $u_1$ ?



4. (20 points) A simple realization of a temporal boundary layer involves the spinning fluid in a cylindrical container. Consider a viscous incompressible fluid (density =  $\rho$ , viscosity =  $\mu$ ) in a solid body rotation (rotational speed at  $\Omega$ ) in a cylindrical container of diameter  $d$ . Mean depth of the fluid is  $h$ . At time  $t = 0$ , the rotation stops. Define the time taken for the fluid to stop rotating as  $\tau$ .
- (a) (10 points) For  $h \gg d$ , write a simple laminar-flow scaling law for  $\tau$ , assuming that the velocity perturbation due to the no-slip condition on the container's sidewall must travel inward a distance  $d/2$  by diffusion.
- (b) (10 points) For  $h \ll d$ , write a simple laminar-flow scaling law for  $\tau$ , assuming that the velocity perturbation due to the no-slip condition on the container's bottom wall must travel upward a distance  $h$  via diffusion.
5. (30 points) For a typical turbulent boundary layer, from the wall, three specific regimes are classified such as a wall layer, overlap layer and outer layer. For each regime, obtain the streamwise velocity distribution as a function of the distance ( $y$ ) from the wall. You need to start from a proper set of variables and the final relation should be given as a non-dimensional form.

These might be useful....

Equations for incompressible flows in Cartesian coordinates (no body force)

$$\begin{aligned} \rho \left( \frac{\partial u}{\partial t} + u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} + w \frac{\partial u}{\partial z} \right) &= -\frac{\partial p}{\partial x} + \mu \nabla^2 u \\ \frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} + \frac{\partial w}{\partial z} &= 0, \quad \rho \left( \frac{\partial v}{\partial t} + u \frac{\partial v}{\partial x} + v \frac{\partial v}{\partial y} + w \frac{\partial v}{\partial z} \right) = -\frac{\partial p}{\partial y} + \mu \nabla^2 v \\ \rho \left( \frac{\partial w}{\partial t} + u \frac{\partial w}{\partial x} + v \frac{\partial w}{\partial y} + w \frac{\partial w}{\partial z} \right) &= -\frac{\partial p}{\partial z} + \mu \nabla^2 w \end{aligned}$$