

Ch 2. Equations of fluid motion

- Continuum $K_n \equiv \lambda / l \ll 1$ λ : mean free path
 $6 \times 10^{-8} \text{ m}$
 Knudsen number

- Eulerian & Lagrangian fields l : flow length scale

$$\frac{D}{Dt} \equiv \frac{\partial}{\partial t} + \underline{U} \cdot \nabla = \frac{\partial}{\partial t} + U_1 \frac{\partial}{\partial x_1} + U_2 \frac{\partial}{\partial x_2} + U_3 \frac{\partial}{\partial x_3}$$

material derivative = local time derivative + convection by \underline{U}

$$= \frac{\partial}{\partial t} + \sum_{i=1}^3 U_i \frac{\partial}{\partial x_i}$$

$$= \frac{\partial}{\partial t} + U_i \frac{\partial}{\partial x_i} \quad \text{tensor notation}$$

- Continuity equation (mass conserv.)

$$\frac{dm}{dt} = 0$$

$$\rightarrow \frac{\partial \rho}{\partial t} + \nabla \cdot (\rho \underline{U}) = 0 \quad \rightarrow \quad \frac{\partial \rho}{\partial t} + \frac{\partial}{\partial x_i} (\rho U_i) = 0$$

$\nabla \cdot \underline{U}$: dilatation

U_i : instantaneous velocity

For const ρ , $\nabla \cdot \underline{U} = 0 \rightarrow \frac{\partial U_i}{\partial x_i} = 0$

\underline{U} is solenoidal or divergence free.

• Momentum equation

τ_{ij} : stress tensor, $\tau_{ij} = \tau_{ji}$: symmetric tensor

$$\underline{\tau} = \begin{pmatrix} \tau_{11} & \tau_{12} & \tau_{13} \\ \tau_{21} & \tau_{22} & \tau_{23} \\ \tau_{31} & \tau_{32} & \tau_{33} \end{pmatrix}$$

$i, j = 1, 2, 3$

$$\rho \frac{DU_j}{Dt} = \frac{\partial \tau_{ij}}{\partial x_i} - \rho g_j$$

$$\left(\frac{\partial U_j}{\partial t} + U_i \frac{\partial U_j}{\partial x_i} \right)$$

$$\frac{\partial}{\partial x_i} \frac{\partial U_i}{\partial x_j} = \frac{\partial}{\partial x_j} \left(\frac{\partial U_i}{\partial x_i} \right) = 0$$

$$\frac{\partial}{\partial x_i} \frac{\partial U_j}{\partial x_i} = \frac{\partial^2 U_j}{\partial x_i \partial x_i} \rightarrow \nabla^2 U_j$$

For constant-property Newtonian fluids,

$$\tau_{ij} = \underbrace{-p \delta_{ij}}_{\text{pressure}} + \underbrace{\mu \left(\frac{\partial U_i}{\partial x_j} + \frac{\partial U_j}{\partial x_i} \right)}_{\text{viscosity}}$$

$$\delta_{ij} = \begin{cases} 1 & \text{for } i=j \\ 0 & \text{for } i \neq j \end{cases}$$

$$\frac{\partial}{\partial x_i} (-p \delta_{ij}) = \frac{\partial p}{\partial x_j}$$

$$\rho \frac{DU_j}{Dt} = - \frac{\partial p}{\partial x_j} + \mu \frac{\partial^2 U_j}{\partial x_i \partial x_i} - \rho g_j$$

$\underline{g} = -\nabla\psi$ ψ : gravitational potential

$P \equiv p - \rho\psi$

$\rho \frac{D\underline{U}}{Dt} = -\frac{\partial P}{\partial x_j} + \mu \frac{\partial^2 \underline{U}}{\partial x_i \partial x_i}$

$\rho \frac{D\underline{U}}{Dt} = -\nabla p + \mu \nabla^2 \underline{U}$

$\rho \left(\frac{\partial \underline{U}}{\partial t} + U_i \frac{\partial \underline{U}}{\partial x_i} \right) = -\frac{\partial p}{\partial x_j} + \mu \frac{\partial^2 \underline{U}}{\partial x_i \partial x_i}$

$\frac{D\underline{U}}{Dt} = -\frac{1}{\rho} \nabla p + \nu \nabla^2 \underline{U}$
 ← kinematic viscosity

Navier-Stokes eq.

For inviscid flow ($\mu=0$), $\tau_{ij} = -p\delta_{ij}$

$\frac{D\underline{U}}{Dt} = -\frac{1}{\rho} \nabla p$ Euler equation

• Role of pressure

$\nabla \cdot \left[\left(\frac{D}{Dt} - \nu \nabla^2 \right) \underline{U} \right] = -\frac{1}{\rho} \nabla p$

$\nabla \cdot \nabla p = \nabla^2 p$

$\rightarrow \left(\frac{D}{Dt} - \nu \nabla^2 \right) (\nabla \cdot \underline{U}) + \left[\nabla \cdot \left(\frac{D}{Dt} - \nu \nabla^2 \right) \underline{U} \right] = -\frac{1}{\rho} \nabla^2 p$

$$\frac{\partial}{\partial x_j} \left(\frac{\partial}{\partial t} + u_i \frac{\partial}{\partial x_i} \right) u_j = \frac{\partial}{\partial x_j} \left(\nu \frac{\partial}{\partial x_i} \right) u_j$$

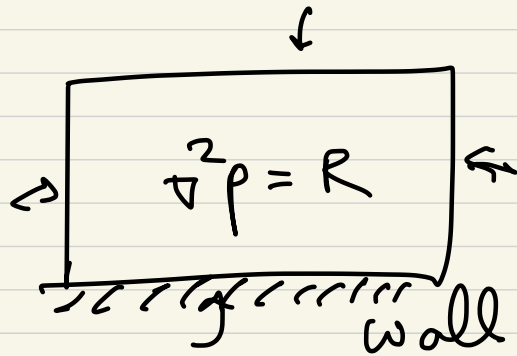
$$= \frac{\partial u_i}{\partial x_j} \frac{\partial u_j}{\partial x_i}$$

$$\rightarrow 0 = -\frac{1}{\rho} \frac{\partial^2 p}{\partial x_i \partial x_i} - \frac{\partial u_i}{\partial x_j} \frac{\partial u_j}{\partial x_i}$$

$$\frac{\partial^2 p}{\partial x_i \partial x_i} = -\rho \frac{\partial u_i}{\partial x_j} \frac{\partial u_j}{\partial x_i}$$

\parallel
 $\nabla^2 p$

\mid
 incomp. flow
 Poisson eq.



① wall, $\underline{u} = 0$

$$\frac{\partial \underline{u}}{\partial t} + (\underline{u} \cdot \nabla) \underline{u} = -\frac{1}{\rho} \nabla p + \nu \nabla^2 \underline{u}$$

② wall, $\frac{\partial p}{\partial n} \Big|_{\text{wall}} = \mu \frac{\partial^2 u_n}{\partial n^2} \Big|_{\text{wall}} = \mathcal{O}(\epsilon)$

If p is a sol., $p + C$ is also a sol.

Comp. flow: $\rho, \underline{u}, T, P$ state eq.
 \uparrow energy eq.

Using Green ft.,

$$P(\underline{x}, t) = P^{(h)}(\underline{x}, t) + \frac{\rho}{4\pi} \iint_V \left. \frac{\partial u_i}{\partial x_j} \frac{\partial u_j}{\partial x_i} \right|_{y, t} \frac{dy}{|x-y|}$$

homo. sol.

• Conserved passive scalars

$\phi(\underline{x}, t)$: conserved passive scalar

In a constant-property flow,

$$\frac{D\phi}{Dt} = \Gamma \nabla^2 \phi$$

Γ : (const & uniform) diffusivity

"

$$\frac{\partial}{\partial x_i} \left(\Gamma \frac{\partial \phi}{\partial x_i} \right) \leftarrow$$

$$\frac{\partial \phi}{\partial t} + (\underline{U} \cdot \nabla) \phi$$

⇓

$$\frac{\partial \phi}{\partial t} + \underbrace{U_i \frac{\partial \phi}{\partial x_i}}_{\phi^0} = \frac{\partial \phi}{\partial t} + \frac{\partial}{\partial x_i} (U_i \phi) - \phi \frac{\partial U_i}{\partial x_i}$$

$$\Rightarrow \frac{\partial \phi}{\partial t} + \frac{\partial}{\partial x_i} (U_i \phi) = \frac{\partial}{\partial x_i} \left(\Gamma \frac{\partial \phi}{\partial x_i} \right)$$

ϕ is conserved because there is no source/sink in this eq.

$$\frac{\partial}{\partial t} \int \phi dt = 0$$

ϕ is passive because it does not change the flow.

ϕ can be temperature $\rightarrow \Gamma$: thermal diffusivity
 $P_r = \nu / \Gamma$

concentration $\rightarrow \Gamma$: molecular diffusivity
 $S_c = \nu / \Gamma$

* boundedness : If the initial and boundary values of ϕ lie within a given range

$$\phi_{\min} \leq \phi \leq \phi_{\max},$$

then $\phi(x, t)$ for all (x, t) also lies in this range.

That is, the values of ϕ greater than ϕ_{\max} or less than ϕ_{\min} cannot occur.

• Vorticity equation

turbulent flow \rightarrow rotational \rightarrow non-zero vorticity $\underline{\omega} \neq 0$

vorticity $\underline{\omega} = \nabla \times \underline{U}$

$\nabla \times$ [N-S eq.]:

vorticity equation

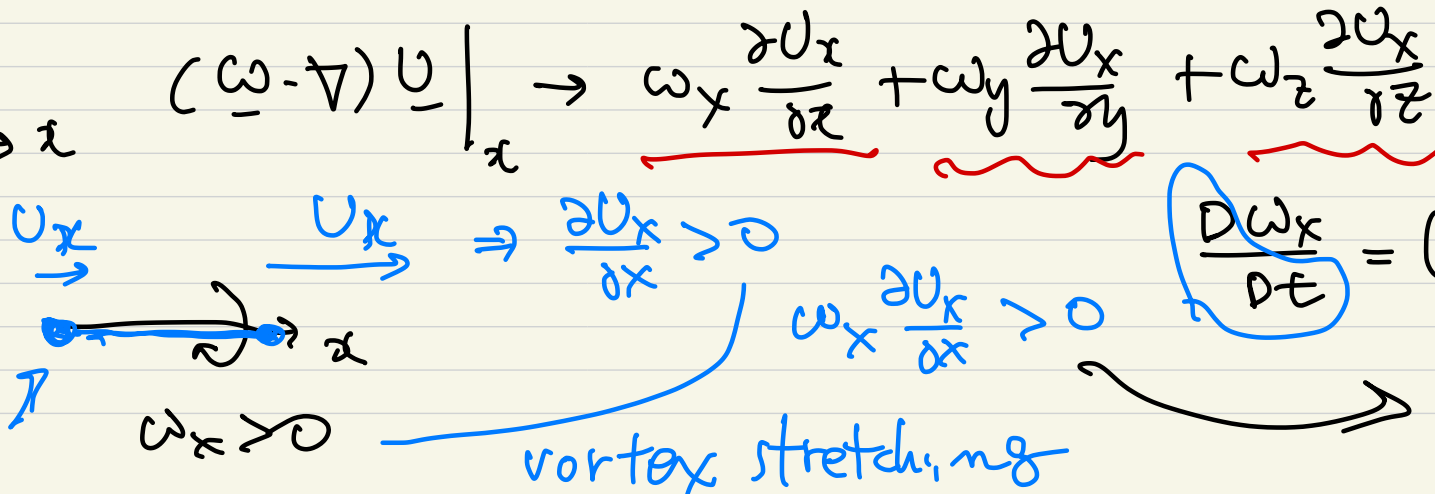
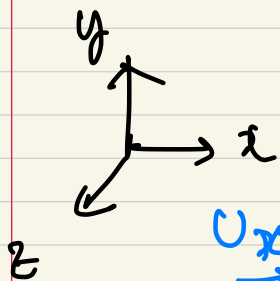
$$\frac{D\underline{\omega}}{Dt} = \frac{\partial \underline{\omega}}{\partial t} + (\underline{U} \cdot \nabla) \underline{\omega} = \underbrace{(\underline{\omega} \cdot \nabla) \underline{U}}_{\text{vortex stretching term}} + \nu \nabla^2 \underline{\omega}$$

$$\frac{\partial \phi}{\partial t} + (\underline{U} \cdot \nabla) \phi = \nu \nabla^2 \phi$$

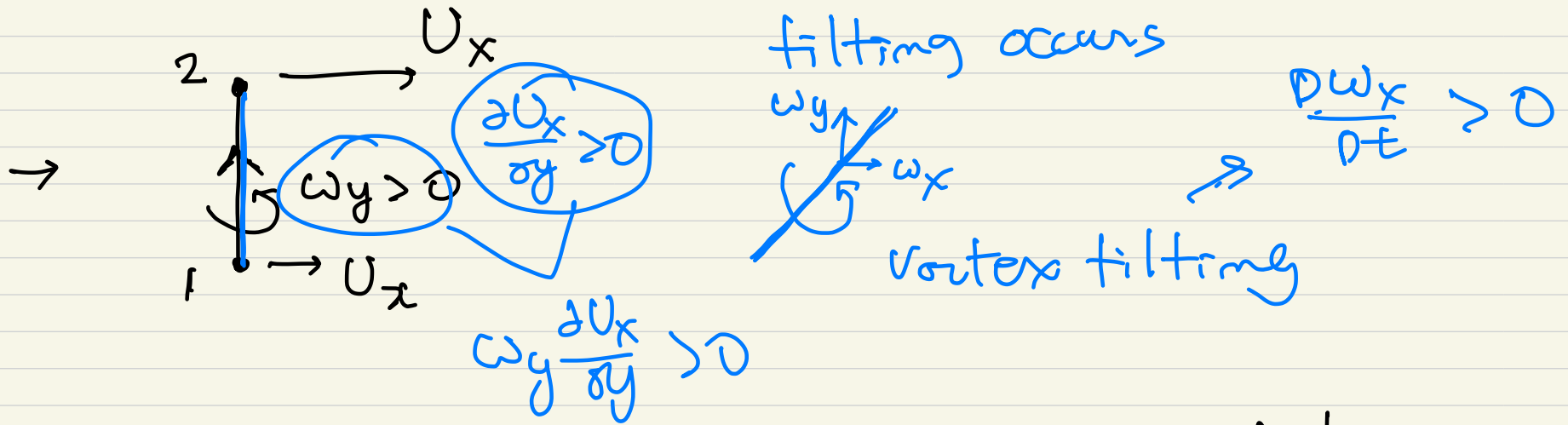
$$\frac{\partial \underline{U}}{\partial t} + (\underline{U} \cdot \nabla) \underline{U} = \underbrace{-\frac{1}{\rho} \nabla p}_{\text{increases } |\underline{\omega}|} + \nu \nabla^2 \underline{U}$$

vortex stretching term

increases $|\underline{\omega}|$



$$\frac{D\omega_x}{Dt} = \underbrace{(\underline{\omega} \cdot \nabla) U_x}_x + \underbrace{\nu \nabla^2 \omega_x}_{\text{decaying}} > 0$$



In inviscid flow, the vorticity vector behaves in the same way as an infinitesimal material line element.

$$\left(\frac{D\underline{\xi}}{Dt} = (\underline{\xi} \cdot \nabla) \underline{v} \right) \text{ for material line}$$

2-D flow (u, v) \rightarrow $\omega_z \neq 0 \Rightarrow (\underline{\omega} \cdot \nabla) \underline{v} = 0$ no vortex stretching

u_x, u_y $\omega_x = \omega_y = 0$ $\frac{D\underline{\omega}}{Dt} = \nu \nabla^2 \underline{\omega}$

↳ one component of $\underline{\omega}$ evolves as a conservative passive scalar.

