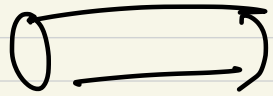
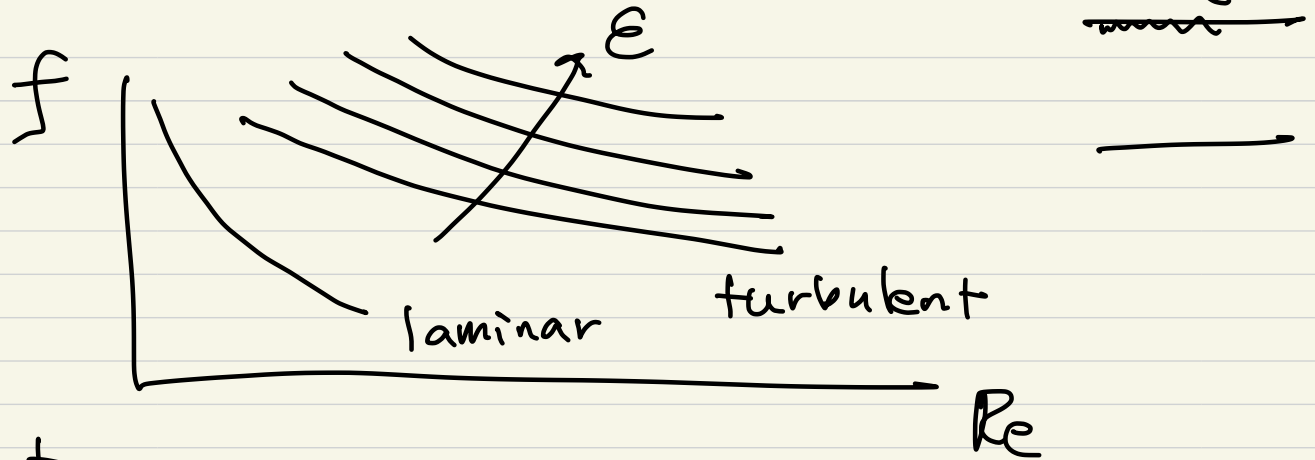
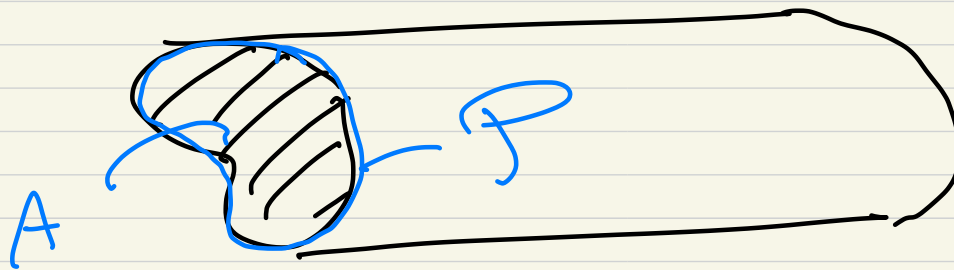


Moody chart



Non-circular duct

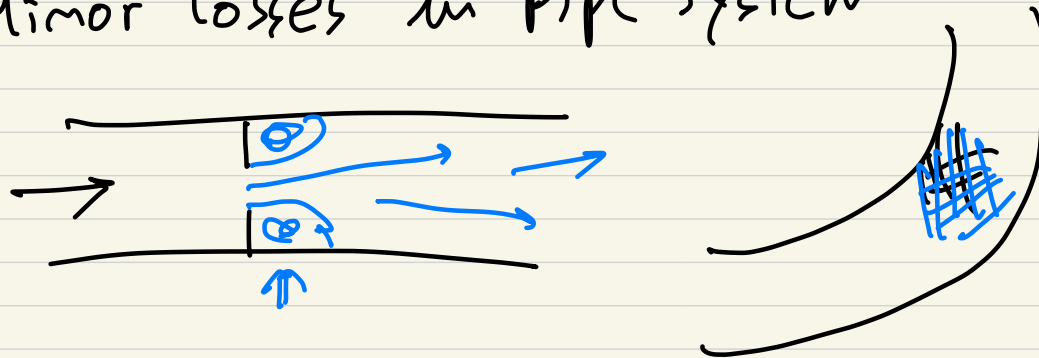


$$D_h \equiv 4A/P$$

hydraulic diameter $\epsilon \cdot \frac{I d^2}{2\pi r} = (d)$

$$Re_{D_h} = V D_h / \nu$$

Minor losses in pipe system



Diffuser

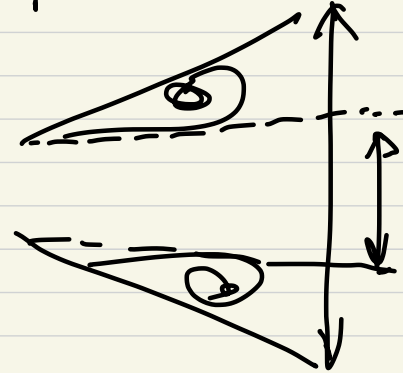
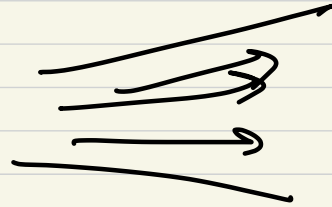
V_1

A_1

$$\rightarrow V_2 < V_1 \Rightarrow P_2 > P_1$$

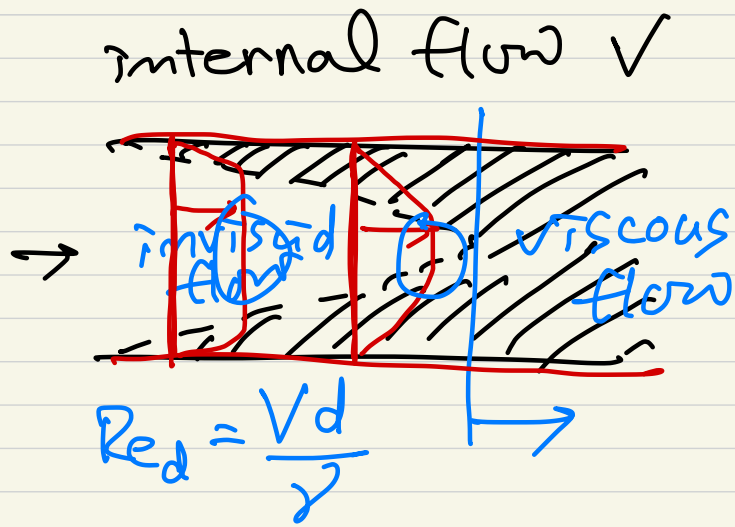
$$A_2 > A_1$$

$$\rho_1 A_1 V_1 = \rho_2 A_2 V_2$$

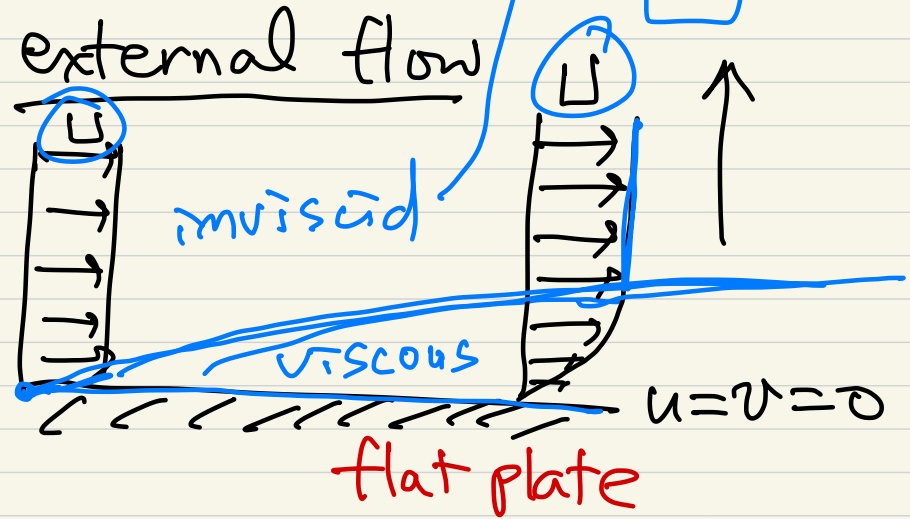


Fluid meters (orifice
nozzle
venturi

Ch. 7 Flow past immersed bodies

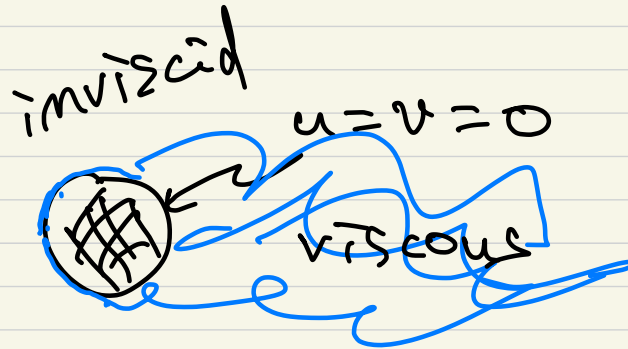


vs. \rightarrow



U

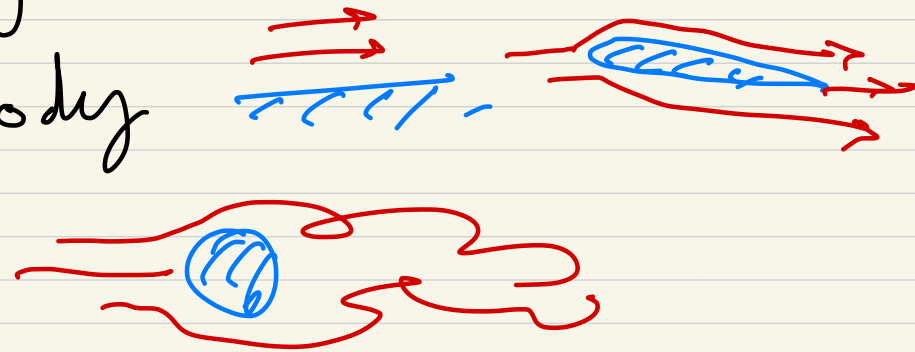
\rightarrow



7.1 Reynolds number and geometry effects

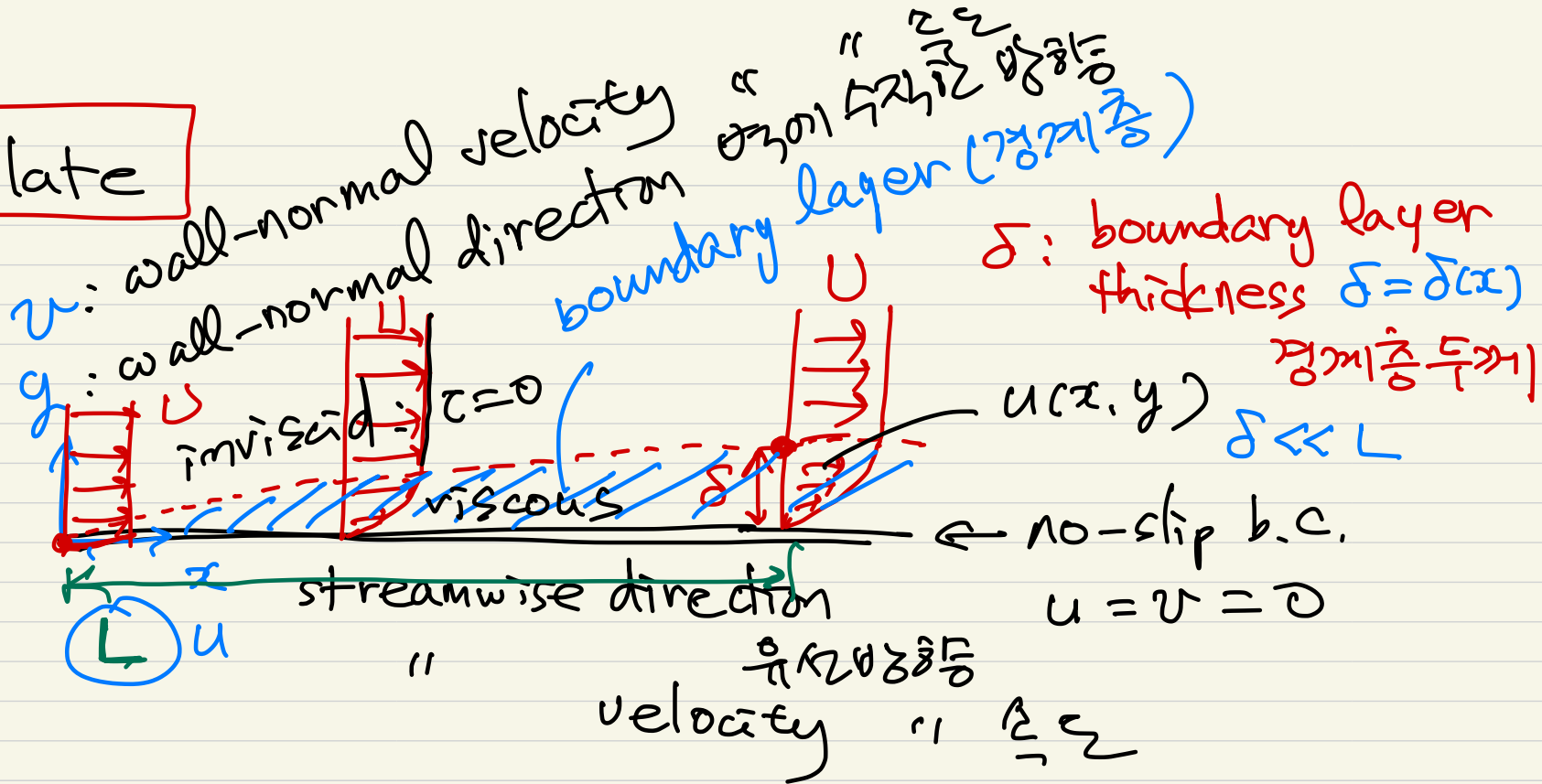
two types : (

- streamlined body
- bluff body

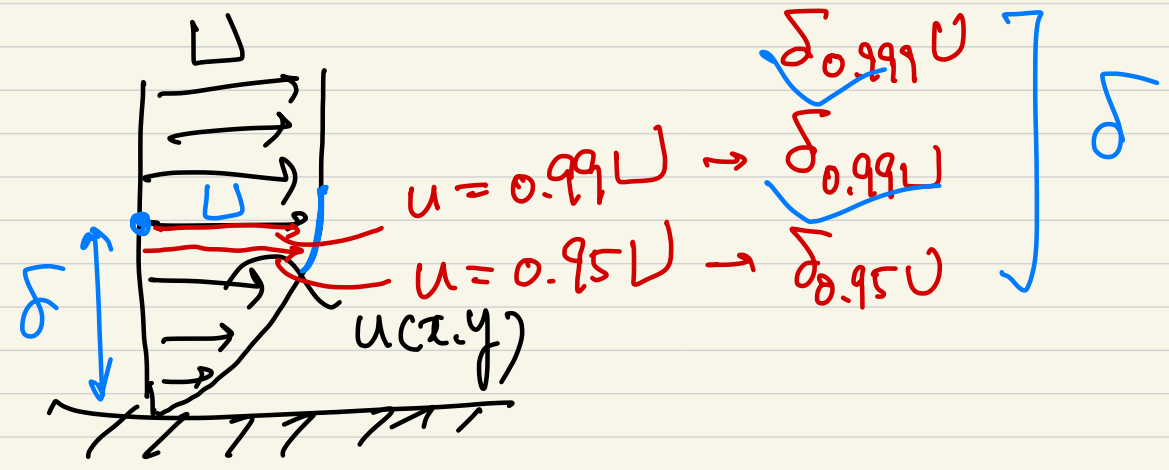


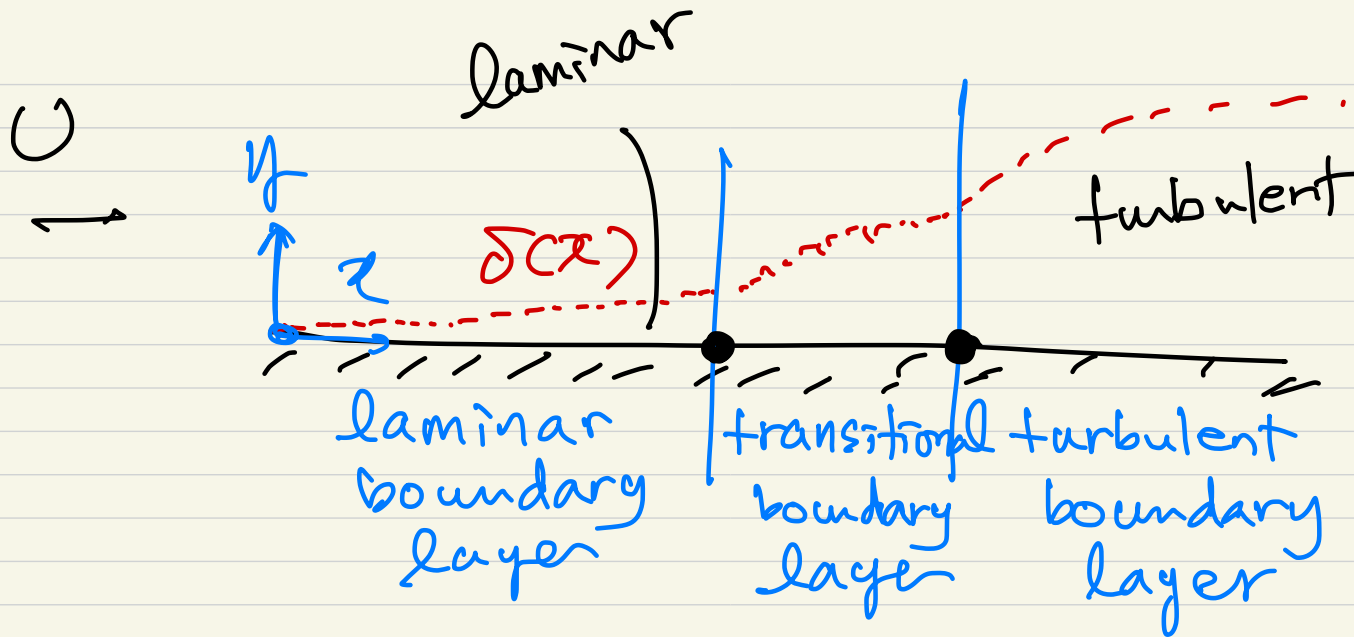
Flat plate

U
 \rightarrow
 free-stream velocity
 자유유동속도



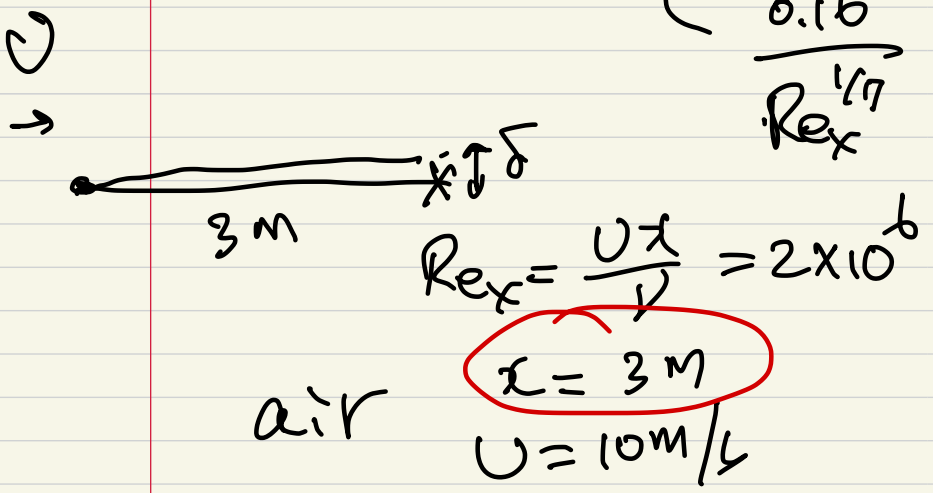
$Re_x = \frac{Ux}{\nu}$, $Re_\delta = \frac{U\delta}{\nu}$ vs. $Re_d = \frac{Ud}{\nu}$





$Re_d = \frac{Ud}{\nu}$
 $\nu = \frac{\mu}{\rho}$
 > 2500 turb
 $< \approx$ lam.

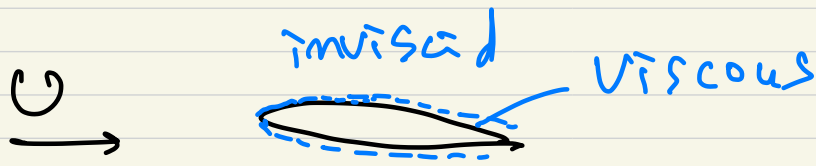
$\frac{\delta}{x} = \begin{cases} \frac{5.0}{\sqrt{Re_x}} & \text{laminar Blasius (1908)} \\ \frac{0.16}{Re_x^{1/4}} & \text{turbulent} \end{cases}$
 $\delta_{lam} \sim x^{1/2}$
 $\delta_{turb} \sim x^{4/5}$



$Re_x = \frac{Ux}{\nu} = 2 \times 10^6$
 $x = 3\text{m}$
 $U = 10\text{m/s}$

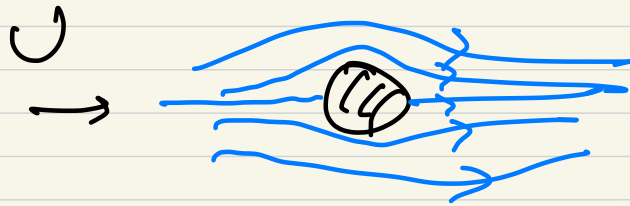
$\delta_{lam.} = \frac{5.0 \times 3}{\sqrt{2 \times 10^6}} \approx 1\text{cm}$
 $\delta_{turb} = \frac{0.16 \times 3}{(2 \times 10^6)^{1/4}} = 6\text{cm}$
 thin boundary layer

• flow around slender bodies



plates } thin boundary layer
airfoils }

• flow around bluff bodies

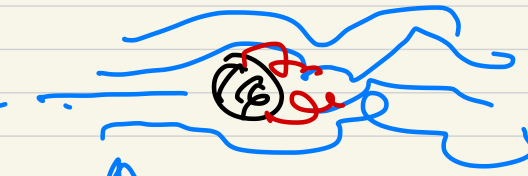


↑
theory
Stokes flow

$U \uparrow \rightarrow Re \uparrow$

flow separation
유동박리

theory

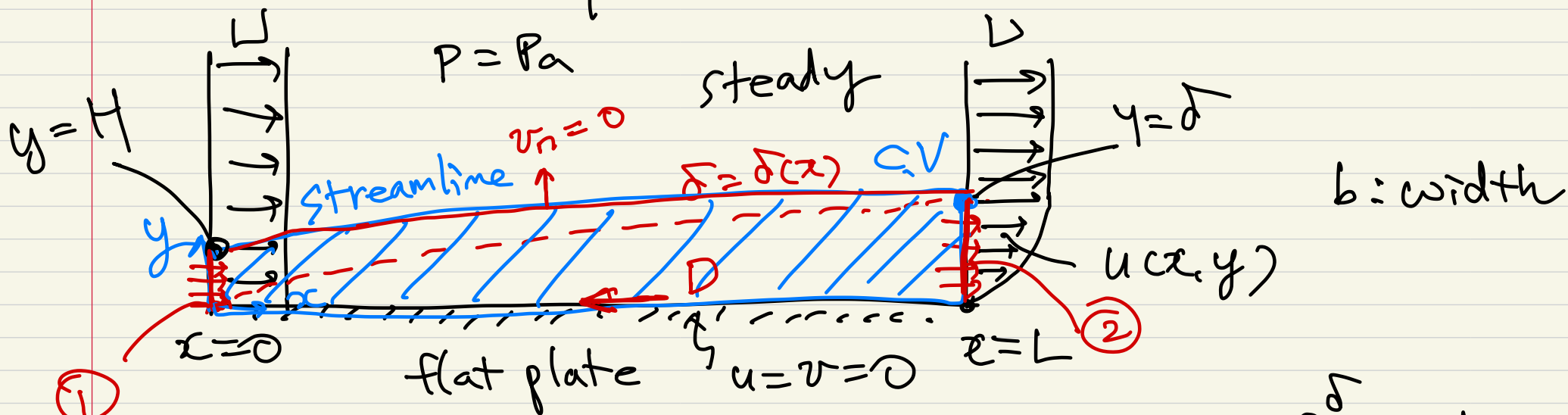


theory fails

↳ experiment

CFD
Computational
fluid dynamics

7.2 Momentum - integral estimates



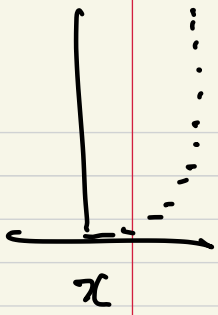
Continuity: $UH = \int_0^{\delta} u dy \rightarrow U^2 H = \int_0^{\delta} u U dy$

x-mom: $\Sigma F_x = -D = \int_{CS} \rho u (\underline{V} \cdot \underline{n}) dA = \int_0^{\delta} \rho u^2 dy \cdot b - \rho U^2 H b$

$= \rho b \left(\int_0^{\delta} u^2 dy - \int_0^{\delta} u U dy \right)$

$\therefore D = \rho b \int_0^{\delta} (uU - u^2) dy = \rho b U^2 \int_0^{\delta} \frac{u}{U} \left(1 - \frac{u}{U}\right) dy$

$\equiv \theta(x)$



$$\theta = \int_0^{\delta} \frac{u}{U} \left(1 - \frac{u}{U}\right) dy$$

: momentum thickness
 운동량 두께

$$D(x) = \rho b U^2 \theta(x)$$

$$\rightarrow \frac{dD}{dx} = \rho b U^2 \frac{d\theta}{dx}$$

$$D(x) \equiv \int_0^x \tau_w(x) dx \cdot b \rightarrow \frac{dD}{dx} = \tau_w b$$

$$\tau_w = \rho U^2 \frac{d\theta}{dx}$$

wall shear stress
 벽 전단 응력

$$c_f \equiv \frac{\tau_w}{\frac{1}{2} \rho U^2}$$

skin-friction coefficient
 마찰 계수

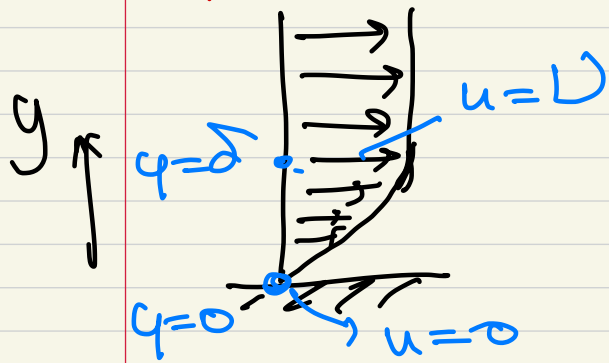
$$= 2 \frac{d\theta}{dx}$$

$$\frac{c_f}{2} = \frac{d\theta}{dx}$$

momentum-integral relation for flat-plate boundary layer flow

Valid for laminar & turbulent flows

• von Karman's assumption on velocity profile



$$\left. \begin{aligned} u &= 0 @ y=0 \\ u &= U @ y=\delta \\ \frac{\partial u}{\partial y} &= 0 @ y=\delta \end{aligned} \right\}$$

$$u = a + by + cy^2$$

$$u(x,y) = U \left(\frac{2y}{\delta} - \frac{y^2}{\delta^2} \right) \quad 0 \leq y \leq \delta$$

$$\theta = \int_0^{\delta} \frac{u}{U} \left(1 - \frac{u}{U} \right) dy = \frac{2}{15} \delta$$

$$\tau_w = \mu \left. \frac{\partial u}{\partial y} \right|_{y=0} = \frac{\mu \cdot 2U}{\delta} = \rho U^2 \frac{d\theta}{dx} = \frac{2}{15} \rho U^2 \frac{d\delta}{dx}$$

$$\rightarrow \frac{\delta^2}{2} = 15 \frac{\nu x}{U}$$

$$\rightarrow \frac{\delta}{x} = 5.5 \sqrt{\frac{\nu}{Ux}} = \frac{5.5}{\sqrt{Re_x}}$$

$$\rightarrow \delta \sim \sqrt{x} \quad \text{cf. } \frac{\delta}{x} = \frac{5.0}{\sqrt{Re_x}} \text{ Blasius}$$

$$\mu \frac{\partial u}{\partial y} = \frac{2}{15} \rho U^2 \frac{d\delta}{dx}$$

$$\frac{1}{15} \frac{\mu}{\rho U} \frac{dx}{x} = \delta d\delta$$

$$\frac{1}{15} \frac{\nu}{Ux} dx = \frac{\delta^2}{2} d\delta$$

$$\frac{\theta}{x} = \theta \cdot \frac{1}{x} = \frac{2}{15} \frac{5.5}{\sqrt{Re_x}} = \frac{0.733}{\sqrt{Re_x}} \rightarrow \theta \sim \sqrt{x}$$

$$C_f = \frac{\tau_w}{\frac{1}{2} \rho U^2} = \frac{2 \mu U / \delta}{\frac{1}{2} \rho U^2} = \frac{4 \mu}{\rho U \delta} = \frac{x}{\delta} \cdot \frac{4 \mu}{\rho U x} = \frac{0.773}{\sqrt{Re_x}}$$

$$\rightarrow C_f \sim x^{-\frac{1}{2}}$$

$$C_f = \frac{0.664}{\sqrt{Re_x}} \text{ Blasius } \uparrow \text{ 10\% error}$$

