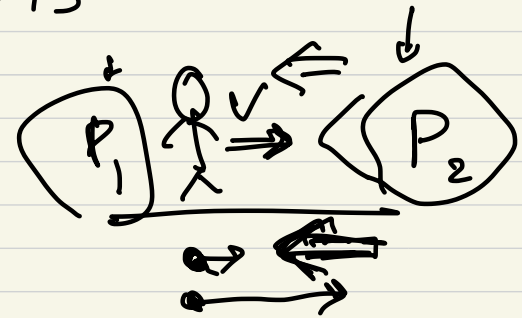


7.5 Boundary layers with pressure gradients

flat plate : $U = \text{const} \rightarrow \frac{dp}{dx} = 0$



$\frac{dp}{dx} > 0$: adverse pres. grad
on, of, z, z, z, v, y

$\frac{dp}{dx} < 0$: favorable " "

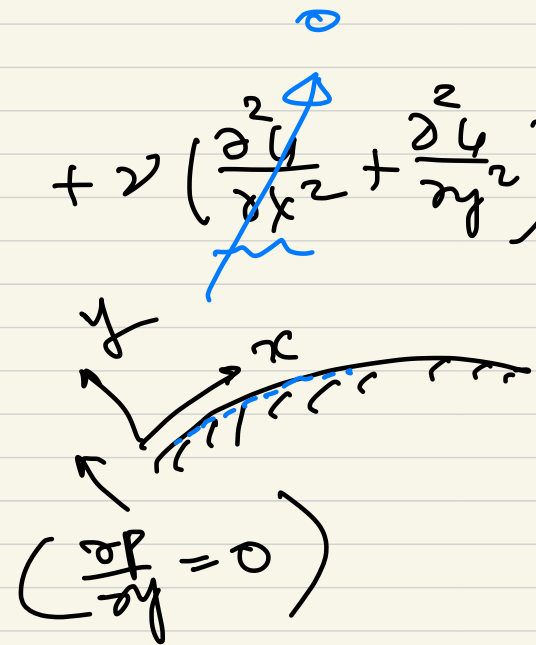
N-S eq. : $\frac{\partial u}{\partial t} + u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} = -\frac{1}{\rho} \frac{\partial p}{\partial x} + \nu \left(\frac{\partial^2 u}{\partial x^2} + \frac{\partial^2 u}{\partial y^2} \right)$

@ $y=0$ (wall), $u=v=0$ (no slip)

N-S $\Rightarrow 0 = -\frac{1}{\rho} \frac{\partial p}{\partial x} + \nu \frac{\partial^2 u}{\partial y^2} \Big|_w$

$\frac{\partial^2 u}{\partial y^2} \Big|_w = \frac{1}{\nu} \frac{dp}{dx}$

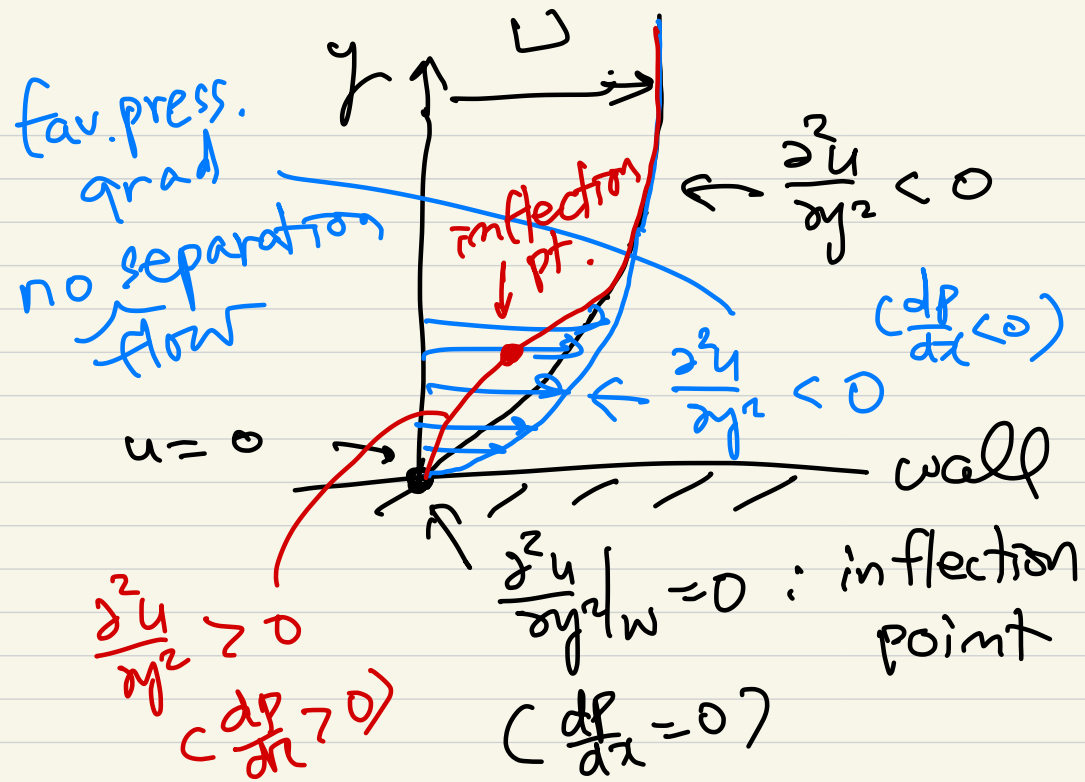
↳ Curvature



if $\frac{dp}{dx} = 0$, $\frac{\partial^2 u}{\partial y^2}|_w = 0$

$\frac{dp}{dx} < 0$, $\frac{\partial^2 u}{\partial y^2}|_w < 0$

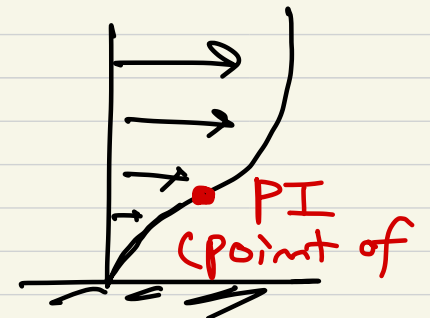
$\frac{dp}{dx} > 0$, $\frac{\partial^2 u}{\partial y^2}|_w > 0$



→ Any boundary layer profile in an adverse press. grad. exhibits a characteristic S shape.

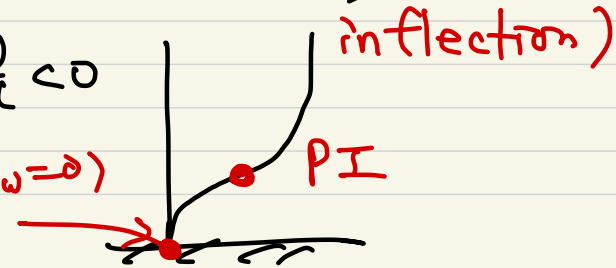
zero press. grad. → $\frac{dp}{dx} = 0$, $\frac{du}{dx} = 0$, no sep.

weak adverse grad → $\frac{dp}{dx} > 0$ → $\frac{du}{dx} < 0$
press. no separation



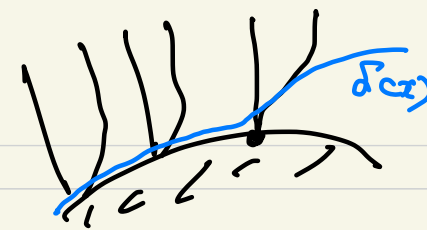
critical adverse press. grad. → $\frac{dp}{dx} > 0$ → $\frac{du}{dx} < 0$

separation pt. $\frac{\partial u}{\partial y}|_w = 0$ ($u_w = 0$)



6
separation starts

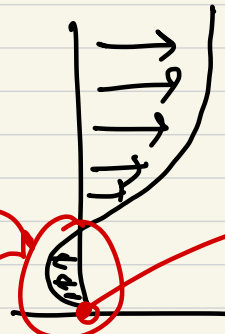
→ boundary layer thickness ↑



excessive adv. press. grad

↓
separated flow region exists

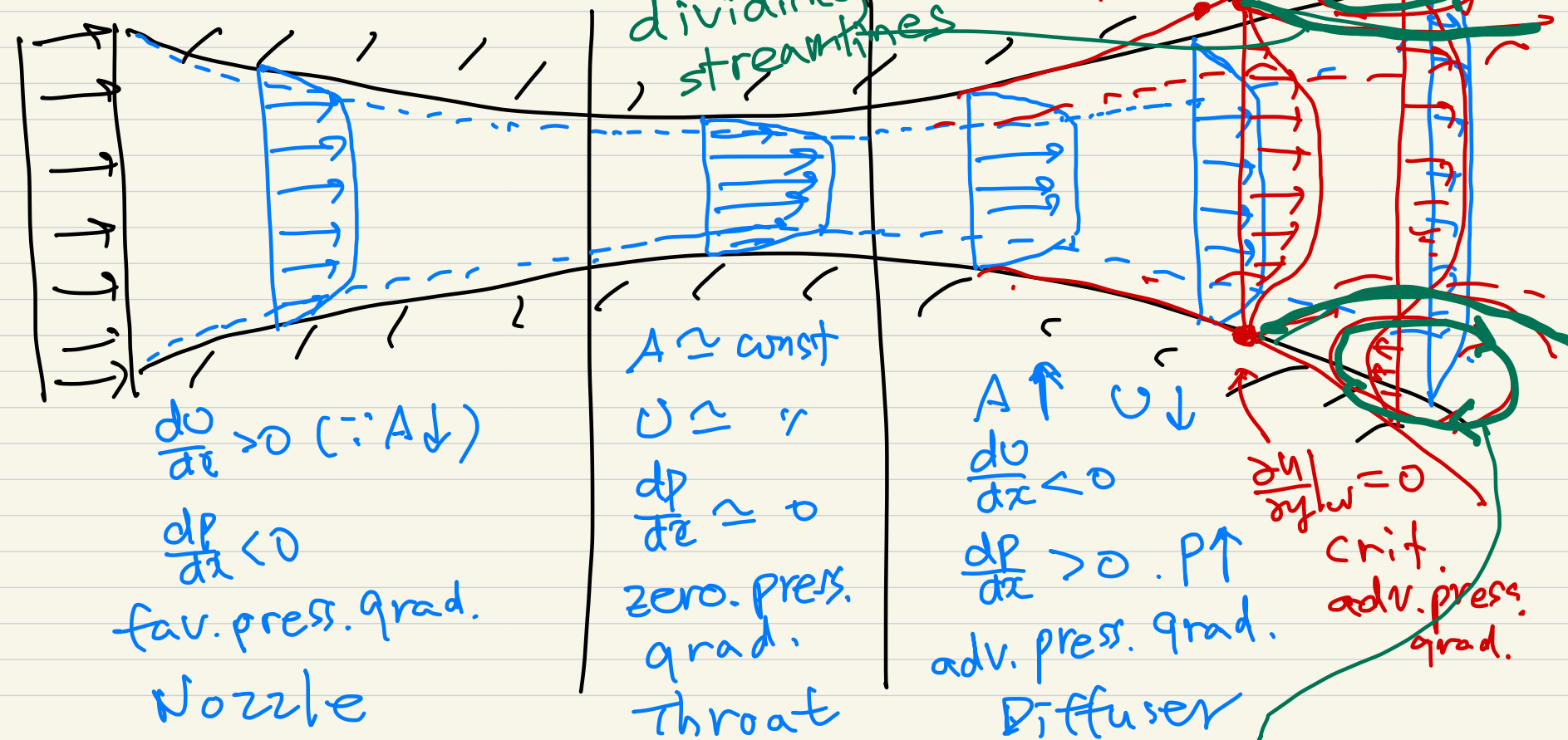
back-flow
reverse flow



$$\frac{\partial u}{\partial y}|_w < 0$$

separation bubble

separation region



$\frac{du}{dx} > 0$ ($\because A \downarrow$)
 $\frac{dp}{dx} < 0$
fav. press. grad.
Nozzle

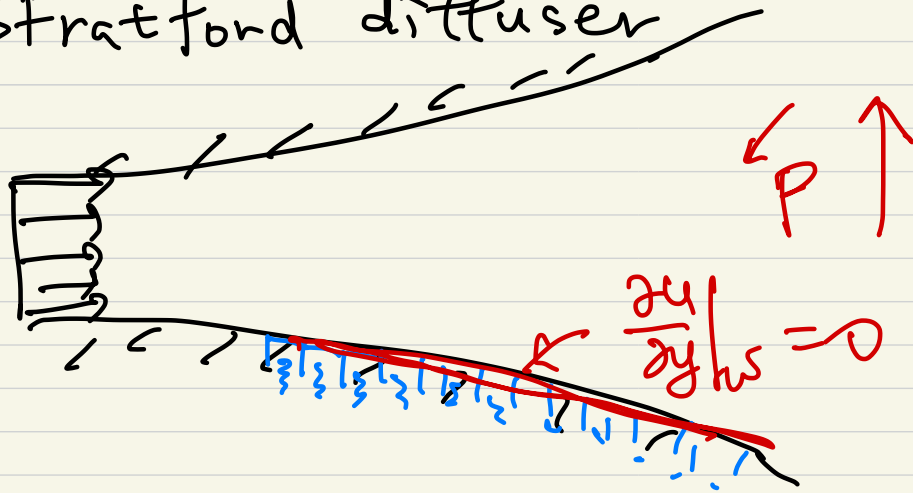
$A \approx \text{const}$
 $U \approx v$
 $\frac{dp}{dx} \approx 0$
zero. press. grad.
Throat

$A \uparrow$ $U \downarrow$
 $\frac{du}{dx} < 0$
 $\frac{dp}{dx} > 0$. $P \uparrow$
adv. press. grad.
Diffuser

$\frac{\partial u}{\partial y}|_w = 0$
crit. adv. press. grad.

dividing streamlines

Stratford diffuser



stall
↓
heavy flow loss

Boundary layer theory
($u \gg v, \frac{\partial}{\partial y}(\cdot) \gg \frac{\partial}{\partial x}(\cdot)$)

is valid only up to the separation pt.

Laminar bdry layer integral theory (Kármán)

$$\frac{\tau_w}{\rho U^2} = \frac{c_f}{2} = \frac{d\theta}{dx} + (2+H) \frac{\theta}{U} \frac{dU}{dx} \quad \left(\frac{dU}{dx} = -\frac{1}{\rho} \frac{1}{U} \frac{dp}{dx} \right)$$

c_f, θ, H open form.

Separation occurs @ $H = 3.5$ laminar flow

↳ $c_f = 0$ $H = 2.4$ turbulent

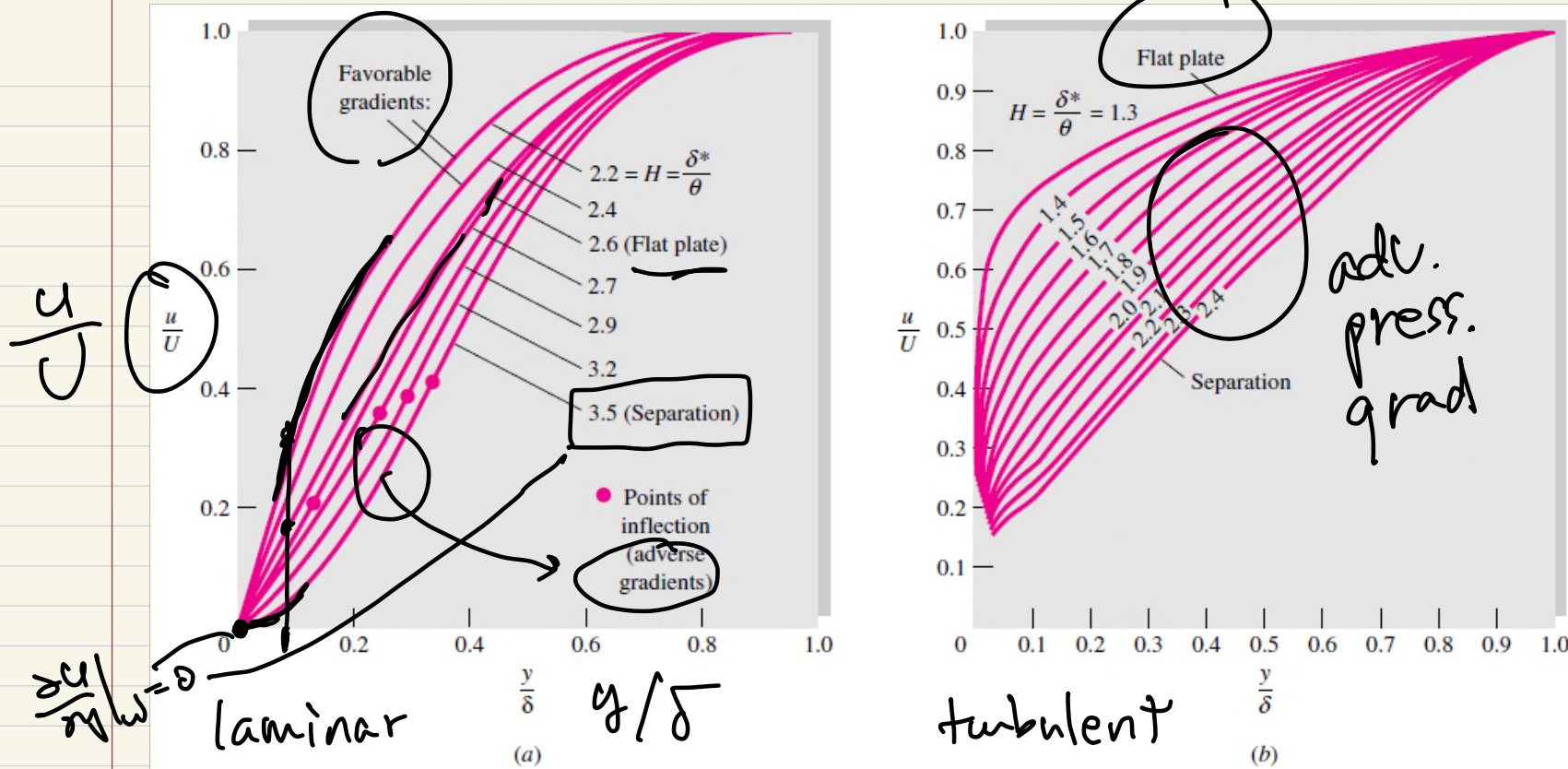
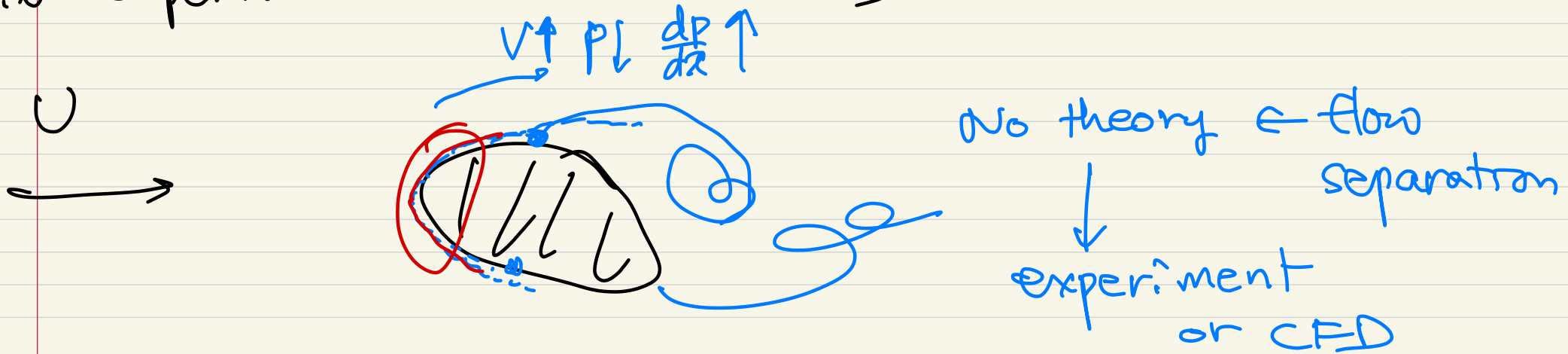


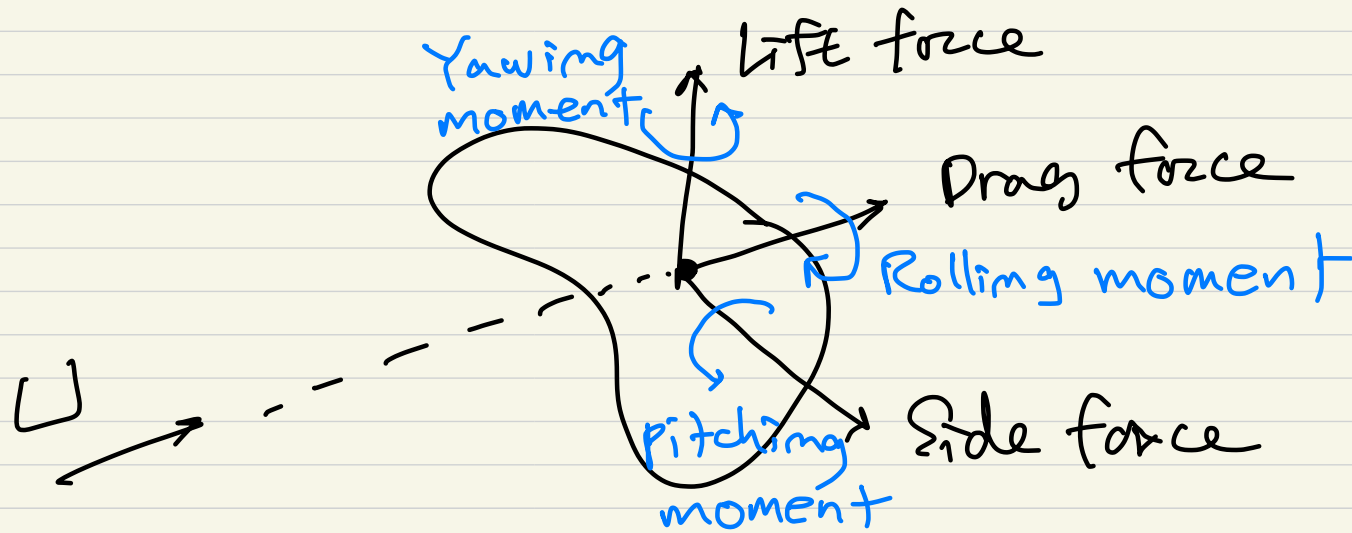
Fig. 7.9 Velocity profiles with pressure gradient: (a) laminar flow; (b) turbulent flow with adverse gradients.

7.6 Experimental external flows



• Drag of 2D & 3D bodies

Performance of lifting bodies \rightarrow Lift, Drag

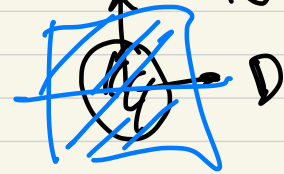
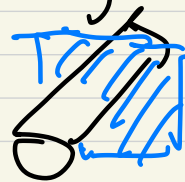
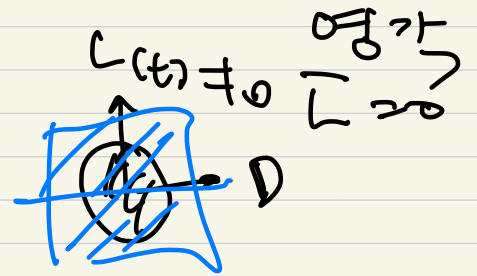
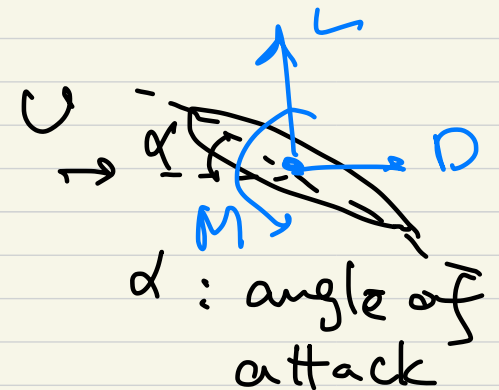


Symmetry about the lift-drag axis

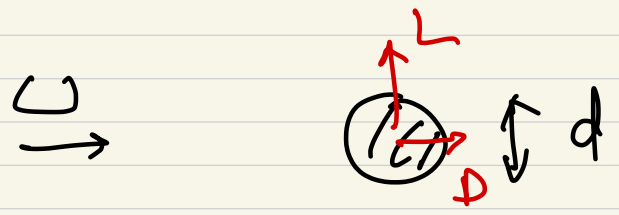
\rightarrow side force, yaw, roll $m_{tm} = 0$

drag, lift, pitching $m_{tm} \neq 0$

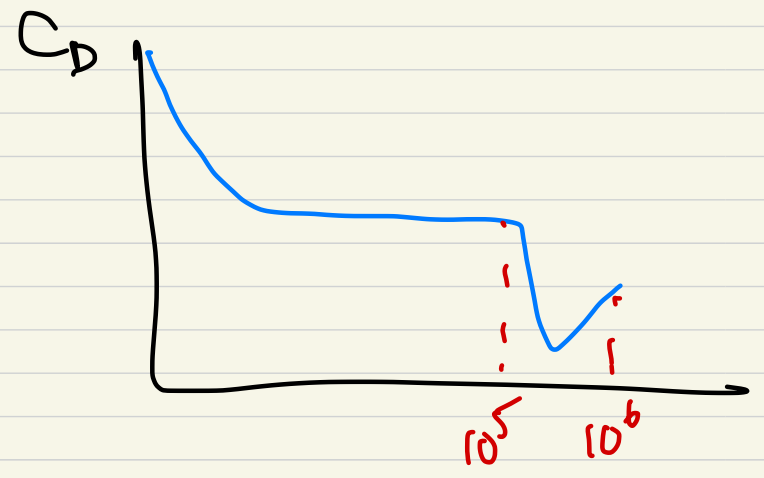
two planes of symmetry \rightarrow Drag $\neq 0$



• similarity (geometric, kinematic, dynamic)
 $[L]$ $[L, T]$ $[L, T, M]$

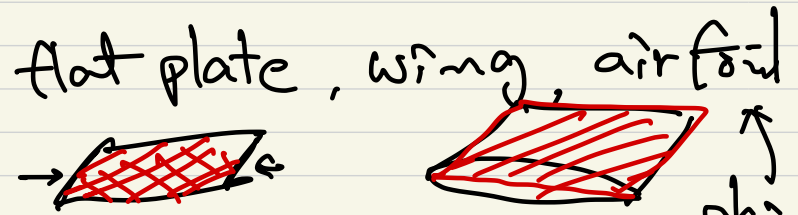


$D = f(U, d, \rho, \mu)$
 dimensional analysis



$\rightarrow C_D = f(Re) \quad Re = Ud/\nu$

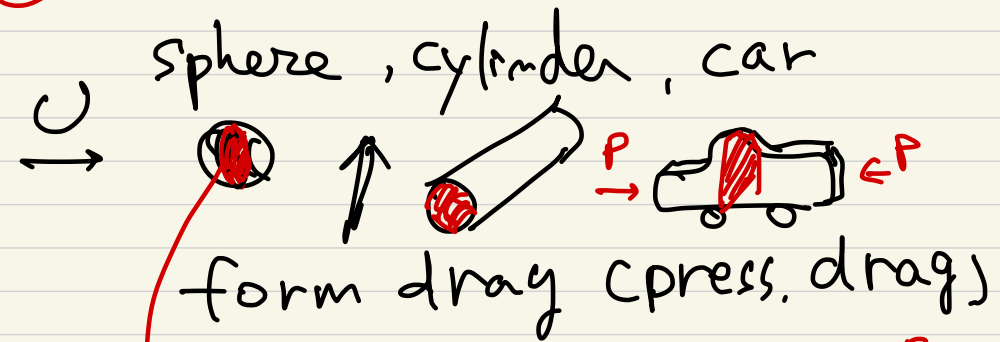
$\frac{D}{\frac{1}{2}\rho U^2 A}$ $A?$



A : planform area

skin friction drag

Streamlined bodies
 friction!



form drag (press. drag)

A : frontal area $\approx P!$
 bluff bodies

surface ship ← skin friction

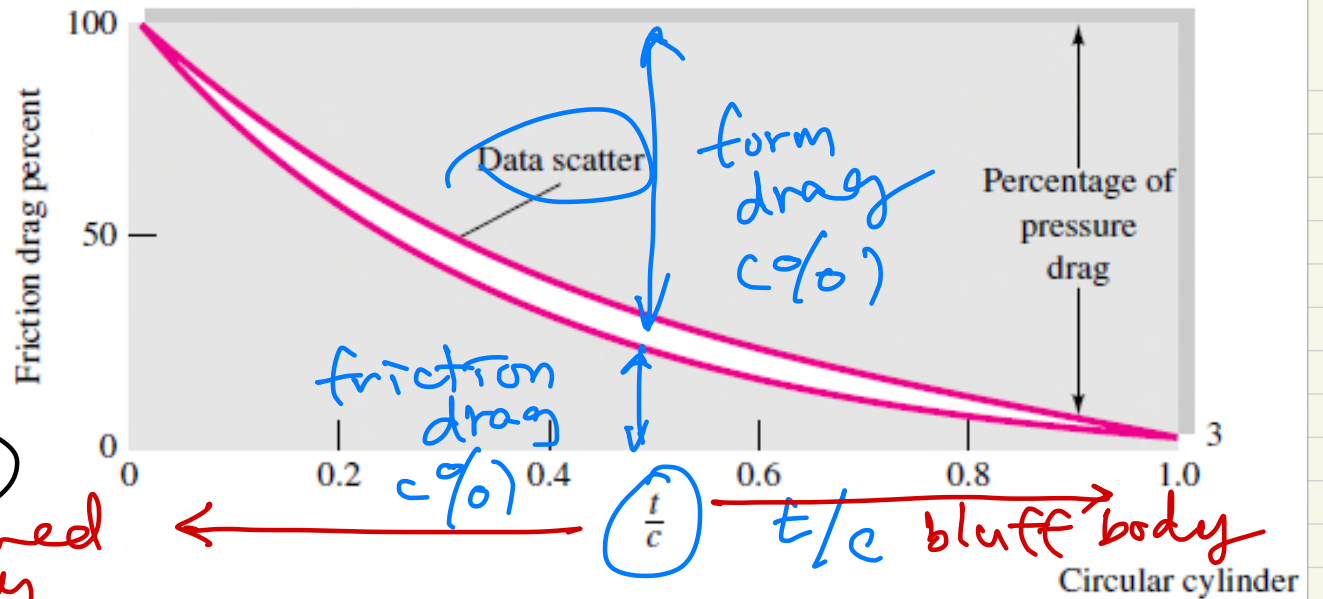
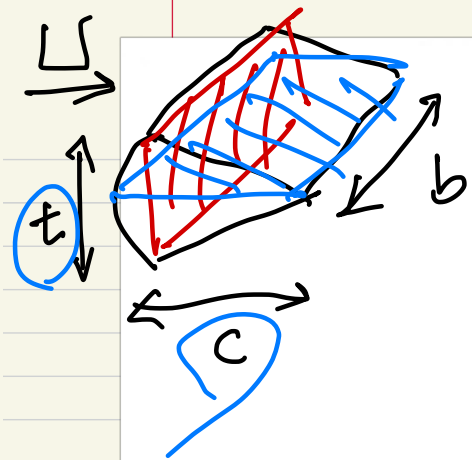


A: wetted surface area

press.

Total drag = Friction drag + Form drag (+ wave drag)

$$C_D = C_{Df} A + C_{Dp} A$$



$$\frac{D}{\frac{1}{2}\rho v^2 A} = C_D$$

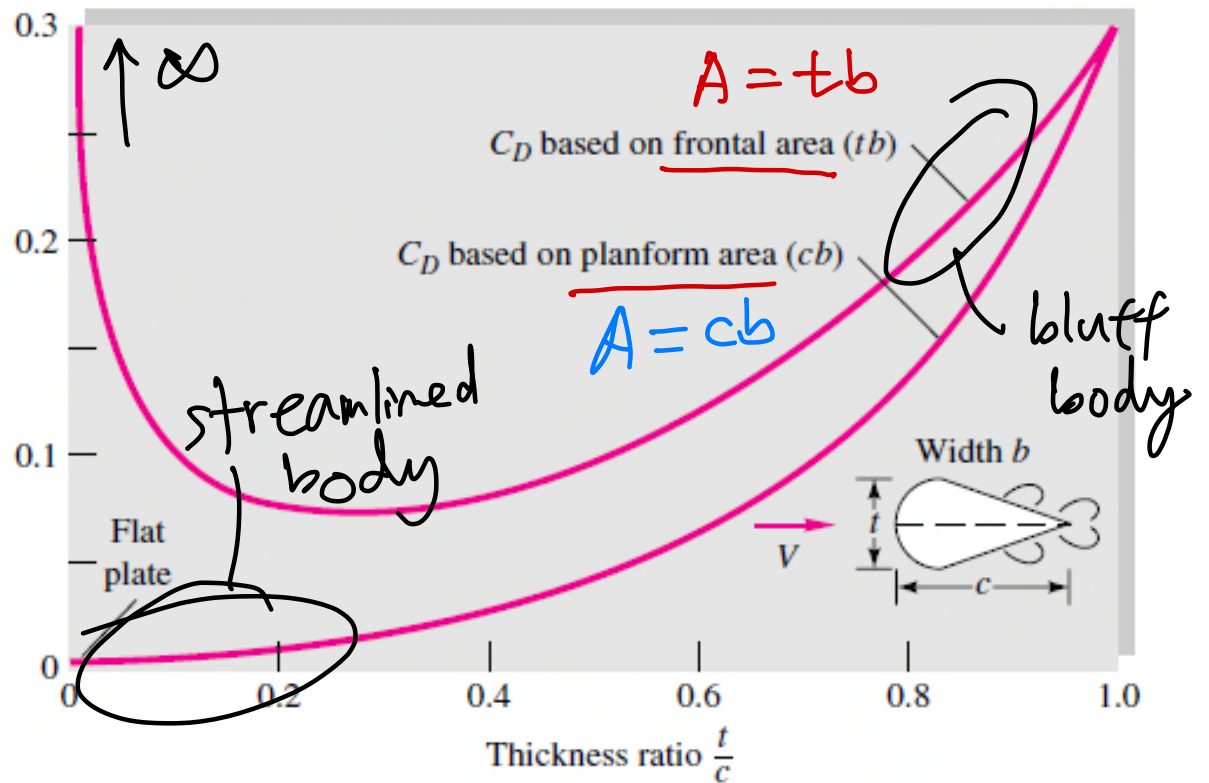


Fig. 7.12 Drag of a streamlined two-dimensional cylinder at $Re_c = 10^6$: (a) effect of thickness ratio on percentage of friction drag; (b) total drag versus thickness when based on two different areas.