

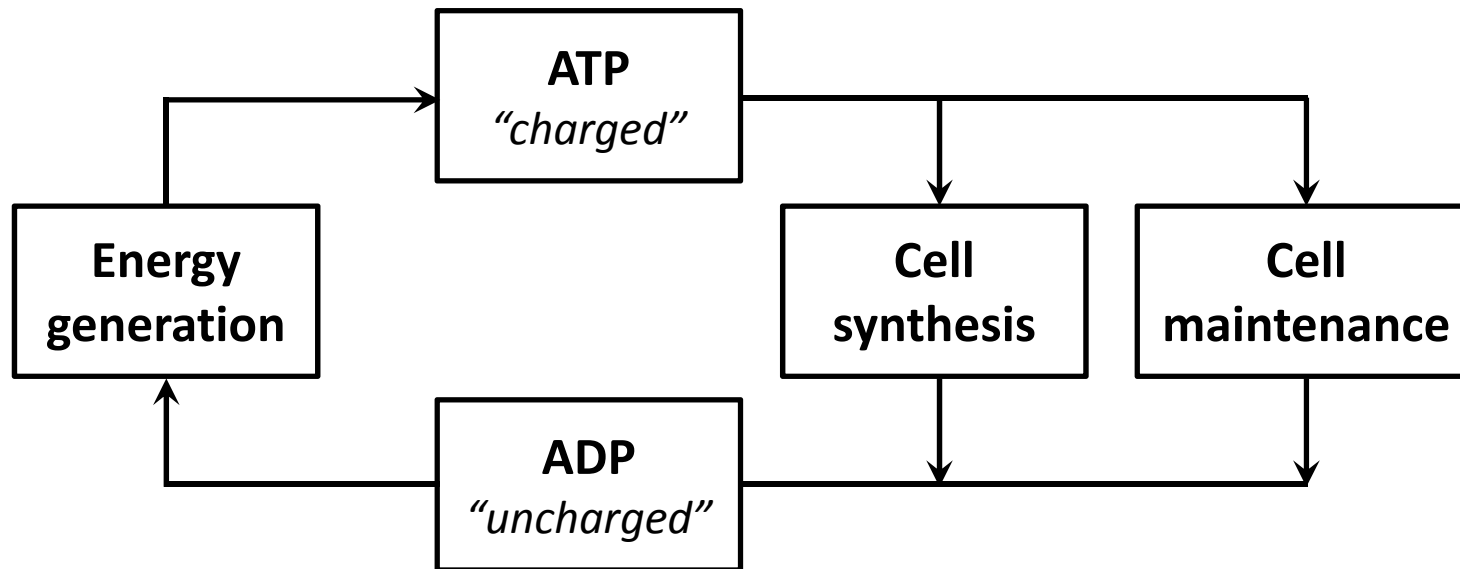
Bacterial energetics

Today's lecture

- Bacterial energetics – overview
- Gibbs free energy of reaction
- Correlation of reaction energetics and yield coefficient

Bacterial energetics

- Microorganisms carry out redox reactions to obtain energy for growth and cell maintenance



Energetics and bacterial growth

- The bacterial cells grow more rapidly when:
 - More energy can be obtained by oxidation of (an e^- equivalent of) e^- donor
 - More energy can be obtained by reduction of (an e^- equivalent of) e^- acceptor
 - When conditions are favorable (abundance of e^- donor, e^- acceptor, nutrients, etc.; low concentration of inhibiting compounds)
 - rapid utilization of substrates

Energetics and bacterial growth

- Consider:

$$Y_n = Y - b \frac{X_a}{-dS/dt}$$

- Larger Y_n when $Y \gg b$: favorable e^- donor and acceptor
- Larger Y_n when $X_a \ll -dS/dt$: favorable conditions for substrate utilization

Gibbs free energy

- “Standard” free energy
 - ΔG^0 , free energy at 25°C, 1 atm, and unit activity for any chemicals involved
 - $\Delta G^{0'}$, standard free energy adjusted to pH=7
- Free energy of formation (ΔG_f)
 - Gibbs free energy that accompanies the formation of 1 mole of the substance from its component elements

Gibbs free energy

- Free energy change of reaction (ΔG_r)
$$\Sigma[(\text{sum of product } \Delta G_f) - (\text{sum of reactant } \Delta G_f)]$$

For a generic reaction written as

$$0 = \sum_{i=1}^n v_{ir} A_i$$

v_{ir} = stoichiometric coefficient, (-) for reactants, (+) for products
 A_i = reaction constituent, reactants or products

$$\Delta G_r = \sum_{i=1}^n v_{ir} \Delta G_f$$

Reaction free energy

Q1: Calculate the standard free energy adjusted pH 7 for the half reaction of 2-chlorobenzoate formation. Use the values of free energy of formation for individual constituents listed in Appendix A.

Q2: Calculate the standard free energy adjusted pH 7 for overall energy reaction with ethanol as an e^- donor and oxygen as an e^- acceptor. Use the half reactions listed in Table 2.2 and 2.3.

Reaction free energy

- For nonstandard conditions,

$$\Delta G_r = \Delta G_r^0 + RT \sum_{i=1}^n v_{ir} \ln a_i$$

a_i = activity of constituent A_i

Caution:

- v_{ir} is negative for reactants and positive for products

- ΔG_r^0 is for standard conditions -- pH=0

From $\Delta G_r^{0'}$, we can calculate ΔG_r^0 by:

$$\Delta G_r^0 = \Delta G_r^{0'} - RTv_H + \ln[10^{-7}]$$

Reaction free energy

Q3: Calculate the free energy of reaction for denitrification of glucose at the following conditions: $T = 25^{\circ}\text{C}$, $\text{pH} = 6.0$, $[\text{C}_6\text{H}_{12}\text{O}_6] = 10^{-3} \text{ M}$, $[\text{NO}_3^-] = 10^{-4} \text{ M}$, $P_{\text{CO}_2} = 3 \times 10^{-4} \text{ atm}$, $P_{\text{N}_2} = 0.78 \text{ atm}$.

Q4: Calculate the free energy of reaction for aerobic ethanol degradation at the following conditions: $T = 20^{\circ}\text{C}$, $\text{pH} = 5.0$, $[\text{C}_2\text{H}_5\text{OH}] = 2 \times 10^{-3} \text{ M}$, $P_{\text{CO}_2} = 3 \times 10^{-4} \text{ atm}$, $P_{\text{O}_2} = 0.21 \text{ atm}$.

Yield coefficient and reaction energetics

- The energy generated by energy reactions is spent to make ATP
- ATP is consumed to drive cell synthesis or cell maintenance
- Cell synthesis involves energy loss (bacteria are not 100% efficient engines!) to synthesize C source to an intermediate compound, and then the intermediate compound to cells

Yield coefficient and reaction energetics

- Energy required to convert carbon source to pyruvate, ΔG_p (heterotrophic bacteria, ammonia as N source):

$$\Delta G_p = 35.09 - \Delta G_c^{0'}$$

(in kJ/e⁻ eq)

35.09 = reaction free energy for formation of pyruvate from CO₂

$\Delta G_c^{0'}$ = reaction free energy for formation of carbon source from CO₂

- Energy required to convert pyruvate to cells, $\Delta G_{pc} = 18.8$ kJ/e⁻ eq

Yield coefficient and reaction energetics

- Energy required for cell synthesis from the carbon source, ΔG_S :

$$\Delta G_S = \frac{\Delta G_p}{\varepsilon^n} + \frac{\Delta G_{pc}}{\varepsilon}$$

ε = energy transfer efficiency

$n = -1$ for $\Delta G_p < 0$ (C-source is at higher energy state than pyruvate);

$+1$ for $\Delta G_p > 0$ (C-source is at lower energy state than pyruvate)

- If energy for cell maintenance is neglected (situation for true yield, Y , and f_s^0):

$$A\varepsilon\Delta G_r + \Delta G_S = 0$$

A = e⁻ equivalent of e⁻ donor used for energy production per equivalent of cells formed

Yield coefficient and reaction energetics

- Solving for A:

$$A = \frac{\Delta G_p / \varepsilon^n + \Delta G_{pc} / \varepsilon}{\varepsilon \Delta G_r}$$

- From A, we can calculate f_s^0 and f_e^0 as:

$$f_s^0 = \frac{1}{1 + A} \quad f_e^0 = 1 - f_s^0 = \frac{A}{1 + A}$$

- Energy transfer efficiency, ε
 - 55-70% under optimal conditions
 - Use 0.6 for ordinary cases

Yield coefficient and reaction energetics

Q5: Estimate f_s^0 and Y for aerobic oxidation of acetate assuming $\epsilon=0.4$ and 0.6 at standard conditions except for a pH of 7.0. Ammonia is available for cell synthesis.