Part 2. The Hydrosphere

Chapter 10.

Distribution of Species in Aquatic Systems

10.1 Single-variable diagrams: Phosphate species

Single variable diagram: a plot of some measure of species conc. Vs. a particular variable like pH, redox status, or conc. of important complexing ligand. E.g.

$$H_3PO_4 \leftrightarrow H_2PO_4^- \leftrightarrow HPO_4^{2^-} \leftrightarrow PO_4^{3^-}$$
 (10.1)

$$K_{a1} = \frac{[H_2 P O_4^{-}][H_3 O^{+}]}{[H_2 P O_4]}$$
(10.2)

$$\alpha_{H_3PO_4} = \frac{[H_3PO_4]}{[H_3PO_4] + [H_2PO_4] + [HPO_4]^{2^-} + [PO_4]^{3^-}}$$
(10.3)

$$\alpha_{H_2PO_4^-} = \frac{[H_2PO_4^-]}{C_p} \tag{10.4}$$

$$\alpha_{HPO_4^{2-}} = \frac{[HPO_4^{2-}]}{C_p} \tag{10.5}$$

$$\alpha_{PO_4^{3-}} = \frac{[PO_4^{3-}]}{C_p} \tag{10.6}$$

10.1 Single-variable diagrams: Phosphate species

Conc. of individual phosphate species:

Table 10.1 Acid dissociation constants for phosphoric acid		
	K_a	pK_a
First dissociation	7.1x10 ⁻³	2.15
Second dissociation	6.3x10 ⁻⁸	7.20
Third dissociation	4.2x10 ⁻¹³	12.38

$$[H_2PO_4^-] = \frac{K_{a1} \times [H_3PO_4]}{[H_2O^+]} \tag{10.7}$$

$$[HPO_4^{2-}] = \frac{K_{a1} \times K_{a2} \times [H_3 PO_4]}{[H_0^+]^2}$$
(10.8)

$$[H_{2}PO_{4}^{-}] = \frac{K_{a1} \times [H_{3}PO_{4}]}{[H_{3}O^{+}]}$$

$$[HPO_{4}^{2-}] = \frac{K_{a1} \times K_{a2} \times [H_{3}PO_{4}]}{[H_{3}O^{+}]^{2}}$$

$$[PO_{4}^{3-}] = \frac{K_{a1} \times K_{a2} \times K_{a3} \times [H_{3}PO_{4}]}{[H_{3}O^{+}]^{3}}$$

$$[O_{4}^{3-}] = \frac{K_{a1} \times K_{a2} \times K_{a3} \times [H_{3}PO_{4}]}{[H_{3}O^{+}]^{3}}$$

$$[O_{4}^{3-}] = \frac{K_{a1} \times K_{a2} \times K_{a3} \times [H_{3}PO_{4}]}{[H_{3}O^{+}]^{3}}$$

$$[O_{4}^{3-}] = \frac{K_{a1} \times K_{a2} \times K_{a3} \times [H_{3}PO_{4}]}{[H_{3}O^{+}]^{3}}$$

$$[O_{4}^{3-}] = \frac{K_{a1} \times K_{a2} \times K_{a3} \times [H_{3}PO_{4}]}{[H_{3}O^{+}]^{3}}$$

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$$[O_{4}^{3-}] = \frac{K_{a1} \times K_{a2} \times K_{a3} \times [H_{3}PO_{4}]}{[H_{3}O^{+}]^{3}}$$

$$C_{p} = [H_{3}PO_{4}] + [H_{2}PO_{4}^{-}] + [HPO_{4}^{2-}] + [PO_{4}^{3-}]$$

$$= [H_{3}PO_{4}](1 + \frac{K_{a1}}{[H_{3}O^{+}]} + \frac{K_{a1} \times K_{a2}}{[H_{3}O^{+}]^{2}} + \frac{K_{a1} \times K_{a2} \times K_{a3}}{[H_{3}O^{+}]^{3}})$$
(10.10)

From eqn 10.3

$$\alpha_{H_3PO_4} = \frac{[H_3PO_4]}{[H_3PO_4](1 + K_{a1}/[H_3O^+] + K_{a1} \times K_{a2}/[H_3O^+]^2 + K_{a1} \times K_{a2} \times K_{a3}/[H_3O^+]^3)}$$
(10.11)

We then multiply t he top and bottom of the right - hand side of the equation by $[H_3O^+]^3$:

$$\alpha_{H_3PO_4} = \frac{[H_3O^+]^3}{[H_3O^+]^3 + [H_3O^+]^2 \times K_{a1} + [H_3O^+] \times K_{a1} \times K_{a2} + K_{a1} \times K_{a2} \times K_{a3}}$$
(10.12)

Using similar calculations, we find that

$$\alpha_{H_2PO_4^-} = \frac{[H_3O^+]^2 \times K_{a1}}{[H_3O^+]^3 + [H_3O^+]^2 \times K_{a1} + [H_3O^+] \times K_{a1} \times K_{a2} + K_{a1} \times K_{a2} \times K_{a3}}$$
(10.13)

$$\alpha_{HPO_4^{2-}} = \frac{[H_3O^+] \times K_{a1} \times K_{a2}}{[H_3O^+]^3 + [H_3O^+]^2 \times K_{a1} + [H_3O^+] \times K_{a1} \times K_{a2} + K_{a1} \times K_{a2} \times K_{a3}}$$
 (10.14)

$$\alpha_{PO_4^{3-}} = \frac{[H_3O^+] \times K_{a1} \times K_{a2} \times K_{a3}}{[H_3O^+]^3 + [H_3O^+]^2 \times K_{a1} + [H_3O^+] \times K_{a1} \times K_{a2} + K_{a1} \times K_{a2} \times K_{a3}}$$
(10.15)

Chapter 10. Distribution of species in aquatic systems 10.1 Single-variable diagrams: Phosphate species

Distribution of phosphate species in open water

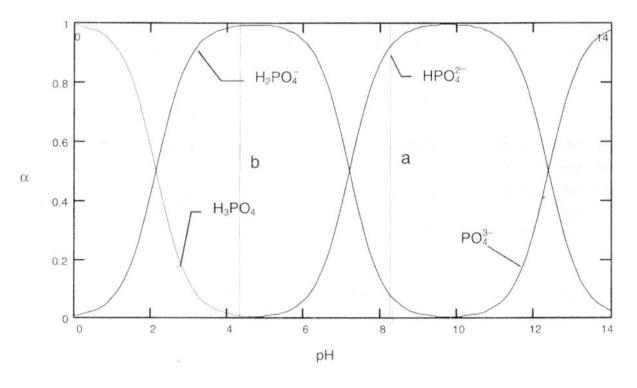


Fig. 10.1 Distribution of phosphorus species expressed as the fraction, α , as a function of aqueous solution pH.

In sea water, dissociation const. of phosphoric acid

10.1 Single-variable diagrams: Cadmium complexes with chloride

Single variable diagram with logarithm scale: E.g. distribution of aq. cadmium chloro complexes as a function of chloride ion concentration.

$$Cd^{2+} + Cl^{-} \leftrightarrow CdCl^{+}$$
 $K_{f1} = \frac{[CdCl^{+}]}{[Cd^{2+}][Cl^{-}]} = 7.9 \times 10$ (10.16)

$$CdCl^{+} + Cl^{-} \leftrightarrow CdCl_{2} \quad K_{f2} = \frac{[CdCl_{2}]}{[CdCl^{+}][Cl^{-}]} = 4.0$$
 (10.17)

$$CdCl_2 + Cl^- \leftrightarrow CdCl_3^- \qquad K_{f3} = \frac{[CdCl_3^-]}{[CdCl_2][Cl^-]} = 2.0$$
 (10.18)

$$CdCl_3^- + Cl^- \leftrightarrow CdCl_4^{2-} \quad K_{f4} = \frac{[CdCl_4^{2-}]}{[CdCl_3^-][Cl^-]} = 0.6$$
 (10.19)

The reactions may also be described using 'overall' steps and the overall stability constants are symbolized as β_f . It is readily seen that

$$\beta_{\text{fn}} = K_{f1} \times K_{f2} \times \cdots K_{fn} \tag{10.20}$$

$$Cd^{2+} + 2Cl^{-} \leftrightarrow CdCl_{2}$$
 $\beta_{f2} = K_{f1} \times K_{f2} = 3.2 \times 10^{2}$ (10.22)

$$Cd^{2+} + 3Cl^{-} \leftrightarrow CdCl_{3}^{-}$$
 $\beta_{f3} = K_{f1} \times K_{f2} \times K_{f3} = 6.4 \times 10^{2}$ (10.23)

$$Cd^{2+} + 4Cl^{-} \leftrightarrow CdCl_{4}^{2-} \qquad \beta_{f4} = K_{f1} \times K_{f2} \times K_{f3} \times K_{f4} = 3.8 \times 10^{2}$$
 (10.24)

10.1 Single-variable diagrams: Cadmium complexes with chloride

Total conc. of cadmium in an aq. solution containing chloride

We can derive expression s for the concentration of each of the five cadmium species in the following way. We begin by dividing eqn 10.25 by $[Cd^{2+}]$:

$$\frac{C_{Cd}}{[Cd^{2+}]} = 1 + \frac{[CdCl^{+}]}{[Cd^{2+}]} + \frac{[CdCl_{2}]}{[Cd^{2+}]} + \frac{[CdCl_{3}^{-}]}{[Cd^{2+}]} + \frac{[CdCl_{4}^{2-}]}{[Cd^{2+}]}$$
(10.26)

Substituti ng the expression s for the β functions,

$$\frac{C_{Cd}}{[Cd^{2+}]} = 1 + \beta_{f1}[Cl^{-}]^{1} + \beta_{f2}[Cl^{-}]^{2} + \beta_{f3}[Cl^{-}]^{3} + \beta_{f4}[Cl^{-}]^{4}$$
(10.27)

Rearrangin g eqn 10.27:

$$[Cd^{2+}] = \frac{C_{Cd}}{1 + \beta_{f,1}[Cl^-]^1 + \beta_{f,2}[Cl^-]^2 + \beta_{f,3}[Cl^-]^3 + \beta_{f,4}[Cl^-]^4}$$
(10.28)

Similarly, the concentrations of other cadmium chloro species are given by

$$[CdCl^{+}] = \frac{\beta_{f1}[Cl^{-}]^{1}C_{Cd}}{1 + \beta_{f1}[Cl^{-}]^{1} + \beta_{f2}[Cl^{-}]^{2} + \beta_{f3}[Cl^{-}]^{3} + \beta_{f4}[Cl^{-}]^{4}}$$
(10.29)

$$[CdCl_2] = \frac{\beta_{f2}[Cl^-]^2 C_{Cd}}{1 + \beta_{f1}[Cl^-]^1 + \beta_{f2}[Cl^-]^2 + \beta_{f3}[Cl^-]^3 + \beta_{f4}[Cl^-]^4}$$
(10.30)

$$[CdCl_3^-] = \frac{\beta_{f3}[Cl^-]^3 C_{Cd}}{1 + \beta_{f1}[Cl^-]^1 + \beta_{f2}[Cl^-]^2 + \beta_{f3}[Cl^-]^3 + \beta_{f4}[Cl^-]^4}$$
(10.31)

$$[CdCl_3^{2-}] = \frac{\beta_{f4}[Cl^-]^4 C_{Cd}}{1 + \beta_{f1}[Cl^-]^1 + \beta_{f2}[Cl^-]^2 + \beta_{f3}[Cl^-]^3 + \beta_{f4}[Cl^-]^4}$$
(10.32)

10.1 Single-variable diagrams: Cadmium complexes with chloride

- E.g. line b, surface water salinity=10 %₀, [Cl⁻¹]=0.16 mol L⁻¹
- [Cd²⁺]=0.04, CdCl⁺=0.52, CdCl₂=0.33, CdCl³⁻=0.10, CdCl₄²⁻=0.01

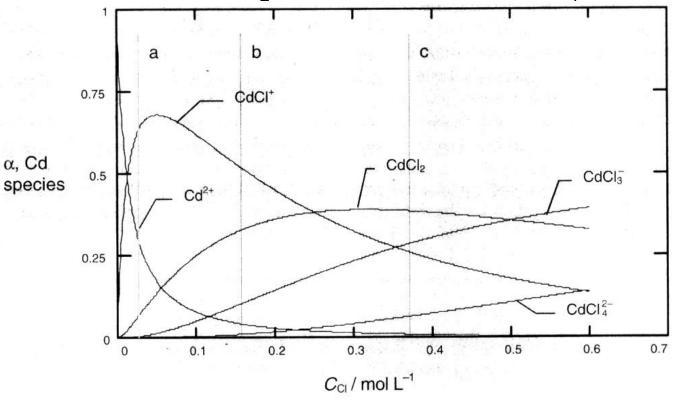


Fig. 10.2 Distribution of cadmium chloro complexes as a function of the concentration of chloride ion in water. The range of chloride concentrations is from zero to 0.56 mol L^{-1} ; the latter value is the approximate concentration in sea water.

10.2 Two-variable diagrams: pE/pH diagrams (Pourbaix diagram)

- Concept of pE: pE =
- A large negative value of pE indicates a large value for the e- activity in solution, implying
- A large positive value of pE: low activity of e- in solution, implying
- pE values in water = -12~25

Consider the simple half reaction

$$Fe^{3+}(aq) + e^{-} \leftrightarrow Fe^{2+}(aq) \tag{10.34}$$

$$K_{eq} = \frac{a_{Fe^{2+}}}{a_{Fe^{3+}} \times a_{e^{-}}}$$
 (10.35)

$$\frac{1}{a_{e^{-}}} = \frac{K_{eq} \times a_{Fe^{3+}}}{a_{Fe^{2+}}} \tag{10.36}$$

Using the definition of pE and taking logs of both sides of eqn 10.36, we have

$$pE = -\log a_{e^{-}} = \log K_{eq} + \log \frac{a_{Fe^{3+}}}{a_{Fe^{2+}}}$$
 (10.37)

Since

$$\Delta G^{\circ} = -2.303 \,\text{RT} \,\log K_{eq} \tag{10.38}$$

$$=-nFE^{\circ} \tag{10.39}$$

10.2 Two-variable diagrams: pE/pH diagrams (Pourbaix diagram)

(n has the usual electroche mical meaning - i.e. the number of electrons transferr ed in the half reaction), at 298K (R = 8.314J K⁻¹mol⁻¹ and F = 96485Cmol⁻¹), we have

$$\log K_{eq} = \frac{nFE^{\circ}}{2.303RT} = \frac{nE^{\circ}}{0.0591}$$
 (10.40)

In this case, n = 1, so

$$\log K_{eq} = \frac{E^{\circ}}{0.0591} \tag{10.41}$$

and

$$pE = \frac{E^{\circ}}{0.0591} + \log \frac{a_{Fe^{3+}}}{a_{Fe^{2+}}}$$
 (10.42)

Under standard conditions, $a_{Fe^{3+}} = a_{Fe^{2+}} = 1$:

$$\log \frac{a_{Fe^{3+}}}{a_{Fe^{2+}}} = \tag{10.43}$$

and

$$pE = pE^{\circ} = \tag{10.44}$$

For non-standard conditions:

$$pE = pE^{\circ} + \tag{10.45}$$

When the standard pE° value and the actual activities (usually approximated by concentrations) of Fe^{3+} and Fe^{2+} are substitute d into this equation, the pE of a particular environmental system can be calculated.

10.2 Two-variable diagrams: pE/pH diagrams (Pourbaix diagram)

In the general case, for a reaction

$$aA + ne^- \leftrightarrow bB \tag{10.46}$$

where A and B are the oxidized and reduced forms of a redox couple, the reaction quotient (Q) is defined as

$$Q = \frac{(a_B)^b}{(a_A)^a} \approx \frac{[B]^b}{[A]^a}$$
 (10.47)

The reaction quotient t akes the form of an equilibriu m constant, but uses activities (or, as an approximat ion, concentrations) that obtain under any conditions, not just those at equilibriu m. The general form of eqn 10.45 is then

(10.48)

10.2 Two-variable diagrams: Methods of calculating pE⁰

Consider a half-reaction

$$Fe^{3+}(aq) + e^{-} \leftrightarrow Fe^{2+}(aq)$$
 $E^{0} = +0.771V$ (10.34)

Therefore

$$pE^0 =$$

from eq (10.44)

Second method, using eqs. (10.40) and (10.44)

A second method for calculatin g pE° makes use of the relations in eqns 10.40 and 10.44

$$\log K_{eq} = \frac{nE^{\circ}}{0.0591} = npE^{\circ} \tag{10.49}$$

$$pE^{\circ} = \frac{\log K_{eq}}{n} \tag{10.50}$$

This relation is applicable when an E° value is not available, but where the appropriate equilibriu m constant is known.

In some cases, several reactions may be combined to produce an overall half reaction.

Consider the half reaction for which no tabulated E° value is easily found:

$$Fe(OH)_3 + 3H_3O^+(aq) + e^- \leftrightarrow Fe^{2+}(aq) + 6H_2O$$
 (10.51)

The reaction is the sum of

$$Fe(OH)_2 \leftrightarrow Fe^{3+}(aq) + 3OH^-(aq)$$
 (10.51a)

$$Fe^{3+}(aq) + e^{-} \leftrightarrow Fe^{2+}(aq)$$
 (10.51b)

$$3H_3O^+(aq) + 3OH^-(aq) \leftrightarrow 6H_2O \tag{10.51c}$$

10.2 Two-variable diagrams: Methods of calculating pE⁰

For reaction 10.51a, $K_a = K_{sp} = 9.1 \times 10^{-39}$ and $\log K_a = -38.0$. For reaction 10.51b, $pE_b^0 = \log K_b = 0.771/0.0591$ and $\log K_b = +13.0$. For reaction 10.51c,

$$K_{\rm c} = \frac{1}{\left(K_{\rm w}\right)^3} = 10^{42}$$

and $\log K_c = +42.0$. For the original, overall reaction

$$\log K_{\rm m} = \log K_{\rm a} + \log K_{\rm b} + \log K_{\rm c}$$
$$= -38.0 + 13.0 + 42.0$$
$$= +17.0$$

Using equation 10.50 (n = 1):

$$pE_{\text{overall}}^{\text{o}} = +17.0.$$

There is a third method for calculating pE^o values and this requires combining eqns 10.38 and 10.49:

$$\Delta G^{o} = -2.303 RT n pE^{o}$$
 (10.52)

$$pE^{o} = \frac{-\Delta G^{o}}{2.303 \, RT \, n} \tag{10.53}$$

Consider the redox reaction

$$SO_4^{2-}(aq) + 10H_3O^+(aq) + 8e^- \Rightarrow H_2S(aq) + 14H_2O$$
 (10.54)

$$\Delta G^{o} = \Delta G^{o}_{f} (H_{2}S) + 14\Delta G^{o}_{f} (H_{2}O) - \Delta G^{o}_{f} (SO_{4}^{2-}) - 10\Delta G^{o}_{f} (H_{3}O^{+}) - 8\Delta G^{o}_{f} (e^{-})$$

Using thermochemical tables and noting that ΔG_f^o for the aqueous electron is 0, and for the hydronium ion, ΔG_f^o has the same value as for water:

$$\Delta G^{o} = -27.86 + 14 \times (-237.18) - 10 \times (-237.18) - (-744.60)$$

= -231.98 kJ

$$pE^{o} = \frac{-(-231.98) \text{ kJ} \times 1000 \text{ J kJ}^{-1}}{2.303 \times 8.314 \text{ J mol}^{-1} \text{ K}^{-1} \times 298.2 \text{ K} \times 8 \text{ mol}}$$
$$= 5.08$$

10.2 Two-variable diagrams: Chromium in tannery wastes

■ Suppose the initial conc. of [Cr³+]=26 mg L⁻¹, then dissolved oxygen in downstream oxidize to Cr₂O₇²⁻, pH=6.5 (a_{H3O}+=10⁻6.5)

The relevant reaction for atmospheri c O_2 in equilibriu m with wate r (often called a well aerated system) is

$$O_{2}(g) + 4H_{3}O^{+}(aq) + 4e^{-} \leftrightarrow 6H_{2}O$$

$$E^{\circ} = 1.23V$$

$$pE^{\circ} =$$

$$(10.55)$$

Using eqn 10.48:

$$pE = pE^{\circ} - \frac{1}{n} \log \frac{1}{P_{O_2} / P^{\circ} \times (a_{H_3O^{+}})^4}$$
$$= 20.8 - \frac{1}{4} \log \frac{1}{0.209 \times (10^{-6.5})^4}$$
$$= 14.1$$

10.2 Two-variable diagrams: Chromium in tannery wastes

Note that in these calculations, the pressure is given as a ratio of P_{O_2}/P^o which is numerically identical to pressure in atmospheres. For oxygen, which makes up 20.9% of the atmosphere, $P_{O_2} = 21\,200\,\text{Pa}$; $P^o = 101\,325\,\text{Pa}$.

For the Cr system:

$$Cr_2O_7^{2-}$$
 (aq) + 14H₃O⁺ (aq) + 6e⁻ \rightleftharpoons 2Cr³⁺ (aq) + 17H₂O (10.56)
 $E^o = 1.36V$ and $pE^o = 23.0$
 $pE = pE^o - \frac{1}{6}log \frac{[Cr^{3+}]^2}{[Cr_2O_7^{2-}](a_{H_2O_7^+})^{14}}$

Since the chromium and oxygen systems are in equilibrium, pE is

$$14.1 = 23.0 - \frac{1}{6} \log \frac{[Cr^{3+}]^2}{[Cr_2O_7^{2-}](10^{-6.5})^{14}}$$

$$= 23.0 - \frac{1}{6} \log \frac{1}{(10^{-6.5})^{14}} - \frac{1}{6} \log \frac{[Cr^{3+}]^2}{[Cr_2O_7^{2-}]}$$

$$= 7.8 - \frac{1}{6} \log \frac{[Cr^{3+}]^2}{[Cr_2O_7^{2-}]}$$

$$\log \frac{[Cr^{3+}]^2}{[Cr_2O_7^{2-}]} = -37.8$$

$$\frac{[Cr^{3+}]^2}{[Cr_2O_7^{2-}]} = 1.6 \times 10^{-38}$$

10.2 Two-variable diagrams: pE/pH diagrams

- In the diagram, areas define the regions where particular species are dominant
- P^0 =101325 Pa =1 atm: this is the min. pressure required for gas evolution from the aq. solution. I.e. when $P_{gas} > P^0$,
- E.g. gas evolution from acidic solution

$$2H_3O^+(aq) + 2e^- \leftrightarrow H_2(g) + 2H_2O$$
 (10.57)

Another type of condition is required for the situation where only soluble species are involved, or where is a soluble species reacting to form one that is insoluble.

Examples of these two cases are

$$Sn^{4+}(aq) + 2e^- \leftrightarrow Sn^{2+}(aq) \tag{10.58}$$

and

$$MnO_2 + 4H_3O^+(aq) + 2e^- \leftrightarrow Mn^{2+}(aq) + 6H_2O$$
 (10.59)

10.2 Two-variable diagrams: pE/pH diagrams

- Consider aq. sulfur system where the species of interest are: SO₄²⁻ (aq), HSO₄⁻ (aq), S(s), HS⁻ (aq), and H₂S (aq)
- To consider first water itself,

$$2H_2O + 2e^- \leftrightarrow H_2(g) + 2OH^-(aq) \tag{10.60}$$

For this reaction

$$E^{\circ} = -0.828V$$

$$pE^{\circ} = -14.0$$

Equation 10.48 for this reaction is written as

(10.61)

(note again that here and in subsequent calculations, we will use concentrations rather than activities except for hydroxyl and hydronium ions).

10.2 Two-variable diagrams: pE/pH diagrams

For the boundary involving a gas, we choose the condition that

$$P_{\text{H}_2} = P^{\text{o}} = 101325 \,\text{Pa}$$

 $pE = -14.0 - \log(a_{\text{OH}^-})$
 $= -14.0 + \text{pOH}$

Since

$$pH + pOH =$$

then

$$pE =$$

This line then defines the boundary for water stability with respect to reduction and is shown as the lower line on Fig. 10.4. Where the pE value is less than the pH value, water is unstable. It is possible also to calculate the same line by taking the reduction reaction to be

$$2H_3O^+ (aq) + 2e^- \rightleftharpoons H_2 (g) + 2H_2O$$
 (10.62)

Considering the other extreme, highly oxidizing conditions, water is unstable with respect to O_2 evolution and the reaction is written as

$$6H_2O \rightleftharpoons 4H_3O^+(aq) + O_2 + 4e^-$$
 (10.63)

For this reaction

$$E^{o} = 1.229 V$$

 $pE^{o} = E^{o}/0.0591 = 20.80$

10.2 Two-variable diagrams: pE/pH diagrams

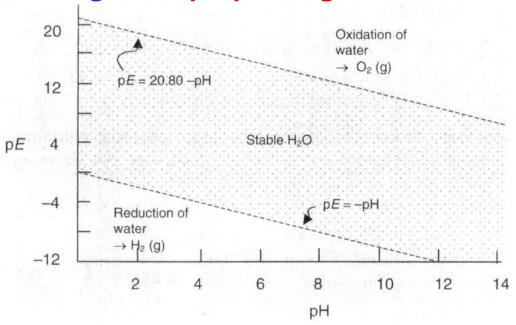


Fig. 10.4 Region of stability and stability boundaries for water on a pE/pH diagram.

$$pE = pE^{\circ} - \frac{1}{4}\log(1/P_{O_2} \times (a_{H_3O^+})^4)$$
 (10.64)

Once again, the boundary condition requires that the pressure of the gas equal atmospheric pressure.

$$P_{O_2} = P^{\circ} = 101,325Pa$$

 $pE = 20.80 - \log(1/a_{H_3O^+})$
 $= 20.80 - pH$

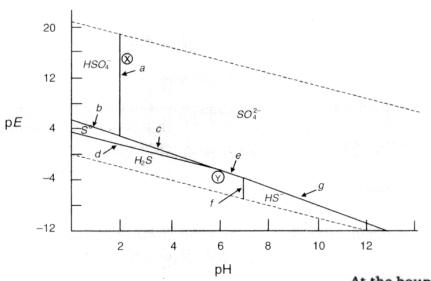
10.2 Two-variable diagrams: The sulfur system

The SO₄²/HSO₄ boundary

The equation describing this boundary requires hydronium ion, but there is no oxidation or reduction involved:

$$SO_4^{2-}(aq) + H_3O^{+}(aq) = HSO_4^{-}(aq) + H_2O$$
 (10.65)

To make things easier, we use H⁺ as an abbreviation for H₃O⁺, the hydronium ion, but of course the result would be the same if the latter species were used in the equations and calculations.



$$\Delta G^{\circ} = \Delta G_{f}^{\circ} (HSO_{4}^{-}) - \Delta G_{f}^{\circ} (SO_{4}^{2-}) - \Delta G_{f}^{\circ} (H^{+})$$

$$= -755.99 - (-744.60) - 0$$

$$= -11.39 \text{ kJ} = -11390 \text{ J}$$

$$\log K = \frac{-\Delta G^{\circ}}{2.303 \text{ RT}}$$

$$= \frac{+11390}{2.303 \times 8.314 \times 298.2}$$

$$= 1.995$$

$$K = \frac{[HSO_4^-]}{[SO_4^{2-}]a_{H^+}}$$

At the boundary, $[HSO_4^-] = [SO_4^{2-}] = 10^{-2} M$, and

Fig. 10.5 The pE/pH for the aqueous sulfur system.

$$K = \frac{1}{a_{H^+}}$$
$$\log K = pH = 1.995$$

Therefore, the boundary between HSO_4^- and SO_4^{2-} is a vertical line at pH 1.995. Below this value, HSO_4^- is the dominant form; above it SO_4^{2-} is most important. See line 'a' on Fig. 10.5.

10.2 Two-variable diagrams: The sulfur system

The HSO₄/S° boundary

$$HSO_4^-$$
 (aq) + 7H⁺ (aq) + 6e⁻ \rightleftharpoons So (s) + 4H₂O (10.66)

$$\begin{split} \Delta G^o &= \Delta G_f^o \; (S) + 4 \Delta G_f^o \; (H_2O) - \Delta G_f^o \; (HSO_4^-) - 7 \Delta G_f^o \; (H^+) - 6 \Delta G_f^o \; (e^-) \\ &= 0 + 4 (-237.18) - (-755.99) - 0 - 0 \\ &= -192.73 \; kJ = -192.730 \; J \end{split}$$

$$pE^{o} = \frac{-\Delta G^{o}}{2.303 \text{ nRT}} = \frac{+192730}{2.303 \times 6 \times 8.314 \times 298.2} = 5.626$$

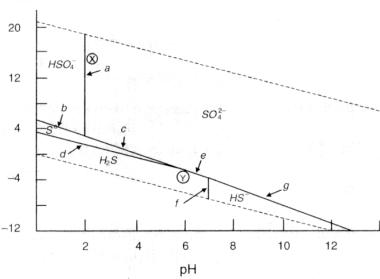
$$pE = pE^{o} - \frac{1}{6} \log \frac{1}{[HSO^{-}](a_{u+})^{7}}$$

At the boundary, $[HSO_4^-] = 10^{-2} \text{ mol L}^{-1}$:

$$pE = 5.626 - \frac{7}{6} \log \frac{1}{a_{H^+}} - \frac{1}{6} \log \frac{1}{10^{-2}}$$

$$= 5.626 - \frac{7}{6} pH - 0.333$$

$$= 5.293 - 1.167 pH$$



This is line 'b' on Fig. 10.5; above it is the domain of HSO₄; below it is elemental sulfur, So.

Fig. 10.5 The pE/pH for the aqueous sulfur system.

10.2 Two-variable diagrams: The sulfur system

The SO₄-/S° boundary

$$SO_4^{2-} (aq) + 8H^+ (aq) + 6e^- = S^o (s) + 4H_2O$$

$$\Delta G^o = \Delta G_f^o (S) + 4\Delta G_f^o (H_2O) - \Delta G_f^o (SO_4^{2-}) - 8\Delta G_f^o (H^+) - 6\Delta G_f^o (e^-)$$

$$= 0 + 4(-237.18) - (-744.60) - 0 - 0$$

$$= -204.12 \text{ kJ} = -204 120 \text{ J}$$

$$pE^o = \frac{\Delta G^o}{2.303 \text{ nRT}} = \frac{+204 120}{2.303 \times 6 \times 8.314 \times 298.2}$$

$$= 5.958$$

$$pE = pE^o - \frac{1}{6} \log \frac{1}{[SO_4^{2-}](a_{H^+})^8}$$
At the boundary, $[SO_4^{2-}] = 10^{-2} \text{ mol } L^{-1}$:
$$pE = 5.958 - \frac{8}{6} \log \frac{1}{a_{H^+}} - \frac{1}{6} \log \frac{1}{10^{-2}}$$

$$= 5.958 - \frac{8}{6} pH - 0.333$$

Fig. 10.5 The pE/pH for the aqueous sulfur system.

This is line 'c' on Fig. 10.5; above it is the domain of SO_4^{2-} , below it S° .

 $= 5.625 - 1.333 \, pH$

10.2 Two-variable diagrams: The sulfur system

The S°/H₂S boundary

$$S(s) + 2H^{+}(aq) + 2e^{-} \rightleftharpoons H_{2}S(aq)$$

$$\Delta G^{o} = \Delta G^{o}_{f}(H_{2}S) - \Delta G^{o}_{f}(S) - 2\Delta G^{o}_{f}(H^{+}) - 2\Delta G^{o}_{f}(e^{-})$$

$$= -27.86 - 0 - 0 - 0$$

$$= -27.86 \text{ kJ} = -27.860 \text{ J}$$

$$pE^{o} = \frac{-\Delta G^{o}}{2.303 \text{ nRT}} = \frac{+27.860}{2.303 \times 2 \times 8.314 \times 298.2}$$

$$= 2.400$$

$$pE = pE^{o} - \frac{1}{2}log\frac{[H_{2}S]}{(a_{H^{+}})^{2}}$$

At the boundary, $[H_2S] = 10^{-2} \text{ mol } L^{-1}$:

$$pE = 2.440 + 1 - pH$$

= 3.440 - pH

This is line 'd' on Fig. 10.5; above it is the domain of S°, below it H2S.

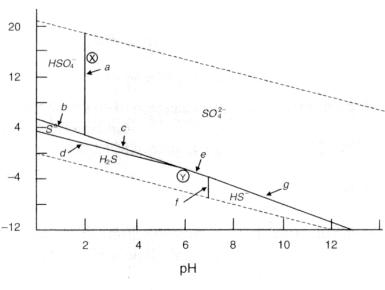


Fig. 10.5 The pE/pH for the aqueous sulfur system.

10.2 Two-variable diagrams: The sulfur system

The SO₄²⁻/H₂S boundary

$$SO_4^{2-} (aq) + 10H^+ (aq) + 8e^- \rightleftharpoons H_2S (aq) + 4H_2O$$

$$\Delta G^o = \Delta G_f^o (H_2S) + 4\Delta G_f^o (H_2O) - \Delta G_f^o (SO_4^{2-}) - 10\Delta G_f^o (H^+) - 8\Delta G_f^o (e^-)$$

$$= -27.86 + 4(-237.18) - (-744.60) - 0 - 0$$

$$= -231.98 \text{ kJ} = -231.980 \text{ J}$$

$$pE^o = \frac{-\Delta G^o}{2.303 \text{ nRT}} = \frac{+231.980}{2.303 \times 8 \times 8.314 \times 298.2}$$

$$= 5.079$$

$$pE = pE^o - \frac{1}{8} \log \frac{[H_2S]}{[SO_4^{2-}](a_{H^+})^{10}}$$
At the boundary, $[H_2S] = [SO_4^{2-}] = 10^{-2} \text{ mol L}^{-1}$:
$$pE = 5.079 - \frac{10}{8} \log \frac{1}{a_{H^+}}$$

Fig. 10.5 The pE/pH for the aqueous sulfur system.

This is line 'e' on Fig. 10.5 (a very small segment, difficult to distinguish from line 'd'); above it is the domain of SO_4^{2-} , below it H_2S .

= 5.079 - 1.25 pH

10.2 Two-variable diagrams: The sulfur system

The H₂S/HS⁻ boundary

$$H_2S(aq) \rightleftharpoons HS^-(aq) + H^+(aq)$$
 (10.70)

As for the HSO_4^-/SO_4^{2-} boundary, this is not a redox reaction and therefore the line will be vertical with the protonated species on the left.

$$\Delta G^{0} = \Delta G^{0}_{f} (HS^{-}) + \Delta G^{0}_{f} (H^{+}) - \Delta G^{0}_{f} (H_{2}S)$$

$$= 12.08 + 0 - (-27.86)$$

$$= 39.94 \text{ kJ} = 39.940 \text{ J}$$

$$\log K = \frac{-\Delta G^{0}}{2.3030RT} = \frac{-39.940}{2.303 \times 8.314 \times 298.2}$$

$$= -6.995$$

$$K = \frac{[HS^{-}]a_{H^{+}}}{[H_{2}S]}$$

$$K = a_{H^{+}}$$

$$\log K = \log[H^{+}] = -pH = -6.995$$

$$pH = 6.995$$
Fig. 10.5 The pE/pH for the aqueous sulfur system.

This is line 'f' on Fig. 10.5; to the left is the domain of H₂S and to the right HS-.

10.2 Two-variable diagrams: The sulfur system

The SO₄²/HS boundary

$$SO_4^{2-} (aq) + 9H^+ (aq) + 8e^- \rightleftharpoons HS^- (aq) + 4H_2O$$
 (10.71)
$$\Delta G^\circ = \Delta G^\circ_f (HS^-) + 4\Delta G^\circ_f (H_2O) - \Delta G^\circ_f (SO_4^{2-}) - 9\Delta G^\circ_f (H^+) - 8\Delta G^\circ_f (e^-)$$

$$= 12.08 + 4(-237.18) - (-744.60) - 0 - 0$$

$$= -192.04 \text{ kJ} = -192.040 \text{ J}.$$

$$pE^\circ = \frac{-\Delta G^\circ}{2.303 \text{ nRT}} = \frac{+192.040}{2.303 \times 8 \times 8.314 \times 298.2}$$

$$= 4.204.$$

$$pE = pE^\circ - \frac{1}{8} \log \frac{[HS^-]}{[SO_4^{2-}](a_{H^+})^9}$$
 At the boundary, $[HS^-] = [SO_4^{2-}] = 10^{-2} \text{ mol L}^{-1}$:
$$pE = 4.202 - \frac{9}{8} \log \frac{1}{a_{H^+}}$$

$$= 4.204 - 1.125 \text{ pH}$$
 This is line 'g' on Fig. 10.5; above it is the domain of SO_4^{2-} , below it HS^-.

Fig. 10.5 The pE/pH for the aqueous sulfur system.

pH

10.2 Two-variable diagrams: The sulfur system

Template of pE/pH diagram

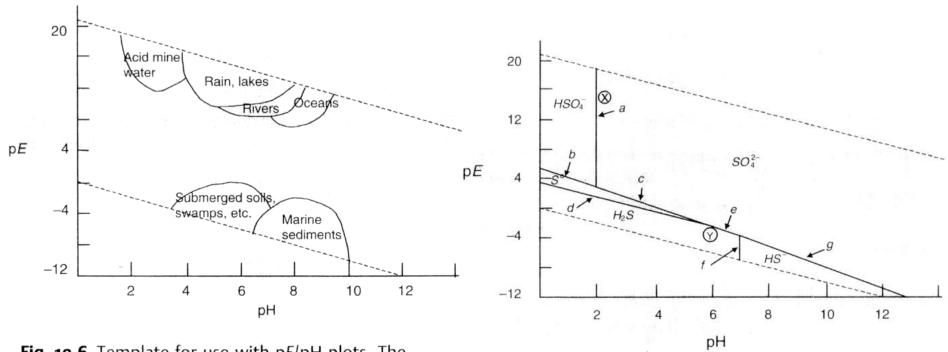


Fig. 10.6 Template for use with pE/pH plots. The indicated areas show typical pE and pH values for commonly encountered aqueous, soil, and sediment environments.

Fig. 10.5 The pE/pH for the aqueous sulfur system.