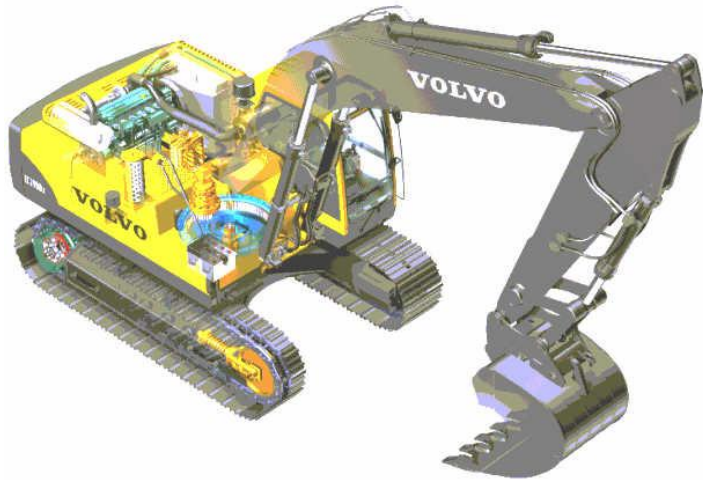


Fluid Systems



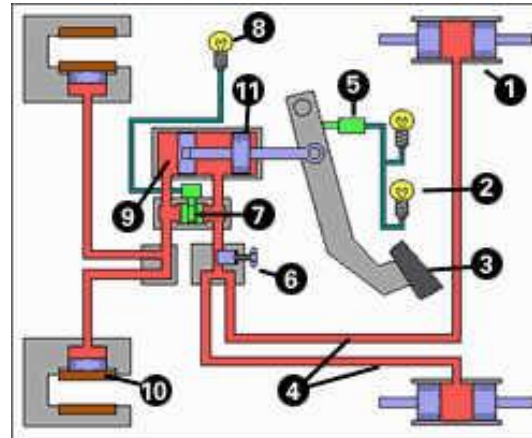
Hydraulic Systems



Excavator

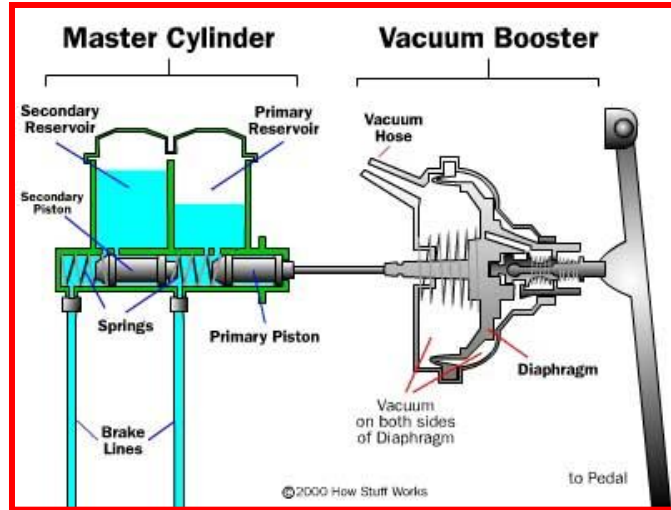
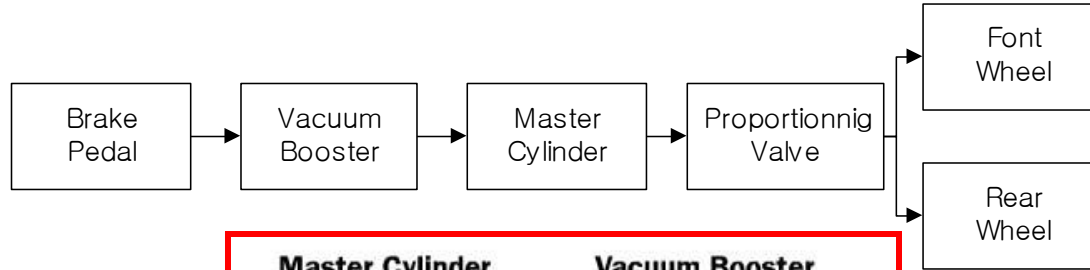


Brake System

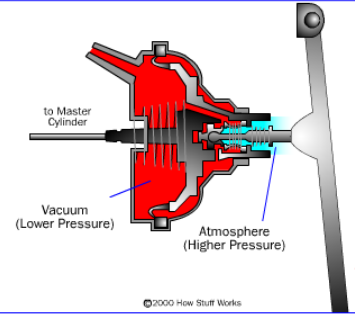


- 1) Wheel Cylinder
- 2) Brake Light
- 3) Brake Pedal
- 4) Rear Brake Lines
- 5) Stop Light Switch (Mechanical)
- 6) Front/Rear Balance Valve
- 7) Pressure Differential Valve
- 8) Brake Warning Lamp
- 9) Brake Fluid
- 10) Brake Pad
- 11) Master Cylinder

Brake System

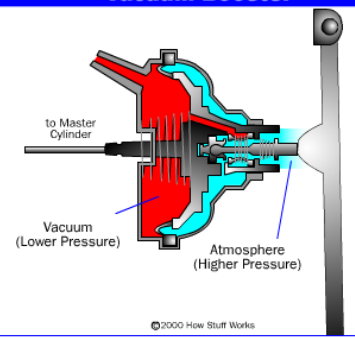


Vacuum Booster

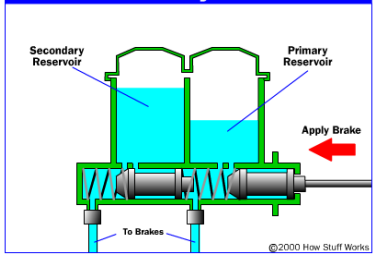


↓ **Apply brake**

Vacuum Booster

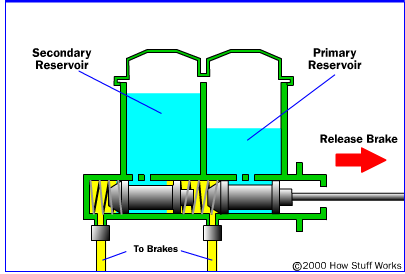


How a Master Cylinder Works



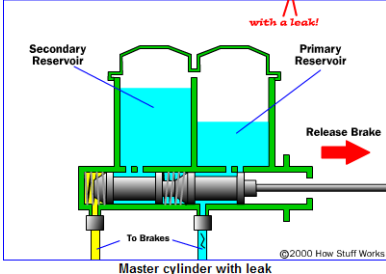
↓ **w/o leak**

How a Master Cylinder Works



↓ **with leak**

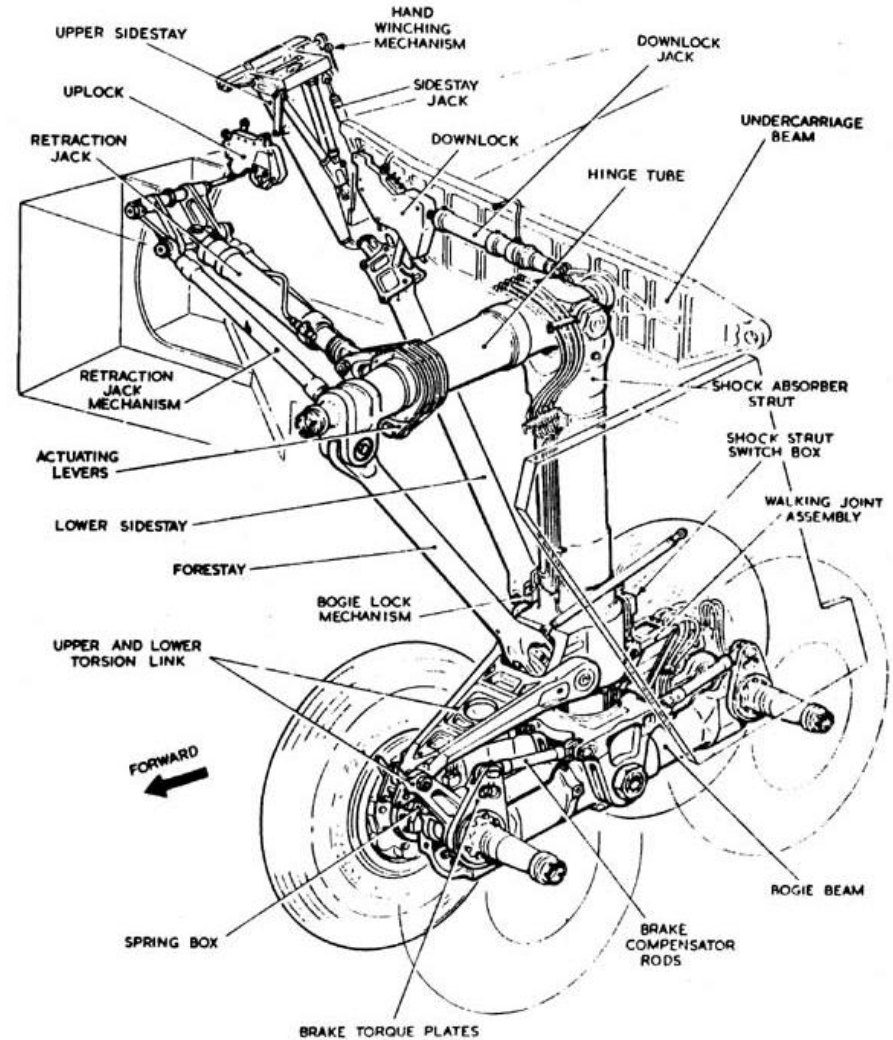
How a Master Cylinder Works



Hydraulic Systems : Landing Gear System

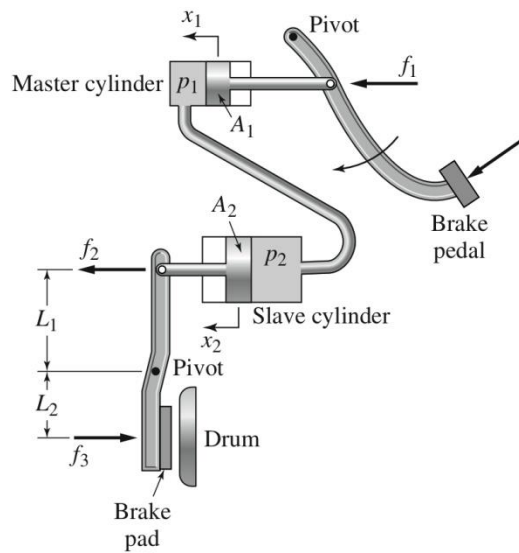


Landing gear system of AIRBUS A330



Conservation of Mass

$$\dot{m} = q_{mi} - q_{mo}$$



$$i) A_1 dx_1 = A_2 dx_2$$

$$ii) p_1 = p_2 + \rho gh$$

$$f_1 =$$

$$f_2 =$$

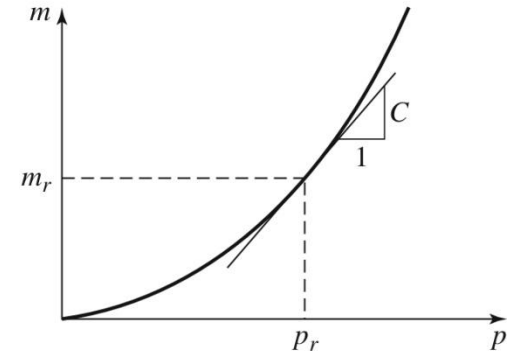
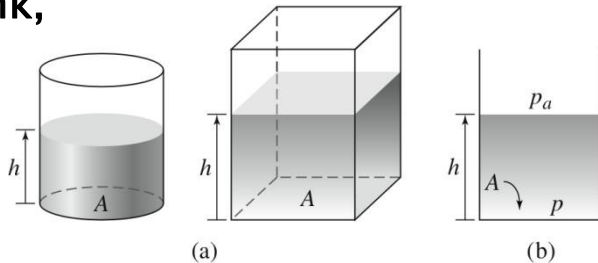
$$f_2 =$$

$$dx_2 =$$

Fluid Capacitance

$$C =$$

For a tank,



General fluid capacitance

$$C = \rho A \frac{dh}{dp} = \rho A \frac{1}{\rho g} = \frac{A}{g}$$

$$\frac{dm}{dt} =$$

$$C \frac{dp}{dt} = \rho A \frac{dh}{dt} = q_{mi} - q_{mo}$$

For liquid level system, C is defined as

$$C = \frac{\text{change in liquid stored } m^3}{\text{change in head } m} = \rho A$$

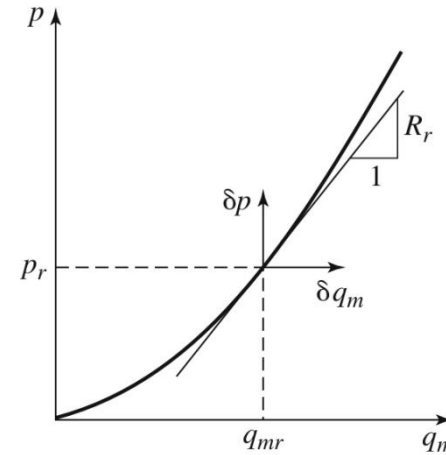
use h(pressure head), instead of p.

Fluid Resistance

$$R = \frac{\Delta p}{q_m}$$

$$q_m = \frac{p}{R} \quad \text{For laminar flow}$$

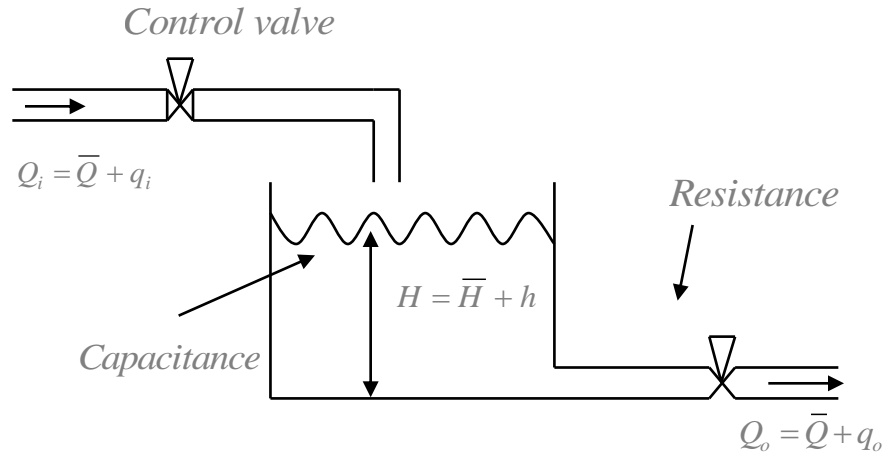
$$q_m = \sqrt{\frac{p}{R_l}} \quad \text{For turbulent flow}$$



For liquid level system, C is defined as

$$R = \frac{\text{change in level difference}}{\text{change in flow rate}} = \frac{m}{m^3 / s} = \frac{dh}{dq_m}$$

Liquid Level Systems



$$R = \frac{\text{change in level difference} \quad m}{\text{change in flow rate} \quad m^3 / s}$$

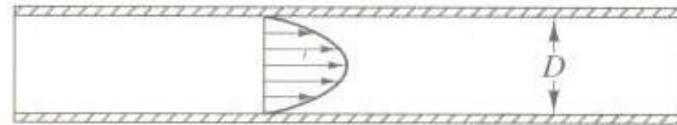
$$C = \frac{\text{change in liquid stored} \quad m^3}{\text{change in head} \quad m}$$

Steady state : $Q_i = \bar{Q} = Q_o =$

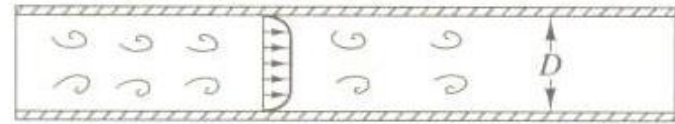
consider, $Q_o = \frac{H}{R}, \quad Q_i - Q_o =$

Basic Concepts

Laminar flow : When the viscous forces are dominant (slow flow, low Re) they are sufficient enough to keep all the fluid particles in line, then the flow is laminar.



Turbulent flow : It can be interpreted that when the inertial forces dominate over the viscous forces (when the fluid is flowing faster and Re is larger) then the flow is turbulent.



Reynolds number (Re) : The ratio of inertial forces to viscous forces.

It is used to determine whether a flow will be laminar or turbulent.

$$Re = \frac{\rho v D}{\mu}$$

μ : the dynamic viscosity of the fluid

ρ : density of the fluid

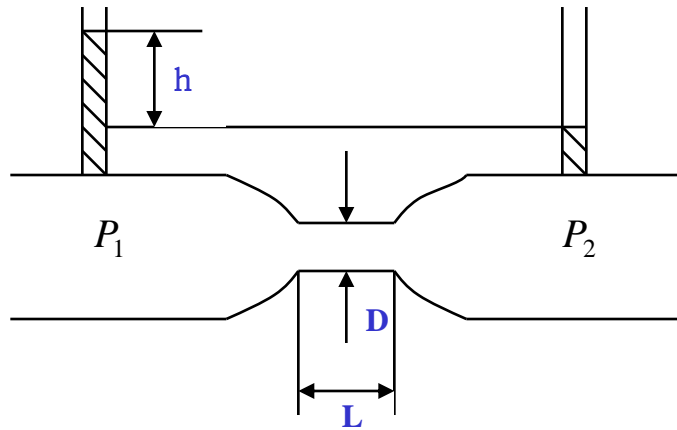
D : diameter

$Re < 2000$: always laminar

$Re > 4000$: always turbulent

Laminar Flow

Cylindrical pipe



$$P_1 - P_2 = \rho gh, \quad Q \frac{128\nu L}{g\pi D^4} = h$$

ν : viscosity,

L : length of pipe

D : diameter of pipe

$$Q = \frac{h}{R} = K_1 h, \quad R = \frac{128\nu L}{g\pi D^4} \quad [s/m^2]$$

Q : steady – state flow rate

K_1 : constant

h : steady – state head

Laminar Flow

Liquid level dynamics :

$$C \frac{dH}{dt} =$$
$$= \bar{Q} + q_i - (\bar{Q} + q_o) = q_i - q_o$$

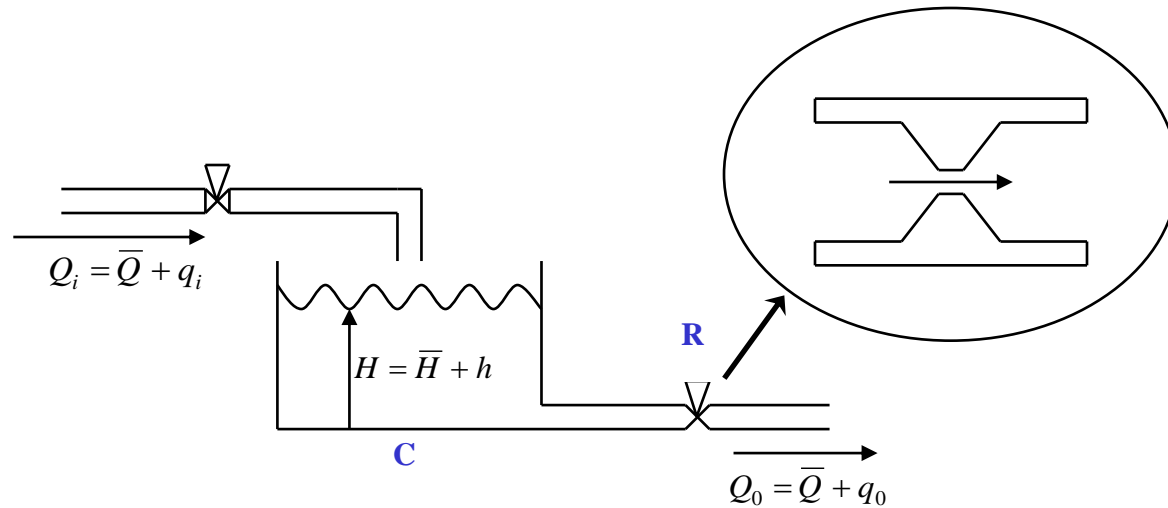
$$\frac{dH}{dt} = \frac{d}{dt}(\bar{H} + h) = \frac{dh}{dt}$$

$$Q_o =$$

$$\rightarrow \frac{dh}{dt} =$$



Turbulent Flow



$$Q = C_d \cdot a \cdot \sqrt{\frac{2}{\rho}(P_1 - P_2)}$$

ρ : density, a : area, C_d : discharge coefficient

steady state: $Q_i = \bar{Q} = Q_o = K_t \sqrt{\bar{H}}$

Turbulent Flow

Liquid level dynamics

$$C \frac{dH}{dt} = Q_i - Q_o = \bar{Q} + q_i - K\sqrt{H}$$

$$\frac{dH}{dt} = \frac{1}{C} Q_i - \frac{1}{C} K\sqrt{H} = f(Q_i, H)$$

$$f(Q_i, H) = f(\bar{Q}_i, \bar{H}) + \left. \frac{\partial f}{\partial Q_i} \right|_{\bar{Q}, \bar{H}} (Q_i - \bar{Q}) + \frac{1}{2!} \frac{\partial^2 f}{\partial Q_i^2} (Q_i - \bar{Q})^2 + \dots$$

$$\dots + \left. \frac{\partial f}{\partial H} \right|_{\bar{Q}, \bar{H}} (H - \bar{H}) + \frac{1}{2!} \frac{\partial^2 f}{\partial H^2} (H - \bar{H})^2 + \dots$$

$$= \frac{1}{C} \bar{Q} - \frac{1}{C} K\sqrt{\bar{H}} + \left(\frac{1}{C} q_i - \frac{K}{C \cdot 2\sqrt{\bar{H}}} h \right) + \text{high order term}$$



Turbulent Flow

$$\frac{dH}{dt} = \frac{d\bar{H}}{dt} + \frac{dh}{dt}$$

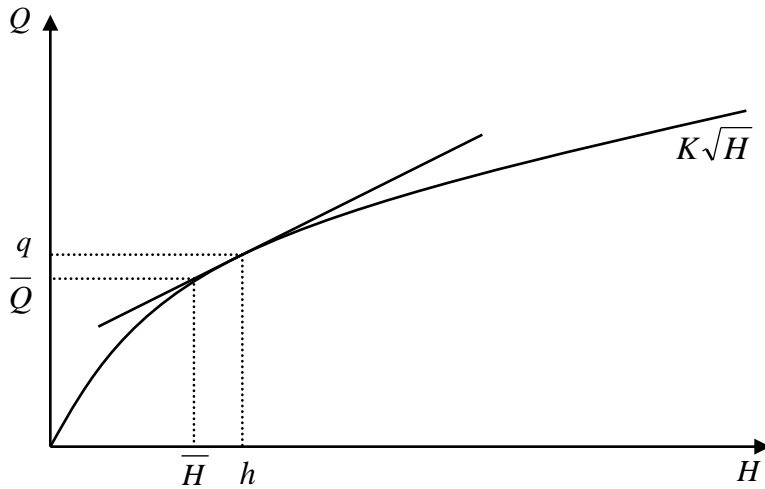
$$\Rightarrow \frac{dh}{dt} = \frac{1}{C} q_i - \frac{K}{C \cdot 2\sqrt{\bar{H}}} h$$

$$q_o = \frac{h}{R}, \quad R = \frac{2\sqrt{\bar{H}}}{K} = \frac{2\bar{H}}{\bar{Q}}, \quad (\bar{Q} = K\sqrt{\bar{H}})$$

$$\therefore \begin{cases} \frac{dh}{dt} = -\frac{1}{CR} h + \frac{1}{C} q_i \\ q_o = \frac{h}{R} \end{cases} \quad \text{for small } q_i$$



Linearization



$$Q = \bar{Q} + q = K\sqrt{\bar{H}} + (\quad) \cdot h$$

$$y = f(x), \quad \bar{y} = f(\bar{x}), \quad x = \bar{x} + \Delta x$$

$$y = f(\bar{x}) + \left. \frac{\partial f}{\partial x} \right|_{\bar{x}} \cdot \Delta x + \frac{1}{2!} \left. \frac{\partial^2 f}{\partial x^2} \right|_{\bar{x}} \cdot \Delta x^2 + \dots$$

$$\approx \bar{y} + \left. \frac{\partial f}{\partial x} \right|_{\bar{x}} \cdot \Delta x$$

$$y - \bar{y} = \left. \frac{\partial f}{\partial x} \right|_{\bar{x}} (x - \bar{x}) = K(x - \bar{x})$$

$$y = f(x_1, x_2) \approx f(\bar{x}_1, \bar{x}_2) + \left. \frac{\partial f}{\partial x_1} \right|_{\bar{x}_1, \bar{x}_2} (x_1 - \bar{x}_1) + \left. \frac{\partial f}{\partial x_2} \right|_{\bar{x}_1, \bar{x}_2} (x_2 - \bar{x}_2)$$

$$= \bar{y} + K_1(x_1 - \bar{x}_1) + K_2(x_2 - \bar{x}_2)$$

$$\therefore y - \bar{y} = K_1(x_1 - \bar{x}_1) + K_2(x_2 - \bar{x}_2)$$



Summary of Liquid Level Systems

Laminar flow

$$\frac{dh}{dt} = -\frac{1}{CR}h + \frac{1}{C}q_i$$

$$\bar{Q} = K \cdot \bar{H} \quad R = \frac{\bar{H}}{\bar{Q}}$$

$$R = \frac{128\nu L}{g\pi D^4}$$

$$q_o = \frac{h}{R}$$

Turbulent flow

$$\frac{dh}{dt} = -\frac{1}{CR}h + \frac{1}{C}q_i$$

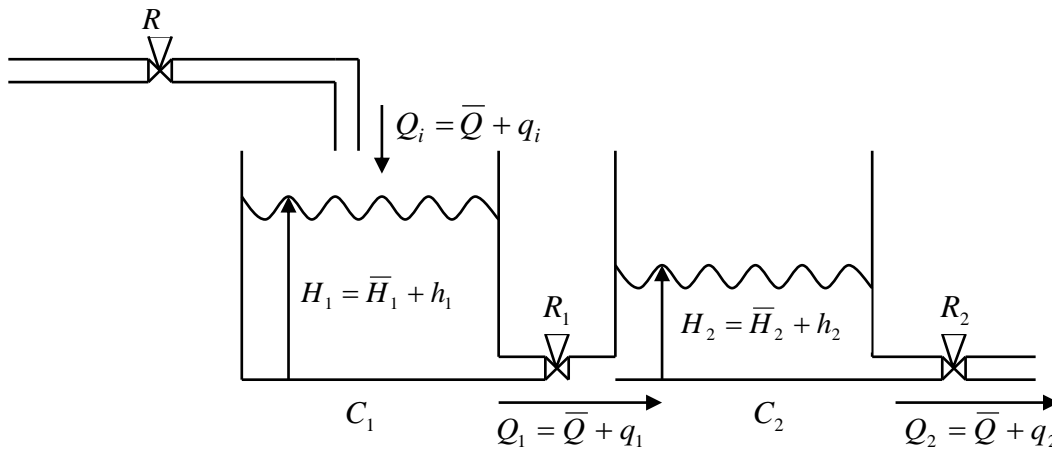
$$q_o = \frac{h}{R}$$

$$R = \frac{2\bar{H}}{\bar{Q}} = \frac{2\sqrt{\bar{H}}}{K} = \frac{2\sqrt{\bar{H}}}{C_d a \sqrt{2g}}$$

$$\left(\because \bar{Q} = K\sqrt{\bar{H}} = C_d a \sqrt{\frac{2}{\rho} \rho g \bar{H}} = C_d a \sqrt{2g} \sqrt{\bar{H}} \right)$$



Liquid Level Systems with Interaction



Steady state :

$$Q_i = \bar{Q} = Q_1 = Q_2$$

$$= \frac{\bar{H}_1 - \bar{H}_2}{R_1} = \frac{\bar{H}_2}{R_2}$$

Liquid level dynamics :

$$C_1 \frac{dH_1}{dt} = \bar{Q} + q_i - (\bar{Q} + q_1) \quad \rightarrow \quad C_1 \frac{dh_1}{dt} = q_i - q_1$$

$$Q_1 = \bar{Q} + q_1 = \frac{1}{R_1} (\bar{H}_1 + h_1 - (\bar{H}_2 + h_2)) \quad \rightarrow \quad q_1 = \frac{h_1 - h_2}{R_1}$$

$$C_2 \frac{dH_2}{dt} = \bar{Q} + q_1 - (\bar{Q} + q_2) \quad \rightarrow \quad C_2 \frac{dh_2}{dt} = q_1 - q_2$$

$$Q_2 = \bar{Q} + q_2 = \frac{\bar{H}_2 + h_2}{R_2} \quad \rightarrow \quad q_2 = \frac{h_2}{R_2}$$

Liquid Level Systems with Interaction

$$\therefore \begin{cases} \frac{dh_1}{dt} = -\frac{1}{C_1} \left(\frac{h_1 - h_2}{R_1} \right) + \frac{1}{C_1} q_i \\ \frac{dh_2}{dt} = \frac{1}{C_2} \left(\frac{h_1 - h_2}{R_1} \right) - \frac{1}{C_2} \frac{h_2}{R_2} \end{cases}$$

$$\text{Transfer Function} = \frac{Q_2(S)}{Q_i(S)} = \frac{1}{R_1 C_1 R_2 C_2 S^2 + (R_1 C_1 + R_2 C_2 + R_2 C_1) S + 1}$$

