

- Conservation of energy ( $\psi = \rho e + \frac{1}{2} \rho \underline{u} \cdot \underline{u}$ )  
 $\uparrow$  internal energy  
 total work done by  $\underline{P} \rightarrow \int_S \underline{u} \cdot \underline{P} dS$   
 $\underline{f} \rightarrow \int_V \underline{u} \cdot \rho \underline{f} dV$

$\underline{q}$  : conductive heat flux leaving the c.v  
 the quantity of heat leaving the fluid mass  
 per unit time per unit surface area =  $\underline{q} \cdot \underline{n}$   
 $\therefore$  net amount of heat leaving the fluid per unit time  
 $= \int_S \underline{q} \cdot \underline{n} dS$

$$\underbrace{\frac{D}{Dt} \int_V (\rho e + \frac{1}{2} \rho \underline{u} \cdot \underline{u}) dV}_{RTT} = \int_S \underline{u} \cdot \underline{P} dS + \int_V \underline{u} \cdot \rho \underline{f} dV - \int_S \underline{q} \cdot \underline{n} dS$$

$$\int_S u_j \delta_{ij} n_i dS \quad \int_V u_j \rho f_j dV \quad \int_S q_j n_j dS$$

$$\int_V \frac{\partial}{\partial x_i} (u_j \delta_{ij}) dV \quad \int_V \frac{\partial q_j}{\partial x_j} dV$$

$$\therefore \frac{\partial}{\partial t} (\rho e + \frac{1}{2} \rho u_j u_j) + \frac{\partial}{\partial x_k} (\rho e + \frac{1}{2} \rho u_j u_j) u_k$$

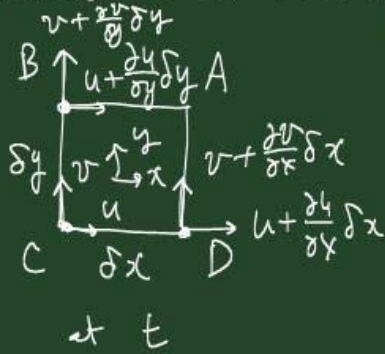
$$= \frac{\partial}{\partial x_i} (u_j \delta_{ij}) + u_j \rho f_j - \frac{\partial q_j}{\partial x_j}$$

After some algebra,

$$\boxed{\rho \frac{\partial e}{\partial t} + \rho u_k \frac{\partial e}{\partial x_k} = \delta_{ij} \frac{\partial u_j}{\partial x_i} - \frac{\partial q_j}{\partial x_j}} \quad \text{energy eq.}$$

- Discussion of conservation eqs.  
 $\sigma_{ij}$  and  $q_j$  should be further specified  
 $\rightarrow$  constitutive eqs,  $\sigma_{ij} \sim f\left(\frac{\partial u_i}{\partial x_j}\right) \parallel$   
 $q_j \sim g\left(\frac{\partial T}{\partial x_j}\right) \parallel$

- rotation and rate of shear



$$\rightarrow \frac{\delta \alpha}{\delta t} = \frac{\partial v}{\partial x}, \quad (\delta y + \frac{\partial v}{\partial y} \delta y \delta t) \delta \beta = \frac{\partial u}{\partial y} \delta y \delta t$$

$$\alpha: \text{counterclockwise} \rightarrow \frac{\delta \beta}{\delta t} = \frac{\partial u}{\partial y} \quad \beta: \text{clockwise}$$

rate of counterclockwise rotation

$$= \frac{1}{2} \left( \frac{\delta \alpha}{\delta t} - \frac{\delta \beta}{\delta t} \right) = \frac{1}{2} \left( \frac{\partial v}{\partial x} - \frac{\partial u}{\partial y} \right)$$

$$\text{rate of shear} = \frac{1}{2} \left( \frac{\delta \alpha}{\delta t} + \frac{\delta \beta}{\delta t} \right) = \frac{1}{2} \left( \frac{\partial v}{\partial x} + \frac{\partial u}{\partial y} \right)$$

In general,

$$\text{rate of rotation} = \frac{1}{2} \left( \frac{\partial u_i}{\partial x_j} - \frac{\partial u_j}{\partial x_i} \right) \text{ anti-symmetric}$$



$$\text{rate of shear} = \frac{1}{2} \left( \frac{\partial u_i}{\partial x_j} + \frac{\partial u_j}{\partial x_i} \right) \text{ symmetric}$$

Deformation-rate tensor  $e_{ij}$


$$e_{ij} = \frac{\partial u_i}{\partial x_j} = \frac{1}{2} \left( \frac{\partial u_i}{\partial x_j} - \frac{\partial u_j}{\partial x_i} \right) + \frac{1}{2} \left( \frac{\partial u_i}{\partial x_j} + \frac{\partial u_j}{\partial x_i} \right)$$

• Constitutive eq.

4 conditions that the stress tensor is supposed to satisfy

- ① fluid at rest  $\rightarrow$  stress is hydrostatic pressure  
 thermodynamic press.  $\rightarrow$  
- ②  $\sigma_{ij}$  is linearly related to  $e_{kl}$  and depends only on that tensor.
- ③ for solid-body rotation of the fluid   
 $\rightarrow$  no shearing action  $\rightarrow$  no shear stress during such a motion.

- ④ no preferred direction in the fluid  
 $\rightarrow$  fluid properties are point fcs. (i.e. isotropic)

①  $\rightarrow \sigma_{ij} = -p \delta_{ij} + \tau_{ij}$   

thermo. press
depends on the fluid motm. called shear stress tensor.

②  $\rightarrow \sigma_{ij} \sim e_{kl} \Rightarrow \tau_{ij} = \alpha_{ijkl} \frac{\partial u_k}{\partial x_l}$   
 $\tau_{ij} = \alpha_{ijkl} \cdot \frac{1}{2} \left( \frac{\partial u_k}{\partial x_l} + \frac{\partial u_l}{\partial x_k} \right) + \alpha_{ijkl} \cdot \frac{1}{2} \left( \frac{\partial u_k}{\partial x_l} - \frac{\partial u_l}{\partial x_k} \right)$

for ③  $\rightarrow \tau_{ij} = 0$  but  $\neq 0$   
 So, this term should go away!



$$\therefore \tau_{ij} = \frac{1}{2} \beta_{ijkl} \left( \frac{\partial u_k}{\partial x_l} + \frac{\partial u_l}{\partial x_k} \right)$$

fluid property cond. (4)  $\rightarrow$  isotropic

$$\begin{aligned} \rightarrow \beta_{ijkl} &= \lambda \delta_{ij} \delta_{kl} + \mu (\delta_{ik} \delta_{jl} + \delta_{il} \delta_{jk}) \\ &+ \mu (\delta_{ik} \delta_{jl} - \delta_{il} \delta_{jk}) \end{aligned} \quad (\text{App. B})$$

is zero when multiplied by shear rate.

$$\therefore \tau_{ij} = \frac{1}{2} \left[ \lambda \delta_{ij} \delta_{kl} + \mu (\delta_{ik} \delta_{jl} + \delta_{il} \delta_{jk}) \right] \left( \frac{\partial u_k}{\partial x_l} + \frac{\partial u_l}{\partial x_k} \right)$$

$$\lambda \delta_{ij} \cdot 2 \frac{\partial u_k}{\partial x_k} \quad 2\mu \left( \frac{\partial u_i}{\partial x_j} + \frac{\partial u_j}{\partial x_i} \right)$$

$$\tau_{ij} = \lambda \delta_{ij} \frac{\partial u_k}{\partial x_k} + \mu \left( \frac{\partial u_i}{\partial x_j} + \frac{\partial u_j}{\partial x_i} \right)$$

$$\sigma_{ij} = -p \delta_{ij} + \lambda \delta_{ij} \frac{\partial u_k}{\partial x_k} + \mu \left( \frac{\partial u_i}{\partial x_j} + \frac{\partial u_j}{\partial x_i} \right)$$

$\sigma_{ij}$ : second-order symmetric tensor.

$$\sigma_{ij} \sim \begin{matrix} \circ & \circ & \circ \\ \circ & \circ & \circ \\ \circ & \circ & \circ \end{matrix}$$

$$+ \begin{matrix} \circ & \circ & \circ \\ \circ & \circ & \circ \\ \circ & \circ & \circ \end{matrix}$$

$\tau_{ij}$ : " " "

coeffs.  $\lambda$  and  $\mu \rightarrow$  determined empirically

$$\therefore \cdot \mathbf{q}_j = -k \frac{\partial T}{\partial x_j} \quad k: \text{thermal conductivity}$$

Fourier law

- Viscosity coefficients

Consider a simple shear flow  $u = u(y)$   
 $v = w = 0$

$$\begin{aligned} \rightarrow \sigma_{12} = \sigma_{21} &= \mu \frac{du}{dy} \Rightarrow \mu : (\text{dynamic}) \text{ viscosity} \\ \sigma_{11} = \sigma_{22} = \sigma_{33} &= -p \quad \nu \equiv \mu/\rho : \text{kinematic} \\ \sigma_{13} = \sigma_{31} = \sigma_{23} = \sigma_{32} &= 0 \quad \text{thermo, press.} \\ &\quad \text{viscosity} \end{aligned}$$