

# Microbial kinetics

# Today's lecture

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- Monod kinetics
- Addressing decay
- Rate of substrate utilization associated with microbial growth

# Monod equation

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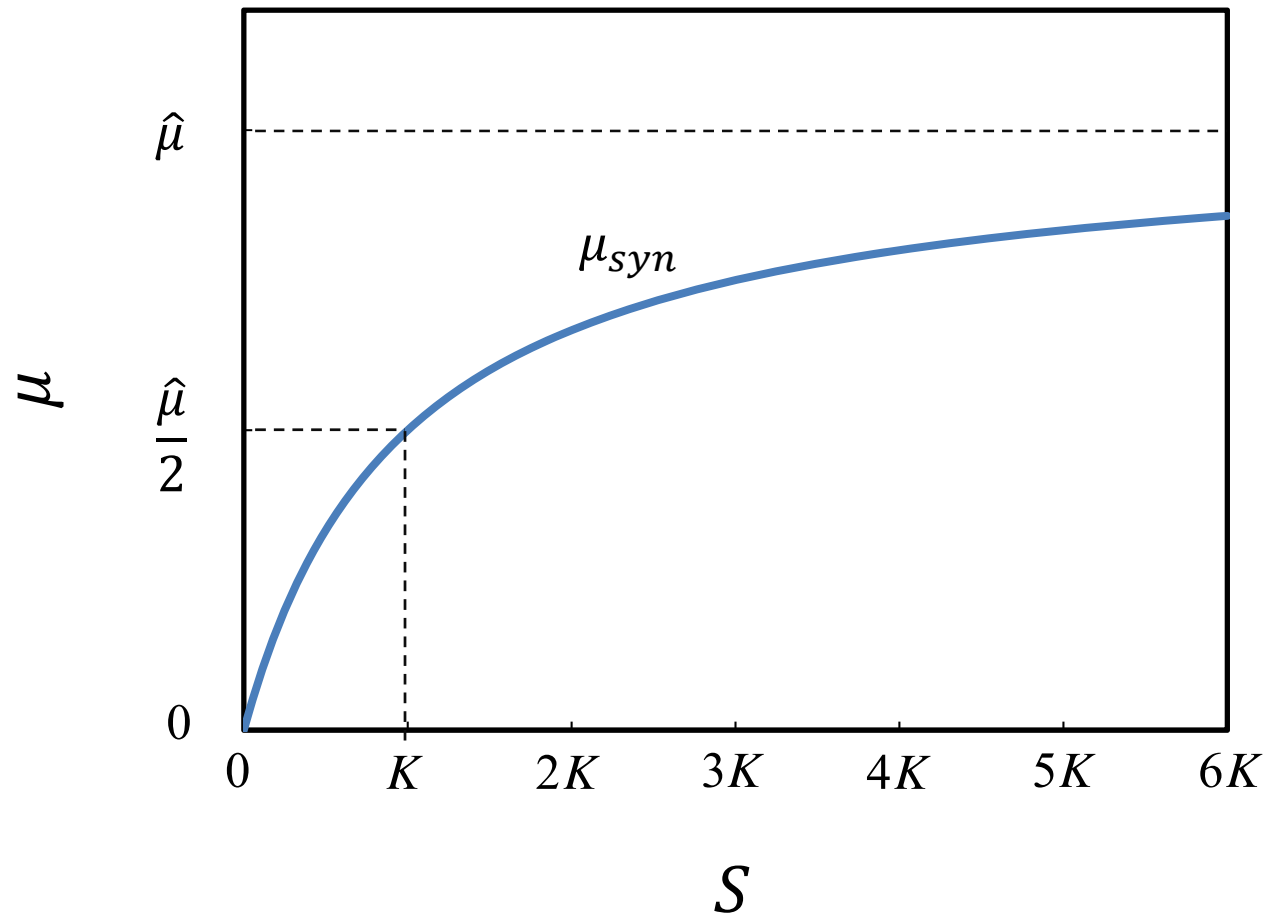
$$\mu_{syn} = \left( \frac{1}{X_a} \cdot \frac{dX_a}{dt} \right)_{syn} = \hat{\mu} \frac{S}{K + S}$$

where

- $\mu_{syn}$  = specific growth rate due to synthesis ( $T^{-1}$ )
- $X_a$  = concentration of active biomass ( $M_x L^{-3}$ )
- $S$  = concentration of the rate-limiting substrate ( $M_s L^{-3}$ )
- $\hat{\mu}$  = maximum specific growth rate ( $T^{-1}$ )
- $K$  = half saturation coefficient ( $M_s L^{-3}$ )

# Monod equation

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# Typical values for K

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Process	K (mg substrate/L)
Aerobic: organic mixtures single organics nitrification	50-150 mg COD/L 1-10 mg COD/L 0.4-2 mg NH <sub>3</sub> -N/L
Anaerobic: denitrification methane fermentation: acetate, propionate sewage sludge	0.06-0.20 mg NO <sub>3</sub> <sup>-</sup> -N/L 600-900 mg COD/L 2000-3000 mg COD/L

# Growth kinetics with decay

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- As discussed in the previous lecture, we assume decay is proportional to cell biomass

$$\left(\frac{dX_a}{dt}\right)_{decay} = -bX_a$$

in the form of specific growth rate,

$$\mu_{dec} = \left(\frac{1}{X_a} \cdot \frac{dX_a}{dt}\right)_{decay} = -b$$

where  $\mu_{dec}$  = specific growth rate due to decay ( $T^{-1}$ )

$b$  = decay coefficient ( $T^{-1}$ )

# Overall bacterial growth kinetics

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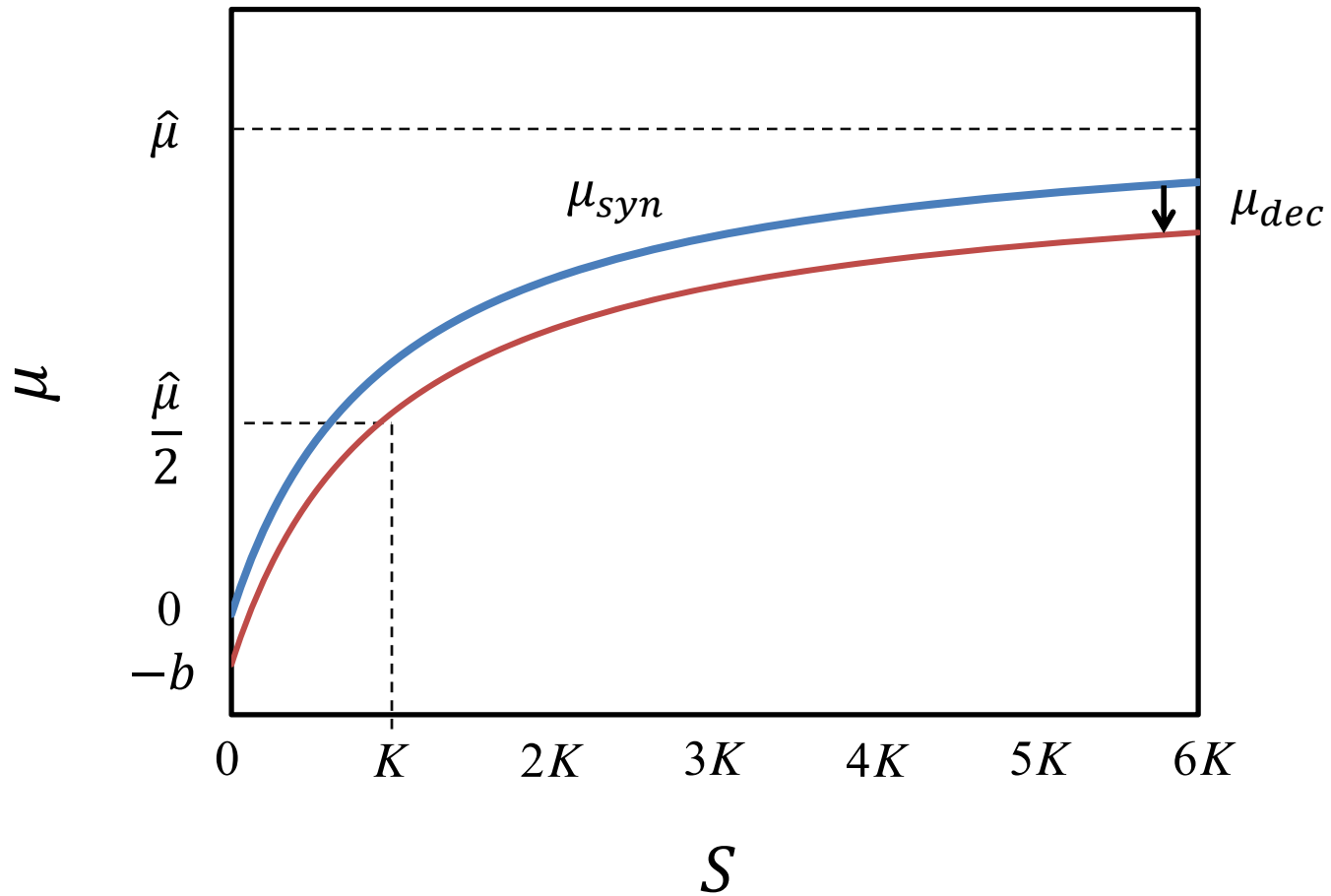
(Net growth) = (New growth) + (Decay)

$$\mu = \frac{1}{X_a} \cdot \frac{dX_a}{dt} = \mu_{syn} + \mu_{dec} = \hat{\mu} \frac{S}{K + S} - b$$

where  $\mu$  = net specific growth rate ( $T^{-1}$ )

# Growth kinetics with decay

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# More on decay

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$$\mu_{dec} = \left( \frac{1}{X_a} \cdot \frac{dX_a}{dt} \right)_{decay} = -b$$

- Most fraction ( $f_d \approx 0.8$ ) is oxidized
- The other fraction ( $1 - f_d \approx 0.2$ ) is accumulated as inert biomass

Rate of oxidation (respiration):  $\left( \frac{1}{X_a} \cdot \frac{dX_a}{dt} \right)_{resp} = -f_d b$

Rate of conversion to inert biomass:

$$\left( \frac{1}{X_a} \cdot \frac{dX_a}{dt} \right)_{inert} = -\frac{1}{X_a} \cdot \frac{dX_i}{dt} = -(1 - f_d)b$$

$X_i =$  inert biomass ( $M_x L^{-3}$ )

# Substrate utilization rate

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Recall that,

$$Y = \frac{\text{(g cells produced)}}{\text{(g substrate utilized)}} = \frac{(dX_a/dt)_{syn}}{-dS/dt}$$

and

$$\mu_{syn} = \left( \frac{1}{X_a} \cdot \frac{dX_a}{dt} \right)_{syn} = \hat{\mu} \frac{S}{K + S}$$

So Monod equation can be also written as:

$$\frac{dS}{dt} = -\frac{1}{Y} \left( \frac{dX_a}{dt} \right)_{syn} = -\frac{\hat{\mu}}{Y} \frac{S}{K + S} X_a$$

# Substrate utilization rate

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Substrate utilization rate,  $r_{ut}$  [ $M_s L^{-3} T^{-1}$ ]

$$r_{ut} = \frac{dS}{dt} = -\frac{\hat{q}S}{K + S} X_a$$

$\hat{q} = \hat{\mu}/Y$ , max. specific rate of substrate utilization ( $M_s M_x^{-1} T^{-1}$ )

Recall that,

$$Y = f_s^0 \frac{M_c}{n_e \cdot (8 \text{ g COD}/e^- \text{ eq})}$$

