# Lecture Note #6

## Double layer structure & adsorption (Ch. 13)

Thermodynamics of the double layer

Experimental evaluation of surface excesses & electrical parameters

Models for double layer structure

Helmholtz model

Gouy-Chapman theory

Stern's modification

Specific adsorption

Studies at solid electrodes

Double layer at solids

Single-crystal electrode surfaces

Solid metal-solution interface

Extent & rate of specific adsorption

Nature of specific adsorption

Adsorption isotherms

Rate of adsorption

Effect of adsorption of electroinactive species

Double layer effects on electrode reaction rates

Reading: Bard, ch. 13

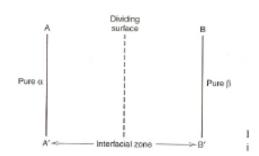
#### Thermodynamics of the double layer

#### Gibbs adsorption isotherm

Suppose an interface of surface area A separating two phases,  $\alpha \& \beta$ 

- → interfacial zone (~ 100 Å)
- → excesses and deficiencies

in the concentration of components



Surface excess (in # of moles of any species)

$$n_i^{\sigma} = n_i^{S} - n_i^{R}$$

 $n_i^{\sigma}$ : excess quantity (any extensive variable, e.g., electrochemical free energy),  $n_i^{S} \& n_i^{R}$ : # of moles of species i in interfacial region for actual & reference systems

# Electrochemical free energy

For the reference system,  $\overline{G}^R = \overline{G}^R(T, P, n_i^R)$ 

For the actual system,  $\overline{G}^S = \overline{G}^S(T, P, A, n_i^S)$ 

$$\begin{split} d\overline{G}^R &= (\partial \overline{G}^R/\partial T)dT + (\partial \overline{G}^R/\partial P) + \sum (\partial \overline{G}^R/\partial n_i^R)dn_i^R \\ d\overline{G}^S &= (\partial \overline{G}^S/\partial T)dT + (\partial \overline{G}^S/\partial P)dP + (\partial \overline{G}^S/\partial A)dA + \sum (\partial \overline{G}^S/\partial n_i^S)dn_i^S \end{split}$$

At const T & P  $\rightarrow$  1<sup>st</sup> two terms can be dropped  $(\partial \overline{G}^R/\partial n_i^R) = \overline{\mu}_i$  (electrochemical potential)  $\rightarrow$  const at equilibrium

$$\overline{\mu_i} = (\partial \overline{G}^R / \partial n_i^R) = (\partial \overline{G}^S / \partial n_i^S)$$

 $(\partial \overline{G}^S/\partial A) = \emptyset$  (surface tension): a measure of the energy required to produce a unit area of new surface

Differential excess free energy

$$\begin{split} d\overline{G}^{\circ} &= d\overline{G}^{S} - d\overline{G}^{R} = \gamma dA + \sum \overline{\mu}_{i} d(n_{i}^{S} - n_{i}^{R}) \\ d\overline{G}^{\circ} &= \gamma dA + \sum \overline{\mu}_{i} dn_{i}^{\circ} \end{split}$$

Euler's theorem for variables, A and n<sub>i</sub> (const T and P)

$$\begin{aligned} \overline{G}^{\sigma} &= (\partial \overline{G}^{\sigma}/\partial A)A + \sum (\underline{\partial} \overline{G}^{\sigma}/\partial n_{i}{}^{\sigma})n_{i}{}^{\sigma} \\ \overline{G}^{\sigma} &= \gamma A + \sum \overline{\mu}_{i}n_{i}{}^{\sigma} \end{aligned}$$

$$d\overline{G}^{\circ} = \gamma dA + \sum \overline{\mu}_{i} dn_{i}^{\circ} + A d\gamma + \sum n_{i}^{\circ} d\overline{\mu}_{i}$$

$$Ad\gamma + \sum n_{i}^{\circ} d\overline{\mu}_{i} = 0$$

Surface excess concentration,  $\Gamma_i = n_i^{\circ}/A$  (excesses per unit area of surface)

$$-dy = \sum \Gamma_i d\overline{\mu_i}$$

Gibbs adsorption isotherm: importance of surface tension for interfacial structure

#### Electrocapillary equation

Consider

M: neutral species

Gibbs adsorption isotherm; components of Hg electrode, ions, neutral

$$-d\gamma = (\lceil_{Hg}d\overline{\mu}_{Hg} + \lceil_e d\overline{\mu}_e^{\ Hg}) + (\lceil_{K^+}d\overline{\mu}_{K^+} + \lceil_{Cl^-}d\overline{\mu}_{Cl^-}) + (\lceil_M d\overline{\mu}^M + \lceil_{H2O}d\overline{\mu}_{H2O})$$

 $\overline{\coprod}_{e}^{Hg}$ : electrons in the mercury phase

Some linkages:

$$\begin{split} \overline{\mu}_{e}^{\,Hg} &= \overline{\mu}_{e}^{\,Cu} \\ \overline{\mu}_{KCl} &= \mu_{KCl} = \overline{\mu}_{K+} + \overline{\mu}_{Cl-} \\ \overline{\mu}_{H2O} &= \mu_{H2O} \\ \overline{\mu}_{M} &= \mu_{M} \\ d\overline{\mu}_{Hg} &= d\overline{\mu}_{Hg}^{\,\,0} = 0 \end{split}$$

$$-d\gamma = \Gamma_{e}d\overline{\mu}_{e}^{\,\,Cu} + (\Gamma_{K+}d\overline{\mu}_{KCl} - \Gamma_{K+}d\overline{\mu}_{Cl-} + \Gamma_{Cl-}d\overline{\mu}_{Cl-}) + (\Gamma_{M}d\mu_{M} + \Gamma_{H2O}d\mu_{H2O}) \end{split}$$

From the equilibrium at the reference interface

$$\begin{aligned} \overline{\mu}_{AgC1} + \overline{\mu}_e^{Cu'} &= \overline{\mu}_{Ag} + \overline{\mu}_{C1} \\ Since \ d\overline{\mu}_{AgC1} &= d\overline{\mu}_{Ag} = 0, \ d\mu_e^{Cu'} = d\mu_{C1} \end{aligned}$$

$$-d\gamma = \Gamma_e d\overline{\mu}_e^{Cu} - (\Gamma_{K+} - \Gamma_{C1-}) d\overline{\mu}_e^{Cu'} + \Gamma_{K+} d\mu_{KC1} + \Gamma_M d\mu_M + \Gamma_{H2O} d\mu_{H2O}$$

Excess charge density on the metallic side of the interface

$$\sigma^{M} = -F \Gamma_{e}$$

Opposite charge density on the solution side

$$\sigma^{S} = -\sigma^{M} = F(\Gamma_{K+} - \Gamma_{C1-})$$

$$d\mu_{e}^{Cu} - d\mu_{e}^{Cu'} = -Fd(\phi^{Cu} - \phi^{Cu'}) = -FdE_{-}$$

E: potential of the mercury electrode with respect to the reference

$$-d\gamma = \sigma^{M}dE_{\perp} + \Gamma_{K+}d\mu_{KCl} + \Gamma_{M}d\mu_{M} + \Gamma_{H2O}d\mu_{H2O}$$

Gibbs-Duhem relation at const T and P

$$\sum X_i d\mu_i = 0$$

Xi: mole fraction

$$X_{H2O}d\mu_{H2O} + X_{KCI}d\mu_{KCI} + X_Md\mu_M = 0$$

Remove  $d\mu_{H2O}$ 

$$-d\gamma = \sigma^M dE_- + [\Gamma_{K^+} - (X_{KCl}/X_{H2O})\Gamma_{H2O}] d\mu_{KCl} + [\Gamma_M - (X_M/X_{H2O})\Gamma_{H2O}] d\mu_M$$

Relative surface excess: measurable parameters

$$\Gamma_{\text{K+(H2O)}} = \Gamma_{\text{K+}} - (X_{\text{KCI}}/X_{\text{H2O}})\Gamma_{\text{H2O}}$$

$$\Gamma_{\text{M(H2O)}} = \Gamma_{\text{M}} - (X_{\text{M}}/X_{\text{H2O}})\Gamma_{\text{H2O}}$$

Cannot measure absolute surface excess of  $K^+$ , but only excess relative to water e.g., zero excess: same mole ratio of adsorption of  $K^+$  and  $H_2O$ 

positive excess:  $K^+ > H_2O$ 

Water: reference component

Dilute solutions: negligible  $(X_i/X_S)\Gamma_S$ 

#### Electrocapillary equation

$$-d\gamma = \sigma^{M}dE_{\perp} + \Gamma_{K+(H2O)}d\mu_{KC1} + \Gamma_{M(H2O)}d\mu_{M}$$

→ all measurable parameters

## Experimental evaluation of surface excesses & electrical parameters Electrocapillarity and the DME

For DME,

$$t_{max} = 2\pi r_c \gamma / mg$$

t<sub>max</sub>: drop lifetime

 $\rightarrow$   $t_{max}$  vs. E has same shape as the electrocapillary curve

#### Excess charge and capacitance

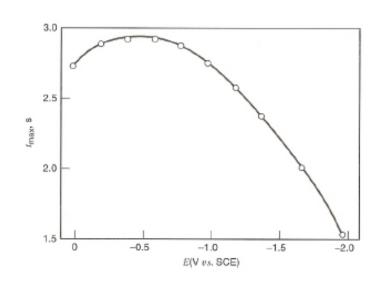
From electrocapillary equation,

$$\sigma^{M} = (\partial \gamma / \partial E_{\text{-}})_{\mu KC1, \mu M}$$

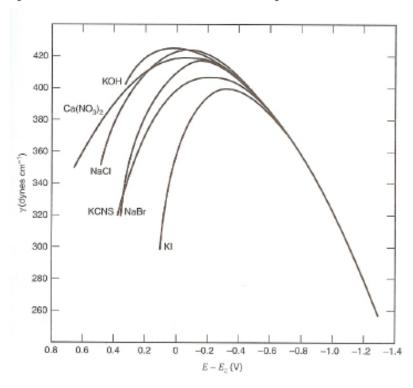
the excess charge on the electrode

→ slope of electrocapillary curve at any E

Drop time of a DME in 0.1 M KCl vs. E



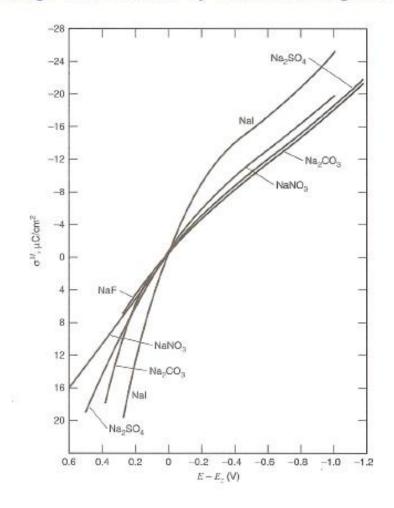
#### Electrocapillary curve in different electrolyte



- → the existence of a <u>maximum</u> in surface tension
- → potential at maximum: "electrocapillary maximum (ECM)"
- $\rightarrow$  curve slope = 0 at ECM  $\rightarrow$  "potential of zero charge" (PZC)  $\sigma^{M} = \sigma^{S} = 0$

At more negative potentials → the electrode surface has a negative excess charge At more positive potentials → positive surface charge

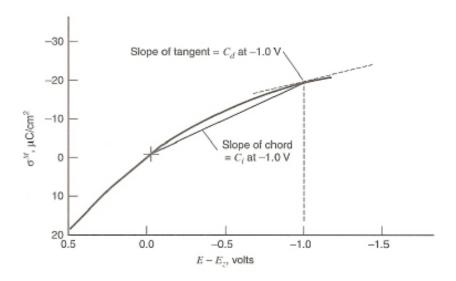
→ Plots of surface charge can be made by differentiating electrocapillary curves



The capacitance of the interface → its ability to store charge in response to a perturbation in potential

$$C_d = (\partial \sigma^M / \partial E)$$

<u>Differential capacitance</u>: the slope of the plot of  $\sigma^{M}$  vs. E



<u>Integral capacitance</u>,  $C_i$  (or K): ratio of total charge density  $(\sigma^M)$  at potential E to the total potential difference

$$C_i = \sigma^M/(E - E_Z)$$

 $E_Z$ : PZC

$$C_i = \int C_d dE / \int dE$$

Average of  $C_d$  over the potential range from  $E_Z$  to E

Differential capacitance is the more useful quantity, in part it is precisely measurable by impedance techniques

Capacitance can be obtained from the electrocapillary curves by double differentiation

$$\lambda = \left[ \right] \quad C^{q} dE$$

#### Relative surface excesses

From electrocapillary equation, relative surface excess of K+ at the interface

$$\Gamma_{\text{K+(H2O)}} = -(\partial \gamma / \partial \mu_{\text{KC1}})_{\text{E-},\mu}$$

Since  $\mu_{KC1} = \mu_{KC1}^0 + RT \ln a_{KC1}$ 

$$\Gamma_{\text{K+(H2O)}} = -(1/\text{RT})(\partial \gamma / \partial lna_{\text{KCl}})_{\text{E-,} \mu\text{M}}$$

→ relative surface excess \(\Gamma\_{K+(H2O)}\) at any potential E- by measuring surface tension for several KCl activities (at const M) Relative surface excess of Cl<sup>-</sup>: from the charge balance  $(\sigma^S = -\sigma^M = F(\Gamma_{K+} - \Gamma_{Cl-})$ 

Fig. 13.2.9: relative surface excess of 0.1 M KF in contact with mercury At potentials positive of E<sub>Z</sub> → surface excess of K<sup>+</sup>: negative → K<sup>+</sup> conc in the interface is smaller than in the bulk (reverse for Cl<sup>-</sup>) At potentials negative of E<sub>Z</sub> → opposite

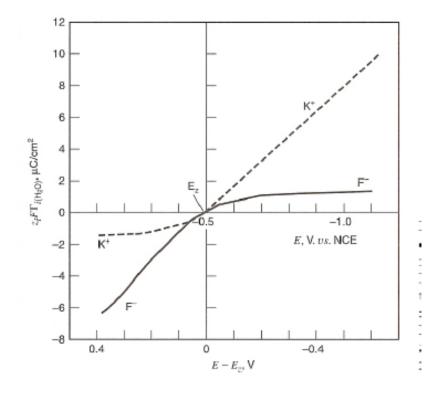
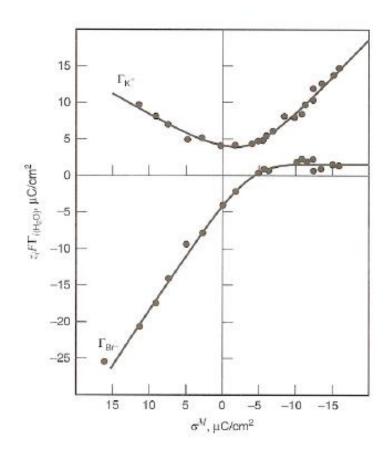


Fig. 13.2.6: 0.1 M KBr At potentials positive of  $E_Z$  (i.e., for  $\sigma^M > 0$ )  $\rightarrow$  surface excess of K<sup>+</sup>: positive  $\rightarrow$  specific adsorption of Br<sup>-</sup> on mercury



#### Models for double layer structure

#### The Helmholtz model

Two sheets of charge, having opposite polarity, separated by a distance of molecular order → equivalent to a parallel-plate capacitor

Relation of stored charge density,  $\sigma$ , and voltage drop V between the plate

$$\sigma = (\varepsilon \varepsilon_0/d)V$$

 $\varepsilon$ : dielectric const of the medium,  $\varepsilon_0$ : permittivity of free space, d: spacing

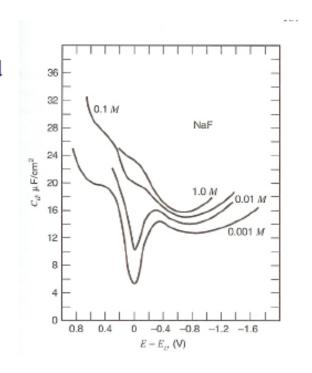
Differential capacitance

$$\partial \sigma / \partial V = C_d = \epsilon \epsilon_0 / d$$

Weakness of this model: predict C<sub>d</sub> is const e.g., Fig. 13.3.1 Differential capacitance vs. E

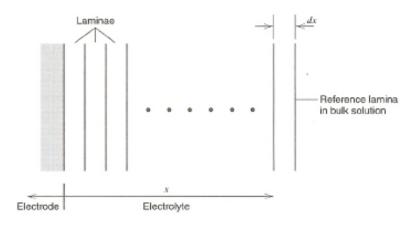
in Hg/NaF interface

- → potential dependence
- → more sophisticated model needed



#### The Gouy-Chapman theory

Charge on the electrode is confined to the surface Charge in the solution: diffusion layer



Population in any lamina (number concentration of species)

$$n_i = n_i^0 \exp(-z_i e \phi/kT)$$

 $n_i^0$ : bulk concentration,  $\phi$ : electrostatic potential ( $\phi$  measured with respect to the bulk)

Total charge per unit volume in any lamina

$$\rho(x) = \sum n_i z_i e = \sum n_i^0 z_i e \exp(-z_i e \phi/kT)$$

 $\rho(x)$  is related to the potential at distance x by the Poisson equation

$$\rho(\mathbf{x}) = -\varepsilon \varepsilon_0 (d^2 \phi / d\mathbf{x}^2)$$

Poisson-Boltzmann equation

$$d^{2}\phi/dx^{2} = -(e/\epsilon \epsilon_{0}) \sum n_{i}^{0} z_{i} \exp(-z_{i} e \phi/kT)$$
$$d^{2}\phi/dx^{2} = (1/2)(d/d\phi)(d\phi/dx)^{2}$$

$$(d\phi/dx)^2 = (2kT/\epsilon\epsilon_0)\sum_{i=0}^{\infty} [\exp(-z_i e\phi/kT) - 1]$$

For z:z electrolyte  $d\phi/dx = -(8kTn^0/\epsilon\epsilon_0)^{1/2}\sinh(ze\phi/2kT)$ 

(a) Potential profile in the diffusion layer

 $\phi_0$ : potential at x = 0 relative to the bulk solution = potential drop across the diffusion layer

$$\tanh(ze\phi/4kT)/\tanh(ze\phi_0/4kT) = e^{-\kappa x}$$
  
 $\kappa = (2n^0z^2e^2/\epsilon\epsilon_0kT)^{1/2}$ 

Where

For dilute aqueous solution ( $\varepsilon = 78.49$ ) at 25°C  $\kappa = (3.29 \times 10^7) \text{zC}^{*1/2}$ 

C\*: bulk z:z electrolyte conc in mol/L, K: cm-1

Potential profile for several different  $\phi_0$ : potential decay away from the surface

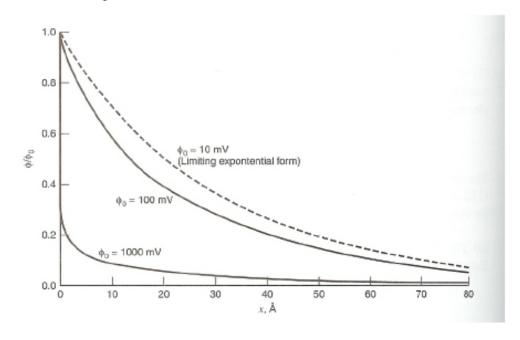
At large φ<sub>0</sub> (a highly charged electrode), the drop is precipitous because the diffusion layer is relatively compact

As φ<sub>0</sub> smaller, the decline is more gradual

If φ<sub>0</sub> is sufficiently low (tanh(zeφ/kT) ~ zeφ/kT)

φ/φ<sub>0</sub> = e -kx

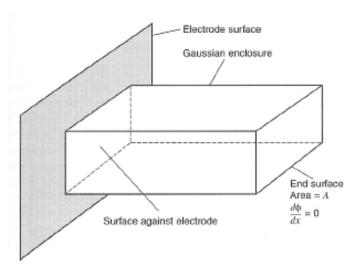
Good approximation for  $\phi_0 \le 50/z$  mV at 25°C



Reciprocal of K: unit of distance and characterizes the spatial decay of potential

- → kind of characteristic thickness of the diffusion layer
- → thicker as conc of electrolyte falls

# (b) Relation between $\sigma^M$ and $\phi$ Suppose Gaussian surface



	•
C*(M) <sup>b</sup>	1/κ(Å)
1	3.0
$10^{-1}$	9.6
$10^{-2}$	30.4
$10^{-3}$	96.2
$10^{-4}$	304

Gauss law, charge

$$q = \varepsilon \varepsilon_0 \int_{\text{surface}} \mathbf{E} \cdot d\mathbf{S}$$

$$= \varepsilon \varepsilon_0 \mathbf{A} (d\phi/d\mathbf{x})_{\mathbf{x}=0}$$
Using  $\mathbf{q}/\mathbf{A} = \sigma^S$  and  $d\phi/d\mathbf{x} = -(8k\mathrm{T} \mathbf{n}^0/\varepsilon \varepsilon_0)^{1/2} \mathrm{sinh}(ze\phi/2k\mathrm{T})$ 

$$\sigma^{S} = -\sigma^{M} = (8kTn^{0}\epsilon\epsilon_{0})^{1/2}\sinh(ze\phi_{0}/2kT)$$

For dilute solution at 25°C

$$\sigma^{M} = 11.7 C^{*1/2} \sinh(19.5 z \phi_{0})$$

Where  $C^*$  is in mol/L for  $\sigma^M$  in  $\mu C/cm^2$ 

(c) Differential capacitance

$$C_d = d\sigma^M/d\phi_0 = (2z^2e^2\epsilon\epsilon_0 n^0/kT)^{1/2}\cosh(ze\phi_0/2kT)$$

For dilute aqueous solutions at 25°C

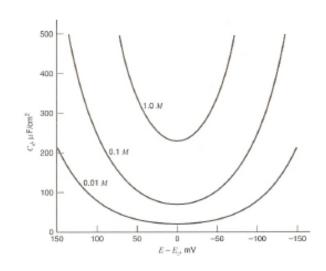
$$C_d = 228zC^{*1/2}\cosh(19.5z\phi_0)$$

where  $C_d$  is in  $\mu F/cm^2$ 

Predicted plot (V-shape) vs. observed one

- i) low conc & near PZC에서만 유사
- ii) 실험치가 예측치보다 훨씬 작음
- → need better theory!

Smaller in experiment than in prediction



#### Stern's modification

Gouy-Chapman model: unlimited rise in differential capacitance with  $\phi_0$ 

- → ions are not restricted with respect to location in solution phase (point charge can approach the surface arbitrarily closely)
- → not realistic: ions have a finite size & cannot approach the surface any closer than the ionic radius. If solvated, larger radius. Solvent layer should be considered

#### X<sub>2</sub>: outer Helmholtz plane (OHP)

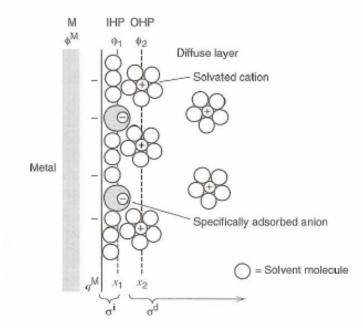


Figure 1.2.3 Proposed model of the double-layer region under conditions where anions are specifically adsorbed.

Poisson-Boltzmann equation for  $x \ge x_2$ 

$$\tanh(ze\phi/4kT)/\tanh(ze\phi/4kT) = e^{-\kappa(x-x^2)}$$

Where  $\phi_2$  is the potential at  $x_2$ 

Field strength at 
$$x_2$$
,  $(d\phi/dx)_{x=x_2} = -(8kTn^0/\epsilon\epsilon_0)^{1/2}\sinh(ze\phi_2/2kT)$ 

Total potential drop across the double layer

$$\begin{split} \varphi_0 &= \varphi_2 - (d\varphi/dx)_{x=x2} x_2 \\ \sigma^M &= -\sigma^S = -\epsilon \epsilon_0 (d\varphi/dx)_{x=x2} = (8kTn^0 \epsilon \epsilon_0)^{1/2} sinh(ze\varphi_2/2kT) \\ \sigma^M &= (8kTn^0 \epsilon \epsilon_0)^{1/2} sinh[ze/2kT(\varphi_0 - \sigma^M x_2/\epsilon \epsilon_0)] \end{split}$$

Differential capacitance

$$\begin{split} C_{d} &= d\sigma^{M}/d\varphi_{0} = (2z^{2}e^{2}\epsilon\epsilon_{0}n^{0}/kT)^{1/2}cosh(ze\varphi_{2}/2kT)/[1 + \\ & (x_{2}/\epsilon\epsilon_{0})(2\epsilon\epsilon_{0}z^{2}e^{2}n^{0}/kT)^{1/2}cosh(ze\varphi_{2}/2kT)] \end{split}$$

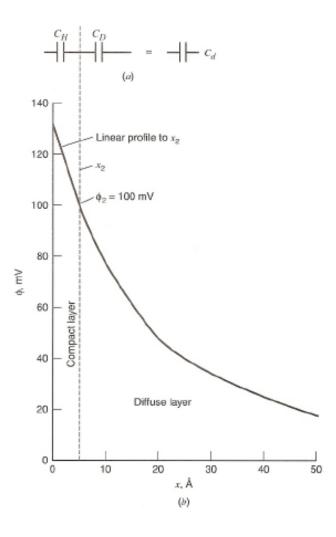
$$1/C_d = x_2/\varepsilon \varepsilon_0 + 1/[(2\varepsilon \varepsilon_0 z^2 e^2 n^0/kT)^{1/2} \cosh(ze\phi_2/2kT)]$$

Two components

$$1/C_d = 1/C_H + 1/C_D$$

C<sub>D</sub>: capacitance of the charge at OHP, C<sub>D</sub>: truly diffuse charge

# Gouy-Chapman-Stern model

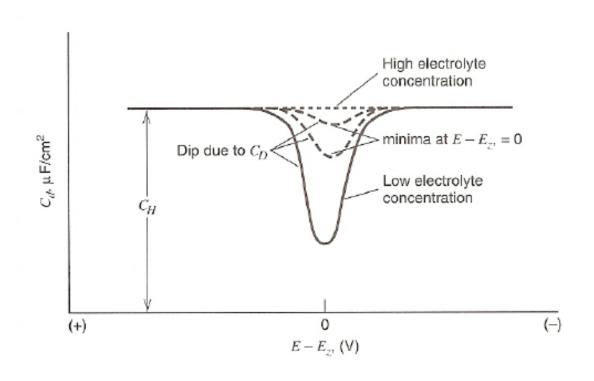


C<sub>H</sub>: independent of potential

C<sub>D</sub>: varies in V-shaped depending potential

 $C_d$ : V-shaped near PZC with low electrolyte conc (characteristic of  $C_D$ )

At large electrolyte conc or large polarization  $\rightarrow C_D$  is so large  $\rightarrow C_H$   $\rightarrow$  Gouy-Chapman-Stern (GCS) model

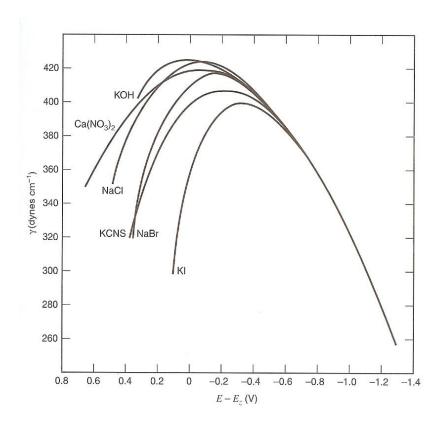


## **Specific adsorption**

Fig.13.2.2

Potential more negative than PZC: decline & same regardless composition (GCS model)

Potential more positive than PZC: depend specifically on the composition  $\rightarrow$  *specific adsorption* of anions: their center: *inner Helmholtz plane* (IHP),  $x_1$ 



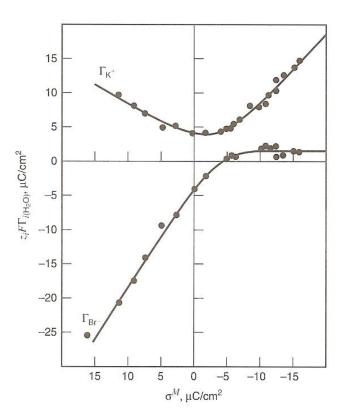


Fig.13.2.6 Br

(i) Specifically adsorbed ion  $\rightarrow$  considering the slopes of  $z_i F \Gamma_{i(H2O)}$  vs.  $\sigma^M = -[F \Gamma_{K+(H2O)} - F \Gamma_{Br-(H2O)}]$ 

In the absence of specific adsorption: charge on the electrode is counterbalanced by the excess of one ion and a deficiency of the other (Fig.13.2.5)

→ Fig. 13.2.6: more positive than PZC → superequivalent adsorption of bromide (considering slopes & compare with Fig. 13.2.5)

## (ii) Esin-Markov effect: shift in PZC with change in electrolyte conc

Table by "Grahame"
$\rightarrow$ shift: linear with $ln[activity]$
$\rightarrow$ slope: Esin-Markov coefficient at $\sigma^M=0$ (non-specific adsorption: EM coeff = 0
$(1/RT)(\partial E_{+}/\partial \ln a_{\rm salt})_{\sigma M} = (\partial E_{+}/\partial \mu_{\rm salt})_{\sigma M}$

Electrolyte	Concentration, <i>M</i>	$E_z$ , V vs. NCE <sup>b</sup>			
NaF	1.0	-0.472			
	0.1	-0.472			
	0.01	-0.480			
	0.001	-0.482			
NaCl	1.0	-0.556			
	0.3	-0.524			
	0.1	-0.505			
KBr	1.0	-0.65			
	0.1	-0.58			
	0.01	-0.54			
KI	1.0	-0.82			
	0.1	-0.72			
	0.01	-0.66			
	0.001	-0.59			

#### Studies at solid electrodes

## **Double layer at solids**

## **Most measurements on mercury**

→ solid electrode: difficulty to reproduce same & clean surface, not atomically smooth...

## Well-defined single crystal electrode surfaces

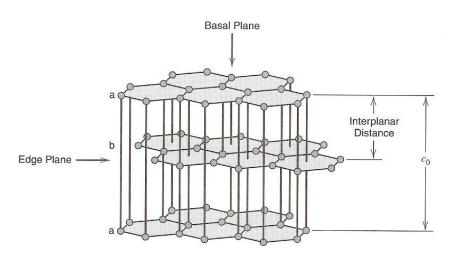
Different crystal faces exhibit different properties (e.g., PZC, work function..)

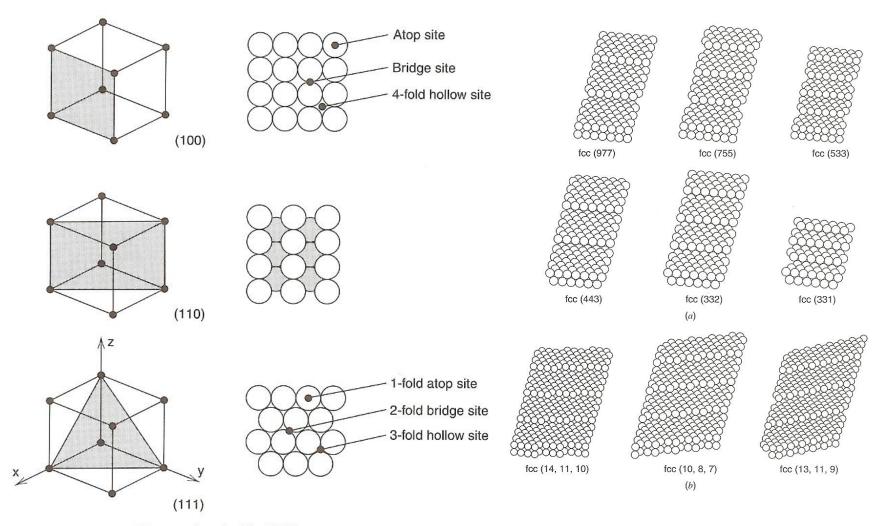
Pt, Pd, Ag, Ni, Cu: FCC crystal structures

- → low-index crystal faces: stable, polishable
- → higher-index planes: more edges, step & kink sites

Reconstruction: minimize surface energy

Carbon: highly oriented pyrolytic graphite (HOPG)





Face-centered cubic (FCC) structure

# Potential of zero charge

**Table 1.** Potentials of zero charge of sp metals,  $E_{\sigma=0}$  (V) vs. the standard hydrogen electrode (SHE).<sup>a</sup>

Hg	Sb	Bi	Bi(111)	Sn	Pb	In	In(Ga)	Tl	Tl(Ga)	Ga	Cd	Zn
-0.19	-0.17	-0.38	-0.41	-0.39	-0.60	-0.65	-0.67	-0.71	-0.69	-0.69	-0.75	-0.91

<sup>&</sup>lt;sup>a</sup>The uncertainty varies mostly between 0.01 and 0.02 V, but it is higher for d metals and lower (0.001 V) for Hg. (Reproduced from Trasatti and Lust (1999)<sup>[16]</sup> by permission of Plenum.)

Table 2. Potentials of zero charge of sd metals,  $E_{\sigma=0}$  (V) vs. SHE.<sup>a</sup>

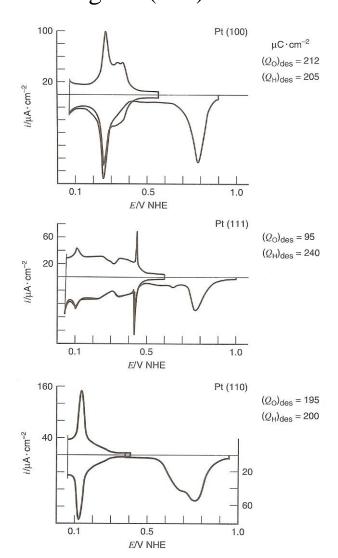
Ag	Ag(111)	Ag(100)	Ag(110)	Au	Au(111)	Au(100)	Au(110)	Cu	Cu(110)
-0.70	-0.45	-0.62	-0.74	0.20	0.56	0.32	0.20	-0.64	-0.69

<sup>&</sup>lt;sup>a</sup>As per Table 1.

cf. Pt: 0.18 V, Ni: -0.33 V

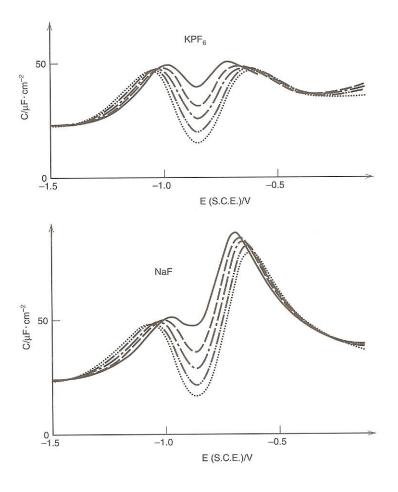
Different crystal faces exhibit different properties (e.g., PZC, work function..) e.g., PZC on Ag(111) (-0.69 V vs. SCE), Ag(110) (-0.98 V),  $\rightarrow$  -0.8 V: carry negative charge in (111), positive charge in (110)

Different catalytic & adsorption properties e.g., different CV in Pt (0.5 M H<sub>2</sub>SO<sub>4</sub>)

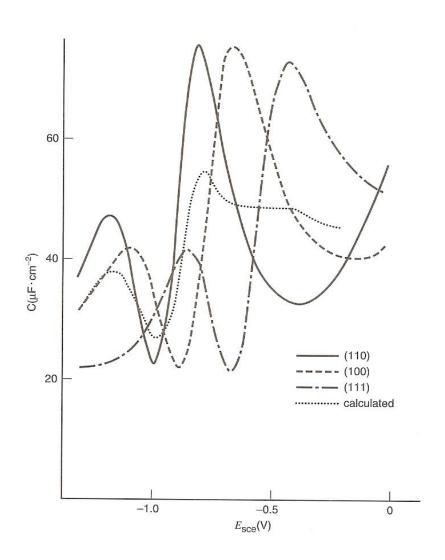


#### **Solid metal-solution interface**

Information on PZC & interface from capacitance measurements Capacitance curves for Ag(100) at different conc of KPF<sub>6</sub> and NaF (top to bottom 100, 40, 20, 10, and 5 mM) Independence of min in capacitance  $\rightarrow$  weakly specifically adsorbed on Ag PZC from capacitance minimum



PZC depends upon crystal faces (e.g., Ag) calculated: polycrystalline (46% (110), 23% (100), 31% (111))

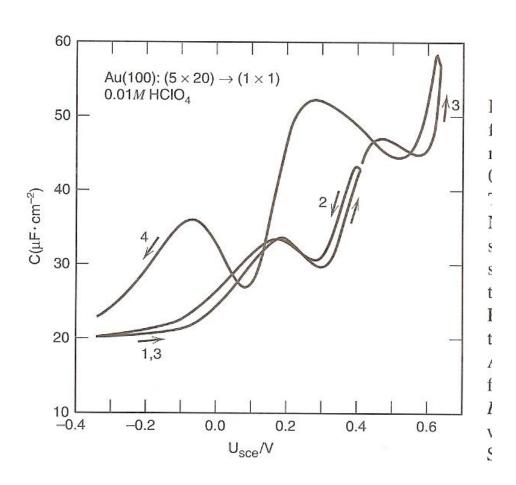


Another complication: surface reconstruction

Au(100): reconstructed (5 x 20) during flame heating

< +0.5 V: maintained (5 x 20)

~+0.7 V: converted to original (100)



## **Extent and rate of specific adsorption**

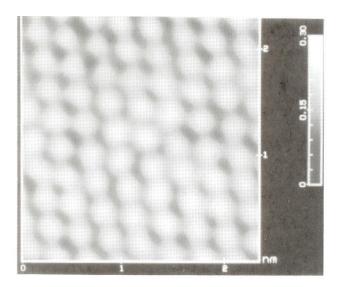
## Nature and extent of specific adsorption

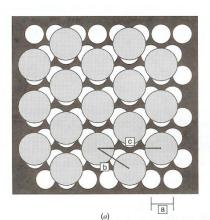
*Commensurate*: molecules adsorb in exact corresponding pattern with surface atoms e.g.,  $1.5 \times 10^{15}$  Au atoms/cm<sup>2</sup> on Au(111), spacing 2.9 Å

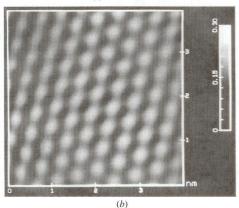
 $\rightarrow$  if adsorbate atoms on atop sites: (1 x 1) superlattice (2.5 x 10<sup>-9</sup> mol/cm<sup>2</sup>)

Iodine or 4-aminothiophenol:  $(\sqrt{30} \times \sqrt{30})R30^{\circ} \rightarrow 1/3$  Au  $(8.3 \times 10^{-10} \text{ mol/cm}^2)$ 

Lower coverage for larger molecules







Roughness factor: actual area/projected area ( $\sim 1.5 - 2$  for smooth electrode)

## **Adsorption isotherms**

Equal electrochemical potentials for bulk & adsorbed species i at equilibrium

$$\begin{array}{c} \mu_i{}^A = \mu_i{}^b \\ \mu_i{}^{0,A} + RT \, \mathit{ln} \, \, a_i{}^A = \mu_i{}^{0,b} + RT \, \mathit{ln} \, \, a_i{}^b \end{array}$$

Standard free energy of adsorption

$$\Delta G_i^0 = \mu_i^{0,A} - \mu_i^{0,b}$$

$$a_i^A = a_i^b e^{-\Delta GiO/RT} = \beta_i a_i^b$$

$$\beta_i = \exp(-\Delta G_i^0/RT)$$

Where

## Langmuir isotherm

## Assumption:

- (a) No interactions between the adsorbed species on the electrode surface
- (b) No heterogeneity of the surface
- (c) At high bulk activities, saturation coverage of the electrode by adsorbate (e.g., to form a monolayer) of amount of  $\Gamma_s$

$$\Gamma_i/(\Gamma_s - \Gamma_i) = \beta_i a_i^b$$

Fractional coverage,  $\theta = \Gamma_i / \Gamma_s$ 

$$\theta/(1-\theta) = \beta_i a_i^b$$

$$\Gamma_i = \Gamma_s \beta_i C_i / (1 + \beta_i C_i)$$

If two species i & j are adsorbed competitively,

$$\Gamma_{i} = \Gamma_{i,s} \beta_{i} C_{i} / (1 + \beta_{i} + \beta_{j})$$
  
$$\Gamma_{j} = \Gamma_{j,s} \beta_{j} C_{j} / (1 + \beta_{i} + \beta_{j})$$

#### Logarithmic Temkin isotherm

Interactions between adsorbed species

$$\Gamma_{i} = (RT/2g)\ln(\beta_{i}a_{i}^{b}) \quad (0.2 < \theta < 0.8)$$

## Frumkin isotherm

Electrochemical free energy of adsorption is linearly related to  $\Gamma_i$ 

$$\Delta G_i^0(Frumkin) = \Delta G_i^0 i (Langmuir) - 2g\Gamma_i$$

$$\beta_i a_i^b = [\Gamma_i / (\Gamma_s - \Gamma_i)] \exp(-2g\Gamma_i / RT)$$

g: J/mol per mol/cm $^2$   $\rightarrow$  increased coverage changes the adsorption E of i Positive g: interactions between adsorbed molecules are attractive Negative g: repulsive interactions

As  $g \rightarrow 0$ , Frumkin isotherm approaches the Langmuir isotherm

## Rate of adsorption

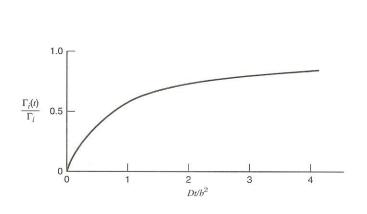
When 
$$\beta_i C_i << 1$$
,  $\Gamma_i = \Gamma_s \beta_i C_i = b_i C_i$   
Where  $b_i = \beta_i \Gamma_s$ 

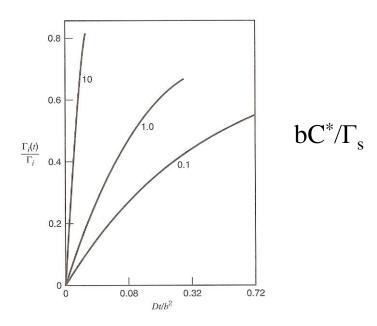
$$\Gamma_{i}(t) = b_{i}C_{i}(0,t)$$

$$\begin{split} C_i(x,\!0) &= {C_i}^*, \ lim \ C_i(x,\!t) = Ci^* \\ \Gamma_i(t) &= \int \ D_i [\partial C_i(x,\!t) / \partial x]_{x=0} \ dt \end{split}$$

$$\Gamma_{i}(t)/\Gamma_{i} = 1 - \exp(D_{i}t/b_{i}^{2}) \operatorname{erfc}[(D_{i}t)^{1/2}/b_{i}]$$

 $\Gamma_i(t)/\Gamma_i$  is independent of  $C_i^*$ , but actually depend on.





## **Effect of adsorption of electroinactive species**

→ such adsorption inhibit (or poison) an electrode reaction or accelerate the electrode reaction (e.g., hydrogen or oxygen)

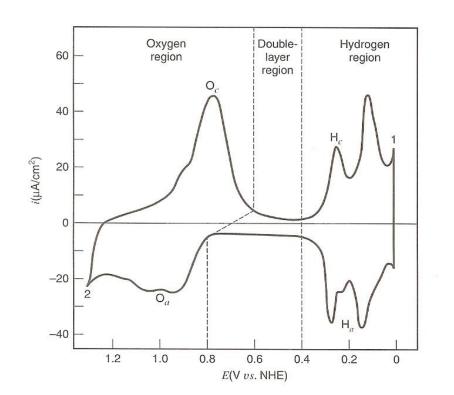
$$k^0 = k_{\theta=0}^{0}(1-\theta) + k_c^{0}\theta$$

Where  $k_{\theta=0}{}^0$  is the standard rate const at the bare surface &  $k_c{}^0$  that at the filmed portions

For completer blockage by the film,  $k_c^0 = 0$ 

For catalysis by the filmed area,  $k_c^0 > k_{\theta=0}^0$ 

Effect of adsorbed substances Hydrogen & oxygen CO & organics



## **Summary**

Electrochemical potential  $(\mu_i) = (\partial G/\partial n_i)$ : const at equilibrium

Surface tension  $(\gamma) = (\partial G/\partial A)$ : a measure of the energy required to produce a unit area of new surface

Surface excess concentration  $(\Gamma_i) = n_i/A$ : excess per unit area of surface

Gibbs adsorption isotherm:  $-d\gamma = \Sigma \gamma_i d\mu_i$  for general interface

Electrocapillary equation:  $-d\gamma = \sigma^M dE + \Sigma \Gamma_i d\mu_i$ 

for electrochemical interface

The excess charge density on the metallic side of interface:  $\sigma^{M} = -\sigma^{S}$ 

 $\rightarrow$  surface tension (γ) vs. charge density:  $\sigma^{\rm M} = -(\partial \gamma/\partial E)_{\mu}$ 

# Surface tension ( $\gamma$ ) vs. charge density: $\sigma^{\rm M} = (\partial \gamma / \partial E)_{\mu}$

