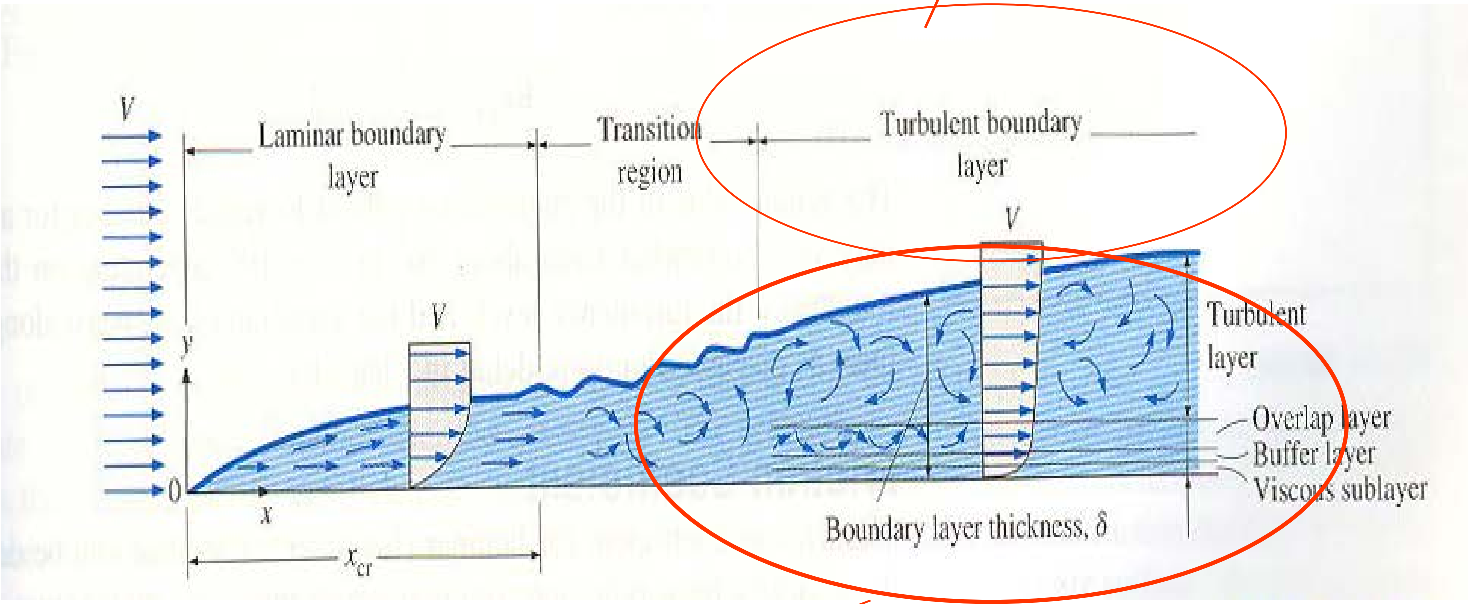
Chapter 7

Flow of a Real Fluid

Potential flow
Irrotational flow



Boundary layer flow
Rotational flow

Chapter 7 Flow of a Real Fluid

Contents

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Objectives

- Introduce the concepts of laminar and turbulent flow
- Examine the condition under which laminar and turbulent flow occur
- Introduce influence of solid boundaries on qualitative views

7.0 Introduction

- Ideal fluid (이상유체; 비점성 비압축성 유체)

\- In Chs.1 ~ 5, the flow of an ideal incompressible fluid was considered.

\- Ideal fluid was defined to be inviscid, devoid of viscosity.

\- There were no frictional effects between moving fluid layers or between the fluid and bounding walls.

- Real Fluid (실제유체; 점성유체)

\- Viscosity introduces resistance to motion by causing shear or friction forces between fluid particles and between these and boundary walls.

\- For flow to take place, work must be done against these resistance forces. In this process energy is converted into heat (mechanical energy loss).

7.0 Introduction

	Ideal (inviscid) fluid	Real (viscous) fluid
Viscosity	inviscid	viscous
Velocity profile	uniform (slip condition)	non-uniform (no-slip)
Eq. of motion	Euler's equation	Navier-Stokes equation (Nonlinear, 2nd-order P.D.E)
Flow Classification	-	Laminar flow Turbulent flow

7.1 Laminar flow

• Laminar flow (층류)

- Agitation of fluid particles is a molecular nature only.

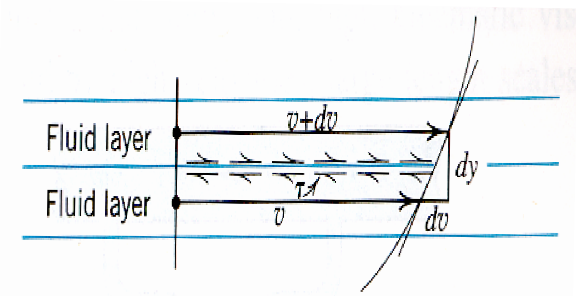
- Length scale ~ order of mean free path of the molecules

- Particles appear to be constrained to motion in parallel paths by the action of viscosity.

- Viscous action damps disturbances by wall roughness and other obstacles. → stable flow

- The shearing stress between adjacent layers is

$$\tau = \mu \frac{dv}{dy}$$



7.1 Laminar flow

• Turbulent flow (난류)

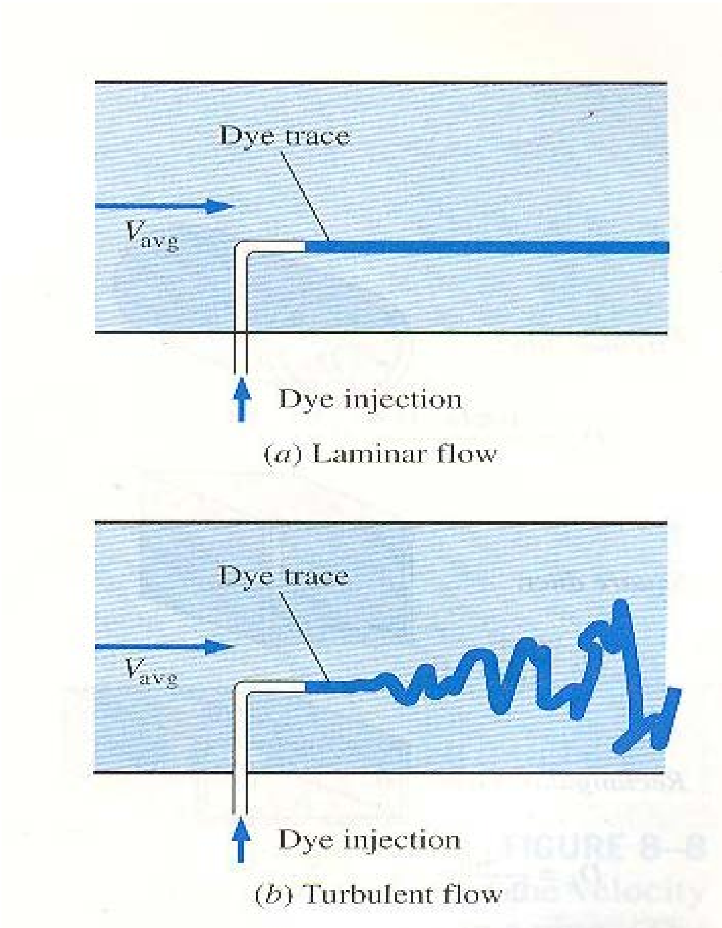
- Fluid particles do not retain in layers, but move in heterogeneous fashion through the flow.

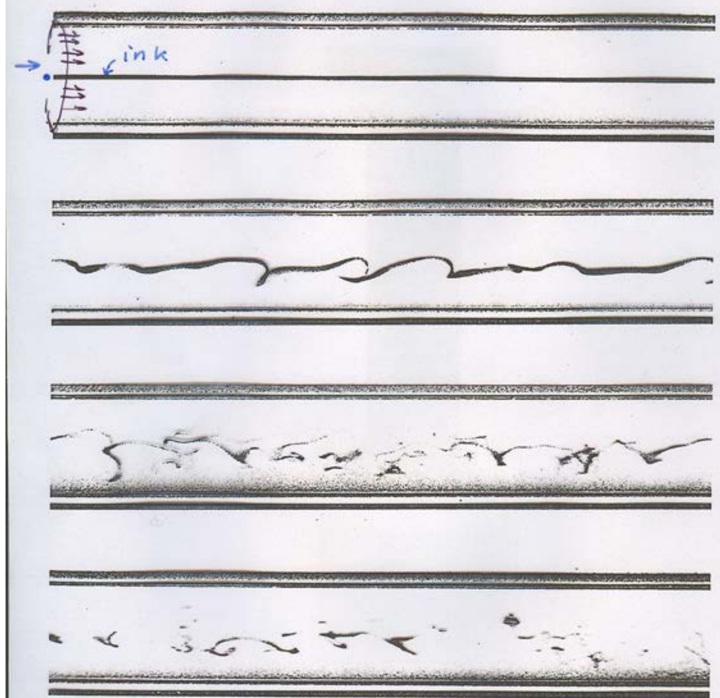
- Particles are sliding past other particles and colliding with some in an entirely random or chaotic manner.

- Rapid and continuous macroscopic mixing of the flowing fluid occurs.

- Length scale of motion >> molecular scales in laminar flow

7.1 Laminar flow





103. Repetition of Reynolds' dye experiment. Osborne Reynolds' celebrated 1883 investigation of stability of flow in a tube was documented by sketches rather than photography. However the original apparatus has survived at the University of Manchester. Using it a century later, N. H. Johannesen and C. Lowe have taken this sequence of photographs. In laminar flow a filament of colored water introduced at a bell-shaped entry extends undisturbed the whole length of the glass tube. Transition is seen in the second of the photographs as the speed is increased; and the last two photographs show fully turbulent flow. Modern traffic in the streets of Manchester made the critical Reynolds number lower than the value 13,000 found by Reynolds.

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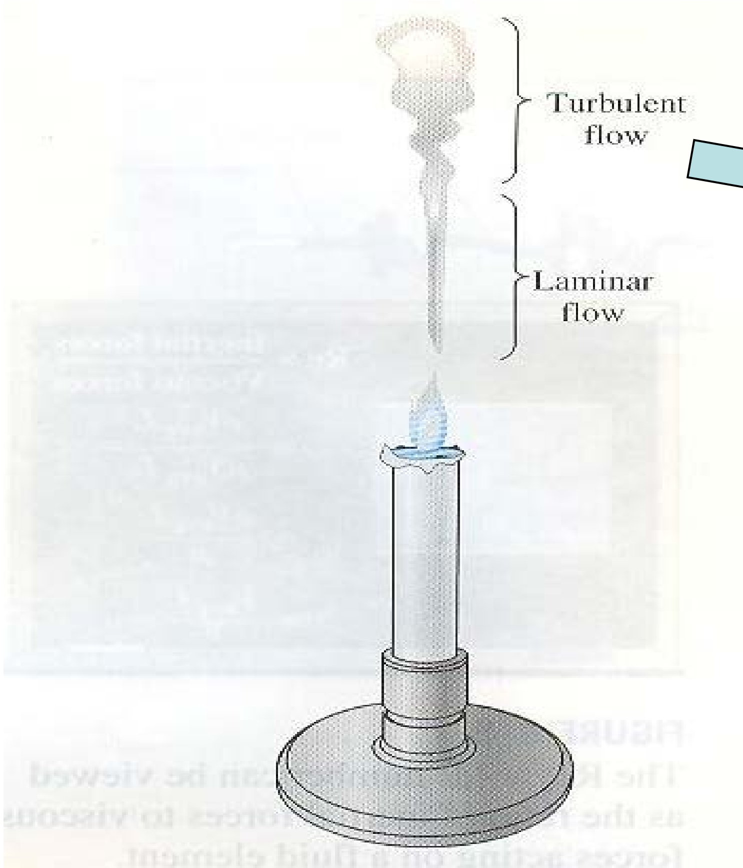
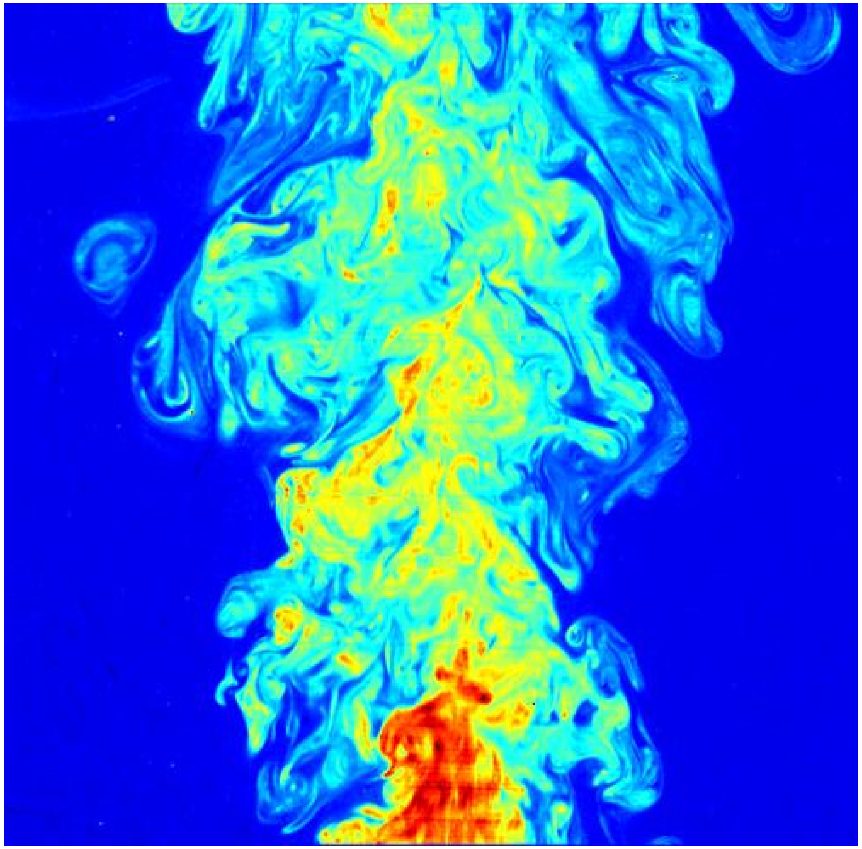
7.1 Laminar flow





7.1 Laminar flow

- Two forces affecting motion

  관성력 vs 점성력

(i) Inertia forces, F_I

~ acceleration of motion

$$F_I = ma = \rho l^3 \left(\frac{V^2}{l} \right) = \rho V^2 l^2$$

(ii) Viscous forces, F_V

~ damping of motion

$$F_V = \tau \ A = \mu \frac{dV}{dy} l^2 = \frac{\mu V l^2}{l} = \mu V l$$

7.1 Laminar flow

- Reynolds number R_e

$$R_e = \frac{F_I}{F_V} = \frac{\rho V^2 l^2}{\mu V l} = \frac{\rho V l}{\mu} = \frac{Vl}{\mu/\rho} = \frac{Vl}{\nu}$$

$$\mu = \text{dynamic viscosity} \qquad (\text{kg m}^{-1}\text{s}^{-1})$$

$$\nu = \frac{\mu}{\rho} = \text{kinematic viscosity} \qquad (\text{m}^2/\text{s})$$

- Inertia forces are dominant → turbulent flow (unstable)

Viscous forces are dominant → laminar flow (stable)

- Reynolds dye stream experiments

low velocity → low Reynolds number → laminar flow

high velocity → high Reynolds number → turbulent flow

7.1 Laminar flow

- Critical velocity (임계속도)

upper critical velocity: laminar → turbulent

lower critical velocity: turbulent → laminar

- Critical Reynolds number

(i) For pipe flow

$$R_e = \frac{Vd}{\nu}, \quad d = \text{pipe diameter} \tag{7.1}$$

$$\begin{cases} R_e < 2100 \rightarrow \text{laminar flow} \cdots \text{lower critical} \quad R_{c1} = 2100 \\ 2100 < R_e < 4000 \rightarrow \text{transition} \cdots \text{upper critical} \quad R_{c2} = 4000 \\ R_e > 4000 \rightarrow \text{turbulent flow} \end{cases}$$

7.1 Laminar flow

(ii) Open channel flow: $R_e < 500 \rightarrow \text{laminar flow}$

$$R_c = \frac{Vd}{\nu} = \frac{V(4R)}{\nu} = 2100 \qquad \therefore\ R_c = \frac{VR}{\nu} \cong 500$$

$$R = \text{hydraulic radius} = A = \frac{\pi d^2/4}{\pi d} = \frac{d}{4}$$

(iii) Flow about a sphere: $R_e < 1 \rightarrow \text{laminar flow}$

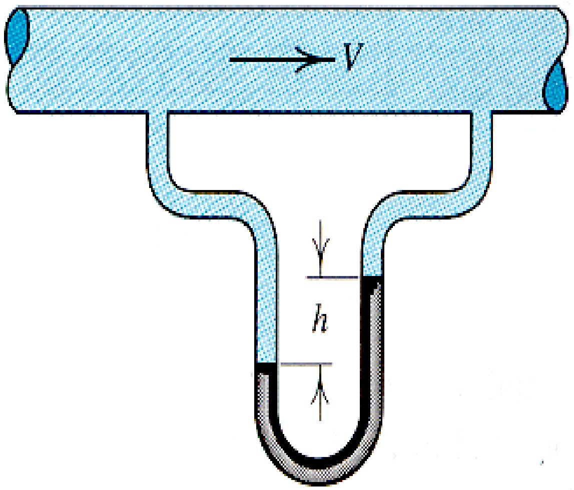
where V = approach velocity; d = sphere diameter

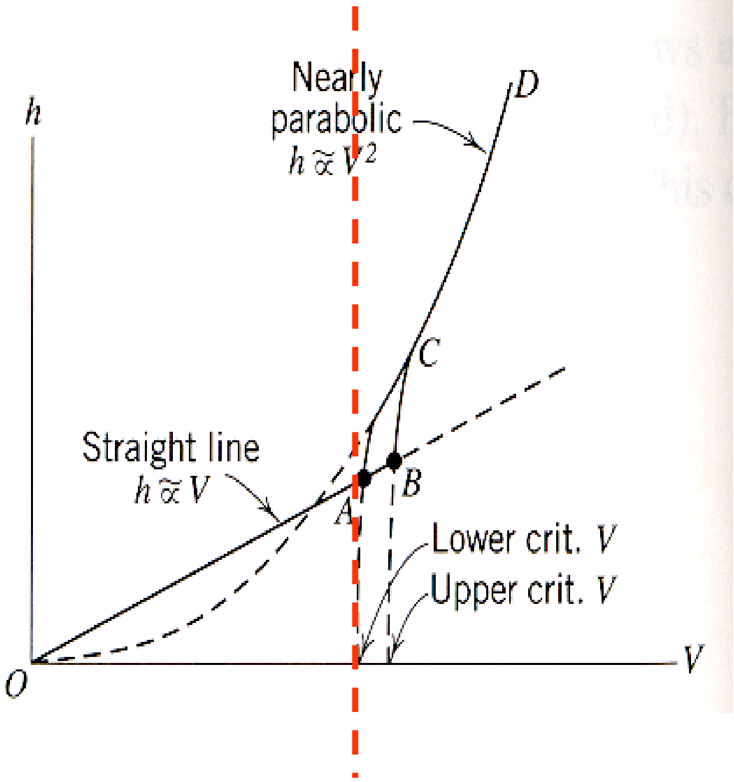
7.1 Laminar flow

- **Experiment for two flow regimes**

For laminar flow : $h_L \propto V^1$

For turbulent flow : $h_L \propto V^2$





7.1 Laminar flow

i) As V is increased → OABCD

OB (laminar flow) → BC (transition region) → CD (turbulent flow)

upper critical velocity

ii) As V is decreased → DCAO

DC (turbulent) → CA (transition) → AO (laminar flow)

lower critical velocity

7.1 Laminar flow

[IP 7.1] p. 233 Water at 15˚C flows in a cylindrical pipe of 30 mm diameter.

$$\nu = 1.339 \times 10^{-6}\ \mathrm{m^2/s} \quad \leftarrow \quad \text{water at } 15^{\circ}\mathrm{C}$$ p.694 A. 2.4b

Find largest flow rate for which laminar flow can be expected.

[Sol]

Take $R_c = 2100$ as the conservative upper limit for laminar flow

(a) For water

$$R_c = 2100 = \frac{Vd}{\nu} = \frac{V\left(30/10^3\right)}{1.139 \times 10^{-6}}$$

$$V_{water} = 0.080\ \mathrm{m/s}$$

$$Q_{water} = 0.0805\left(\frac{\pi}{4}(0.03)^2\right) = 5.69 \times 10^{-5}\ \mathrm{m^3/s}$$

7.1 Laminar flow

(b) For air

$$\nu_{air} = 1.46 \times 10^{-5} \ \text{m}^2/\text{s}$$

$$\left(\mu_{air} / \rho \ = \ 1.8 \times 10^{-5} \ \text{pa} \cdot \text{s} \, / \, 1.225 \ \text{kg}/\text{m}^3 \right)$$

$$V_{air} = 1.022 \ \text{m/s}$$

$$Q_{air} = 7.22 \times 10^{-4} \ \text{m}^3/\text{s} \approx 13 \, Q_{water}$$

$$\mu_{air} < \mu_{water}$$

$$V_{c,air} > V_{c,water}$$

7.2 Turbulent Flow and Eddy Viscosity

• Turbulent flow

- Turbulence is found in the atmosphere, in the ocean, in most pipe flows, in rivers and estuaries, and in the flow about moving vehicles and aircrafts.

- Turbulence is generated primarily by friction effects at solid boundaries (wall turbulence) or by the interaction of fluid streams that are moving past each other with different velocities (free turbulence) (shear flow).

7.2 Turbulent Flow and Eddy Viscosity

- Characteristics of turbulent flow (Tennekes & Lumley, 1972)

① Irregularity or randomness in time and space (불규칙성, 무작위성)

② Diffusivity or rapid mixing → high rates of momentum and heat transfer (확산)

③ High Reynolds number

④ 3D vorticity fluctuations → 3D nature of turbulence (3차원 와류)

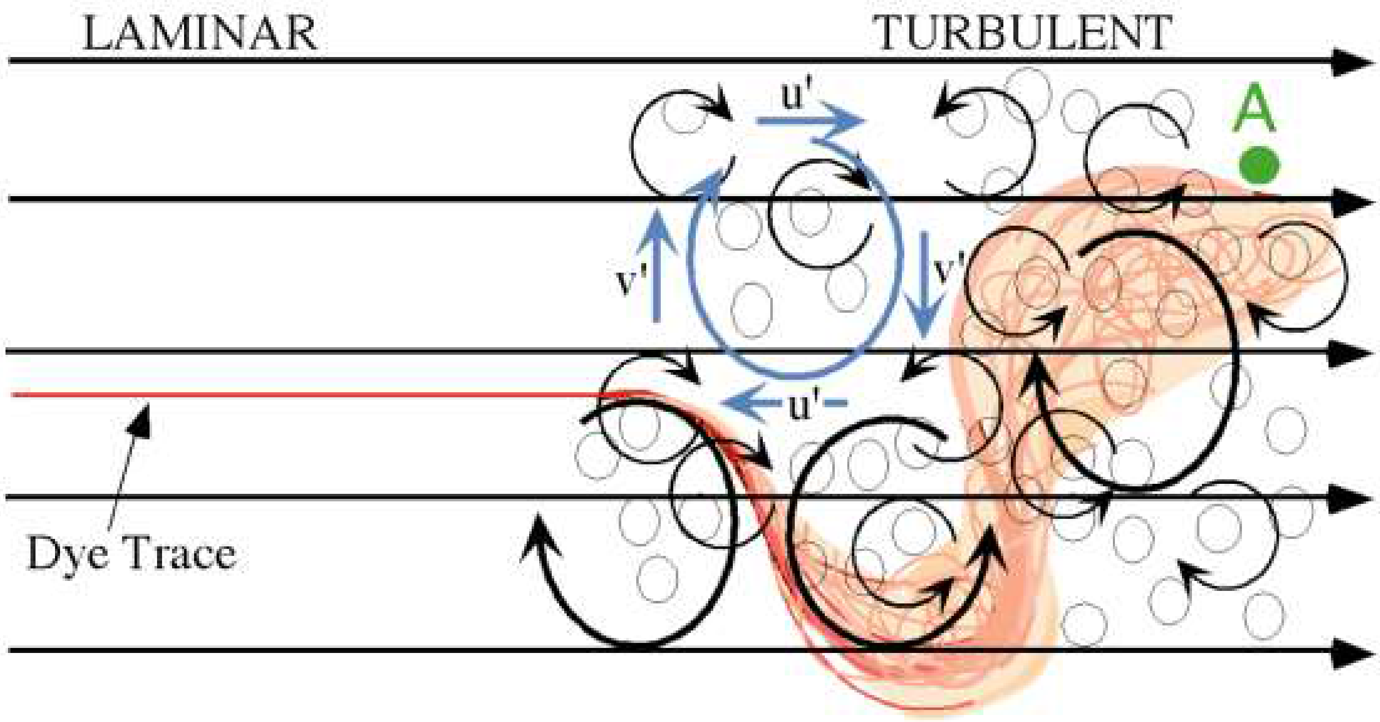
⑤ Dissipation of the kinetic energy of the turbulence by viscous shear stresses

[Energy cascade: energy supply from mean flow to turbulence] (에너지 소산)

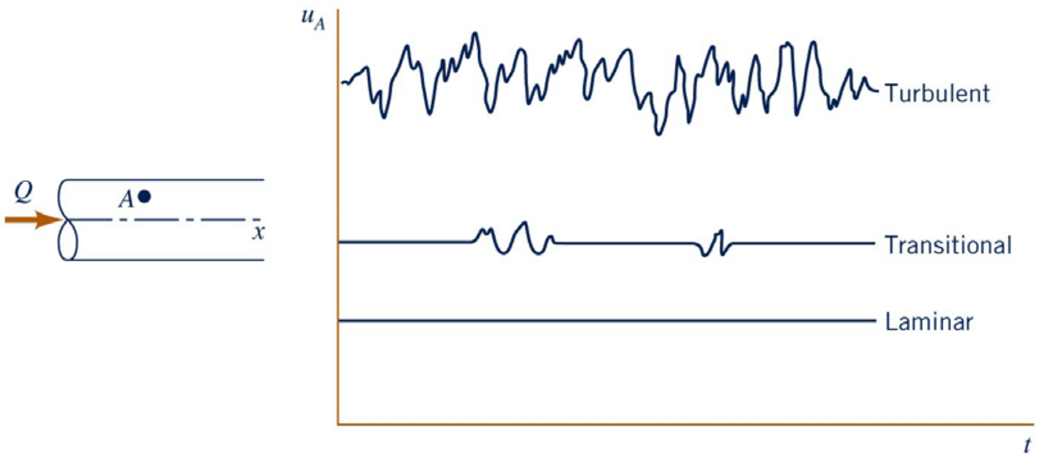
⑥ Continuum phenomenon even at the smallest scales

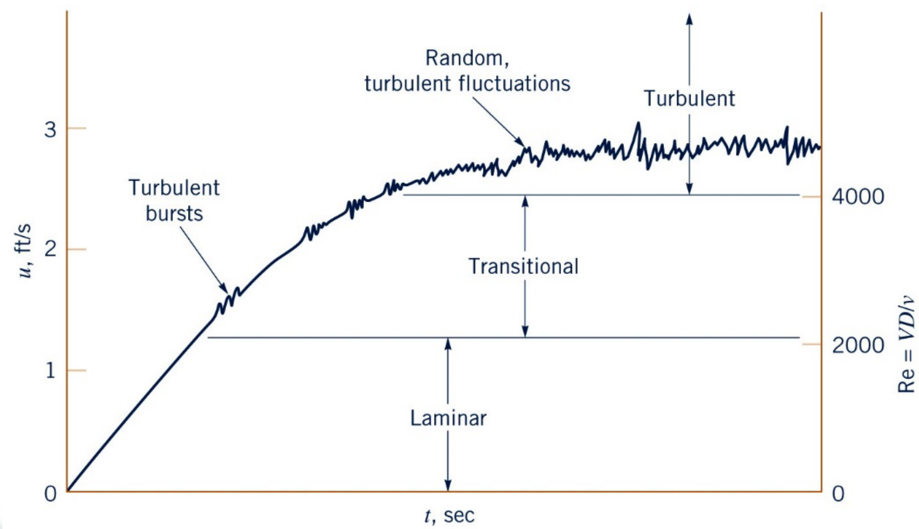
⑦ Feature of fluid flows, not a property of fluids themselves

7.2 Turbulent Flow and Eddy Viscosity

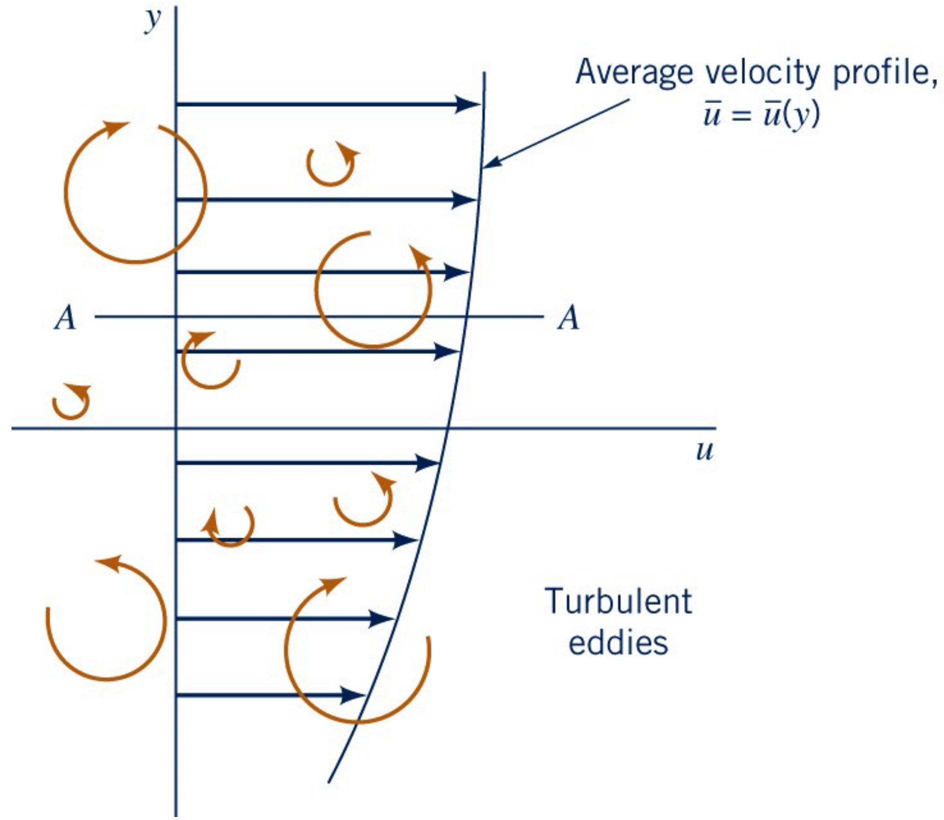


7.2 Turbulent Flow and Eddy Viscosity



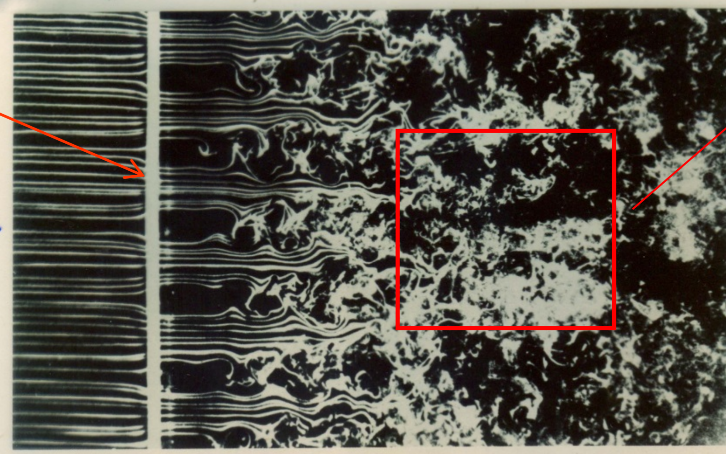


7.2 Turbulent Flow and Eddy Viscosity



7.2 Turbulent Flow and Eddy Viscosity

Coarse grid

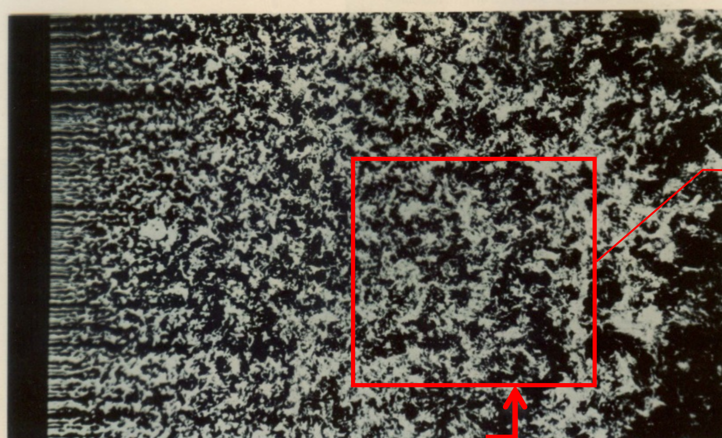


Non-isotropic turbulence

152. Generation of turbulence by a grid. Smoke wires show a uniform laminar stream passing through a $^1/_{16}$-inch plate with ¾-inch square perforations. The Reynolds number is 1500 based on the 1-inch mesh size. Instability of the shear layers leads to turbulent flow downstream. *Photograph by Thomas Corke and Hassan Nagib*

grid turbulence

Fine grid



Isotropic turbulence

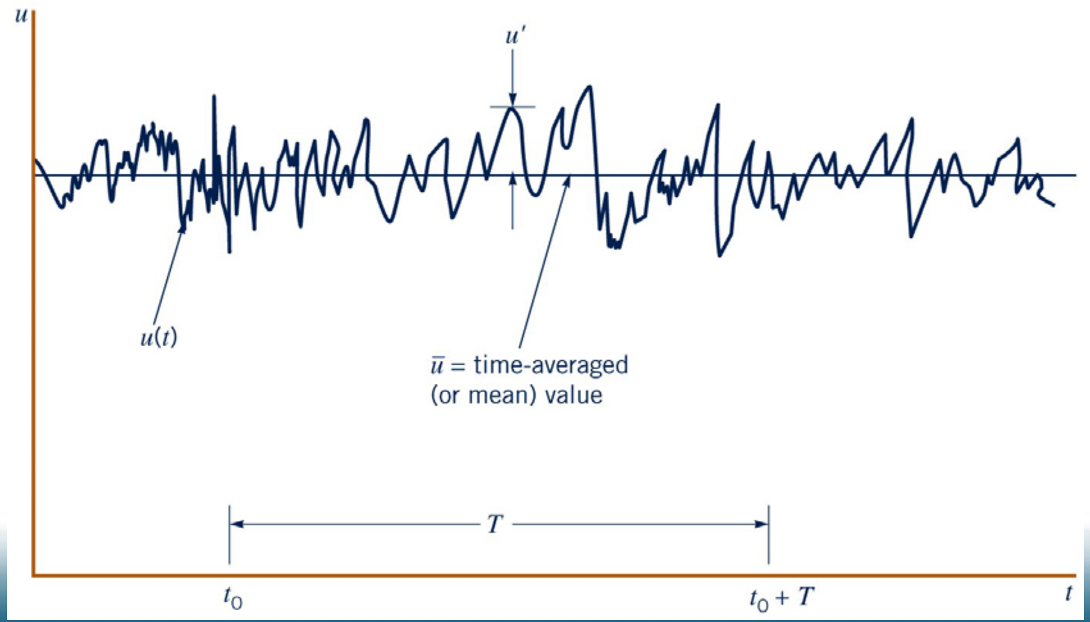
153. Homogeneous turbulence behind a grid. Behind a finer grid than above, the merging unstable wakes quickly form a homogeneous field. As it decays downstream, it provides a useful approximation to the idealization of isotropic turbulence. *Photograph by Thomas Corke and Hassan Nagib*

7.2 Turbulent Flow and Eddy Viscosity

• Turbulence

- Because turbulence is an entirely chaotic motion of small fluid masses, motion of individual fluid particle is impossible to trace.

→ Mathematical relationships may be obtained by considering the average motion of aggregations of fluid particles or by statistical methods.



7.2 Turbulent Flow and Eddy Viscosity

- Decomposition of turbulent flow

$$v_x(t) = \overline{v} + v_x'$$

$$v_y(t) = \overline{v} + v_y'$$

$v(t) =$ instantaneous turbulent velocity

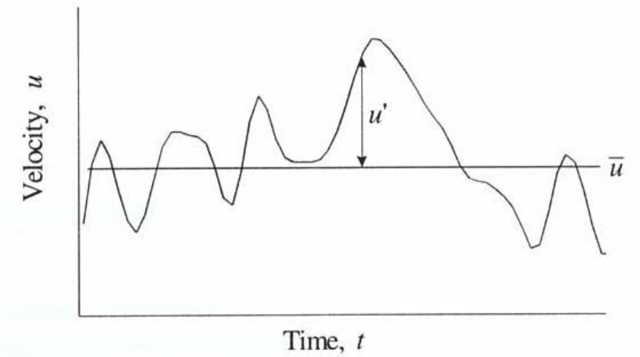
$\overline{v} =$ time mean velocity $= \frac{1}{T}\int_0^T v(t)\,dt$

$v_x' =$ turbulent fluctuation in *x*-direction

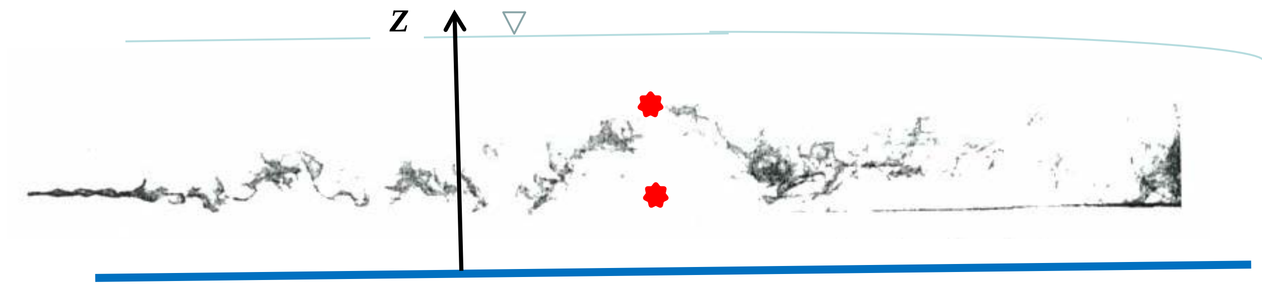
$v_y' =$ turbulent fluctuation in *y*-direction

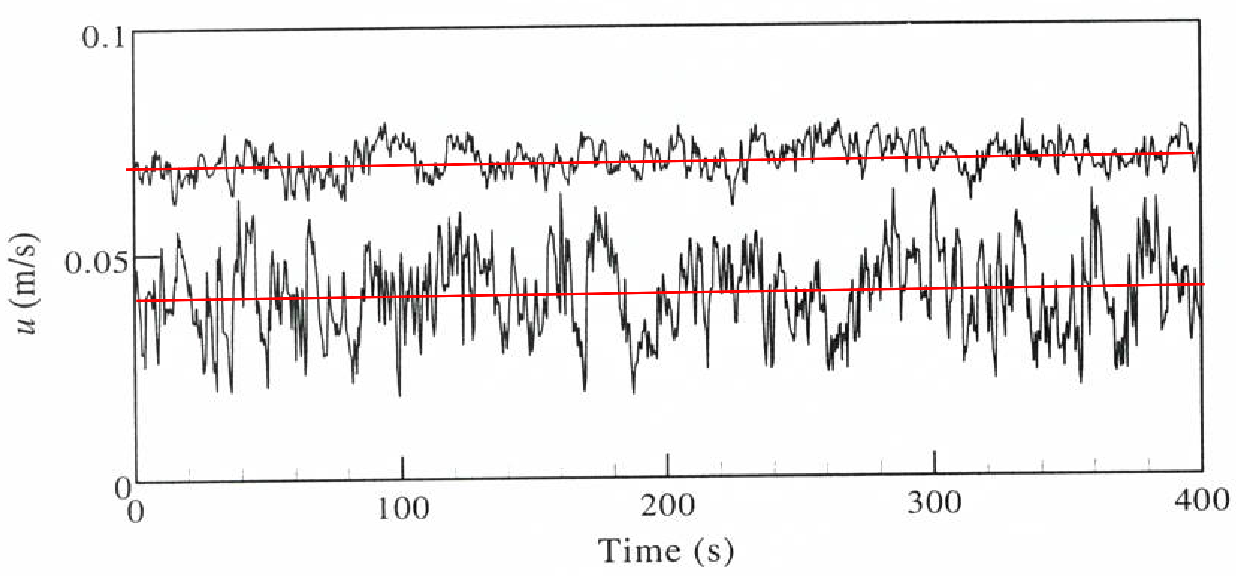
$$\overline{v_x'} = \frac{1}{T}\int_0^T v_x'\,dt = 0$$

$$\overline{v_y'} = 0$$



7.2 Turbulent Flow and Eddy Viscosity





7.2 Turbulent Flow and Eddy Viscosity

turbulent intensity: $$\text{rms} = \sqrt{\overline{(v_x')^2}} = \left[\frac{1}{T}\int_0^T v_x'^2 dt\right]^{1/2}$$ 난류강도

• relative intensity of turbulence $= \dfrac{\sqrt{\overline{v_x'^2}}}{\bar{v}}$

• Mean time interval, T

T = times scale = meaningful time for turbulence fluctuations

- air flow: $10^{-1} \sim 10^{0}$ sec

- pipe flow: $10^{-1} \sim 10^{0}$ sec

- open flow: $10^{0} \sim 10^{1}$ sec

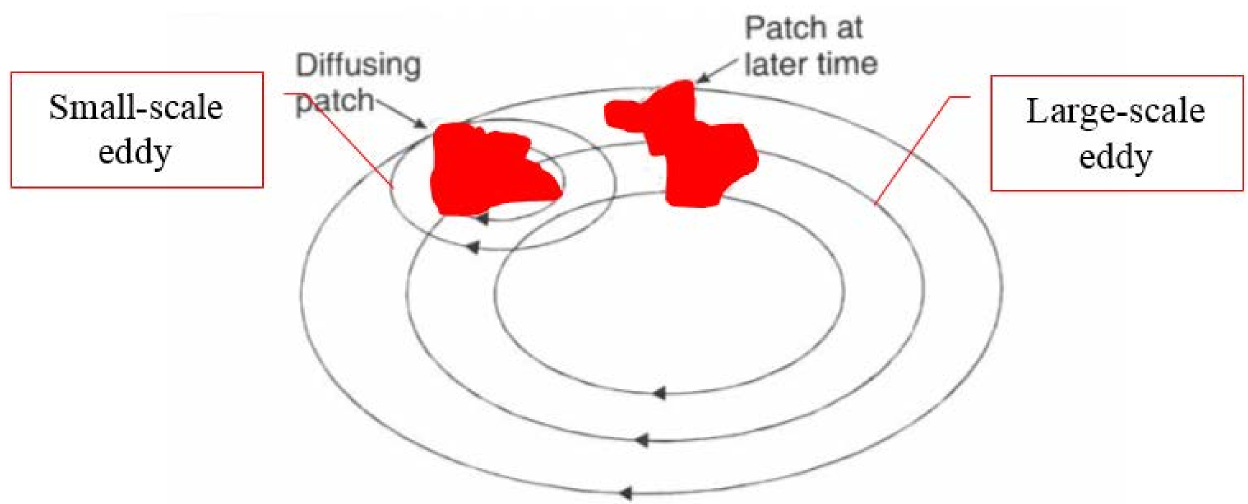
7.2 Turbulent Flow and Eddy Viscosity

T ~ measure of the scale of the turbulence

- maximum size of the turbulent eddies $\propto$ size of boundary

~ order of (pipe radius, channel width or depth, boundary layer thickness)

→ The intensity of turbulence increases with velocity, and scale of turbulence increases with boundary dimensions.



7.2 Turbulent Flow and Eddy Viscosity

[Re] Measurement of turbulence

(i) Hot-wire anemometer

~ use laws of convective heat transfer

~ Flow past the (hot) sensor cools it and decrease its resistance and output voltage.

~ record of random nature of turbulence

(ii) Laser Doppler Velocitymeter (LDV)

~ use Doppler effect

(iii) Acoustic Doppler Velocitymeter (ADV)

(iv) Particle Image Velocimetry (PIV)

7.2 Turbulent Flow and Eddy Viscosity

Figure 15.21 Two forms of hot-wire anemometer probes:
(a) wire mounted normal to probe axis,
(b) wire mounted parallel to probe axis

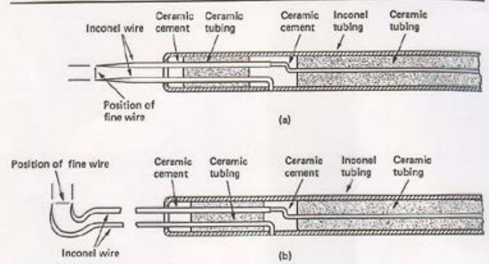
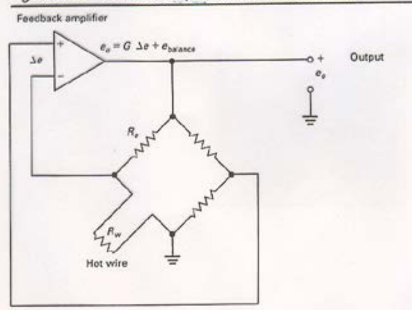
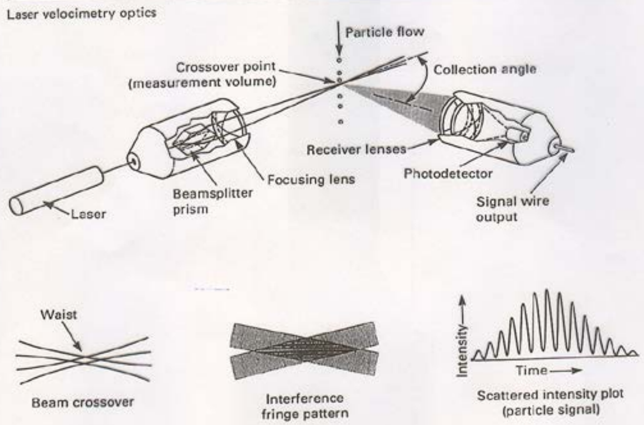


Figure 15.22 Constant-temperature-anemometer bridge circuit



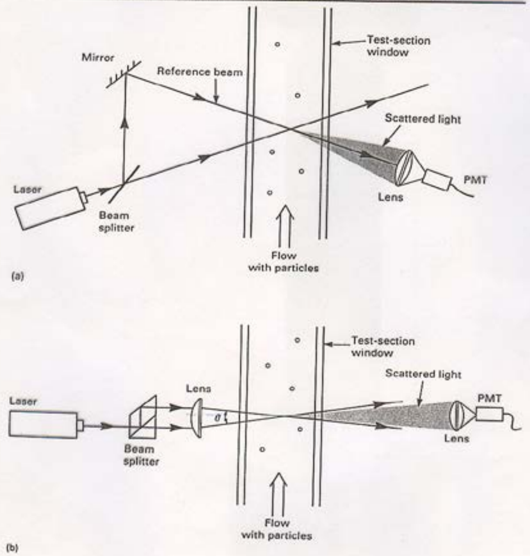
7.2 Turbulent Flow and Eddy Viscosity

Figure 15.25 LDA transmitter and receiver packages (Courtesy of David Carr, Aerometrics Inc., Sunnyvale, CA)



7.2 Turbulent Flow and Eddy Viscosity

Figure 15.24 Laser-Doppler optical systems: (a) reference-beam arrangement, (b) differential-Doppler arrangement



fringe spacing:

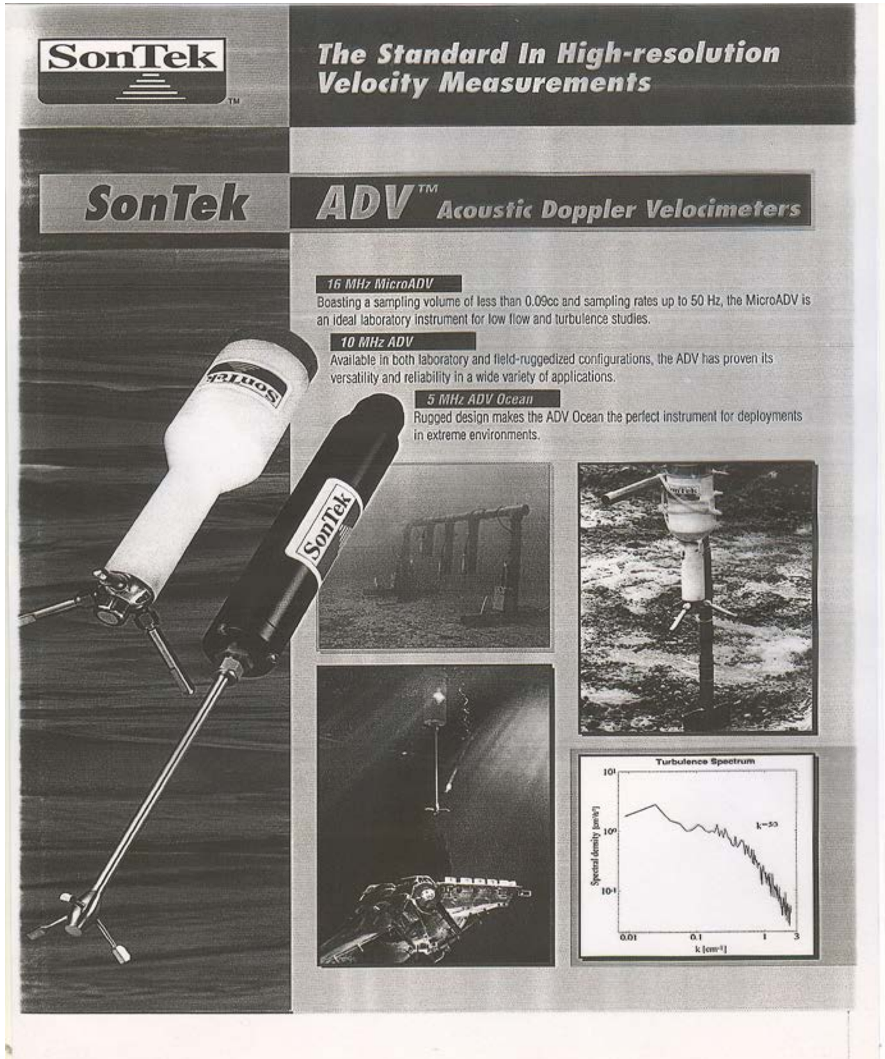
$$f_D = \frac{V_x}{\delta} = \left(\frac{2V_x}{\lambda}\right)\sin\left(\frac{\theta}{2}\right), \qquad (15.18)$$

where

f_D = the Doppler-shift frequency,

V_x = the particle velocity in the direction normal to the fringes.

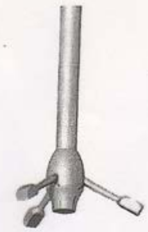
7.2 Turbulent Flow and Eddy Viscosity



7.2 Turbulent Flow and Eddy Viscosity

SonTek

MicroADV



High Resolution Acoustic Doppler Velocimeter

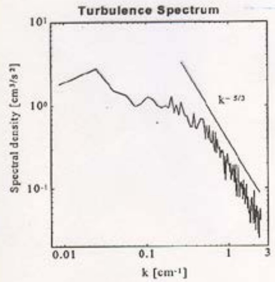
The SonTek MicroADV is the most significant breakthrough in current meter technology since the original SonTek ADV.

The original SonTek ADV has compared favorably with Laser systems costing ten times as much; the MicroADV fares even better.

The higher acoustical frequency of 16MHz makes the MicroADV the optimal instrument for laboratory work for several reasons:

- **Small sampling volume – less than 0.1 cm³**
- **High sampling rates – up to 50 Hz**
- **Small optimal scatterer – excellent for low flows**

Like all SonTek instruments, the MicroADV is extremely simple to set up and use. Most users are taking high quality data within minutes of receiving the system.

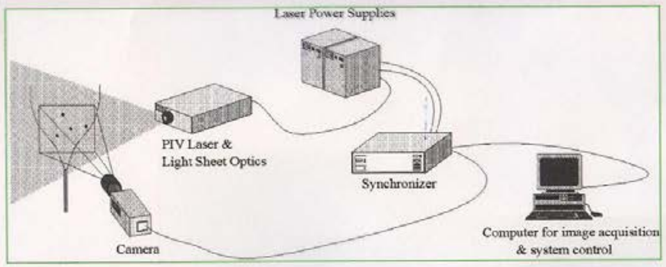


Additional Features:

- **Three axis velocity measurement**
- **High accuracy – 1% of measured**
- **Large velocity range – 1 mm/s - 2.5 m/s**
- **Excellent low flow performance**
- **No recalibration requirement**
- **Low price**
- **Comprehensive software**

The ADV, like all SonTek instruments, comes complete with our no-questions-asked warranty and our renowned customer service. The MicroADV is available from SonTek and authorized SonTek representatives worldwide.

7.2 Turbulent Flow and Eddy Viscosity




Laser Source

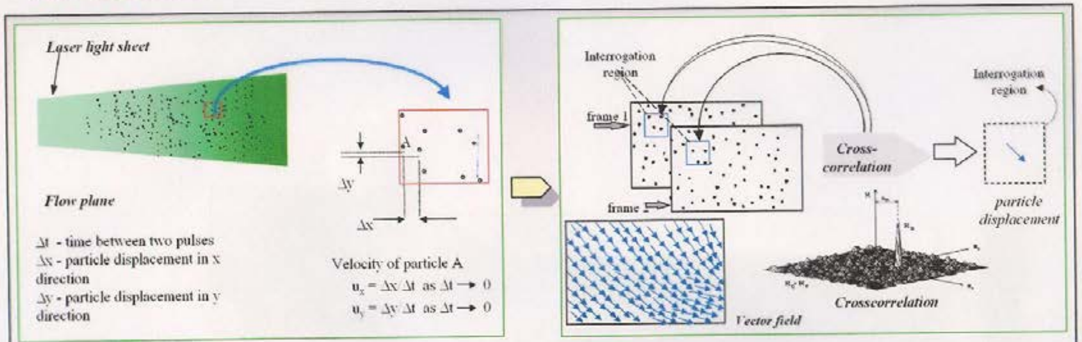

CCD Camera

Synchronizer

- ⇨ Two Continuum Minilite Nd-YAG Lasers
- ⇨ Kodak Megaplus ES 1.0 CCD Camera
- ⇨ Seeded With Hollow Glass Spheres
- ⇨ Time of Acquisition: (30Hz; for 22 seconds)
- ⇨ Using *INSIGHT* Software for PIV Processing

7.2 Turbulent Flow and Eddy Viscosity

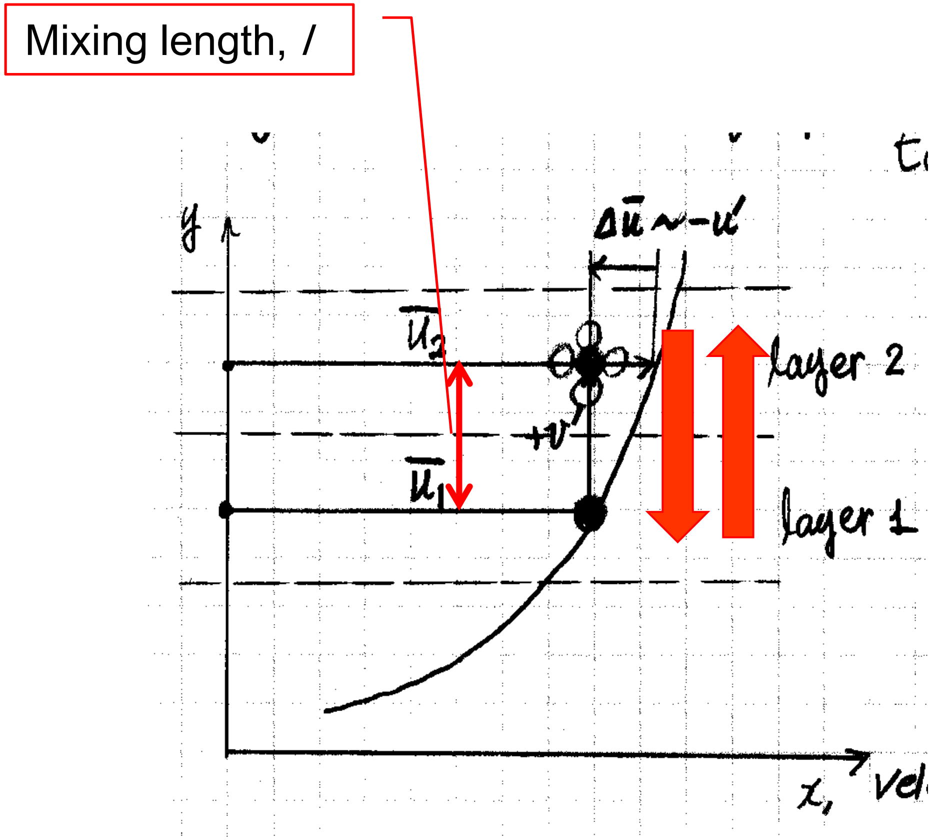
PIV System



- ⇨ Main principle of PIV: measurement of displacement Δx and Δy of images
- ⇨ Subsystem of PIV
  - imaging subsystem : laser, beam delivery system, light optics
  - image capture system : CCD camera, camera interface, synchronizer-master control
  - analysis and display subsystem
- ⇨ Synchronizer system: synchronize camera with laser pulses
- ⇨ Double-frame cross-correlation technique : no overlapping

7.2 Turbulent Flow and Eddy Viscosity

- Shearing stresses in turbulent flow



7.2 Turbulent Flow and Eddy Viscosity

Let time mean velocity $v = \overline{v}$

Thus, velocity gradient is $\dfrac{dv}{dy}$

Now consider momentum exchange by fluid particles moved by turbulent fluctuation (운동량 교환)

Mass moved to the lower layer tends to speed up the slower layer

Mass moved to the upper layer tends to slow down the faster layer

→ This is the same process as if there were a shearing stress between two layers.

7.2 Turbulent Flow and Eddy Viscosity

• Problem of useful and accurate expressions for turbulent shear stress in terms of mean velocity gradients and other flow properties

1) Boussinesq (1877)

~ suggest the similar equation to laminar flow equation

$$\tau = \varepsilon \frac{dv}{dy} \quad (7.2)$$

ε = eddy viscosity

= property of flow (not of the fluid alone)

$=f$ (structure of the turbulence, space)

$$\tau_{total} = (\mu + \varepsilon)\frac{dv}{dy}$$

where μ = viscosity action, ε = turbulence action

7.2 Turbulent Flow and Eddy Viscosity

2) Reynolds (1895)

~ suggest the turbulent shear stress with time mean value of the product of $v_x' v_y'$

$$\tau = -\rho \overline{v_x' v_y'}$$ ~ Reynolds stress

v_x' = fluctuating velocity along the direction of general mean motion

v_y' = fluctuating velocity normal to the direction of general mean motion

$\overline{v_x' v_y'}$ = time mean value of the product of $v_x' v_y'$

$$= \frac{1}{T} \int v_x' v_y' dt$$

7.2 Turbulent Flow and Eddy Viscosity

- Prandtl (1926)

~ propose that small aggregations of fluid particles are transported by turbulence a certain mean distance, *l*, from regions of one velocity to regions of another. (혼합거리)

~ termed the distance as the mixing length

→ **Prandtl's mixing length theory**

$$\tau = \rho l^2 \left(\frac{dv}{dy} \right)^2 \qquad (7.3)$$

where l = mixing length = $f(y)$

7.2 Turbulent Flow and Eddy Viscosity

Comparing Eqs. (7.2) and (7.3) gives

$$\varepsilon = \rho l^2 \frac{dv}{dy} \qquad (7.4)$$

• Flow near the boundary wall

~ turbulence is influenced by the wall = wall turbulence

$$l = \kappa y \qquad (7.5)$$

where $\kappa =$ von Karman constant ≈ 0.4; $y =$ distance from wall

$$\tau = \rho \kappa^2 y^2 \left(\frac{dv}{dy} \right)^2 \qquad (7.6)$$

7.2 Turbulent Flow and Eddy Viscosity

[IP 7.2] p. 238 Laminar flow

Show that if laminar flow is parabolic velocity profile, the shear stress profile must be a straight line.

[Sol]

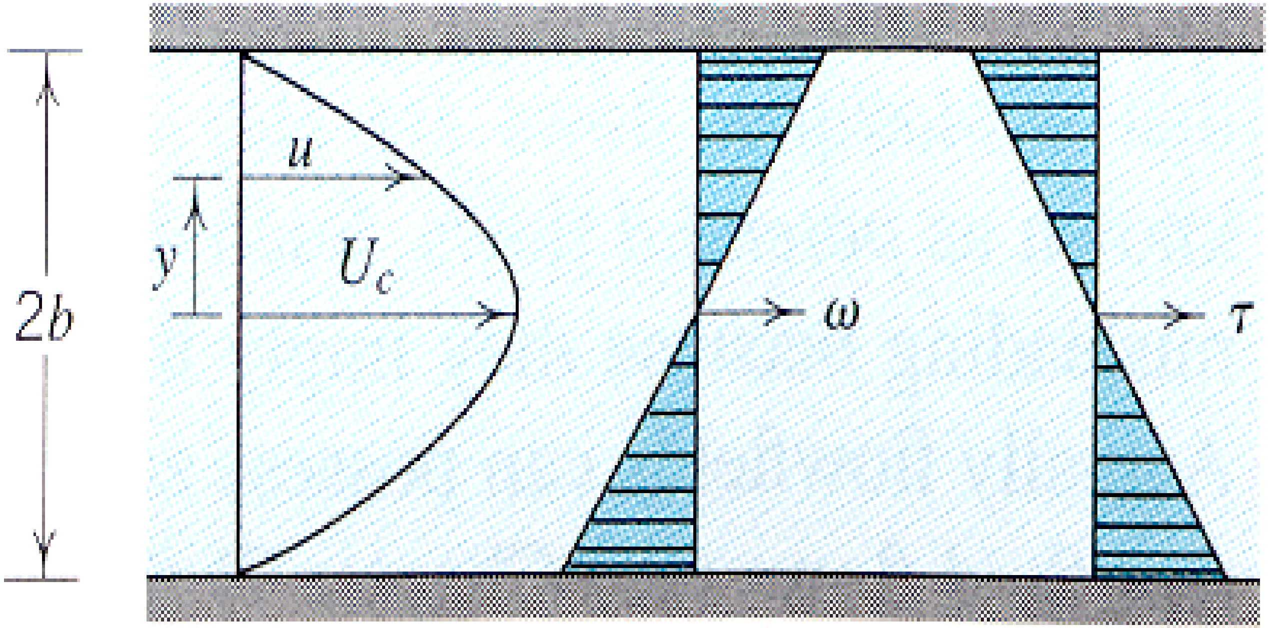
$$\tau = \mu \frac{dv}{dy}$$

$$v = C_1 y^2 + C_2 \quad \rightarrow \quad \text{parabolic}$$

$$\frac{dv}{dy} = 2\, C_1\, y$$

$$\therefore \quad \tau = 2\, C_1\, \mu\, y = C\, y \quad \rightarrow \quad \text{straight line}$$

7.2 Turbulent Flow and Eddy Viscosity



7.2 Turbulent Flow and Eddy Viscosity

[IP 7.3] p. 238 Turbulent flow in a pipe

A turbulent flow of water occurs in a pipe of 2 m diameter.

$$v = 10 + 0.8 \ln y$$

$$\tau\Big|_{y=1/3m} = 103 \text{ Pa}$$

Calculate ε, l, κ

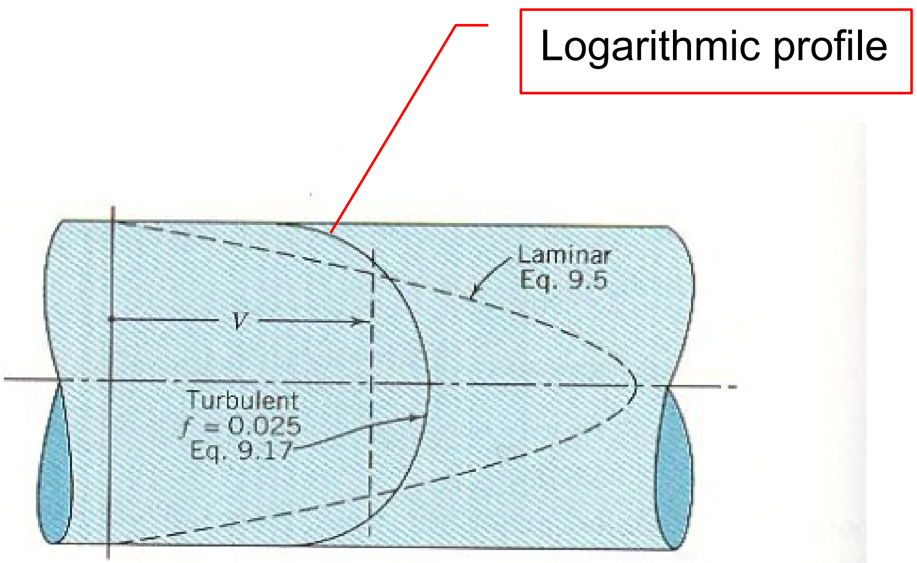


Fig. 9.5

7.2 Turbulent Flow and Eddy Viscosity

Solution:

$$\tau = \varepsilon \frac{dv}{dy}$$

$$= \rho l^2 \left(\frac{dv}{dy} \right)^2$$

$$= \rho \kappa^2 y^2 \left(\frac{dv}{dy} \right)^2$$

$$\left. \frac{dv}{dy} \right|_{y=1/3m} = \left. \frac{0.8}{y} \right|_{y=1/3m} = 2.4 \ s^{-1}$$

(a): $103 = \varepsilon (2.4)$ $\quad \varepsilon = 42.9 \ \text{Pa} \cdot \text{s}$ $\quad \mu = 1.002 \times 10^{-3} \ Pa \cdot s$

(b): $103 = 10^3 \ l^2 (2.4)^2$ $\quad l = 0.134 \text{ m} \approx 10\% \text{ of pipe radius}$

(c): $103 = 10^3 \ \kappa^2 \left(\frac{1}{3} \right)^2 (2.4)^2$ $\quad \kappa = 0.401$

7.3 Fluid Flow Past Solid Boundaries

- 점성유체의 운동 방정식(7.15절)

- Navier-Stokes 방정식

점성력

$$\frac{\partial u}{\partial t}+u\frac{\partial u}{\partial x}+v\frac{\partial u}{\partial y}+w\frac{\partial u}{\partial z}=-\frac{1}{\rho}\frac{\partial p}{\partial x}+\nu\left(\frac{\partial^2 u}{\partial x^2}+\frac{\partial^2 u}{\partial y^2}+\frac{\partial^2 u}{\partial z^2}\right)$$

$$\frac{\partial v}{\partial t}+u\frac{\partial v}{\partial x}+v\frac{\partial v}{\partial y}+w\frac{\partial v}{\partial z}=-\frac{1}{\rho}\frac{\partial p}{\partial y}+\nu\left(\frac{\partial^2 v}{\partial x^2}+\frac{\partial^2 v}{\partial y^2}+\frac{\partial^2 v}{\partial z^2}\right)$$

$$\frac{\partial w}{\partial t}+u\frac{\partial w}{\partial x}+v\frac{\partial w}{\partial y}+w\frac{\partial w}{\partial z}=-\frac{1}{\rho}\frac{\partial p}{\partial z}+\nu\left(\frac{\partial^2 w}{\partial x^2}+\frac{\partial^2 w}{\partial y^2}+\frac{\partial^2 w}{\partial z^2}\right)-g$$

- 연속방정식

$$\frac{\partial u}{\partial x}+\frac{\partial v}{\partial y}+\frac{\partial w}{\partial z}=0$$

7.3 Fluid Flow Past Solid Boundaries

- 점성유체의 운동 방정식의 해석

1) Navier-Stokes 방정식에서 점성항 무시 → Euler 방정식 → Bernoulli 공식
2) Potential flow 로 해석

- d'Alembert 의 역설:

- 점성력의 영향을 무시해서는 안되는 영역이 있음
- 경계면 부근에서는 점성계수의 값이 작더라도 속도경사의 크기가 매우 크기 때문에 전단력이 커짐.

$$\tau = \mu \frac{du}{dy}$$

- 경계층에서는 점성력의 영향이 크며 에너지의 손실에 직접 영향을 미침

7.3 Fluid Flow Past Solid Boundaries

- 경계층 이론 (Prandtl, 1904)

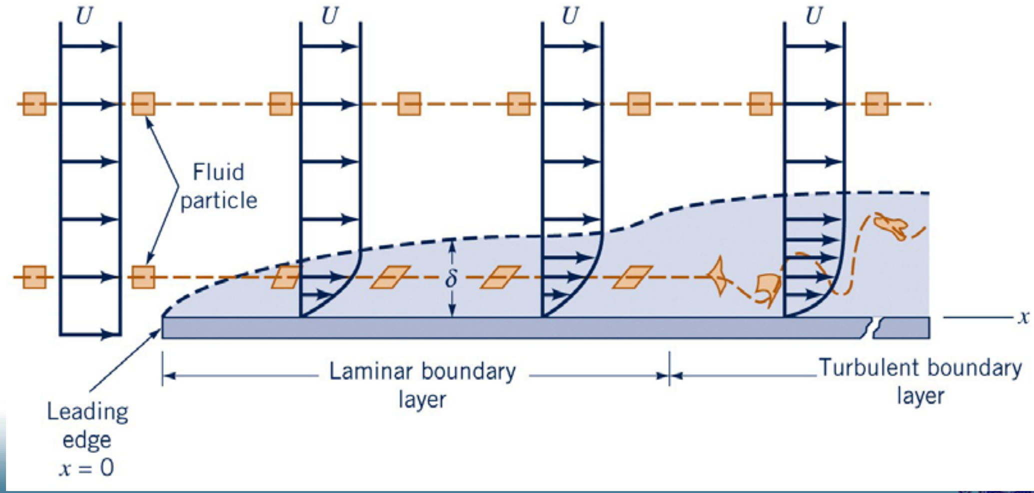
- 평판이 일정한 유속 *V* 로 움직이는 유체속에 있을 때 이 평판이 유체 흐름에 미치는 영향 해석

- 경계층은 시작점에서 작으나 뒤로 갈수록 커짐

- *V*가 커질수록 경계층의 두께는 얇아짐

- 경계층은 매우 얇으며 따라서 경계층내의 압력은 밖의 압력과 같음 → 미지수 감소

- 층류경계층에 이어 난류경계층이 형성



7.3 Fluid Flow Past Solid Boundaries

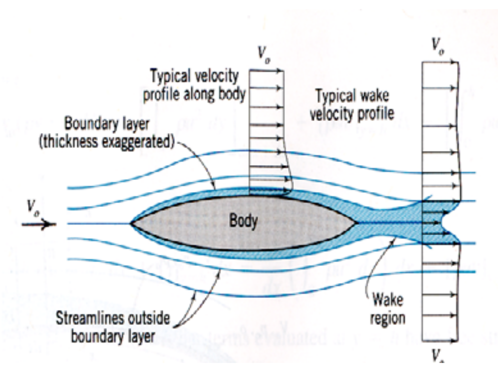
- Flow phenomena <u>near a solid boundary ← friction</u>

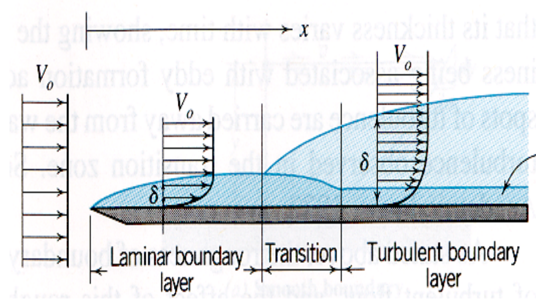
  - external flows: flow around an object immersed in the fluid

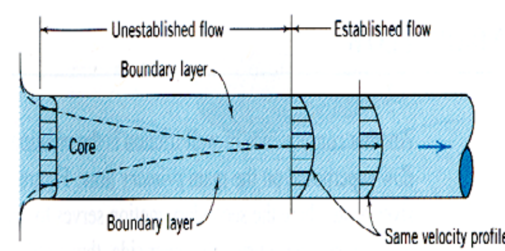
    (over a wing or a flat plate, etc.)

  - internal flows: flow between solid boundaries

    (flow in pipes and channels)







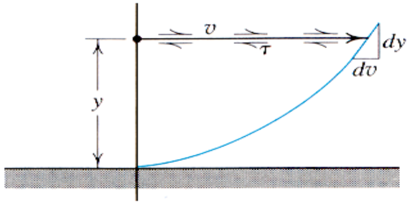
7.3 Fluid Flow Past Solid Boundaries

(1) Laminar flow over smooth (미끈한 면) or rough boundaries (거친 면)

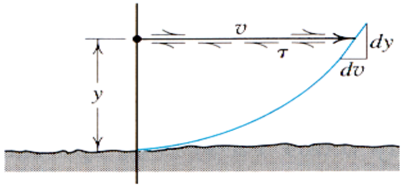
~ possesses essentially the same properties, the velocity being zero at the boundary surface and the shear stress throughout the flow

~ surface roughness has no effect on the flow as long as the roughness are small relative to the flow cross section size.

→ viscous effects dominates the whole flow



(a) Smooth boundary



(b) Rough boundary

7.3 Fluid Flow Past Solid Boundaries

(2) Turbulent flow over smooth or rough boundaries

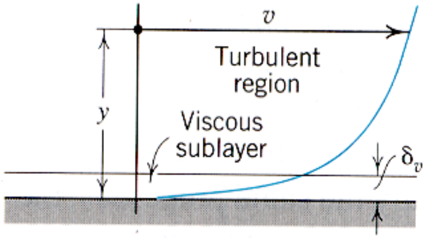
- Flow over a smooth boundary is always separated from the boundary by a sublayer of viscosity-dominated flow (laminar flow). (층류저층)

[Re] Existence of laminar sublayer

Boundary will reduce the available mixing length for turbulence motion.

→ In a region very close to the boundary, the available mixing length is reduced to zero (i.e., the turbulence is completely extinguished).

→ a film of viscous flow over the boundary results in.



(a) Smooth boundary

7.3 Fluid Flow Past Solid Boundaries

- Shear stress:

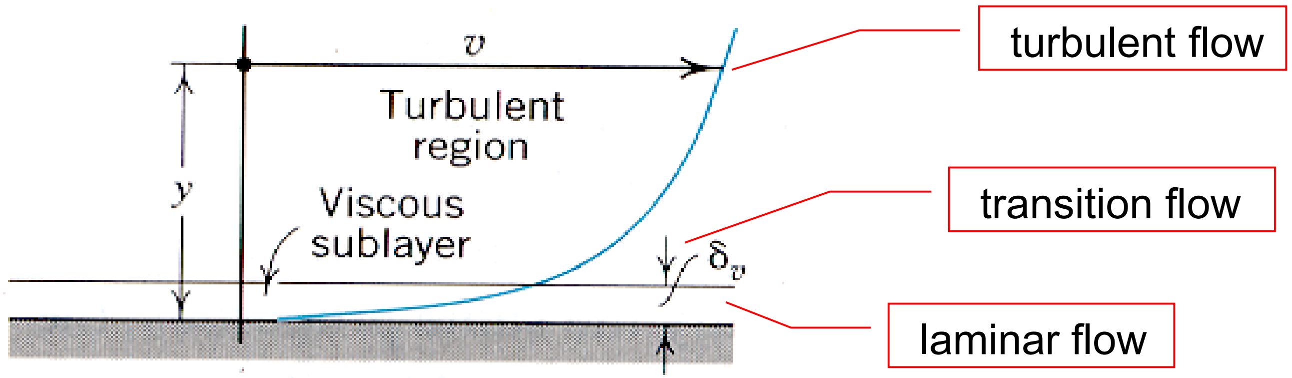
  Inside the viscous sublayer: $\tau = \mu \dfrac{dv}{dy}$

  Outside the viscous sublayer: $\tau = \rho\, l^2 \left(\dfrac{dv}{dy}\right)^2$

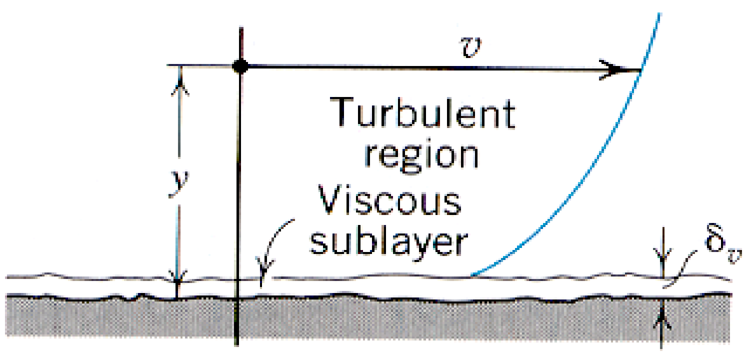
- Between the turbulent region and the viscous sublayer lies a transition zone in which shear stress results from a complex combination of both turbulent and viscous action.

→The thickness of the viscous sublayer varies with time. The sublayer flow is unsteady.

7.3 Fluid Flow Past Solid Boundaries



(a) Smooth boundary



(b) Rough boundary

7.3 Fluid Flow Past Solid Boundaries

- Roughness of the boundary surface affects the physical properties (velocity, shear, friction) of the fluid motion.

→ The effect of the roughness is dependent on the relative size of roughness and viscous sublayer.

- Classification of surfaces based on ratio of absolute roughness e to viscous sublayer thickness δ_v

i) Smooth surface: $\frac{e}{\delta_v} \le 0.3$

- Roughness projections are completely submerged in viscous sublayer.

→ They have no effect on the turbulence.

7.3 Fluid Flow Past Solid Boundaries

ii) Transition: $0.3 < \frac{e}{\delta_v} < 10$

iii) Rough surface: $10 \leq \frac{e}{\delta_v}$

- However, the thickness of the viscous sublayer depends on certain properties of the flow.

→ The same boundary surface behave as a smooth one or a rough one depending on the size of the Reynolds number and of the viscous sublayer.

$$\delta_v = f\left(\frac{1}{R_e} \right)$$

$$i)\, v \uparrow \;\rightarrow\; R_e \uparrow \;\rightarrow\; \delta_v \downarrow \;\rightarrow\; \text{rough surface}$$

$$ii)\, v \downarrow \;\rightarrow\; R_e \downarrow \;\rightarrow\; \delta_v \uparrow \;\rightarrow\; \text{smooth surface}$$

7.4 Flow Establishment-External Flows

- **Boundary layer concept by Prandtl (1904)**

  - Inside boundary layer - frictional effects

  - Outside boundary layer – frictionless (irrotational; potential) flow

- Mechanism of boundary layer growth

① Velocity of the particle at the body wall is zero.

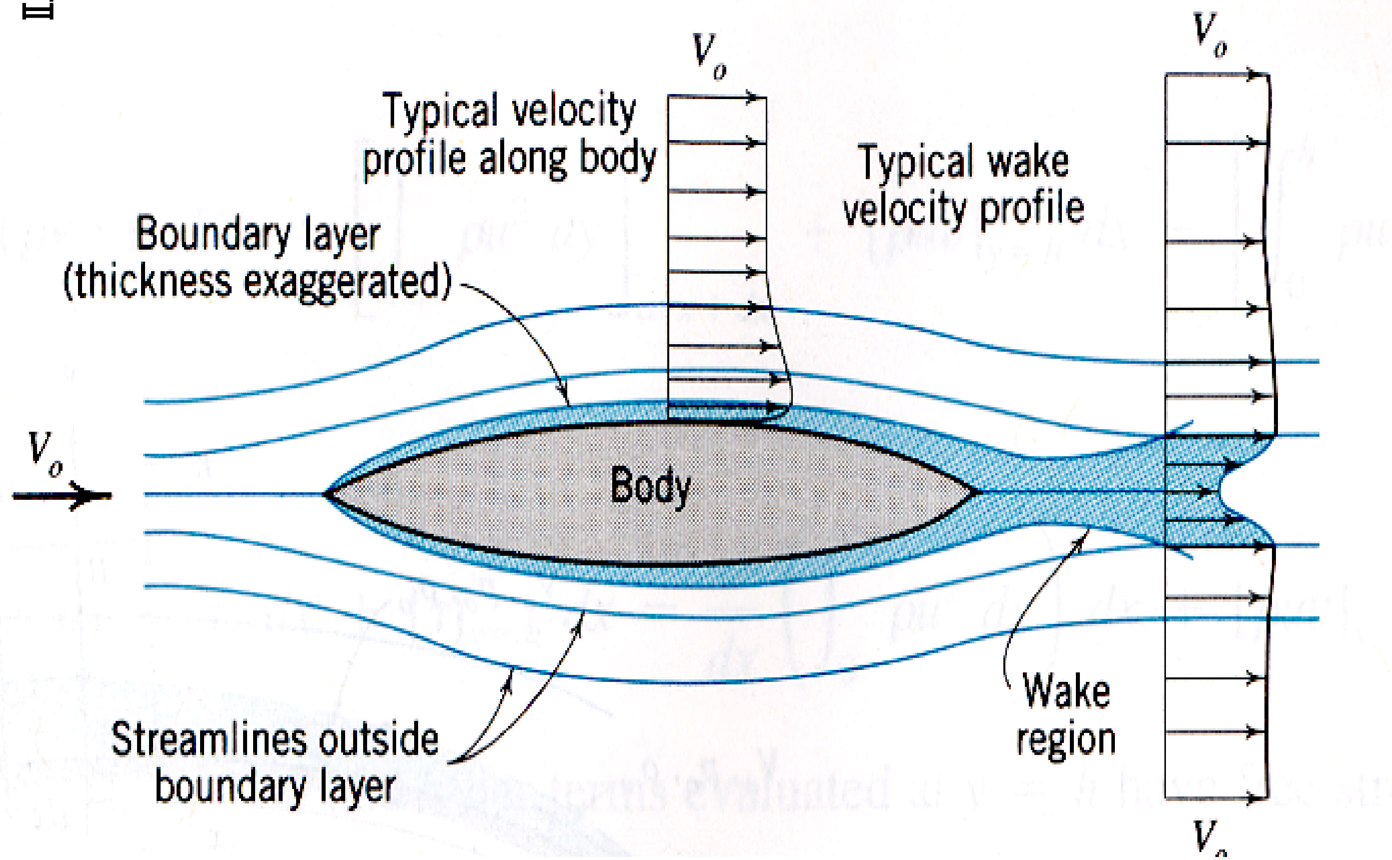
② Velocity gradient $\left(dv/dy\right)$ in the vicinity of the boundary is very high.

③ Large frictional (shear) stresses in the boundary layer $\left(\tau = \mu\left(dv/dy\right)\right)$ slow down successive fluid elements.

④ Boundary layers steadily thicken downstream along the body.

7.4 Flow Establishment-External Flows

- 20세기 초 비행기의 등장
- 독일학자: Prandtl, von Karman
- 우주항공산업



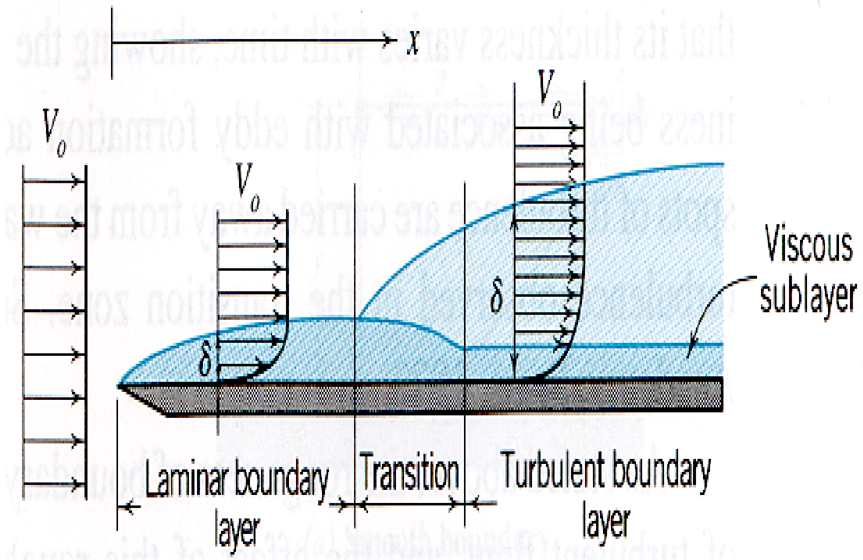
7.4 Flow Establishment-External Flows

- Flow establishment over a smooth flat plate

→ Boundary layer flow: laminar → transition → turbulent

- Laminar boundary layer

~ Viscous action is dominant.



$$R_x = \frac{V_0 x}{\nu} \qquad R_{x_c} = 500,000 \quad (7.7a)$$

$$R_\delta = \frac{V_0 \delta}{\nu} \qquad R_{\delta_c} = 4,000 \quad (7.7b)$$

$R_x < 500,000$ or $R_\delta < 4,000$

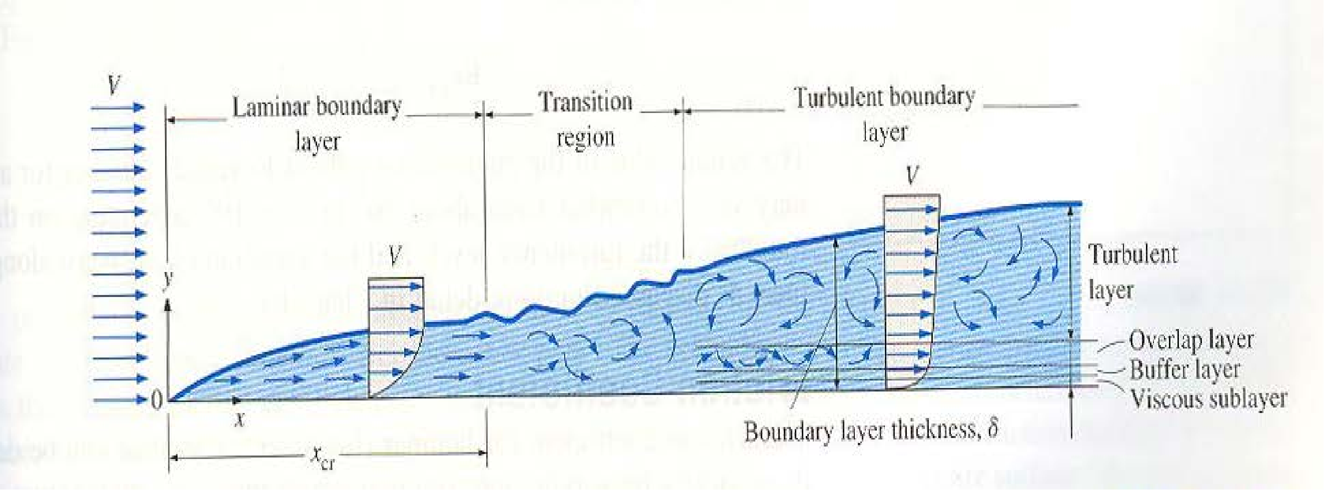
→ laminar boundary layer expected

7.4 Flow Establishment-External Flows

- Turbulent boundary layer

~ Laminar sublayer exists.

$$R_x > 500,000 \text{ or } R_\delta > 4,000$$



7.7 Separation

- Separation of moving fluid from boundary surfaces is important

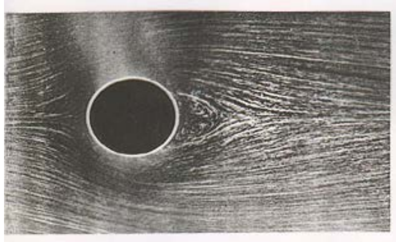
~ difference between ideal (inviscid) and real flow.

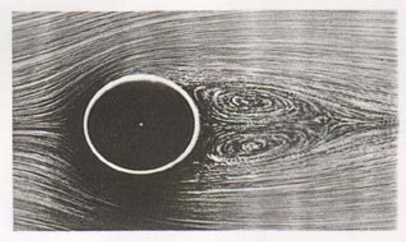
- Ideal fluid flow: no separation

  symmetrical streamline

- Flow of real fluid: separation, eddy, wake

  asymmetric flowfields

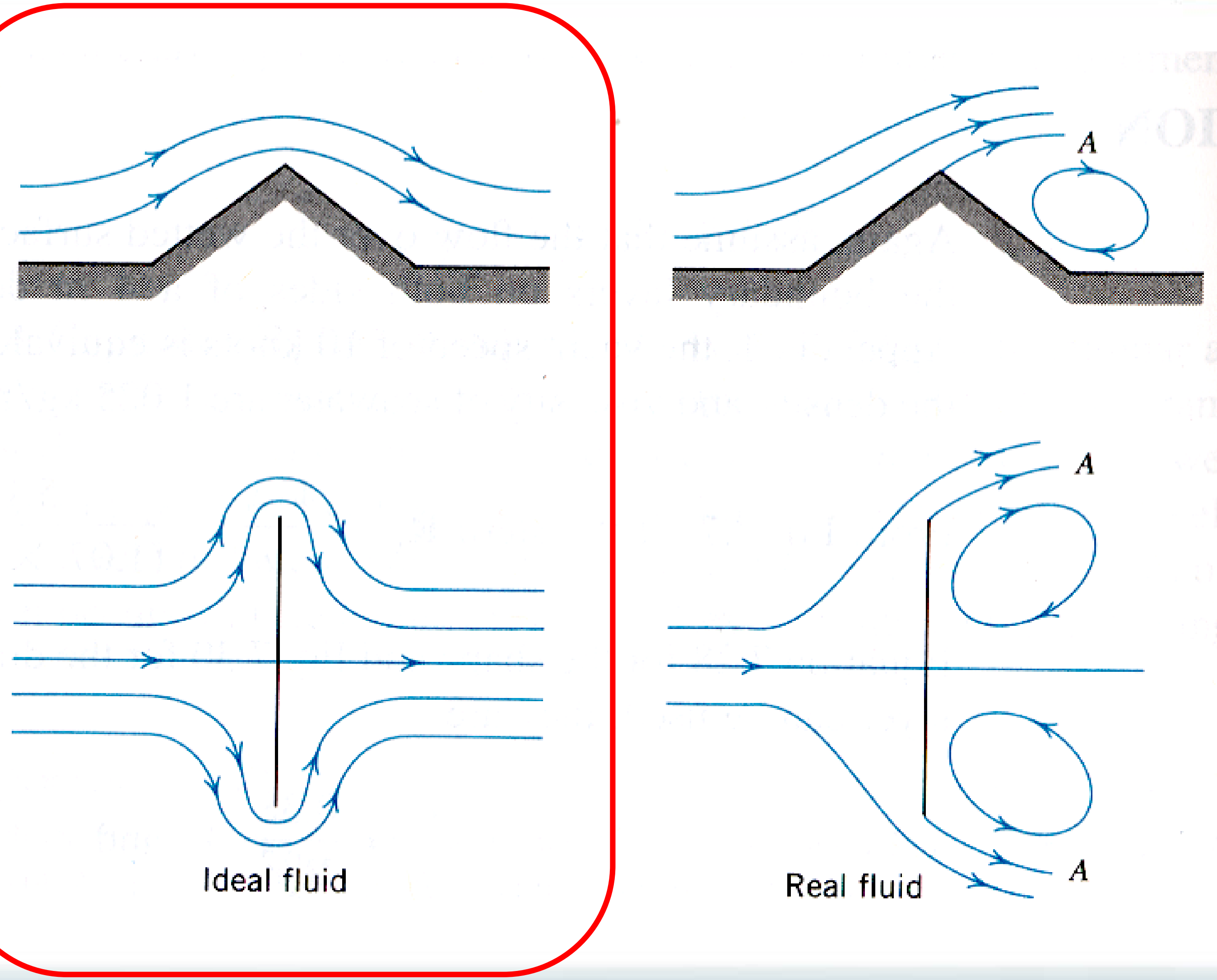




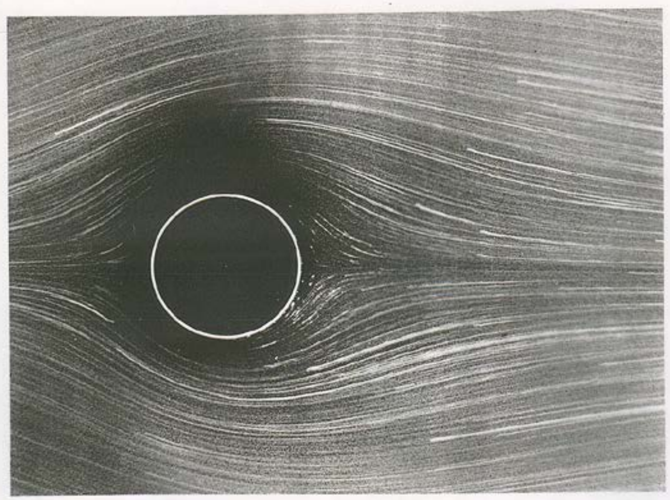
[Re] Eddy:

- unsteady (time-varying)
  - forming, being swept away, and re-forming
  - absorbing energy from the mean flow and dissipation it into heat

7.7 Separation



7.7 Separation



24. Circular cylinder at R=1.54. At this Reynolds number the streamline pattern has clearly lost the fore-and-aft symmetry of figure 6. However, the flow has not yet separated at the rear. That begins at about R=5, though the value is not known accurately. Streamlines are made visible by aluminum powder in water. *Photograph by Sadatoshi Taneda*

25. Sphere at R=9.8. Here too, with wall effects negligible, the streamline pattern is distinctly asymmetric, in contrast to the creeping flow of figure 8. The fluid is evidently moving very slowly at the rear, making it difficult to estimate the onset of separation. The flow is presumably attached here, because separation is believed to begin above R=20. Streamlines are shown by magnesium cuttings illuminated in water. *Photograph by Madeleine Coutanceau and Michele Payard*

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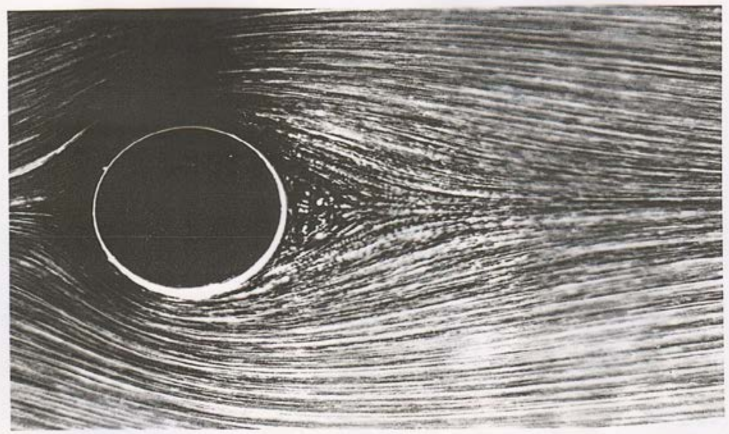
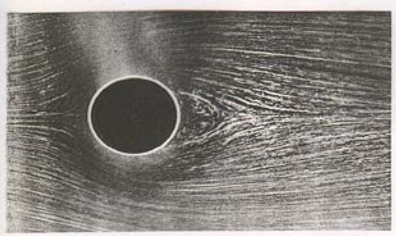
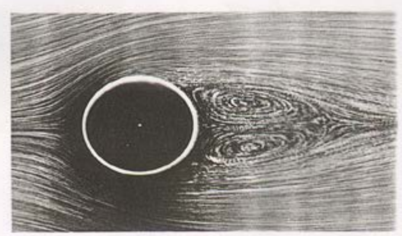
7.7 Separation



40. **Circular cylinder at $R=9.6$.** Here, in contrast to figure 24, the flow has clearly separated to form a pair of recirculating eddies. The cylinder is moving through a tank of water containing aluminum powder, and is illuminated by a sheet of light below the free surface. Extrapolation of such experiments to unbounded flow suggests separation at $R=4$ or 5, whereas most numerical computations give $R=5$ to 7. *Photograph by Sadatoshi Taneda*



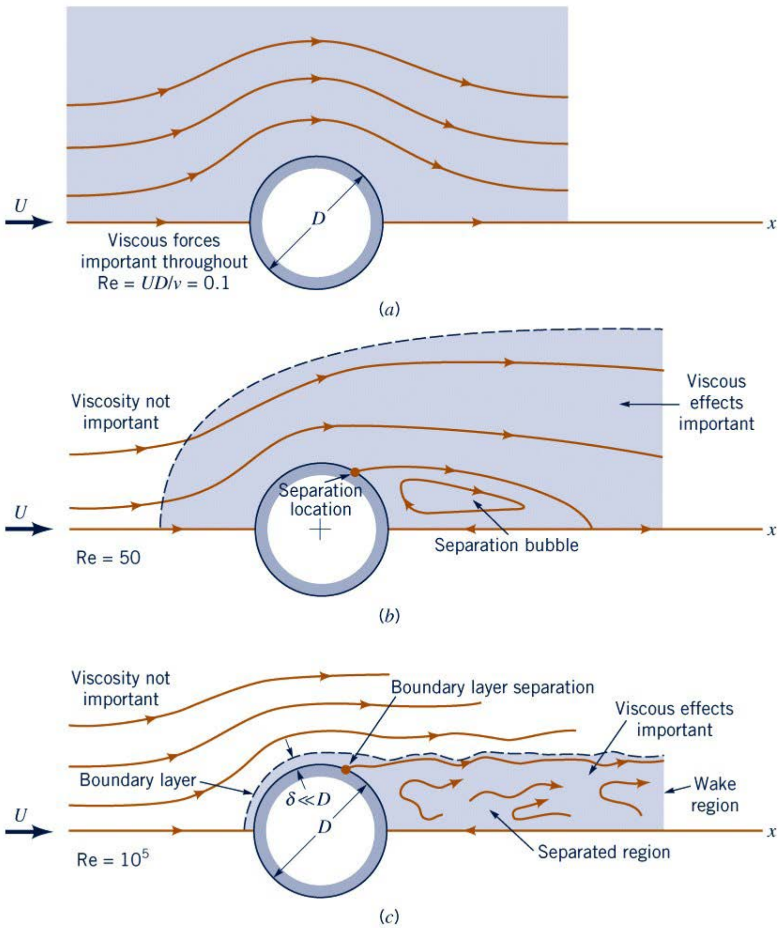
41. **Circular cylinder at $R=13.1$.** The standing eddies become elongated in the flow direction as the speed increases. Their length is found to increase linearly with Reynolds number until the flow becomes unstable above $R=40$. *Taneda 1956a*



42. **Circular cylinder at $R=26$.** The downstream distance to the cores of the eddies also increases linearly with Reynolds number. However, the lateral distance between the cores appears to grow more nearly as the square root. *Photograph by Sadatoshi Taneda*

28

7.7 Separation



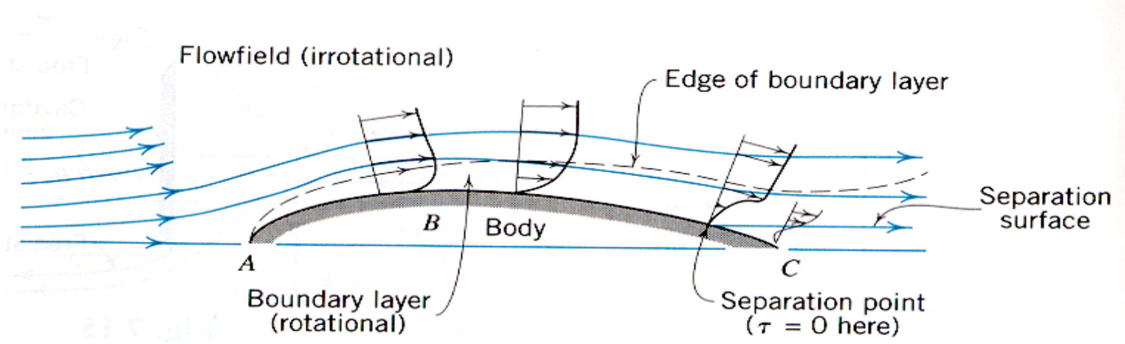
7.7 Separation

- From <u>*A* to *B*</u>, the pressure falls because the flow is accelerating.

→ This produces a <u>favorable pressure gradient</u> which strengthens the boundary layer.

- From <u>*B* to *C*</u>, the pressure rises as the flow decelerates because the body is thinning.

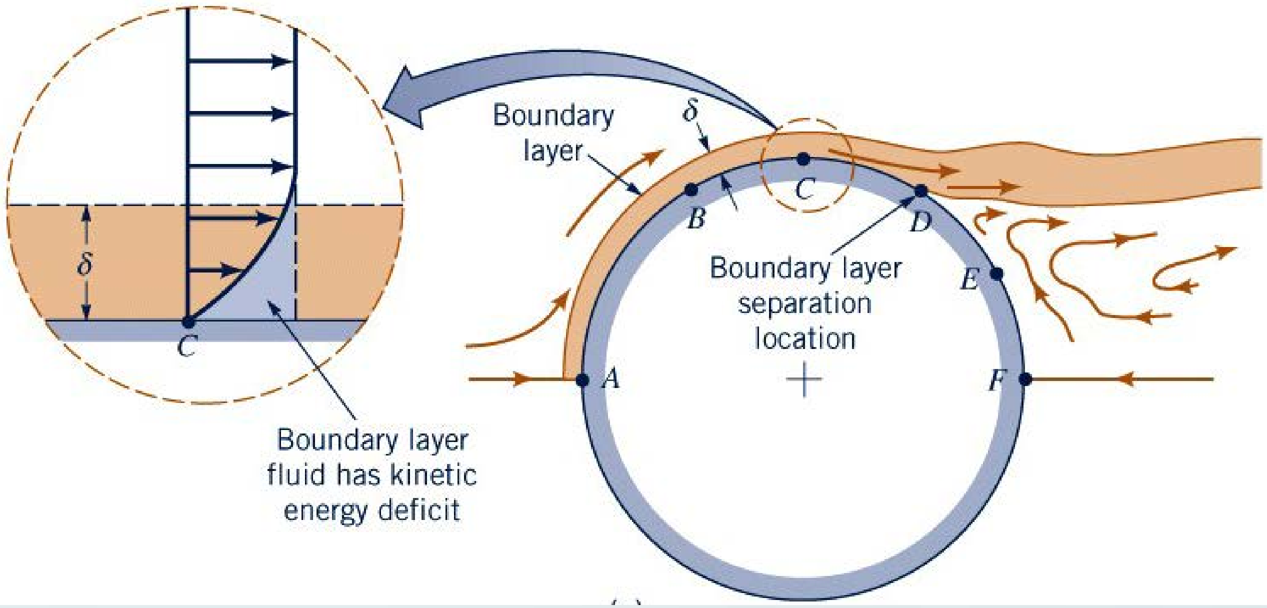
→ This produces an <u>adverse (unfavorable) pressure gradient</u> which weakens the boundary layer sufficiently to cause separation.



7.7 Separation

A → C: 유속 증가, 순압력 경사, 경계층내에서 에너지 손실 발생

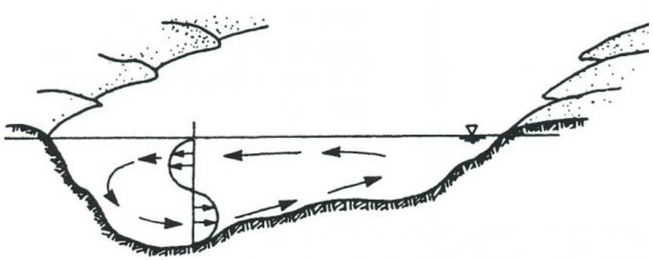
C → F: 유속 감소, 역압력 경사, 경계층내에서 에너지 손실때문에 유속이 매우 작아져서 역압력 경사를 이겨내지 못하고 흐름이 멈추고 흐름박리현상이 발생함

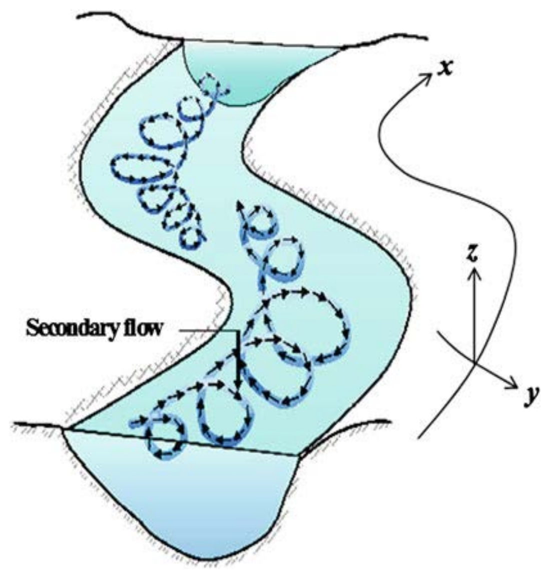


7.8 Secondary Flow

- Another consequence of wall friction is the creation of a flow within a flow, a <u>secondary flow superposed on the main primary flow</u>.

- Secondary flow occurring at the cross section of the meandering river



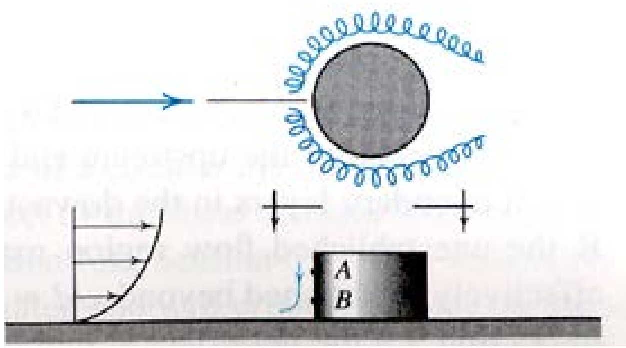


7.8 Secondary Flow

- Horseshoe-shaped vortex around the bridge pier:

~ Downward secondary flow from *A* to *B* induces a vortex type of motion, the core of the vortex being swept downstream around the sides of the pier.

~ This principle is used on the wings of some jet aircraft, vortex generators being used to draw higher energy fluid down to the wing surface to forestall large-scale separation.



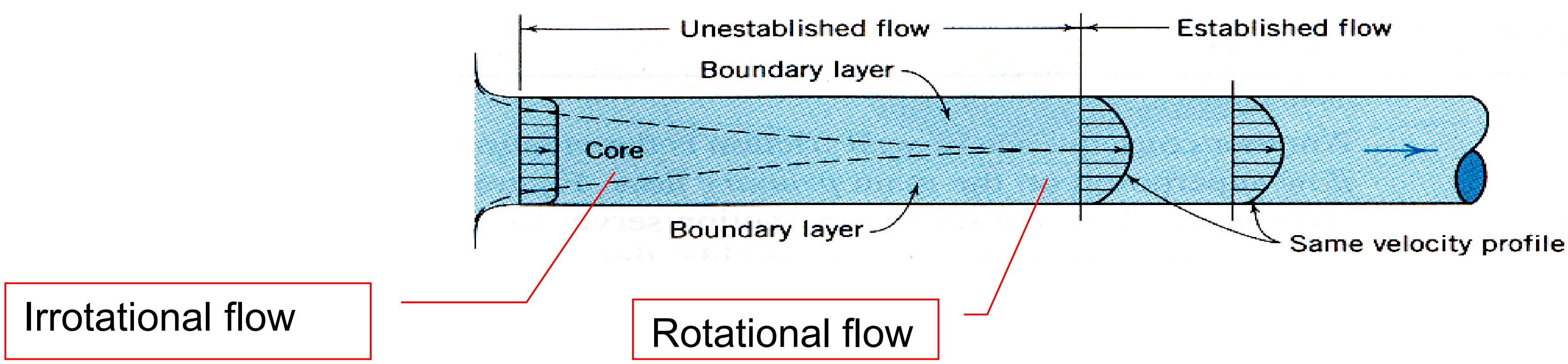
7.9 Flow Establishment – Pipe Flows

- Flow establishment

At the entrance to a pipe, viscous effects begin their influence to lead a growth of the boundary layer.

- Unestablished flow zone (미확립흐름구간):

~ dominated by the growth of boundary layers accompanied by diminishing core of irrotational fluid at the center of the pipe



7.9 Flow Establishment – Pipe Flows

- Established flow zone (확립흐름구간):

~ Influence of wall friction is felt throughout the flow field.

~ There is no further changes in the velocity profiles.

~ Flow is everywhere rotational.

- Flow in a boundary layer may be laminar if $R_e \left(= \frac{Vd}{\nu} \right) < 2100$ or turbulent if $Re \geq 2100$.

7.9 Flow Establishment – Pipe Flows

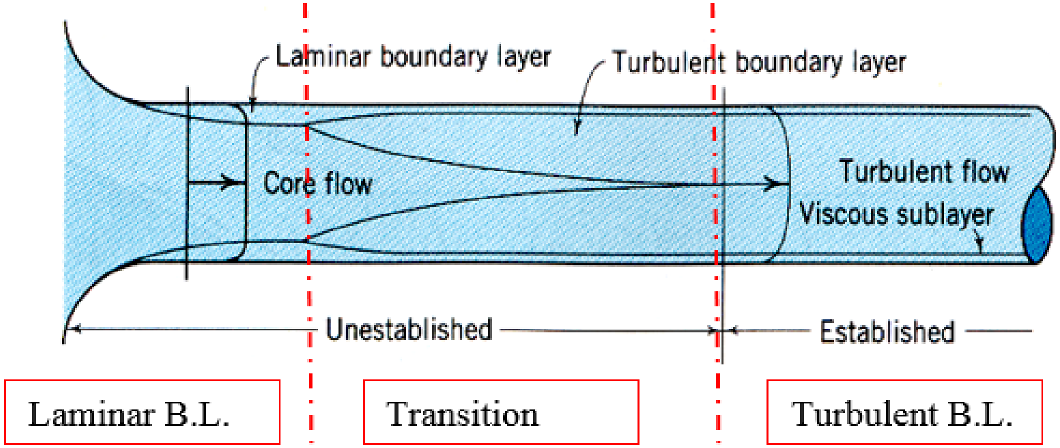
1) Laminar flow

$x =$ length of unestablished flow zone

$$\frac{x}{d} \approx \frac{R_e}{20} \quad \left(\approx \frac{2100}{20} \approx 100\right)$$

Thus, $x < 100\, d \rightarrow$ unestablished flow

2) Turbulent flow



7.10 Shear Stress and Head Loss

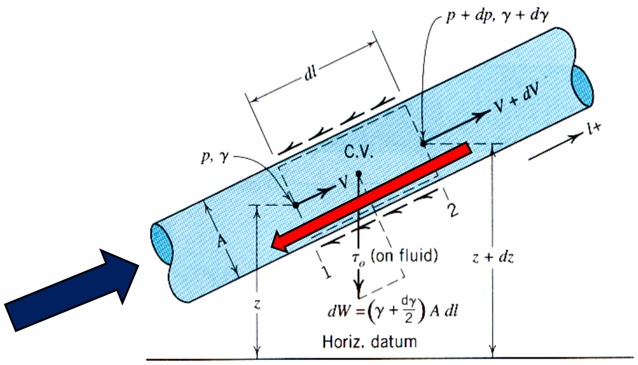
What is the effect of the friction forces on the boundary of a control volume, such as the inside of a pipe?

→ The impulse-momentum equation provides a clear answer.

• Wall shear stress τ_0 is a basic resistance to flow.

~ acting on the periphery of the streamtube opposing the direction of the fluid motion

~ cause energy dissipation (energy loss $= h_L$)



7.10 Shear Stress and Head Loss

Now, apply impulse-momentum equation between ① & ② along the direction of streamtube

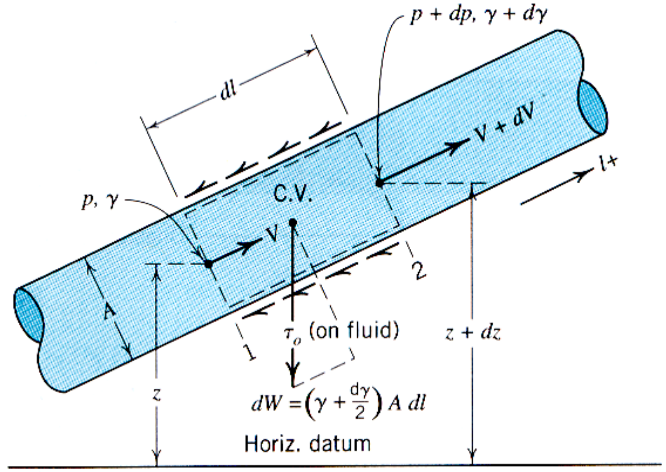
Shear force is included for real fluid.

$$\sum \vec{F} = Q\rho\left(\vec{V}_2 - \vec{V}_1\right)$$

$$pA - (p + dp)A - \tau_0 P dl - \left(\gamma + \frac{d\gamma}{2}\right) A dl \frac{dz}{dl}$$

$$= (V + dV)^2 A(\rho + d\rho) - V^2 A\rho$$

in which P = perimeter of the streamtube



7.10 Shear Stress and Head Loss

Assume momentum correction factor, $\beta_1 = \beta_2 = 1$

Neglect smaller terms containing products of differential quantities

$$-dpA - \tau_0 Pdl - \gamma Adz = 2A\rho VdV + AV^2 d\rho$$

$$= A\left\{\rho d\left(V^2\right) + V^2 d\rho\right\} = Ad\left(\rho V^2\right)$$

Divide by $A\gamma$

$$\frac{dp}{\gamma} + \frac{V}{g}dV + dz = -\frac{\tau_0 dl}{\gamma}\frac{P}{A}$$

$$\frac{dp}{\gamma} + d\left(\frac{V^2}{2g}\right) + dz = -\frac{\tau_0 dl}{\gamma R_h}$$

where $R_h = \dfrac{A}{P} = \text{hydraulic radius}$

7.10 Shear Stress and Head Loss

For established incompressible flow, γ is constant; $d\left(1/\gamma\right)=0$

$$d\left(\frac{p}{\gamma}+\frac{V^2}{2g}+z\right)=-\left(\frac{\tau_0 dl}{\gamma R_h}\right)$$

Integrating this between points 1 and 2 yields

$$\left(\frac{p_1}{\gamma}+\frac{V_1^{\ 2}}{2g}+z_1\right)-\left(\frac{p_2}{\gamma}+\frac{V_2^{\ 2}}{2g}+z_2\right)=\frac{\tau_0\left(l_2-l_1\right)}{\gamma R_h} \qquad (7.8)$$

Now, note that the difference between total heads is the drop in the energy line between points 1 and 2. Thus, Eq. (7.8) can be rewritten as

$$\frac{p_1}{\gamma}+\frac{V_1^{\ 2}}{2g}+z_1=\frac{p_2}{\gamma}+\frac{V_2^{\ 2}}{2g}+z_2+h_{L_{1-2}} \qquad (7.9)$$

→ Work-energy equation for real fluid flow

7.10 Shear Stress and Head Loss

Comparing (7.8) and (7.9) gives

Head loss

$$h_{L_{1-2}} = \frac{\tau_0 (l_2 - l_1)}{\gamma R_h} \qquad (7.10)$$

Resistance to flow

Solving for shear stress gives

$$\tau_0 = \frac{\gamma R_h h_L}{l} = \gamma R_h S_f$$

where $S_f = \text{enegy slope} = \frac{h_L}{l}$

[Re] Head loss is attributed to a "rise in the internal energy of the fluid caused by the viscous shear stresses."

7.10 Shear Stress and Head Loss

- Distribution of shear stress in the pipe flow

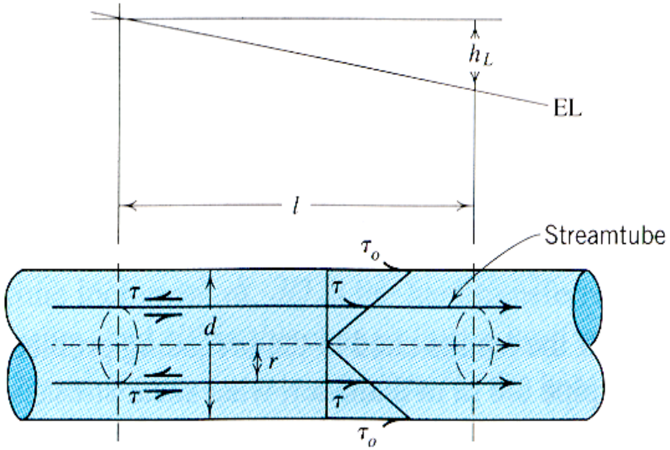
Consider the streamtube of radius *r*

$$\tau_0 \rightarrow \tau$$

$$R_h \rightarrow \frac{r}{2}$$

$$h_{L_{1-2}} \rightarrow h_L$$

$$l_2 - l_1 \rightarrow l$$



Substituting these into (7.10) gives

$$\tau = \left(\frac{\gamma h_L}{2l}\right) r \qquad (7.11)$$

→ The shear stress in the fluid varies linearly with distance from the centerline of the pipe.

~ applicable to both laminar and turbulent flow in pipes

7.10 Shear Stress and Head Loss

[IP 7.6] p. 262

Water flows in a 0.9 m by 0.6 m rectangular conduit (full flow).

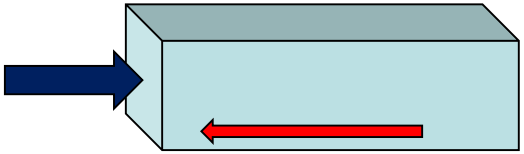
$$\Delta l = 60 \text{ m}$$

$$\Delta h_L = 10 \text{ m}$$

Calculate the resistance stress exerted between fluid and conduit walls.

[Sol]

$$\tau_0 = \frac{\gamma R_h}{\Delta l} \Delta h_L$$



$$R_h = \frac{A}{P} = \frac{0.9 \times 0.6}{2(0.9 + 0.6)} = \frac{0.54}{3} = 0.18 \text{ m}$$

$$\therefore \quad \tau_0 = \frac{9.8 \times 10^3 \times 0.18}{60} \cdot 10 = 0.29 \text{ kPa}$$

7.10 Shear Stress and Head Loss

~ Flow is not axi-symmetric

→ τ_0 is mean shear stress on the perimeter

[IP 7.7] p. 262 Water flow in a cylindrical pipe

Water flows in a cylindrical pipe of 0.6 m in diameter.

$$\tau_0 = \frac{\gamma h_L}{\Delta l} R_h = \frac{\left(9.8 \times 10^3\right)}{60} \frac{0.6}{4} = 0.25 \text{ kPa}$$

$$\tau = \tau_0 \frac{r}{R}$$

τ in the fluid at a point 200 mm from the wall:

$$\tau\Big|_{r=100\,\text{mm}} = \tau_0 \frac{(0.3-0.2)}{0.3} = \frac{1}{3}\left(0.25\right) = 0.083 \text{ kPa}$$

7.11 The First Law of Thermodynamics for Real Fluid

To derive the relationship between shear stresses and energy dissipation

Apply First Law of Thermodynamics

$$\frac{dQ}{dt}+\frac{dW}{dt}=\frac{dE}{dt} \qquad (7.12)$$

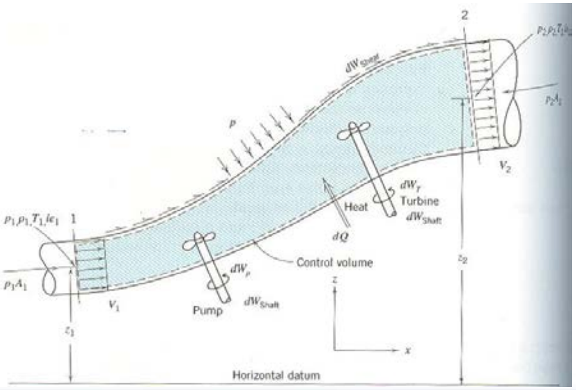
where $dQ=$ heat transferred to the system

$dW=$ work done on the system

$dE=$ change in the total energy of the system

1) Include internal energy in total *E*

$$E=\iiint_{System} i\cdot dm=\iiint_{System}\left(gz+\frac{V^2}{2}+ie\right)\cdot\rho dVol$$



7.11 The First Law of Thermodynamics for Real Fluid

Apply the Reynolds Transport Theorem to evaluate the rate of change of an extensive property, in this case energy, *dE/dt*

→ steady state form of the Reynolds Transport Theorem

$$\frac{dE}{dt} = \iint_{c.s.out} i\rho\vec{v}\cdot\overrightarrow{dA} + \iint_{c.s.in} i\rho\vec{v}\cdot\overrightarrow{dA} \qquad (3) \qquad \frac{\partial}{\partial t}\left(\iiint_{c.v.} i\rho\, dvol\right) \rightarrow dropped$$

where i = energy per unit mass

$$i = gz + \frac{V^2}{2} + ie \qquad (4)$$

Potential energy (gz), Kinetic energy ($\frac{V^2}{2}$), Internal energy (ie)

Substituting (4) into (3) gives

$$\frac{dE}{dt} = \iint_{c.s.out}\left(gz + \frac{V^2}{2} + ie\right)\rho\vec{v}\cdot\overrightarrow{dA} + \iint_{c.s.in}\left(gz + \frac{V^2}{2} + ie\right)\rho\vec{v}\cdot\overrightarrow{dA} \quad (5)$$

7.11 The First Law of Thermodynamics for Real Fluid

$$\frac{dE}{dt} = \left(gz_2 + \frac{V_2^{\ 2}}{2} + ie_2 \right) \cdot \left(\rho_2 V_2 A_2 \right) - \left(gz_1 + \frac{V_1^{\ 2}}{2} + ie_1 \right) \cdot \left(\rho_1 V_1 A_1 \right)$$

$$= \dot{m} \left(gz_2 + \frac{V_2^{\ 2}}{2} + ie_2 \right) - \dot{m} \left(gz_1 + \frac{V_1^{\ 2}}{2} + ie_1 \right) \qquad (6)$$

$$\frac{1}{\dot{m}} \frac{dE}{dt} = \left(gz_2 + \frac{V_2^{\ 2}}{2} + ie_2 \right) - \left(gz_1 + \frac{V_1^{\ 2}}{2} + ie_1 \right) \qquad (7.13)$$

$$\dot{m} = \rho_1 V_1 A_1 = \rho_2 V_2 A_2 = \text{mass flowrate}$$

7.11 The First Law of Thermodynamics for Real Fluid

2) Evaluate the work done on the fluid system (dW)

- Flow work done via fluid entering or leaving the control volume

→ Pressure work $= p \times \mathrm{area} \times$ distance

→ Net pressure work rate = pressure force x distance / time = pressure force x velocity

$$\frac{dW_{flow}}{dt} = p_1 A_1 V_1 - p_2 A_2 V_2$$

$$\frac{1}{\dot{m}} \frac{dW_{flow}}{dt} = \frac{p_1}{\rho_1} - \frac{p_2}{\rho_2} \qquad (7.14)$$

- Shear work is zero because the boundary is fixed

$$W_{shear} = 0$$

7.11 The First Law of Thermodynamics for Real Fluid

- Shaft work

$W_T \leq 0$ (energy is extracted from the system)

$W_p \geq 0$ (energy is put in)

→ Net shaft work rate on the fluid = $\frac{dW_{shaft}}{dt} = Q\gamma\left(E_P - E_T\right)$

where $E_P\,(E_T) =$ work done per unit weight of fluid flowing

$$\frac{1}{\dot{m}}\frac{dW_{shaft}}{dt} = gE_P - gE_T \qquad (7.15)$$

3) Consider heat transfer rate *dQ/dt* in terms of q_H

q_H = heat added to the fluid in the control volume per unit of mass

$$\frac{dQ}{dt} = \dot{m}q_H \qquad (7.16)$$

7.11 The First Law of Thermodynamics for Real Fluid

- Combine (7.12) ~(7.16) to derive general energy equation for steady incompressible flow

$$\left(\frac{p_1}{\gamma}+\frac{V_1^{\,2}}{2g}+z_1\right)+E_p=\left(\frac{p_2}{\gamma}+\frac{V_2^{\,2}}{2g}+z_2\right)+E_T+\frac{1}{g}\left(ie_2-ie_1-q_H\right) \qquad (7.17)$$

$$\left(\frac{p_1}{\gamma}+\frac{V_1^{\,2}}{2g}+z_1\right)+E_p=\left(\frac{p_2}{\gamma}+\frac{V_2^{\,2}}{2g}+z_2\right)+E_T+h_{L_{1-2}} \qquad (7.18)$$

Conversion of energy into heat

where

$$h_{L_{1-2}}=\frac{\tau_0\left(l_2-l_1\right)}{\gamma R_h}=\frac{1}{g}\left(ie_2-ie_1-q_H\right) \qquad (7.19)$$

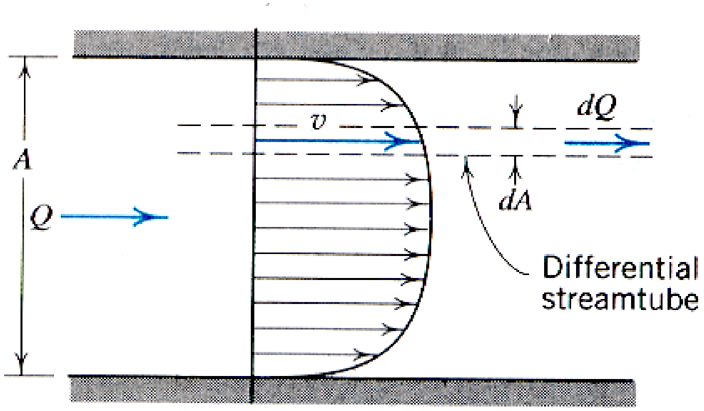
7.12 Velocity Distribution

In a real fluid flow, the shearing stresses produce velocity distributions.

→ non-uniform velocity distribution

Total kinetic energy flux $(J/s) = \frac{\rho}{2}\iint v^3 dA$ (7.14)

Total momentum flux(N) $= \rho\iint_A v^2 dA$ (7.15)



7.12 Velocity Distribution

[Re] $$K.E. = \frac{1}{2}mv^2 = \frac{1}{2}\rho vol\, v^2$$

$$K.E./time = \frac{1}{2}\rho\frac{vol}{t}v^2 = \frac{1}{2}\rho Q v^2 = \frac{1}{2}\rho A v v^2 = \frac{1}{2}\rho A v^3$$

momentum flux $= \frac{mv}{t} = \rho\frac{vol}{t}v = \rho Q v = \rho A v^2$

Use mean velocity V and total flow rate Q

Total kinetic energy $= \alpha Q \gamma \frac{V^2}{2g} = \frac{\gamma}{2g} Q V^2 \alpha = \frac{\rho}{2} Q V^2 \alpha$ (7.16)

Momentum flux $= \beta Q \rho V$ (7.17)

where α, β = correction factors

7.12 Velocity Distribution

(1) Energy correction factor

Combine (7.14) and (7.16)

$$\frac{\rho}{2}\alpha QV^2 = \frac{\rho}{2}\int_A v^3 dA$$

$$\alpha = \frac{1}{V^2}\frac{\int_A v^3 dA}{Q} = \frac{1}{V^2}\frac{\int_A v^3 dA}{\int_A v dA}$$

where $Q = \int_A v dA$

(2) Momentum correction factor

Combine (7.15) and (7.17)

$$\beta Q \rho V = \rho \int_A v^2 dA$$

$$\beta = \frac{1}{V}\frac{\int_A v^2 dA}{Q} = \frac{1}{V}\frac{\int_A v^2 dA}{\int_A v dA}$$

7.12 Velocity Distribution

[Ex] $\alpha = \beta = 1$ for uniform velocity distribution

$\alpha = 1.54$, $\beta = 1.20$ for parabolic velocity distribution (laminar flow)

$$v = v_c \left(1 - r^2 / R^2\right)$$

$\alpha = 1.1$, $\beta = 1.05$ for turbulent flow

• Correction in the Bernoulli equation in real fluid flow

→ nonuniform velocity distribution

→ bundle of energy lines

→ use single effective energy line of aggregation of streamlines $= \alpha \dfrac{V^2}{2g}$

$$\alpha_1 \frac{V_1^2}{2g} + \frac{p_1}{\gamma} + z_1 = \alpha_2 \frac{V_2^2}{2g} + \frac{p_2}{\gamma} + z_2 + h_{L_{1-2}} \qquad (7.18)$$

where $h_{L_{1-2}}$ = head loss between sections 1 and 2

Homework Assignment # 7

Homework Assignment # 7

Due: 1 week from today

1. (Prob. 7.1)

When 0.0019 m^3/s of water flow in a 76 mm pipe line at 21^{o}C, is the flow laminar or turbulent?

2. (Prob. 7.7)

A fluid flows in a 75 mm pipe which discharges into a 150 mm line. What is the Reynolds number in the 150 mm pipe if that in the 75 mm pipe is 20,000?

Homework Assignment # 7

3. (Prob. 7.12)

A turbulent flow in a boundary layer has a velocity profile

$$v = \frac{v_*}{\kappa} \ln y + C$$

where κ is the Karman constant and the *friction velocity* is defined as

$$v_* = \sqrt{\frac{\tau_o}{\rho}}$$

τ_o is the wall shear stress. Find expressions for the eddy viscosity ε and the shear stress $\tau(y)$ if the mixing length relationship $l = \kappa y$ is assumed valid.

Homework Assignment # 7

4. (Prob. 7.17)

When oil (kinematic viscosity 1×10^{-4} m^2/s, specific gravity 0.92) flows at a mean velocity of 1.5 m/s through a 50 mm pipeline, the head lost in 30 m of pipe is 5.4 m. What will be the head loss when the velocity is increased to 3 m/s?

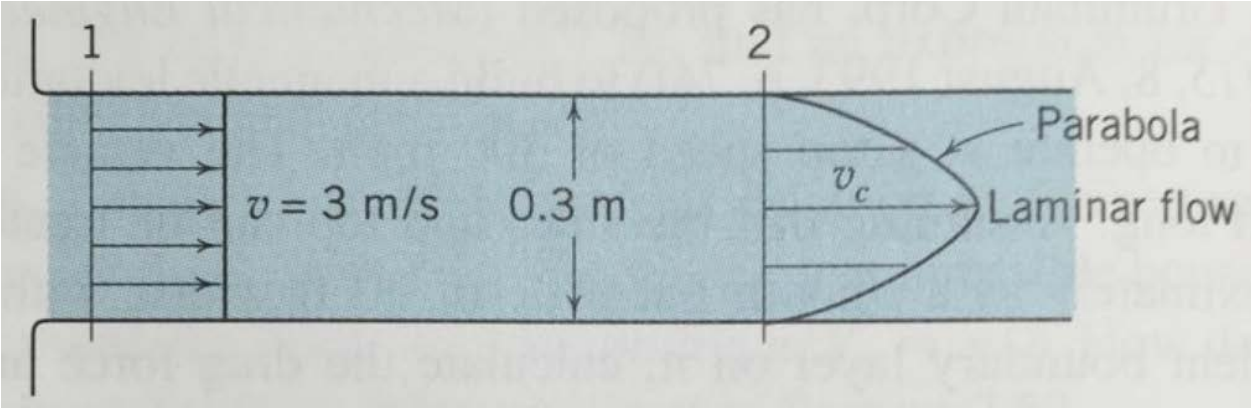
5. (Prob. 7.52)

If the head lost in 30 m of 75 mm pipe is 7.6 m when a certain quantity of water flows therein, what is the total dragging force exerted by the water on this reach of pipe?

Homework Assignment # 7

6. (Prob. 7.58)

If a zone of unestablished flow may be idealized ti the extent shown and the centerline may be treated as a streamline in an ideal fluid, calculate the drag force exerted by the sidewalls (between sections 1 and 2) on the fluid if the flow is (a) two-dimentional and 0.3 m wide nomal to the paper and (b) axisymmetric. The fluid flowing has specific gravity 0.90.



Homework Assignment # 7

7. (Prob. 7.69)

If the velocity profiles at the upstream and downstream ends of the mixing zone of a jet pump may be approximated as shown, and wall friction may be neglected, calculate the rise of pressure from section 1 to section 2, and the power lost in the mixing process. Water is flowing.