

Equations of Continuity and Motion (6/6)









Contents

- 15.1 Vortex Motion
- Problems

Objectives

- Derive 3D equations of continuity and motion
- Derive Navier-Stokes equation for Newtonian fluid
- Study solutions for simplified cases of laminar flow
- Derive Bernoulli equation for irrotational motion and frictionless flow
- Study solutions for vortex motions





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- Vortex
- fluid motion in which streamlines are concentric circles

- Forced vortex
- Rotational cylinder

- Free vortex
- Typhoon, drain hole vortex













15.1.1 Vortex

For <u>steady flow</u> of an <u>incompressible fluid</u>, apply Navier-Stokes equations in cylindrical coordinates







Continuity Eq.: Eq. (11.10)

$$\frac{1}{r}\frac{\partial}{\partial r}\left(rv_{r}\right) + \frac{1}{r}\frac{\partial}{\partial \theta}\left(v_{\theta}\right) + \frac{\partial}{\partial z}\left(v_{z}\right) = 0$$
$$\frac{1}{r}\frac{\partial}{\partial \theta}\left(v_{\theta}\right) = 0 \longrightarrow \frac{\partial v_{\theta}}{\partial \theta} = 0$$

(15.1)

Navier-Stokes Eq.: Eq. (11.9)

1) *r*-comp.

$$\rho \left(\frac{\partial v_r}{\partial t} + v_r \frac{\partial v_r}{\partial r} + \frac{v_\theta}{r} \frac{\partial v_r}{\partial \theta} - \frac{v_\theta^2}{r} + v_z \frac{\partial v_r}{\partial z} \right)$$





$$= -\frac{\partial p}{\partial r} + \mu \left\{ \frac{\partial}{\partial r} \left(\frac{1}{r} \frac{\partial}{\partial r} \left[r v_r \right] \right) + \frac{1}{r^2} \frac{\partial^2 v_r}{\partial \theta^2} - \frac{2}{r^2} \frac{\partial v_{\theta}}{\partial \theta} + \frac{\partial^2 v_r}{\partial z^2} \right\} + \rho g_r$$

$$\frac{v_{\theta}}{r} = \frac{1}{\rho} \frac{\partial p}{\partial r}$$
(15.2a)

2) *θ* -comp.

 $\rho \left(\frac{\partial v_{\theta}}{\partial t} + y_r' \frac{\partial v_{\theta}}{\partial r} + \frac{v_{\theta}}{r} \frac{\partial v_{\theta}}{\partial \theta} - \frac{v_r v_{\theta}}{r} + y_z' \frac{\partial v_{\theta}}{\partial z} \right)$ $= -\frac{1}{r}\frac{\partial p}{\partial \theta} + \mu \left\{ \frac{\partial}{\partial r} \left(\frac{1}{r}\frac{\partial}{\partial r} [rv_{\theta}] \right) + \frac{1}{r^{2}}\frac{\partial^{2} y_{\theta}}{\partial \theta^{2}} - \frac{2}{r^{2}}\frac{\partial v_{r}}{\partial \theta} + \frac{\partial^{2} y_{\theta}}{\partial z^{2}} \right\} + \rho g_{\theta}$





$$\therefore 0 = \frac{\mu}{\rho} \frac{\partial}{\partial r} \left[\frac{1}{r} \frac{\partial}{\partial r} (r v_{\theta}) \right]$$

3) *z*-comp.

 $\rho \left(\frac{\partial v_z}{\partial t} + y_r' \frac{\partial v_z}{\partial r} + \frac{v_\theta}{r} \frac{\partial v_z}{\partial \theta} - \frac{v_r v_\theta}{r} + v_z \frac{\partial v_z}{\partial \tau} \right)$ $= -\frac{\partial p}{\partial z} + \mu \left\{ \frac{1}{r} \frac{\partial}{\partial r} \left(r \frac{\partial v_z}{\partial r} \right) + \frac{1}{r^2} \frac{\partial^2 y_z}{\partial \theta^2} + \frac{\partial^2 y_z}{\partial z^2} \right\} + \rho g_z$ $0 = -\frac{1}{\rho} \frac{\partial p}{\partial z} + g_z = -\frac{1}{\rho} \frac{\partial p}{\partial h} - g$



(15.2b)

(15.2c)

Integrate
$$\theta$$
 -Eq. 15.2 b) w.r.t. r

$$0 = \frac{\partial}{\partial r} \left[\frac{1}{r} \frac{\partial}{\partial r} (r v_{\theta}) \right]$$

$$C_{1} = \frac{1}{r} \frac{\partial}{\partial r} (rv_{\theta})$$
$$rC_{1} = \frac{\partial}{\partial r} (rv_{\theta})$$

Integrate again

$$\frac{r^2}{2}C_1 + C_2 = rv_\theta \qquad (A)$$

$$v_\theta = \frac{C_1}{2}r + \frac{C_2}{r} \qquad (B)$$
need 2 BCs (15.3)





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15.1 Vortex Motion

$$\frac{\partial p}{\partial h} = -\rho g = -\gamma$$

$$p = -\gamma h$$
(15.4)
(15.5)

\rightarrow <u>hydrostatic pressure</u> distribution





15.1.2 Forced Vortex - rotational flow

Consider cylindrical container of radius R is rotated at a <u>constant angular</u> <u>velocity</u> Ω about a vertical axis Substitute BCs into Eq. (15.3)

i)
$$r = 0$$
, $v_{\theta} = 0$
 $\rightarrow (A): 0 + C_2 = 0$ $\therefore C_2 = 0$

ii)
$$r = R$$
, $v_{\theta} = R\Omega$
 $\rightarrow (B) : R\Omega = \frac{C_1}{2}R$ $\therefore C_1 = 2\Omega$









Eq. (B) becomes

$$v_{\theta} = \frac{2\Omega}{2}r = \Omega r$$
 \rightarrow solid-body rotation (15.6)



$$r - Eq.: \frac{\Omega^2 r^2}{r} = \frac{1}{\rho} \frac{\partial p}{\partial r}$$
$$\rightarrow \qquad \frac{\partial p}{\partial r} = \rho \Omega^2 r$$

(15.7)

(15.4)



$$z - Eq.: \frac{\partial p}{\partial h} = -\gamma$$



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15.1 Vortex Motion

Consider total derivative dp

$$dp = \frac{\partial p}{\partial r}dr + \frac{\partial p}{\partial h}dh = \rho \Omega^2 r dr - \gamma dh$$

Integrate once

$$p = \rho \Omega^2 \frac{r^2}{2} - \gamma h + C_3$$

Incorporate B.C. to decide C_3

$$r=0; \hspace{0.2cm} h=h_{_{0}} \hspace{0.2cm} ext{and} \hspace{0.2cm} p=p_{_{0}}$$

$$p_0 = 0 - \gamma h_0 + C_3$$
 : $C_3 = p_0 + \gamma h_0$













- Rotation components in cylindrical coordinates
- Eq. (10.15):

$$\omega_{z} = \frac{1}{2} \left(-\frac{1}{r} \frac{\partial v_{r}}{\partial \theta} + \frac{v_{\theta}}{r} + \frac{\partial v_{\theta}}{\partial r} \right)$$
$$= \frac{1}{2} \left(\frac{r\Omega}{r} + \frac{\partial}{\partial r} (r\Omega) \right) = \frac{1}{2} (\Omega + \Omega) = \Omega$$

vorticity
$$= 2\omega_z = 2\Omega \neq 0$$

\rightarrow rotational flow

 \rightarrow Forced vortex is generated by the transmission of tangential <u>shear stresses</u>.





15.1.3 Irrotational or free vortex

Free vortex: drain hole vortex, tornado, hurricane, morning glory spillway









For irrotational flow,

 $\frac{p}{\gamma} + h + \frac{{v_{\theta}}^2}{2g} =$ Constant throughout the fluid field z coincides with h $\left(\frac{\partial h}{\partial r} = \frac{\partial h}{\partial \theta} = 0, \frac{\partial h}{\partial z} = 1\right)$ Differentiate w.r.t r $\frac{1}{\gamma}\frac{\partial p}{\partial r} + \frac{\partial h}{\partial r} + \frac{1}{g}v_{\theta}\frac{\partial v_{\theta}}{\partial r} = 0$ $p = p_{\text{atm}}$ (1)(2) $\therefore \quad \frac{\partial p}{\partial r} = -\rho v_{\theta} \frac{\partial v_{\theta}}{\partial r}$ (A)





(B)

15.1 Vortex Motion

Eq (15.2a): *r*-Eq. of N-S Eq.

$$\frac{\partial p}{\partial r} = \rho \frac{{v_{\theta}}^2}{r}$$

Equate (A) and (B)

$$-\rho v_{\theta} \frac{\partial v_{\theta}}{\partial r} = \rho \frac{{v_{\theta}}^2}{r} \quad \rightarrow \quad -\frac{\partial v_{\theta}}{\partial r}r = v_{\theta} \tag{C}$$

Integrate using separation of variables

$$\int \frac{1}{v_{\theta}} \partial v_{\theta} = \int -\frac{1}{r} \partial r$$





$$\ln v_{\theta} = -\ln r + C$$

$$\ln v_{\theta} + \ln r = \ln \left(v_{\theta} r \right) = C$$

 $v_{\theta}r = C_4 \sim \text{constant}$ angular momentum

$$v_{\theta} = \frac{C_4}{r} \tag{15.10}$$

[Cf] Forced vortex

$$v_{\theta} = \Omega r \tag{15.6}$$

$$B$$



(D)





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15.1 Vortex Motion

Radial pressure gradient





Total derivative



$$dp = \frac{\partial p}{\partial r}dr + \frac{\partial p}{\partial h}dh = \rho \frac{C_4^2}{r^3}dr - \gamma dh$$





Integrate once

$$p = -\rho \frac{C_4^2}{2r^2} - \gamma h + C_5$$
 (E)

B.C.:
$$r = \infty$$
: $h = h_0$ and $p = p_0$

Substitute B.C. into Eq. (E)

$$p_{0} = -\gamma h_{0} + C_{5} \qquad C_{5} = p_{0} + \gamma h_{0}$$

$$p - p_{0} = \gamma (h_{0} - h) - \rho \frac{C_{4}^{2}}{2r^{2}} \qquad (15.11)$$

[Cf] Forced vortex:
$$p - p_0 = \frac{\rho}{2}\Omega^2 r^2 + \gamma (h_0 - h)$$
 (15.8)







• Locus of free surface is given when $p = p_0$

$$h = h_0 - \frac{C_4^2}{2gr^2} \rightarrow \text{hyperboloid of revolution}$$

[Cf] Forced vortex:
$$h = h_0 + \frac{\Omega^2}{2g}r^2$$
 (15.9)

• Circulation

$$ds = rd\theta$$

$$\Gamma = \oint \vec{q} \cdot d\vec{s} = \int_{0}^{2\pi} \underline{v_{\theta}} rd\theta = \left[C_{4}\theta\right]_{0}^{2\pi} = 2\pi C_{4} \neq 0$$

$$v_{\theta}r = C_{4}$$



(15.12)





 \rightarrow Even though flow is irrotational, circulation for a contour enclosing the <u>origin</u> is not zero because of the <u>singularity point</u>.

Vorticity component *w*_z

$$\omega_{z} = -\frac{1}{r} \frac{\partial v_{r}}{\partial \theta} + \frac{v_{\theta}}{r} + \frac{\partial v_{\theta}}{\partial r}$$

Substitute $v_{\theta} = \frac{C_{4}}{r}$

$$\omega_z = \frac{C_4}{r^2} + \frac{\partial}{\partial r} \left(\frac{C_4}{r} \right) = \frac{C_4}{r^2} - \frac{C_4}{r^2} = 0 \qquad \rightarrow \underline{\text{Irrotational motion}}$$





At *r* = 0 of <u>drain hole vortex</u>, <u>either fluid does not occupy the space or fluid</u>

is rotational (forced vortex) when drain in the tank bottom is suddenly closed.

- \rightarrow Rankine combined vortex
- \rightarrow Fluid motion is ultimately <u>dissipated through viscous action</u>.







• Stream function, ψ

$$v_{\theta} = \frac{\partial \psi}{\partial r} = \frac{C_4}{r} = \frac{\Gamma}{2\pi r} \qquad C_4 = \frac{\Gamma}{2\pi}$$

$$\psi = \frac{\Gamma}{2\pi} \int \frac{dr}{r} = \frac{\Gamma}{2\pi} \ln r = K \ln r$$

where Γ = vortex strength





















Homework Assignment # 5

Due: 2 weeks from today

1. (6-4) Consider an incompressible two-dimensional flow of a viscous fluid in the xy-plane in which the body force is due to gravity. (a) Prove that the divergence of the vorticity vector is zero. (This expresses the conservation of vorticity, $\nabla \cdot \vec{\zeta} = 0.$ (b) Show that the <u>Navier-Stokes equation</u> for this flow can be written in terms of the vorticity as $\frac{d\bar{\zeta}}{dt} = v \nabla^2 \bar{\zeta}$. (This is a "diffusion" equation and indicates that vorticity is diffused into a fluid at a rate which depends on the magnitude of the kinematic viscosity.) Note that $d\vec{\zeta}/d_{t}$ is the substantial derivative.

$$\vec{\zeta} = \nabla \times \vec{q} = \vec{i}\,\xi + \vec{j}\eta + \vec{k}\,\zeta \qquad \xi = \frac{\partial w}{\partial y} - \frac{\partial v}{\partial z} \qquad \eta = \frac{\partial u}{\partial z} - \frac{\partial w}{\partial x}$$



2. (6-5) Consider a steady, incompressible laminar flow between parallel plates as shown in Fig. 6-4 for the following conditions: a = 0.03 m, U = 0.3 m/sec, $\mu = 0.476 \text{ N} \cdot \text{sec/m}^2$, $\partial p / \partial x = 625 \text{ N/m}^3$ (pressure increases in + *x*-direction). (a) Plot the velocity distribution, u(z), in the *z*-direction. Use Eq. (6.24) (b) In which direction is the net fluid motion? (c) Plot the distribution of shear stress τ_{zx} in the *z*-direction.







3. (6-7) An incompressible liquid of density ρ and viscosity μ flows in a thin film down glass plate inclined at an angle α to the horizontal. The thickness, a, of the liquid film normal to the plate is constant, the velocity is everywhere parallel to the plate, and the flow is steady. Neglect viscous shear between the air and the moving liquid at the free surface. Determine the variation in longitudinal velocity in the direction normal to the plate, the shear stress at the plate, and the <u>average velocity</u> of flow.





Problems

4. (6-11) Consider steady *laminar flow* in the horizontal axial direction through the <u>annular space between two concentric circular tubes</u>. The radii of the inner and outer tube are r_1 and r_2 , respectively. Derive the expression for the velocity distribution in the direction as a function of viscosity, pressure gradient $\partial p / \partial x$, and tube dimensions.







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Problems

5. (6-15) The <u>velocity potential</u> for a steady incompressible flow is given by $\Phi = (-a/2)(x^2 + 2y - z^2)$, where *a* is an arbitrary constant greater than zero. (a) Find the equation for the velocity vector $\vec{q} = \vec{i}u + \vec{j}v + \vec{k}w$ (b) Find the equation for the streamlines in the *xz*(*y* = 0) plane.

(c) Prove that the continuity equation is satisfied.

6. (6-21) The velocity variation across the radius of a <u>rectangular bend</u> (Fig. 6-22) may be approximated by a <u>free vortex</u> distribution $v_{\theta} r = const$. Derive an expression for the <u>pressure difference between the inside and</u> <u>outside of the bend</u> as a function of the discharge *Q*, the fluid density ρ , and the geometric parameters *R* and *b*, assuming frictionless flow.





Problems





