

< Chemical Kinetics III >

* Reaction Mechanism.

The sequence of elementary chemical reactions that occur as a fuel is oxidized is termed the reaction mechanism.

H₂ combustion → tens of oxns
Hydrocarbon → hundreds of oxns.

* Chain Reactions

① Initiation (The chain is initiated by the production of highly reactive intermediate from stable molecular reactants.

The intermediates are free radical species, e.g. H, O, OH. The radicals react with stable molecules.

② Branching - to produce more radicals

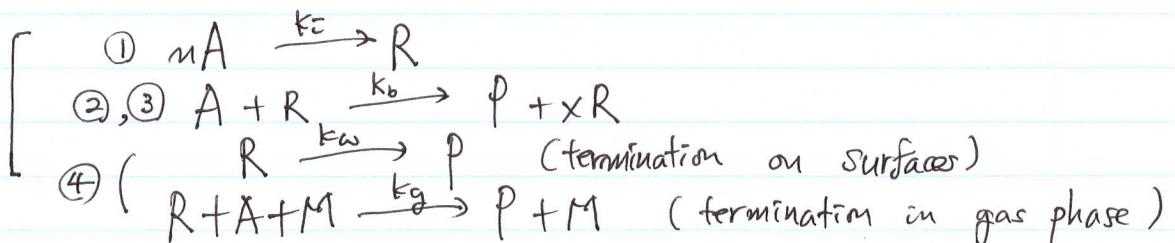
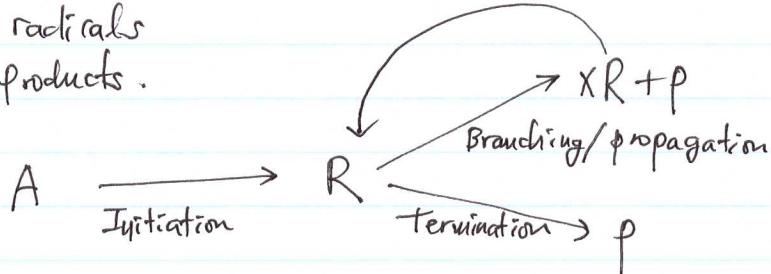
③ Propagation - to generate new radicals of same number.

④ Termination - to eliminate radicals.

A: reactants

R: radicals

f: products.



$$\frac{d[R]}{dt} = k_c [A]^m + (x-1) k_b [R][CA] - k_g [R][A][M] - k_w [R]$$

$$r_p = k_p [A]^m$$

$$k_1 = k_b[A]$$

$$K_2 \equiv K_g [A] [M] + k_\omega$$

$$\therefore \frac{d[R]}{dt} = r_0 + (a-1)K_1[R] - K_2[R]$$

$$\frac{d[R]}{dt} = r_0 - \underbrace{(k_1 + k_2)[R]}_{\equiv k_{\text{total}}} \left(1 - \frac{\alpha k_1}{k_1 + k_2}\right)$$

$$\boxed{\therefore \frac{d[R]}{dt} = r_0 - k_{\text{total}}[R] (1 - \alpha \chi)} \\ \alpha \equiv \frac{k_1}{k_{\text{total}}}$$

$$\frac{d[RP]}{dt} = k_{\text{total}}[R]$$

- Case 1 : $\alpha \chi = 0$

$\alpha > 0 \therefore \chi = 0 \Rightarrow$ no R (radical) production.

$$\frac{d[R]}{dt} = r_0 - k_{\text{total}}[R]$$

\uparrow fast removal of radicals
 \uparrow initiation rxn is very slow.

$$\therefore \frac{d[R]}{dt} \approx 0 = r_0 - k_{\text{total}}[R]$$

$$\Rightarrow \frac{d[RP]}{dt} = r_0 \Leftarrow \text{very slow rxn.}$$

Non-explosive

- Case 2 : $0 < \alpha \chi < 1$

Assumption. k_{total} & r_0 = constant.

\hookrightarrow no depletion of reactants & $T = \text{constant}$.

$$R = R(t)$$

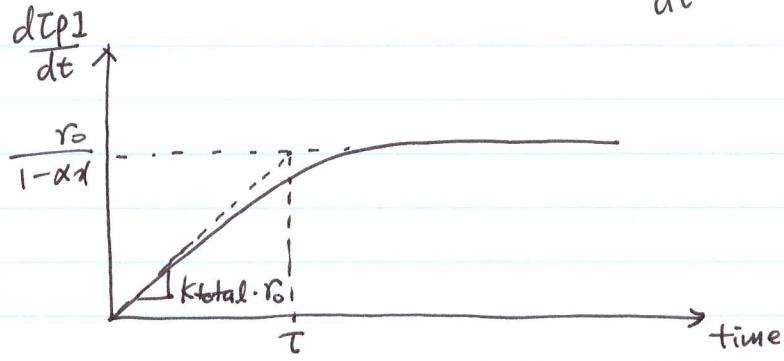
then, $\frac{d[R]}{dt} = r_0 - k_{\text{total}}[R](1 - \alpha \chi)$ is a first-order O.D.B.

$$\Rightarrow [R] = \left(\frac{r_0}{k_{\text{total}}(1 - \alpha \chi)}\right) (1 - \exp(-k_{\text{total}}(1 - \alpha \chi)t))$$

$$\text{characteristic time } \tau \equiv \frac{1}{k_{\text{total}}(1 - \alpha \chi)}$$

$$\therefore [R] = r_0 \tau (1 - e^{-\frac{t}{\tau}})$$

for $t \ll \tau$, $[R] = r_0 t$
 $t \gg \tau$, $[R] = r_0 \tau \Rightarrow \frac{d[R]}{dt} = \frac{r_0}{1-\alpha\alpha} = \text{constant.} > r_0$



- Case 3 : $\alpha x > 1$.
 $\alpha > 1$, $x > 1$

ODE soln : $[R] = - \left\{ \frac{r_0}{k_{\text{total}}(1-\alpha x)} \right\} (\exp(k_{\text{total}}(\alpha x - 1)t) - 1)$

$$\tau' = \frac{1}{k_{\text{total}}(\alpha x - 1)}$$



$$t \ll \tau', [R] = r_0 t$$

$$\frac{d[R]}{dt} = k_{\text{total}} r_0 t$$

$$t \gg \tau', [R] = r_0 \tau' \exp(t/\tau')$$

$$\frac{d[R]}{dt} = - \left[\frac{r_0}{1-\alpha x} \right] \exp(t/\tau') \Rightarrow \text{exponentially increasing}$$

* $\alpha x = 1$ is the boundary between fast ($\alpha x > 1$) and slow ($\alpha x < 1$) reactions

at this limit $k_1(x-1) = k_2$

$$\text{recall } \alpha = \frac{k_1}{k_1 + k_2}, \alpha_{x=1} = \frac{xk_1}{k_1 + k_2}$$

~~$(x-1)k_b[A] = k_g[A][M] + k_w \leftarrow \text{independent of initiation rxn.}$~~

$\Rightarrow R \text{ production} = R \text{ removal} \Rightarrow \frac{d[R]}{dt} = 0$

$$\therefore [R]_{\text{gss}} = \frac{k_g[A][M]^m}{(1-x)k_b[A] + k_g[A][M] + k_w}$$

Explosive behavior can be expressed by $[R]_{\text{gss}} \rightarrow \infty$

$\Rightarrow \text{denominator} = 0$.

$$\therefore x = 1 + \frac{[A][M] + k_w/k_g}{k_b[A]/k_g} = f$$

• if $x < f \Rightarrow \text{slow rxn with steady } [R]$

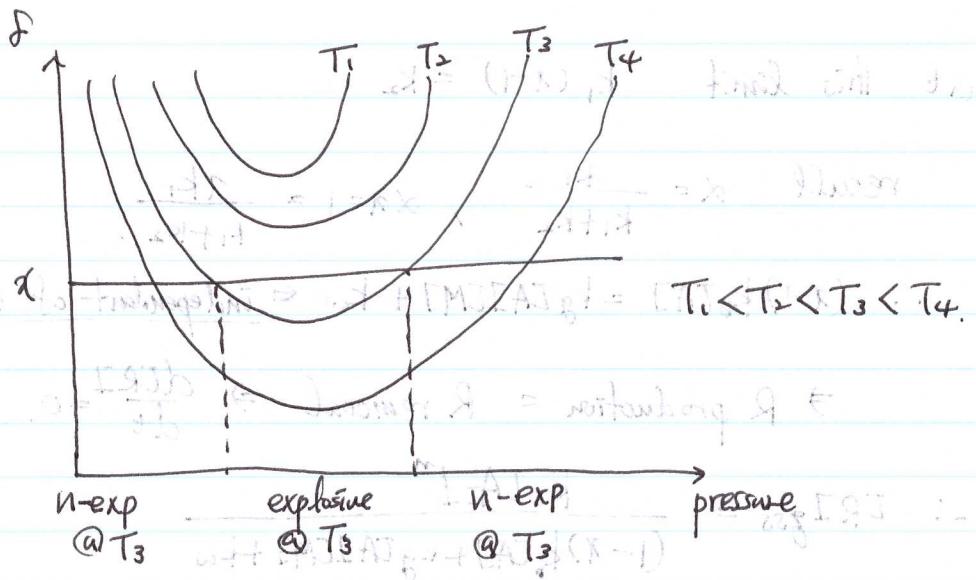
* $[M] \& [A]$ are proportional to pressure

$\Rightarrow P \rightarrow \infty \Rightarrow f \rightarrow \infty \therefore x \text{ is always less than } f.$
 $\Rightarrow \text{non-explosive}$

* when $P \rightarrow \infty \Rightarrow f \rightarrow \infty \therefore x \text{ is always less than } f.$
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• k_b/k_g increases rapidly with increasing temperature,
while k_w/k_g is a weak function of temperature
 $\therefore T \uparrow \Rightarrow f \text{ decreases.}$

* Cross-over temperature : branching and termination rates are equal.



at P_3 ρ_3 \rightarrow homogeneous and no potential energy

\rightarrow detonation \leftarrow

$$P_3 = \frac{P_{\text{init}} + P_{\text{ext}}}{2} + \frac{1}{2} = P_{\text{det}}$$

LSI model this way $\rightarrow b > s$ \rightarrow

min. of detonation \rightarrow LSI & EMJ
front end width \rightarrow $b - s$ \rightarrow $s < b$ \rightarrow
 \rightarrow explosive front \rightarrow
front end width \rightarrow $b - s$ \rightarrow $b > s$ \rightarrow detonation front

explosive front \rightarrow front end width \rightarrow
front end width \rightarrow front end width \rightarrow
detonation front \rightarrow detonation front

so when detonation front pulled in front end width \rightarrow
detonation front