

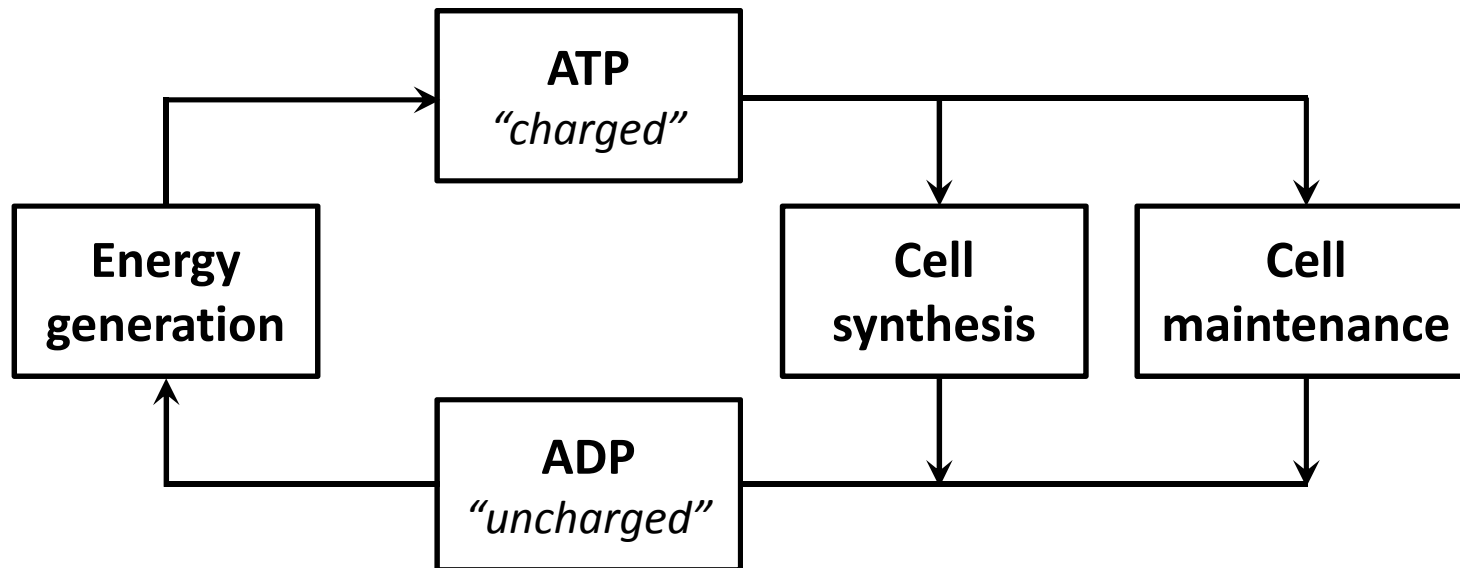
Bacterial energetics

Today's lecture

- Bacterial energetics – overview
- Gibbs free energy of reaction
- Correlating reaction energetics and yield coefficient

Bacterial energetics

- Microorganisms carry out redox reactions to obtain energy for growth and cell maintenance



Energetics and growth: thoughts

- Bacterial cells grow more rapidly when:
 - More energy is obtained by oxidation of (an e^- equivalent of) an e^- donor
 - More energy is obtained by reduction of (an e^- equivalent of) an e^- acceptor
 - Conditions are favorable...
 - for rapid utilization of substrates
 - abundance of e^- donor, e^- acceptor, nutrients, etc.
 - low concentration of inhibiting compounds

Energetics and growth: math

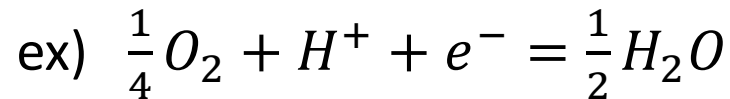
$$Y_n = Y - b \frac{X_a}{-dS/dt}$$

- $Y_n \uparrow$ when $Y \uparrow$: favorable e⁻ donor and acceptor
- $Y_n \uparrow$ when $X_a \ll -dS/dt$: favorable conditions for substrate utilization

** We will discuss about the $-dS/dt$ term in forthcoming lectures!*

Gibbs free energy: standard conditions

- “Standard” free energy
 - ΔG^0 , free energy at 25°C, 1 atm, and unit activity for any chemicals involved
 - $\Delta G^{0'}$, standard free energy adjusted to pH=7



ΔG^0 is for

$$\begin{aligned}\{O_2\} &= P_{O_2} = 1 \text{ atm} \\ \{H^+\} &= 1 \text{ (pH = 0)} \\ \{H_2O\} &= 1\end{aligned}$$

$\Delta G^{0'}$ is for

$$\begin{aligned}\{O_2\} &= P_{O_2} = 1 \text{ atm} \\ \text{pH=7 } (\{H^+\}) &= 10^{-7} \\ \{H_2O\} &= 1\end{aligned}$$

$\{H_2O\} = 1$ applies to any dilute aqueous solutions

Free energy of formation, ΔG_f

- Gibbs free energy that accompanies the formation of 1 mole of the substance from its component elements

Gibbs free energy change of reaction

- Free energy change of reaction, ΔG_r
 $\Sigma(\text{product } \Delta G_f) - \Sigma(\text{reactant } \Delta G_f)$

For a generic reaction written as

$$0 = \sum_{i=1}^n v_{ir} A_i$$

v_{ir} = stoichiometric coefficient, (-) for reactants, (+) for products

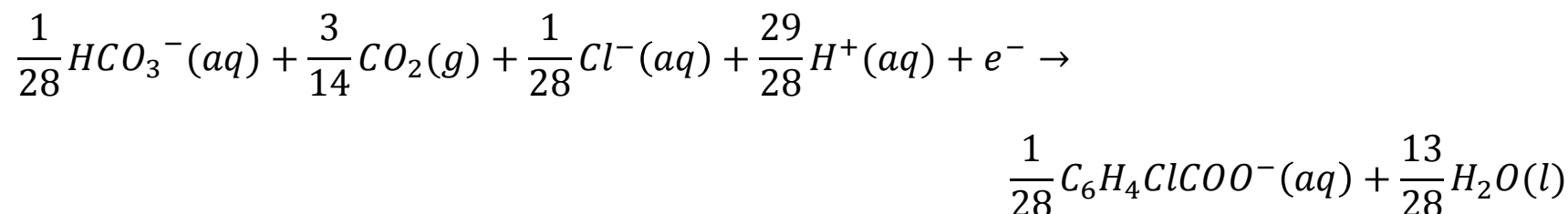
A_i = reaction constituent, reactants or products

ΔG_r can be written as

$$\Delta G_r = \sum_{i=1}^n v_{ir} \Delta G_f$$

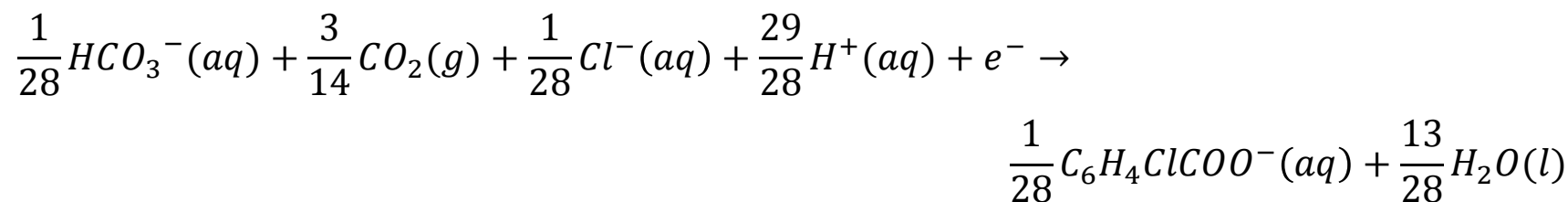
Reaction free energy

Q1: Calculate the standard free energy adjusted pH 7 for the half reaction of 2-chlorobenzoate formation as given below.



Use the following values of free energy of formation (in textbook Appendix A):

Species	$\text{HCO}_3^- (\text{aq})$	$\text{CO}_2 (\text{g})$	$\text{Cl}^- (\text{aq})$	$\text{H}^+ (\text{aq}, 10^{-7})$	$\text{C}_6\text{H}_4\text{ClCOO}^- (\text{aq})$	$\text{H}_2\text{O} (\text{l})$
$\Delta G_f^{0'} @ 25^\circ\text{C}$ (kJ/mole)	-586.85	-394.36	-31.35	-39.87	-237.9	-237.18



Species	HCO ₃ ⁻ (aq)	CO ₂ (g)	Cl ⁻ (aq)	H ⁺ (aq, 10 ⁻⁷)	C ₆ H ₄ ClCOO ⁻ (aq)	H ₂ O(l)
ΔG _f ^{0'} @ 25°C (kJ/mole)	-586.85	-394.36	-31.35	-39.87	-237.9	-237.18

$$\Delta G_r = \sum_{i=1}^n v_{ir} \Delta G_f$$

v_{ir} = stoichiometric coefficient, (-) for reactants, (+) for products

$$\Delta G_r^{0'} = (-) \left\{ \frac{1}{28} \times (-586.85) + \frac{3}{14} \times (-394.36) + \frac{1}{28} \times (-31.35) + \frac{29}{28} \times (-39.87) \right\} + \left\{ \frac{1}{28} \times (-237.9) + \frac{13}{28} \times (-237.18) \right\}$$

$$= 29.26 \text{ kJ/e}^- \text{ eq}$$

Reaction free energy

Q2: Calculate the standard free energy adjusted pH 7 for overall energy reaction with ethanol as an e^- donor and oxygen as an e^- acceptor. Use the half reactions listed in Table 2.2 and 2.3.

$$R_d: \text{O-5} \quad \Delta G_r^{0'} = 31.18 \text{ kJ}/e^- \text{ eq}$$

$$R_a: \text{I-14} \quad \Delta G_r^{0'} = -78.72 \text{ kJ}/e^- \text{ eq}$$

$$R_e = R_a - R_d \quad \Delta G_r^{0'}(R_e) = \Delta G_r^{0'}(R_a) - \Delta G_r^{0'}(R_d)$$

$$R_a: \quad \frac{1}{4}O_2 + H^+ + e^- = \frac{1}{2}H_2O \quad = -78.72 - 31.18$$

$$-R_d: \quad \frac{1}{12}C_2H_5OH + \frac{1}{4}H_2O = \frac{1}{6}CO_2 + H^+ + e^- \quad = -109.90 \text{ kJ}/e^- \text{ eq}$$

$$R_e: \quad \frac{1}{12}C_2H_5OH + \frac{1}{4}O_2 = \frac{1}{6}CO_2 + \frac{1}{4}H_2O$$

Reaction free energy: general conditions

- For nonstandard conditions,

$$\Delta G_r = \Delta G_r^0 + RT \sum_{i=1}^n v_{ir} \ln a_i$$

a_i = activity of constituent A_i

R = gas constant, 8.314×10^{-3} kJ/mole – K

T = absolute temperature, K

Caution:

- v_{ir} is negative for reactants and positive for products

- ΔG_r^0 is for standard conditions -- pH=0

From $\Delta G_r^{0'}$, we can calculate ΔG_r^0 by:

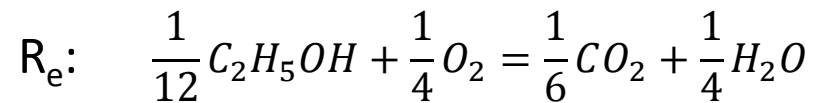
$$\Delta G_r^0 = \Delta G_r^{0'} - RT v_{H^+} \ln[10^{-7}]$$

Reaction free energy

Q3: Calculate the free energy of reaction for aerobic ethanol degradation at the following conditions: $T = 20^\circ\text{C}$, $\text{pH} = 5.0$, $[\text{C}_2\text{H}_5\text{OH}] = 2 \times 10^{-3} \text{ M}$, $P_{\text{CO}_2} = 3 \times 10^{-4} \text{ atm}$, $P_{\text{O}_2} = 0.21 \text{ atm}$.

From Q2,

$$\Delta G_r^{0'} = -109.90 \text{ kJ}/e^- \text{ eq}$$



$$\Delta G_r^0 = \Delta G_r^{0'} - RTv_H + \ln[10^{-7}] = G_r^{0'} - 0 = G_r^{0'}$$

$$\Delta G_r = \Delta G_r^0 + RT \sum_{i=1}^n v_{ir} \ln a_i$$

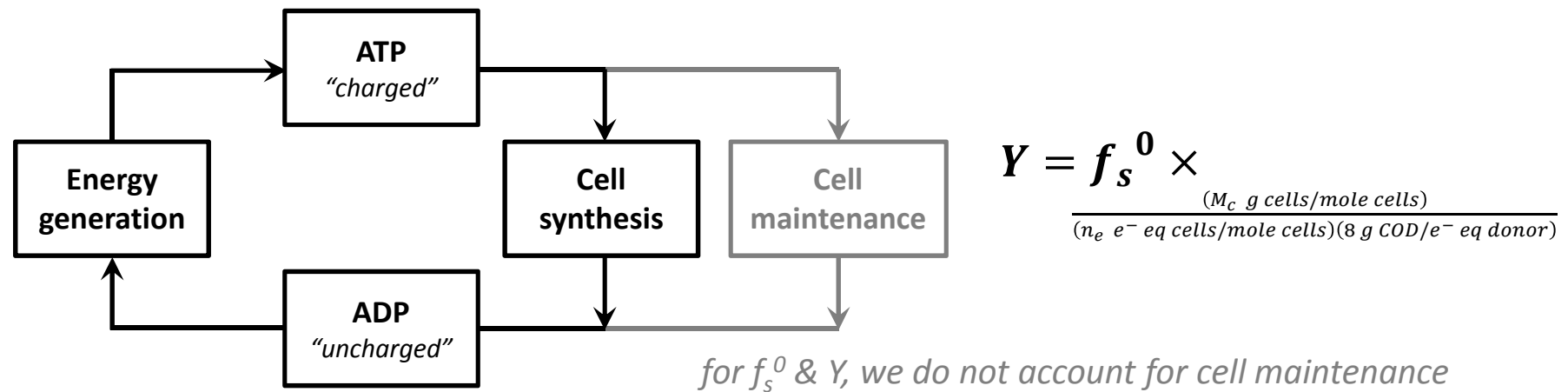
$$= -109.90 \text{ kJ}/e^- \text{ eq} + (8.314 \times 10^{-3} \text{ kJ}/\text{mole} - K) \times (293 \text{ K})$$

$$\times \left\{ -\frac{1}{12} \ln(2 \times 10^{-3}) - \frac{1}{4} \ln(0.21) + \frac{1}{6} \ln(3 \times 10^{-4}) + \frac{1}{4} \ln(1) \right\}$$

$$= -110.98 \text{ kJ}/e^- \text{ eq}$$

$a_{H_2O} = 1$ for aqueous solutions; you may omit the water term

Deriving f_s^0 or Y by thermodynamic principles



- To determine f_s^0 or Y we consider the energy balance for cell synthesis
 - energy is needed ($\text{ATP} \rightarrow \text{ADP}$) to synthesize cells [1]
 - energy reaction (R_e) supplies the required energy ($\text{ADP} \rightarrow \text{ATP}$) [2]
 - At steady state,
 - energy required for [1] = energy supplied by [2]

Two steps of cell synthesis, the efficiency

- We conceptualize the cell synthesis mechanism into two steps

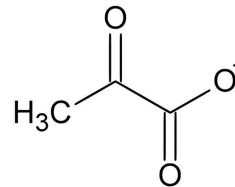
C-source

Organics (heterotrophs)
 CO_2/HCO_3^- (autotrophs)

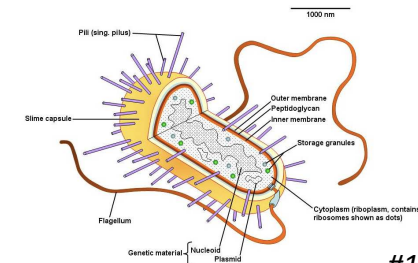


Building block

e.g., pyruvate (CH_3COCOO^-)



Cells



- 1) Carbon source is metabolized to form a building block
- 2) The building block is synthesized to a cell

- We should consider that bacteria are not 100% efficient engines -- each step involves energy loss!

ΔG_p (C-source \rightarrow pyruvate), ΔG_{pc} (pyruvate \rightarrow cells)

- Energy required to convert carbon source to pyruvate, ΔG_p (heterotrophic bacteria, ammonia as N source):

$$\Delta G_p = 35.09 - \Delta G_c^{0'}$$

(in kJ/e⁻ eq)

35.09 = reaction free energy for formation of pyruvate from CO₂

$\Delta G_c^{0'}$ = reaction free energy for formation of carbon source from CO₂

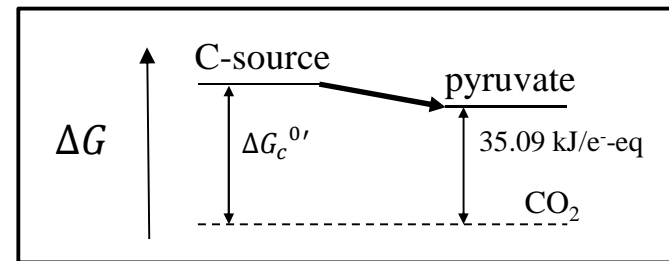
- Energy required to convert pyruvate to cells, $\Delta G_{pc} = 18.8$ kJ/e⁻ eq
(estimated value for a cell formula of C₅H₇O₂N using NH₄⁺ as a N source)

ΔG_S (C-source \rightarrow cells)

- Energy required for cell synthesis from the carbon source, ΔG_S :

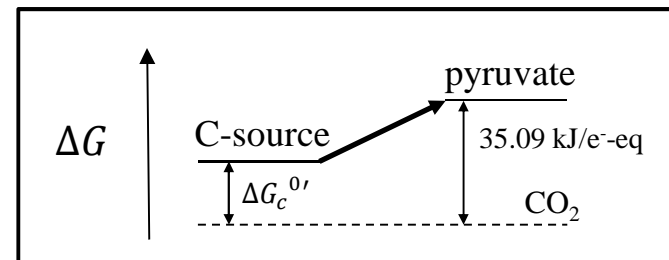
if $\Delta G_p < 0$ (C-source is at higher energy state than pyruvate)

$$\Delta G_S = \varepsilon \Delta G_p + \frac{\Delta G_{pc}}{\varepsilon}$$



if $\Delta G_p > 0$ (C-source is at lower energy state than pyruvate)

$$\Delta G_S = \frac{\Delta G_p}{\varepsilon} + \frac{\Delta G_{pc}}{\varepsilon}$$



ε = energy transfer efficiency

Energy balance of overall reaction

- The energy obtained by an energy reaction is used to synthesize cells
- Energy obtained = Energy used (at steady state)
- Keep in mind that bacteria cannot use 100% of the energy available by an energy reaction (energy transfer efficiency, ε)
- Therefore we write

$$A\varepsilon\Delta G_r + \Delta G_s = 0$$

A = e⁻ equivalent of e⁻ donor used for energy production per e⁻ equivalent of cells formed

ΔG_r = reaction free energy for energy reaction = $\Delta G_a - \Delta G_d$ (per e⁻-eq)

ΔG_s = energy required for cell synthesis from the carbon source (per e⁻-eq)

Deriving f_s^0 or Y by thermodynamic principles

- Solving for A :
$$A = -\frac{\Delta G_p / \varepsilon^n + \Delta G_{pc} / \varepsilon}{\varepsilon \Delta G_r}$$

$n = -1$ for $\Delta G_p < 0$
 $+1$ for $\Delta G_p > 0$

- From A , we can calculate f_s^0 and f_e^0 as:

$$f_s^0 = \frac{1}{1 + A} \quad f_e^0 = 1 - f_s^0 = \frac{A}{1 + A}$$

- Energy transfer efficiency, ε
 - 55-70% under optimal conditions
 - Use 0.6 for ordinary cases

Deriving f_s^0 or Y by thermodynamic principles

Q4: Estimate f_s^0 and Y for aerobic oxidation of acetate assuming $\epsilon=0.4$ and 0.6 at standard conditions except for a pH of 7.0. Ammonia is available for cell synthesis.

From O-1, $\Delta G_c^{0'} = 27.40 \text{ kJ}/e^- \text{ eq}$

$$\Delta G_p = 35.09 - 27.40 = 7.69 \text{ kJ}/e^- \text{ eq}$$

$$\Delta G_r = \Delta G_a - \Delta G_d = -78.72 - 27.40 = -106.12 \text{ kJ}/e^- \text{ eq}$$

$$\Delta G_d = 27.40 \text{ kJ}/e^- \text{ eq}, \quad \Delta G_a = -78.72 \text{ kJ}/e^- \text{ eq} \quad (\text{from I-14})$$

$$\Delta G_p > 0 \rightarrow n = +1$$

$$A = -\frac{\frac{\Delta G_p}{\epsilon^n} + \frac{\Delta G_{pc}}{\epsilon}}{\epsilon \Delta G_r} = -\frac{\frac{7.69}{\epsilon^{+1}} + \frac{18.8}{\epsilon}}{-106.12\epsilon}$$

$\epsilon = 0.4 : A = 1.56$	$f_s^0 = \frac{1}{1 + A}$	$f_s^0 = 0.39, Y = 0.28 \text{ g cells/g COD}$
$\epsilon = 0.6 : A = 0.69$	$\xrightarrow{\hspace{10em}}$	$f_s^0 = 0.59, Y = 0.42 \text{ g cells/g COD}$
$Y = f_s^0 \frac{M_c}{n_e \cdot (8 \text{ g COD}/e^- \text{ eq})}$		

References

#1) <https://cronodon.com/BioTech/Bacteria.html>