

# Anaerobic fermentation & oxidation

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- **Applications**

- Stabilization of waste sludge
- Treatment of high-strength organic wastes
- Pretreatment step for conventional biological treatment

- **Advantage**

- Low biomass yield
- Energy production in the form of methane (of recent interest!)
  - WWTP -- ~2% of total energy cost in USA
  - Target on energy positive treatment of wastewater

- **Disadvantage**

- Effluent quality usually not as good as aerobic treatment



*Before construction (Jan 15)*

Hongchun energy town, Korea  
(animal manure + food waste)

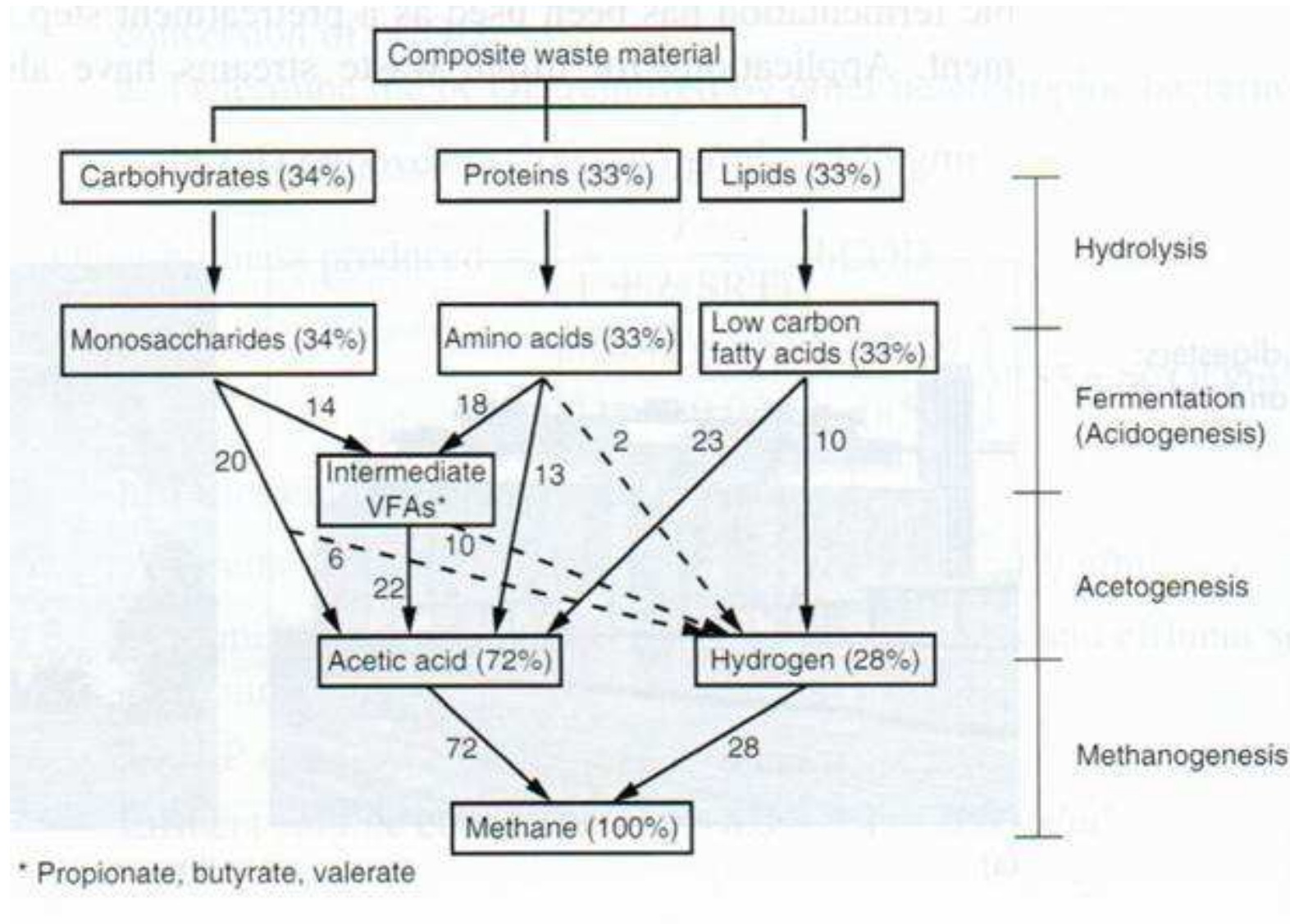
*After construction (Feb 18)*





Dear Island wastewater treatment plant, MA, USA  
(sewage sludge)

# Pathway of anaerobic conversion of wastes



# Steps of anaerobic conversion (1)

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- **Hydrolysis**

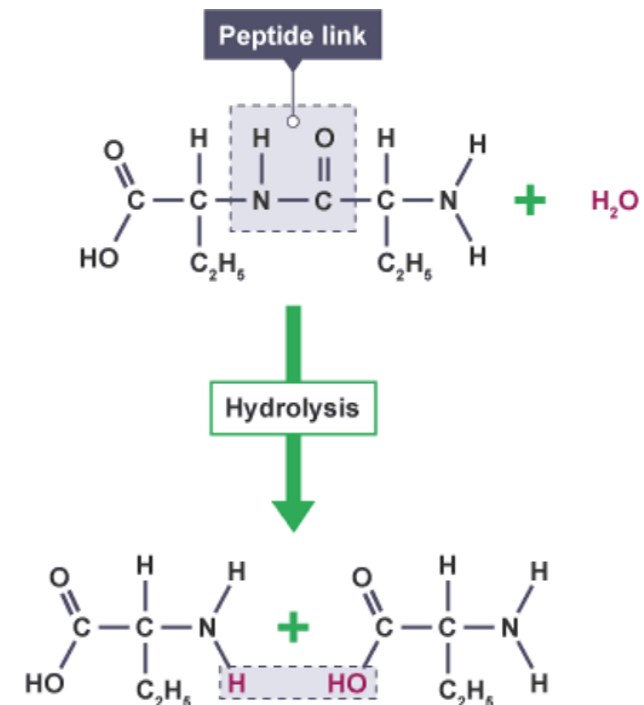
- Particulates - - - - → Soluble molecules - - - - → Monomers
- By extracellular enzymes

- **Acidogenesis (fermentation)**

- Use: sugars, amino acids, fatty acids (both e<sup>-</sup> donor & acceptor)
- Produce: VFAs, CO<sub>2</sub>, H<sub>2</sub>

- **Acetogenesis**

- Use: VFAs other than acetate
- Produce: acetate, H<sub>2</sub>, CO<sub>2</sub>



# Steps of anaerobic conversion (2)

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- **Methanogenesis**

- By methanogens (belongs to domain **Archaea**)
- Two groups of methanogens
  - *acetoclastic* methanogens: acetate  $\rightarrow$  CH<sub>4</sub> + CO<sub>2</sub>
  - *hydrogenotrophic* methanogens: H<sub>2</sub> + CO<sub>2</sub>  $\rightarrow$  CH<sub>4</sub>
- In anaerobic digestion process, ~72% methane from acetic acid & ~28% from H<sub>2</sub> ( $\rightarrow$  gas production of ~65% CH<sub>4</sub> & ~35% CO<sub>2</sub>)

# Syntrophic relationship

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- Methanogens – acidogens & acetogens
  - Acidogens & acetogens: produce H<sub>2</sub>, acetate, etc.
  - Methanogens: cleans up the acido/acetogenesis end products
    - Acetogens require relatively low H<sub>2</sub> partial pressure
- Often called as “*Interspecies hydrogen transfer*”



# COD balance for anaerobic process

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$$\text{(COD utilized)} = \text{(Biomass COD)} + \text{(Methane COD)}$$

- No  $e^-$  acceptor consumed!
- COD of methane = 64 g COD/mole  $\text{CH}_4$   
= 2.86 g COD/L  $\text{CH}_4$  (@ 0°C, 1 atm)

# COD balance for anaerobic process

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**Q:** An anaerobic reactor, operated at 35°C, is used to process a wastewater stream with a flow of 3000 m<sup>3</sup>/d and a bCOD concentration of 5000 g/m<sup>3</sup>. At 95% bCOD removal and a net biomass yield of 0.04 g VSS/g COD, what is the amount of methane produced in m<sup>3</sup>/d?

# Process kinetics

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- Low yield coefficients
  - Low energy gain by chemical transformation
  - Fermentation:  $Y \sim 0.06 \text{ g VSS/g COD}$ ;  $b \sim 0.02 \text{ d}^{-1}$
  - Methanogenesis:  $Y \sim 0.03 \text{ g VSS/g COD}$ ;  $b \sim 0.008 \text{ d}^{-1}$
- Consider two steps:
  - Hydrolysis
  - Soluble substrate utilization for fermentation and methanogenesis
    - Methanogenesis the rate-limiting step
- High SRT is needed (around 40 d) due to slow degradation rate

# Process stability

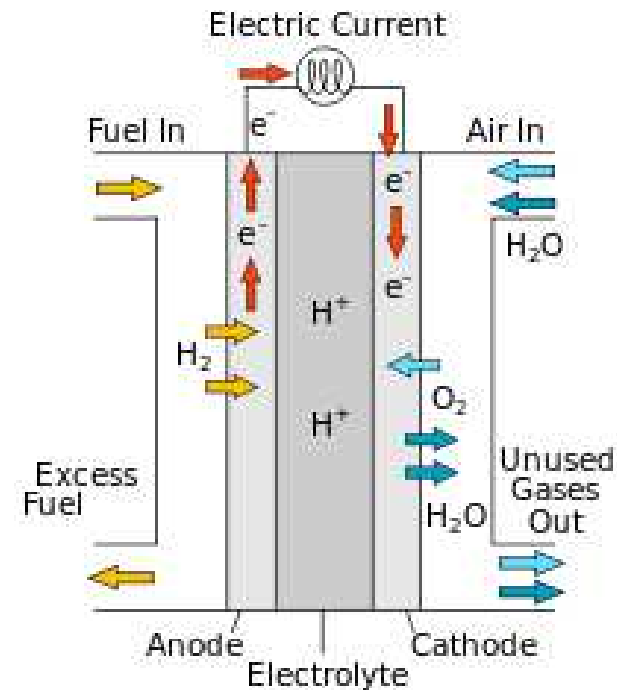
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- Kinetics of VFA production is faster than utilization (methanogenesis)
- At steady state, sufficient methanogen population is established to maintain low VFA concentration ( $<200 \text{ g/m}^3$ ) &  $\text{pH} \geq 7.0$
- Unstable digester operation may develop under transient loading conditions (VFA production  $>$  utilization): VFA accumulation & pH drop
- Low pH leads to decline in methanogenic activity: process failure
- Methanogenic inhibition can also occur by acetate accumulation (acetate conc.  $> 3000 \text{ g/m}^3$ )

# Microbial fuel cells

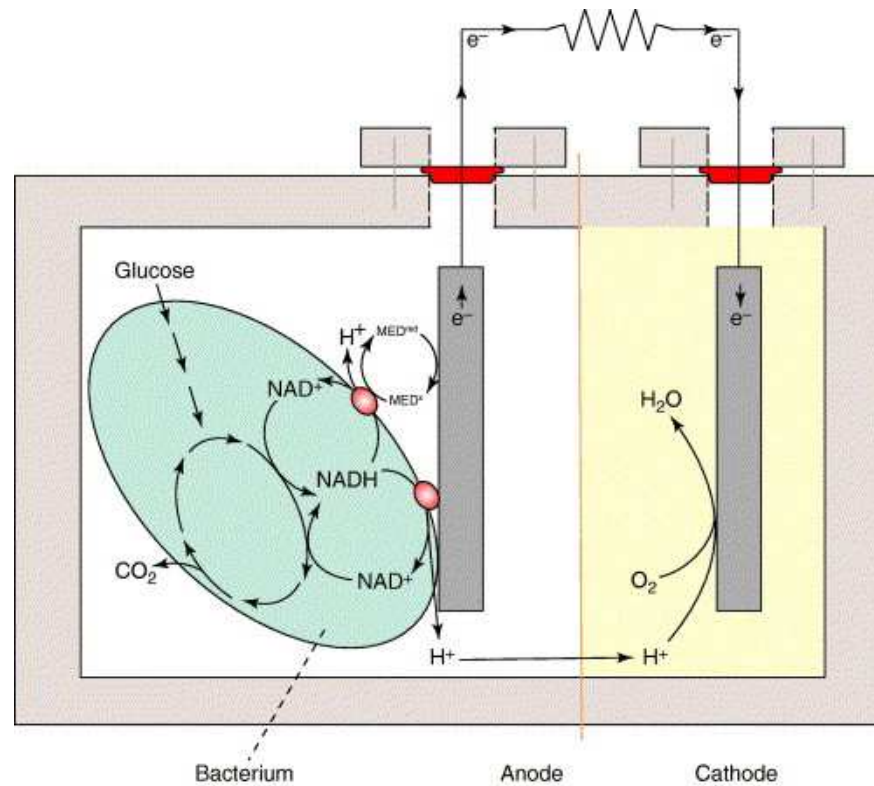
# Fuel cell

- A device that converts the chemical energy from a fuel into electricity through an electrochemical reaction of hydrogen with oxygen or another oxidizing agent
- Each half reaction of the overall redox reaction occurs separately at each electrode
  - Oxidation half reaction (Anode)  
ex)  $\frac{1}{2}H_2 \rightarrow H^+ + e^-$
  - Reduction half reaction (Cathode)  
ex)  $\frac{1}{4}O_2 + H^+ + e^- \rightarrow 2H_2O$
  - Electrons move through the electric circuit (electricity generated)
  - $H^+$  move through the electrolyte



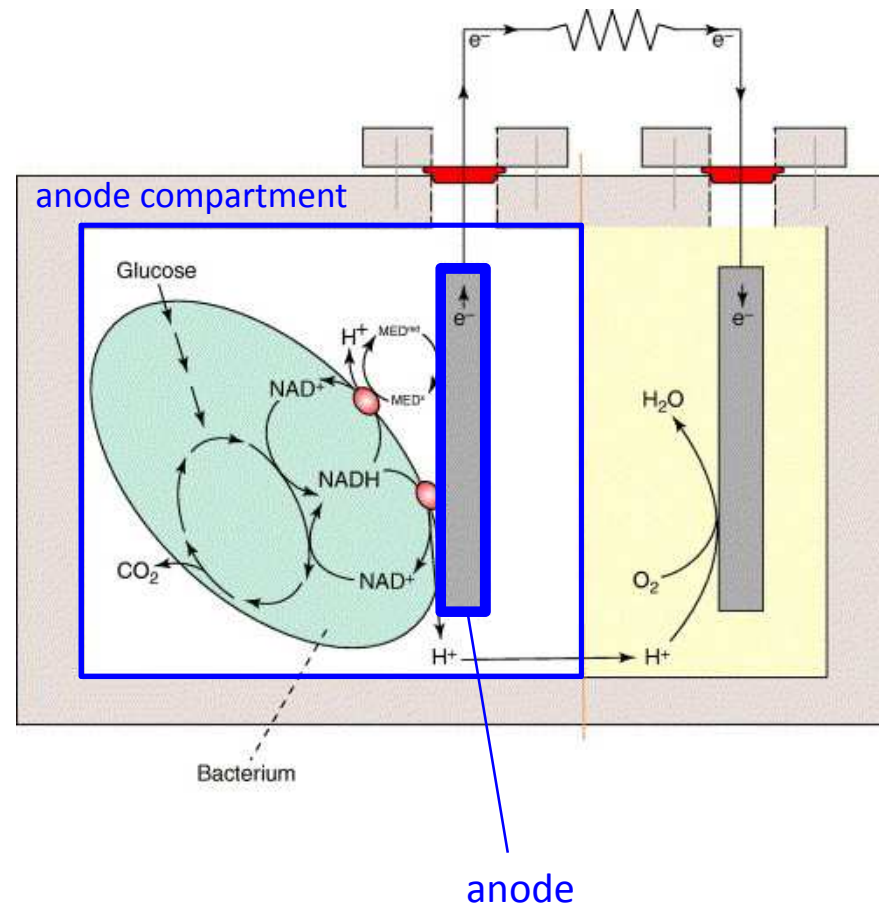
# Microbial Fuel Cell (MFC)

- A device that converts the chemical energy to electrical energy by the action of microorganisms
- The redox reaction is catalyzed by microorganisms



# MFC – Anode compartment

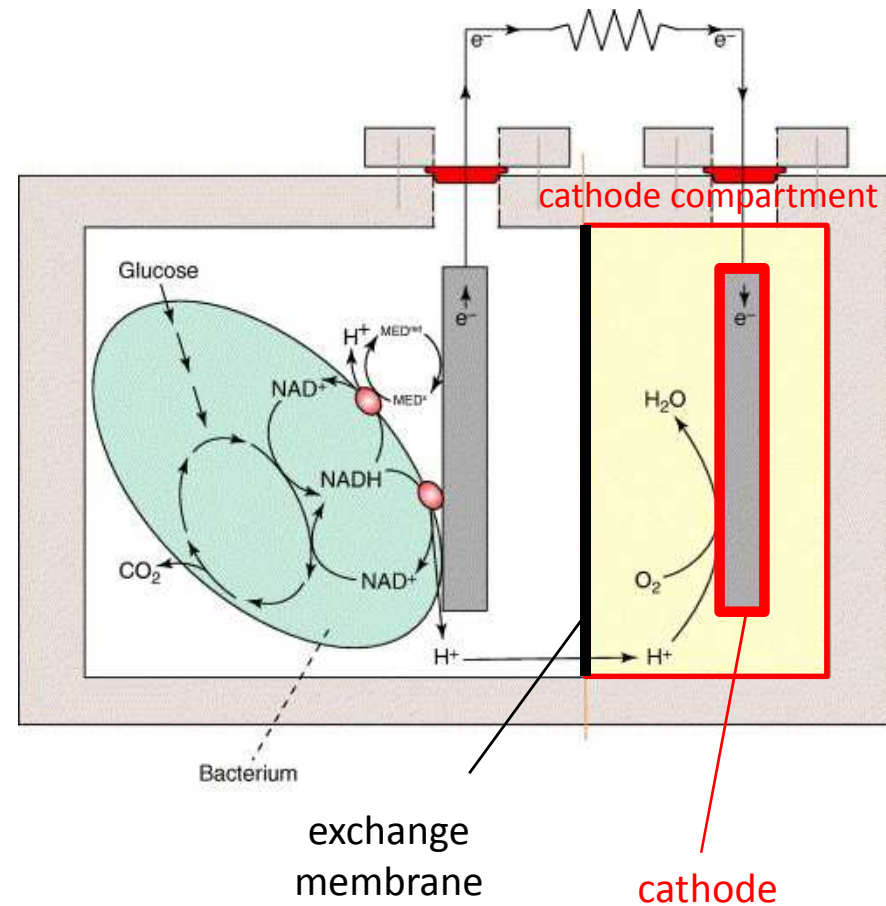
- Anode
  - Should be conductive, bio-compatible, chemically stable with substrate
  - Stainless steel mesh, graphite plates or rods
- Bacteria live in the anode compartment and oxidize the substrate provided
- Anode compartment should be kept low in DO
- Substrates: usually organics – carbohydrates, protein, VFAs, cellulose, and wastewater





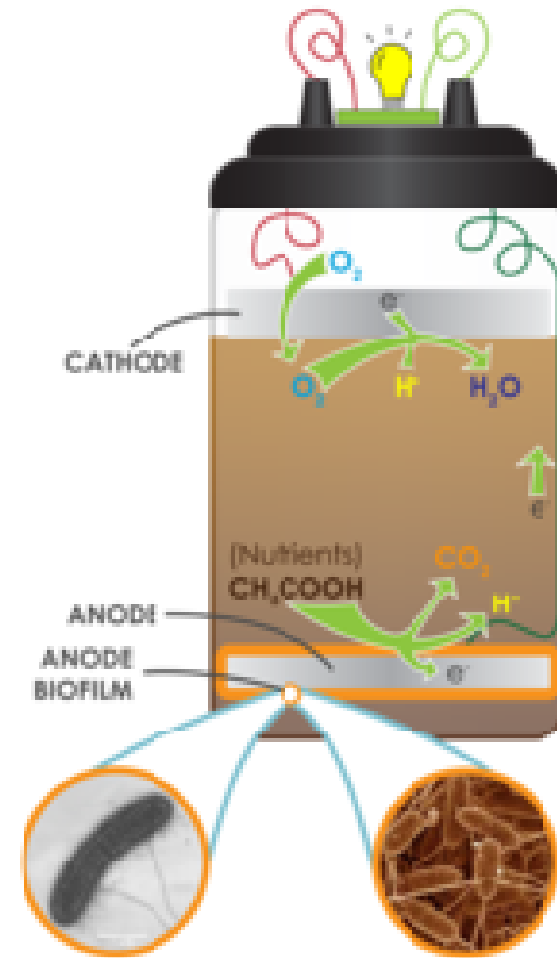
# MFC – Cathode compartment / EM

- Cathode compartment
  - Usually oxygen is used as an oxidizing agent
  - Catalysts used for the oxygen reduction reaction: Pt most common
- Exchange membrane
  - Allows proton ( $H^+$ ) to flow from the anode compartment to cathode compartment



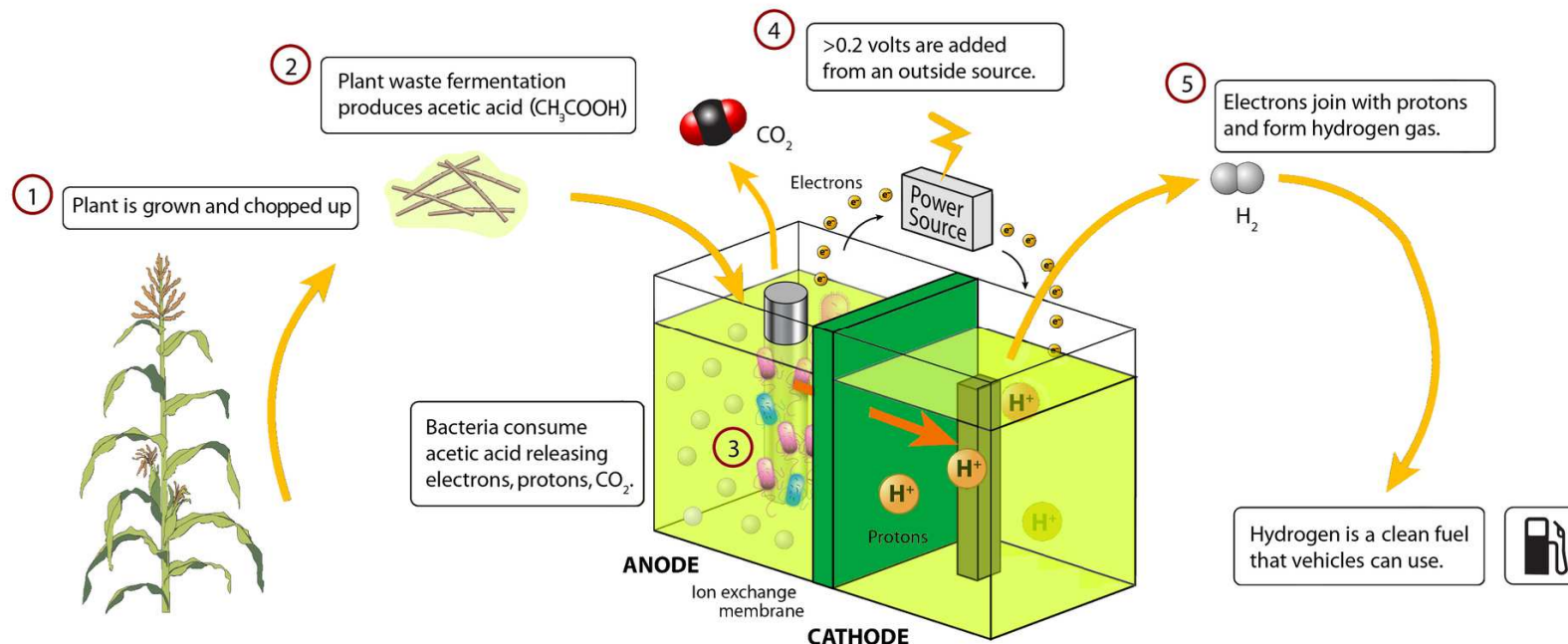
# Soil-based MFCs

- Soil serves as
  - Anode compartment
  - Proton exchange membrane
- And soil provides
  - Microorganisms
  - Nutrients



# Microbial electrolysis cell (MEC)

- Not an electricity-generating, but electricity-consuming process to produce hydrogen or methane as a fuel
- Hydrogen is produced by reducing protons at the cathode
  - The voltage required to reduce protons is provided by: substrate utilization by microorganisms at the anode + additional voltage supply from an outside source



# MFC – pros & cons

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- Advantages
  - Generation of energy out of bio-waste / organic matter
  - Direct conversion of substrate energy to electricity
  - No gas treatment required
  - Aeration may not be needed (the cathode may be passively aerated)
- Disadvantages
  - Low power density: losses of electric potential significant
  - High initial cost