Energy-efficient or energyproducing biological processes

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# **Energy-efficient/producing bioprocesses**

- Simultaneous removal of ammonia and nitrite (NO<sub>2</sub><sup>-</sup>):
  Anammox
- Anaerobic digestion
- Microbial fuel cells
- Mainstream anaerobic process: **AFBR-AFMBR**

## **Anaerobic ammonia oxidation (Anammox)**

• Anaerobic oxidation of ammonia to produce nitrogen gas

 $NH_4^+ + NO_2^- \rightarrow N_2 + H_2O$ 

 $e^{-}$  donor  $e^{-}$  acceptor

- Requires aerobic nitritation of ammonia to NO<sub>2</sub><sup>-</sup> for the process to occur (~55% conversion of NH<sub>4</sub>-N to NO<sub>2</sub>-N)
- By autotrophic bacteria

 $\rightarrow$  No organic carbon consumption during the process

### **Anammox mechanism**

 $NH_4^+ + NO_2^- \rightarrow N_2 + H_2O$ 

- Proposed metabolic model (Van de Graaf et al., 1997)
  - 1) Reduction of nitrite to hydroxylamine (NH<sub>2</sub>OH)
  - 2) Condensation of hydroxylamine with ammonium to hydrazine  $(N_2H_4)$
  - 3) Oxidation of hydrazine to nitrogen gas
- Some formation of NO<sub>3</sub>-N from NO<sub>2</sub>-N
  - To provide the reducing power to fix  $CO_2$

 $CO_2 + 2NO_2^- + H_2O \rightarrow CH_2O + 2NO_3^-$ 

• Overall reaction (Strous et al., 1999)

 $\begin{array}{l} 1.0N{H_4}^+ \ + \ 1.32N{O_2}^- \ + \ 0.066HC{O_3}^- \ + \ 0.13H^+ \\ \\ \rightarrow \ 1.02N_2 \ + \ 0.26N{O_3}^- \ + \ 0.066CH_2{O_{0.5}}N_{0.021} \ + \ 2.03H_2{O_{0.5}}N_{0.021} \ + \ 2.03H_2{O_{0.5}}N_2{O_{0.5$ 

### **Anammox process**

#### • Microorganisms for Anammox

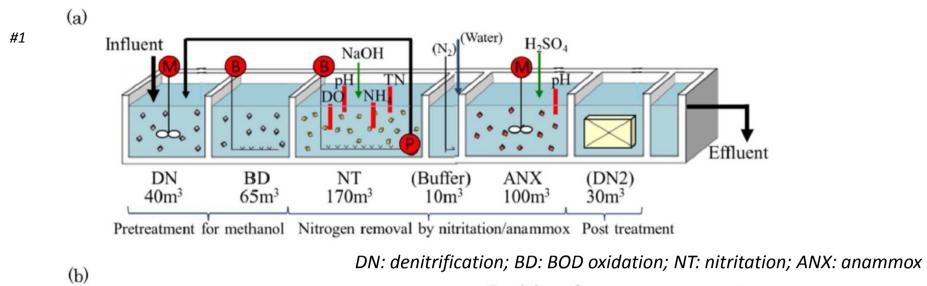
- Forms dense granular flocs
- Slowly growing (low Y value)
- High bacterial concentration (10<sup>10~</sup>10<sup>11</sup> cells/mL) should be maintained for good Anammox activity

#### Advantages

- Substantially lower aeration requirement  $\rightarrow$  low cost, low carbon footprint
- Low sludge production
- Good sludge settling properties

#### • Limitations/challenges

- Long time required for process setup/recovery after sludge loss
- Optimum pH = 8  $\rightarrow$  may need chemical input
- Difficult to achieve partial nitrification (nitritation)



Inside of anammox reactor



Fig. 1. (a) Schematic diagram and (b) photograph of full-scale anammox plant using gel carriers.

# **Anaerobic digestion**

### Applications

Treatment of waste sludge & high-strength organic wastes

#### Advantage

- Low biomass yield
- Energy production in the form of methane (of recent interest!)
  - WWTP -- ~3% of total energy cost in USA
  - Target on energy positive treatment of wastewater

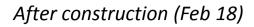
### • Disadvantage

- Effluent quality usually not as good as aerobic treatment



Before construction (Jan 15)

Hongchun energy town, Korea (animal manure + food waste)







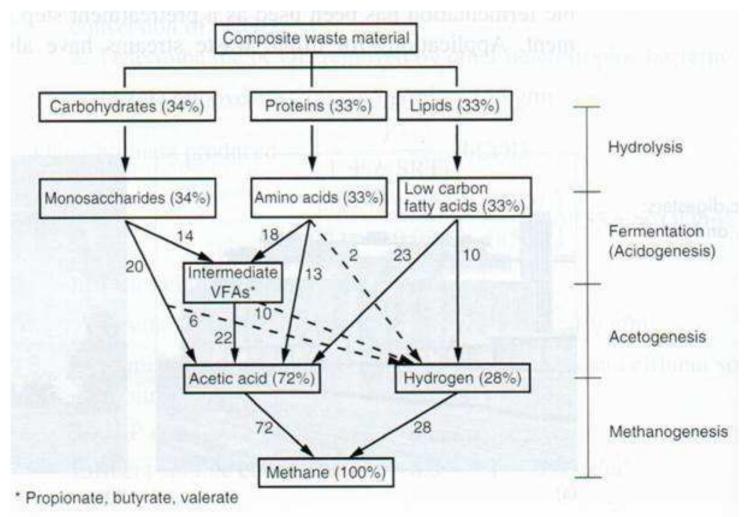
Anaerobic digestion tank

#### Biogas storage tank



Suyeong wastewater treatment plant, Busan, Korea (sewage sludge)

# **Anaerobic digestion: Key steps**



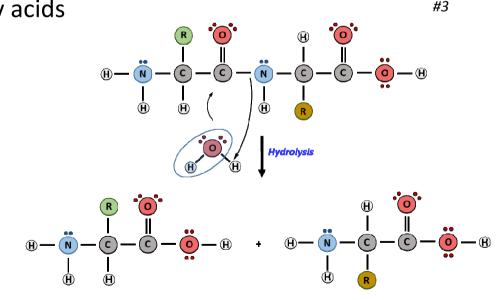
# **Anaerobic digestion: Key steps**

### • Hydrolysis

- − Particulates - - → Soluble molecules - - → Monomers
- By extracellular enzymes

### • Acidogenesis (fermentation)

- Use: sugars, amino acids, fatty acids (both e- donor & acceptor)
- Produce: VFAs, CO<sub>2</sub>, H<sub>2</sub>
- Acetogenesis
  - Use: VFAs other than acetate
  - Produce: acetate, H<sub>2</sub>, CO<sub>2</sub>



# **Anaerobic digestion: Key steps & syntrophy**

### Methanogenesis

- By methanogens (belongs to domain Archaea)
- Two groups of methanogens
  - *aceticlastic* methanogens: <u>acetate</u>  $\rightarrow$  CH<sub>4</sub> + CO<sub>2</sub>
  - hydrogenotrophic methanogens:  $\underline{H}_2 + \underline{CO}_2 \rightarrow \underline{CH}_4$
- − In anaerobic digestion process, ~72% methane from acetic acid & ~28% from H<sub>2</sub> (→ gas production of ~65% CH<sub>4</sub> & ~35% CO<sub>2</sub>)

### • Syntrophic relationship

- Methanogens acidogens & acetogens
  - Acidogens & acetogens: produce H<sub>2</sub>, acetate, etc.
  - Methanogens: cleans up the acido/acetogenesis end products
- "Interspecies hydrogen transfer"

## **Process kinetics**

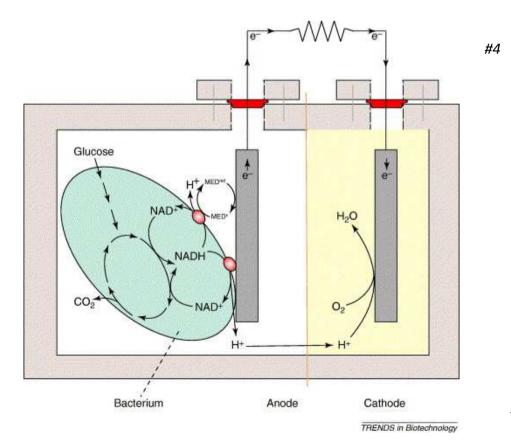
- Low yield coefficients
  - Low energy gain by chemical transformation
  - Fermentation: Y ~ 0.06 g VSS/g COD; b ~ 0.02 d<sup>-1</sup>
  - Methanogenesis: Y ~ 0.03 g VSS/g COD; b ~ 0.008 d<sup>-1</sup>
- Steps determining the rate
  - Hydrolysis or methanogenesis
  - Typically hydrolysis for biomass (e.g., microorganisms, plant matter) & methanogenesis for food waste & manure
- High SRT is needed (around 40 d) due to slow degradation rate

## **Process stability**

- Kinetics of VFA production is faster than utilization (methanogenesis)
- At steady state, sufficient methanogen population is established to maintain low VFA concentration (<200 g/m<sup>3</sup>) & pH≥7.0
- Unstable digester operation may develop under transient loading conditions (VFA production > utilization): VFA accumulation & pH drop
- Low pH leads to decline in methanogenic activity: process failure

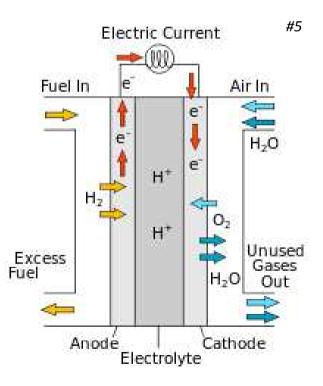
# **Microbial fuel cells (MFCs)**

- A device that converts the chemical energy to electrical energy by the action of microorganisms
- The redox reaction is catalyzed by microorganisms



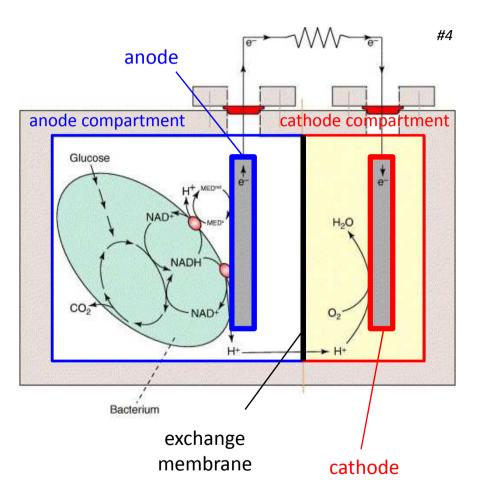
# cf) Fuel cells

- A device that converts the chemical energy from a fuel into electricity through an electrochemical reaction of hydrogen with oxygen or another oxidizing agent
- Mechanism
  - At the anode
    - ex)  $\frac{1}{2}H_2 \rightarrow H^+ + e^-$
  - At the cathode
    - ex)  $\frac{1}{4}O_2 + H^+ + e^- \rightarrow 2H_2O$
  - H<sup>+</sup> moves through the electrolyte



# **Things occurring in MFCs**

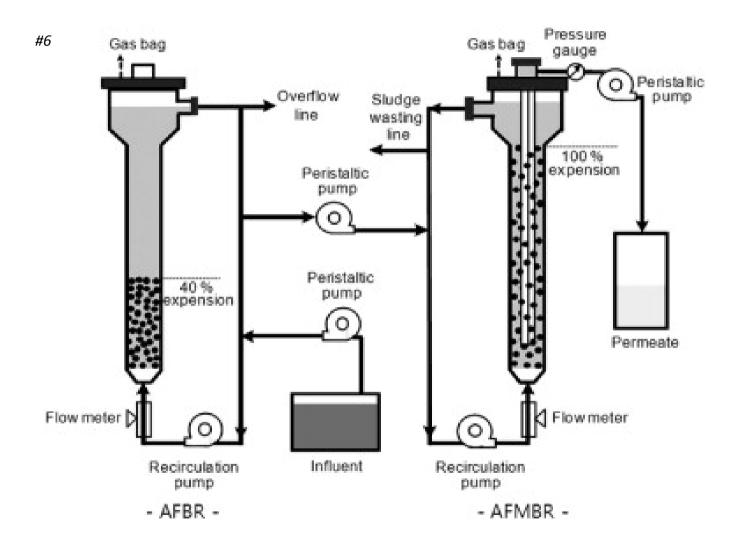
- At the anode compartment
  - Wastewater (or organic wastecontaining water) is fed
  - Bacteria live and oxidize the organics provided
  - Should be kept low in DO
- At the cathode compartment
  - Oxygen is reduced to water
  - Catalyst (ex: Pt) is used as cathode
- Exchange membrane
  - Allows H<sup>+</sup> to flow from the anode compartment to cathode compartment



## **MFCs: pros & cons**

- Advantages
  - Generation of energy out of bio-waste / organic matter
  - Direct conversion of substrate energy to electricity
  - No gas treatment required
  - Aeration may not be needed (the cathode may be passively aerated)
- Disadvantages
  - Low power density: losses of electric potential significant
  - High initial cost

### Mainstream anaerobic process: AFBR-AFMBR



AFBR: anaerobic fluidized bed bioreactor AFMBR: anaerobic fluidized bed membrane bioreactor

## **AFBR-AFMBR**

- Concept
  - Two-step anaerobic process for low-strength wastewater
  - Granular activated carbon (GAC) as media for attached growth
  - Membrane filtration for solid/liquid separation
- Pilot scale demonstration successful, with acceptable effluent quality
- Advantages
  - Those for MBR apply
  - + Energy recovery (CH<sub>4</sub>)
  - + No aeration requirements
- Limitation
  - Those for MBR apply
  - + Limited field demonstration
  - + Effluent quality may not be always good enough

## References

- #1) Isaka, K., Kimura, Y., matsuura, M., Osaka, T., Tsuneda, S. (2017) First full-scale nitritation-anammox plant using gel entrapment technology for ammonia plant effluent. Biochemical Engineering Journal, 112: 115-122.
- *#2)* Metcalf & Eddy, Aecom (2014) Wastewater Engineering: Treatment and Resource Recovery, 5<sup>th</sup> ed. McGraw-Hill, p. 656.
- #3) https://wou.edu/chemistry/courses/online-chemistry-textbooks/ch450-and-ch451-biochemistry-defininglife-at-the-molecular-level/chapter-2-protein-structure/
- *#4)* Rabaey, K., Verstraete, W. (2005) Microbial fuel cells: novel biotechnology for energy generation. Trends in Biotechnology, 23(6): 291-298.
- #5) https://en.wikipedia.org/wiki/Fuel\_cell
- *#6) Kim, J., Kim, K., Ye, H., Lee, E., Shin, C., McCarty, P. L., Bae, J. (2011) Anaerobic fluidized bed membrane bioreactor for wastewater treatment. Environmental Science & Technology, 45: 576-581.*