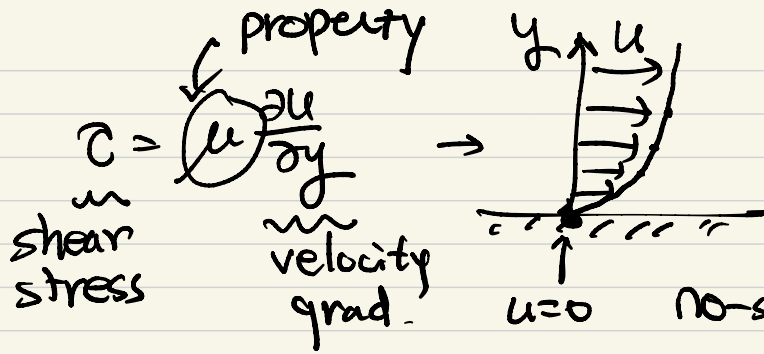


# Review

- Viscosity

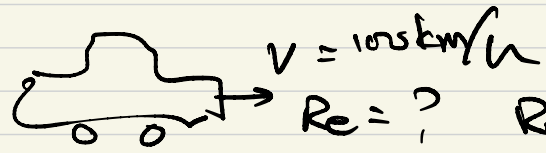


$F = ma$   
 (Newtonian fluid)  
Non-Newtonian

- Reynolds number

$$Re = \frac{\rho U L}{\mu} = \frac{UL}{\nu}$$

$\nu = \frac{\mu}{\rho}$  : kinematic viscosity  
 $\frac{m^2}{s}$   
 $1.5 \times 10^{-5}$  air  
 $10^{-6}$  water



$$Re = \frac{UL}{\nu} = \frac{150 \times 1000 / 3600 \times 4}{1.5 \times 10^{-5}} = 10^9$$

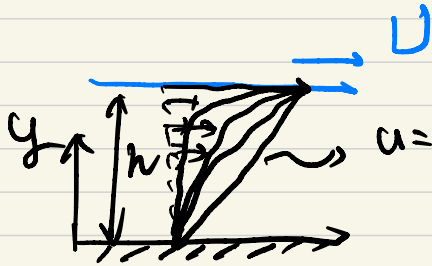
$$Re = \frac{\rho U L}{\mu} = \frac{\rho U^2}{\frac{\mu U}{L}} = \frac{\text{inertia}}{\text{shear stress}}$$

$$\tau = \mu \frac{\partial u}{\partial y} = \left[ \mu \frac{U}{L} \right]$$

$Re \uparrow$  inertial effect  $\uparrow$

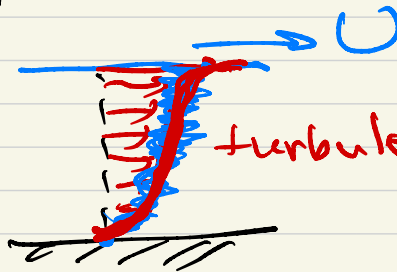
$U^2 \rightarrow$  nonlinear  $\uparrow$  turbulence

• Couette flow



$$u = \frac{y}{h} \cdot U$$

laminar flow ( $\frac{\rho U h}{\mu} < \frac{2300}{\pi}$ )

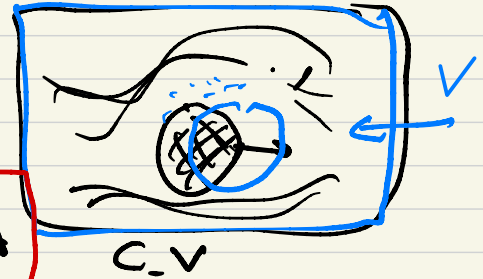


turbulent flow ( $\frac{\rho U h}{\mu} > \frac{2300}{\pi}$ )

- System vs. control volume

Reynolds transport theorem

$$\frac{dB_{sys}}{dt} = \frac{d}{dt} \int_{C.V} \beta \rho dV + \int_{C.S} \beta \rho (\underline{V}_r \cdot \underline{n}) dA$$

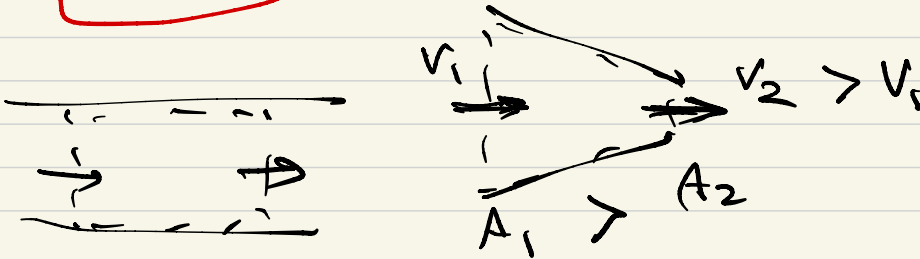


$$\beta = dB/dm, \quad \underline{V}_r = \underline{V} - \underline{V}_C$$

- mass conservation:  $B_{sys} = m$ ,  $\frac{dB}{dm} = 1$

$$\Rightarrow \frac{dm}{dt} = \frac{d}{dt} \int_{C.V} \rho dV + \int_{C.S} \rho (\underline{V}_r \cdot \underline{n}) dA$$

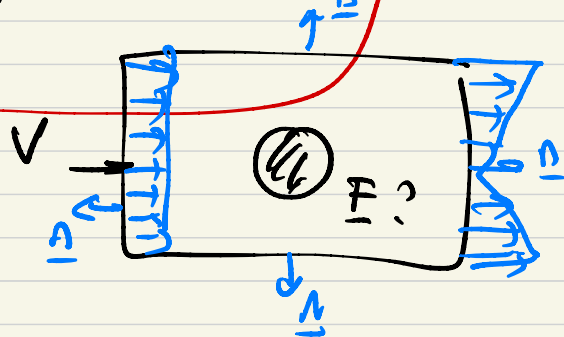
0



• mfm conservation  $R_{sys} = mV$ ,  $\beta = \frac{dB}{dt} = V$

$$\rightarrow \frac{d}{dt}(mV) \equiv \sum \underline{F}$$

$$= \frac{d}{dt} \int_{c.v} \rho \underline{V} dV + \int_{c.s} \rho \underline{V} (\underline{V} \cdot \underline{n}) dA$$

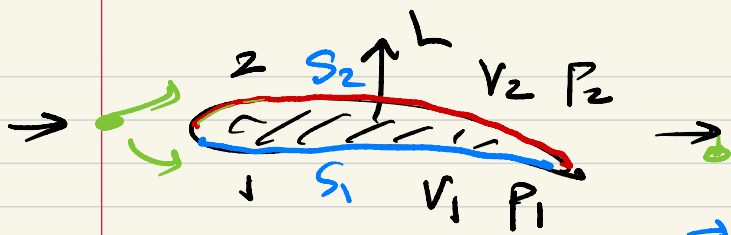


Bernoulli eq.

$$\int_1^2 \frac{\partial V}{\partial t} ds + \int_1^2 \frac{1}{\rho} dp + \frac{1}{2}(V_2^2 - V_1^2) + g(z_2 - z_1) = 0$$

unsteady frictionless flow along a streamline

$$\frac{P_1}{\rho} + \frac{V_1^2}{2} + gz_1 = \frac{P_2}{\rho} + \frac{V_2^2}{2} + gz_2 = \text{const}$$



$$S_2 > S_1 \Rightarrow V_2 > V_1$$

$$\Rightarrow P_2 < P_1 \rightarrow L \uparrow$$

Angular momentum cons.  
energy

$$\underline{v} = (u, v, w) \text{ three-dimensional}$$

Ch. 4

$$\frac{\partial}{\partial t}(\rho \underline{v}) + \nabla \cdot (\rho \underline{v} \underline{v}) = \rho \underline{g} - \nabla p + \nabla \cdot (\mu \nabla \underline{v})$$

unsteady

Navier-Stokes eq.  
nonlinear inertia term

press. term

linear viscous term

$$\frac{\partial}{\partial t}(\rho u) + \rho u \frac{\partial u}{\partial x} + \rho v \frac{\partial u}{\partial y} + \rho w \frac{\partial u}{\partial z} = \rho g_x - \frac{\partial p}{\partial x} + \mu \left( \frac{\partial^2 u}{\partial x^2} + \frac{\partial^2 u}{\partial y^2} + \frac{\partial^2 u}{\partial z^2} \right)$$

coupled

continuity eq.  ~~$\frac{\partial \rho}{\partial t} + \nabla \cdot (\rho \underline{V}) = 0$~~

• stream function  $\psi$

$$u = \frac{\partial \psi}{\partial y}, \quad v = -\frac{\partial \psi}{\partial x}$$

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0$$

~~$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} + \frac{\partial w}{\partial z} = 0$$~~

$\psi = \text{const}$  : streamline

• vorticity ( $\underline{\omega}$ ) vs. vortex ( $\rho \underline{\omega} \frac{r^2}{2}$ )

You are not supposed to understand turbulence because it is turbulence.