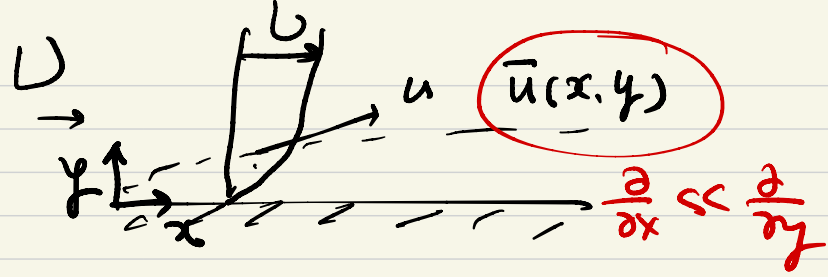


$$u = \bar{u} + u'$$

$$\overline{uv} = \bar{u}\bar{v} + \overline{u'v'}$$

N-S eq.



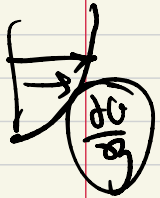
$$\Rightarrow \rho \frac{\partial}{\partial x}(\bar{u}\bar{u}) + \rho \frac{\partial}{\partial y}(\bar{u}\bar{v}) + \rho \frac{\partial}{\partial z}(\bar{u}\bar{w}) = - \frac{\partial \bar{p}}{\partial x}$$

$$+ \frac{\partial}{\partial x} \left(\underbrace{\mu \frac{\partial \bar{u}}{\partial x}}_{\text{viscous stress}} - \underbrace{\rho \overline{u'u'}}_{\text{turbulent stress}} \right) + \frac{\partial}{\partial y} \left(\underbrace{\mu \frac{\partial \bar{u}}{\partial y}}_{\text{viscous stress}} - \underbrace{\rho \overline{u'v'}}_{\text{turbulent stress}} \right) + \frac{\partial}{\partial z} \left(\underbrace{\mu \frac{\partial \bar{u}}{\partial z}}_{\text{viscous stress}} - \underbrace{\rho \overline{u'w'}}_{\text{turbulent stress}} \right)$$

viscous stress

turbulent stress

Reynolds stress



$$\tau = \mu \frac{\partial \bar{u}}{\partial y} - \rho \overline{u'v'}$$

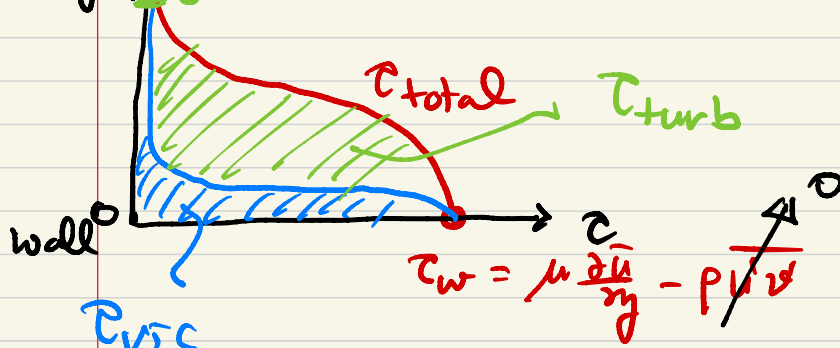
τ_{total}
total shear stress

τ_{vis}
viscous shear stress

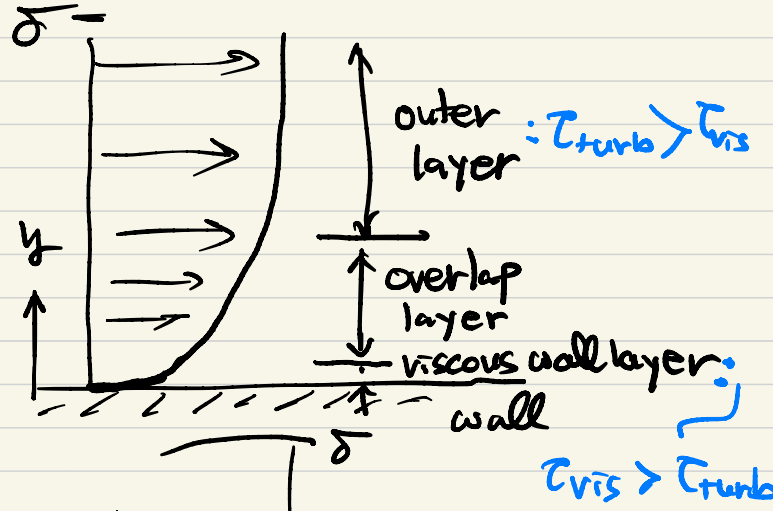
τ_{turb} turbulent shear stress
Reynolds " "

$$\tau = \mu \frac{\partial \bar{u}}{\partial y} - \rho \overline{u'v'}$$

τ_{vis} τ_{turb}



@ wall, $u = v = w = 0$
 $u' = v' = w' = 0$
 $u'v' = 0$



• wall layer: Prandtl (1930)

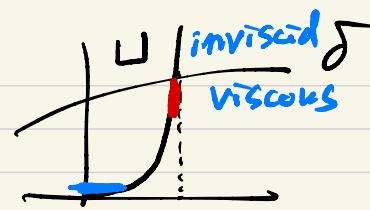
$$\bar{u} = f(\rho, \mu, y, \tau_w, \dots) \neq f(\delta)$$

dimensional analysis $\rightarrow \frac{\bar{u}}{u^*} = F\left(\frac{yu^*}{\nu}\right)$ $u^* = \sqrt{\frac{\tau_w}{\rho}}$: wall shear velocity

$u^+ \equiv \frac{\bar{u}}{u^*}$, $y^+ \equiv \frac{yu^*}{\nu}$ \rightarrow $u^+ = F(y^+)$: law of the wall

- Outer layer : von Karman (1933)

$$U - \bar{u} = g(\rho, \mu, y, \tau_w, \delta) \neq g(\mu)$$



velocity defect

$$\rightarrow \frac{U - \bar{u}}{u^*} = G\left(\frac{y}{\delta}\right) : \text{velocity defect law}$$

- overlap layer (log layer) : Millikan (1937)

$$\frac{\bar{u}}{u^*} = \frac{1}{K} \ln \frac{y u^*}{\nu} + B$$

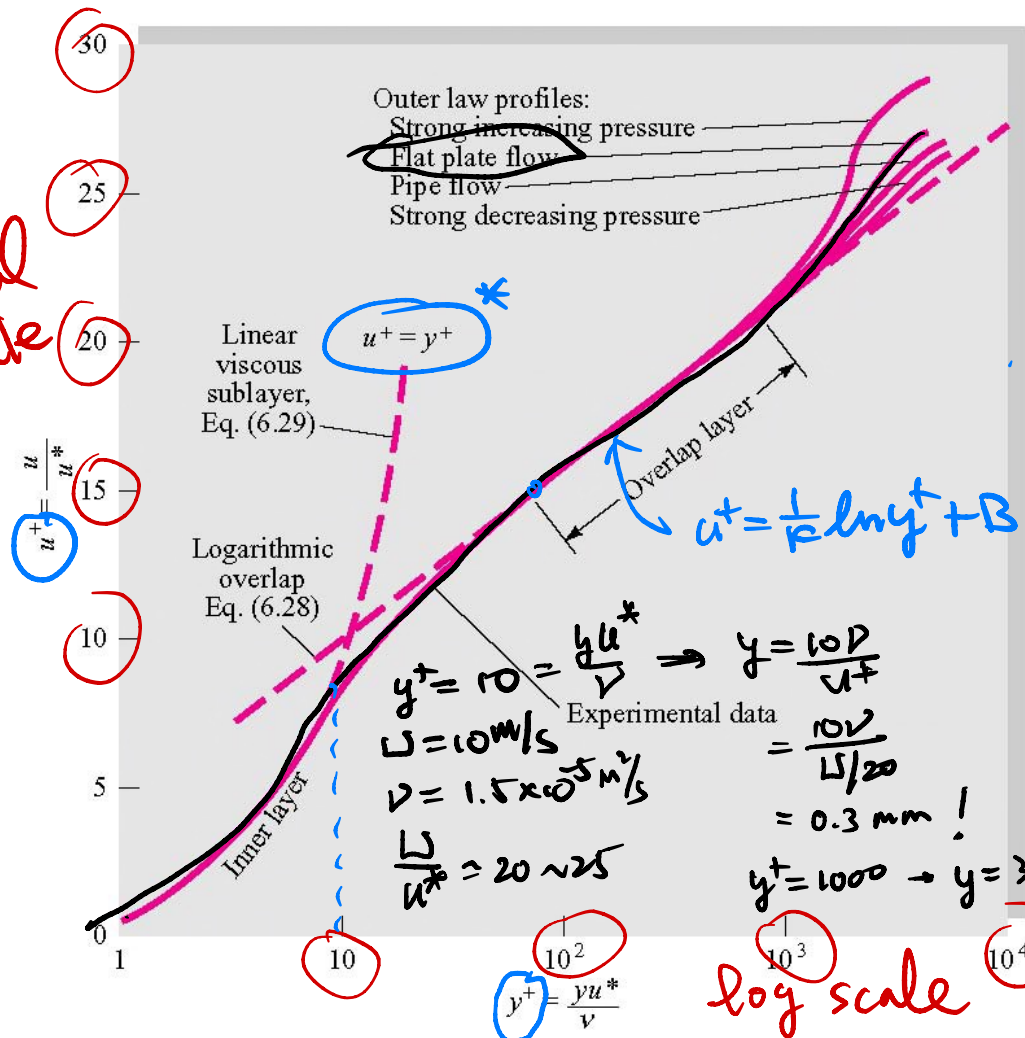
$K = 0.41$: von Karman constant

$$\rightarrow u^+ = \frac{1}{K} \ln y^+ + B : \text{log law}$$

$B = 5.0$

($K = 0.4, B = 5.5$)

real scale



$$u^+ = F(y^+)$$

$$\frac{U - \bar{u}}{u^*} = F\left(\frac{y}{\delta}\right)$$

$$u^+ = \frac{1}{k} \ln y^+ + B$$

$$\bar{u}(y) = \bar{u}_w + y \frac{\partial \bar{u}}{\partial y} \Big|_w + \frac{1}{2} y^2 \frac{\partial^2 \bar{u}}{\partial y^2} \Big|_w + \dots$$

$$\tau_w = \mu \frac{\partial \bar{u}}{\partial y} \Big|_w$$

$$\bar{u} = y \cdot \frac{\tau_w}{\mu} \quad u^* = \sqrt{\frac{2\tau_w}{\rho}}$$

$$\frac{\bar{u}}{u^*} = y \cdot \frac{\tau_w}{\mu} \cdot \frac{1}{u^*} \quad \tau_w = \rho u^{*2}$$

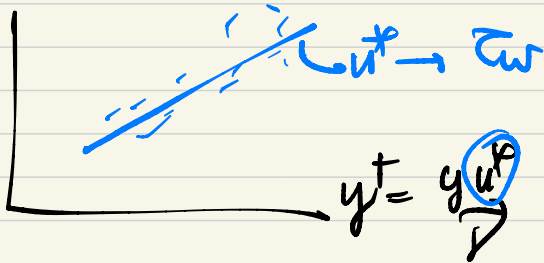
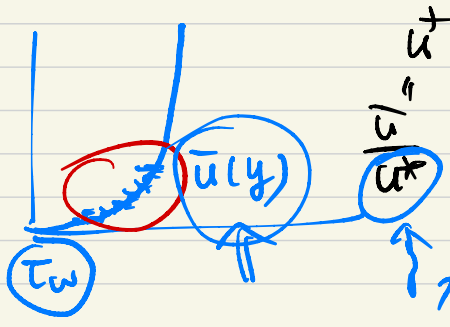
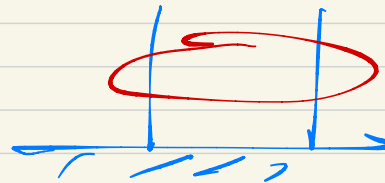
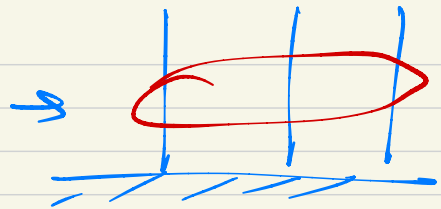
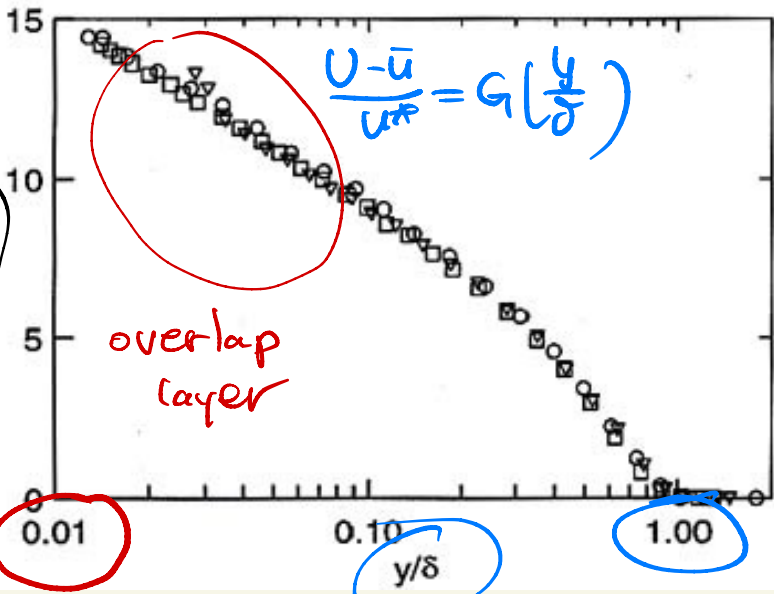
$$= y \cdot \frac{\rho u^{*2}}{\mu} = y u^{*2}$$

$$\bar{u}^+ = y^+$$

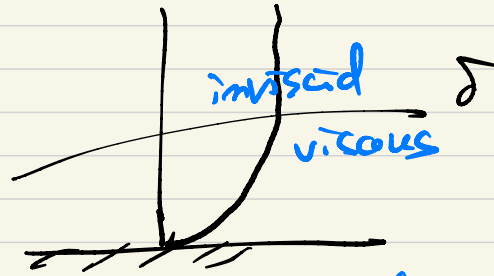
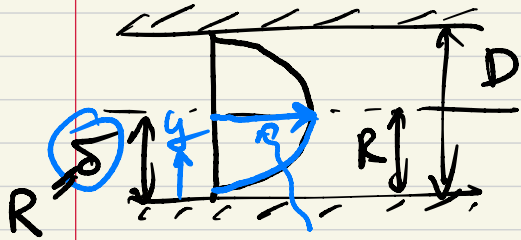
log scale

$$\frac{U - \bar{u}}{u^*}$$

$$u^+ - U^+$$



- turbulent pipe flow



viscous \rightarrow log law is approx. satisfied @ $y = \delta$

$$\frac{\bar{u}}{u^*} = \frac{1}{\kappa} \ln \frac{y u^*}{\nu} + B$$

$$\text{@ } y = \delta, \quad \frac{U}{u^*} = \frac{1}{\kappa} \ln \frac{\delta u^*}{\nu} + B$$

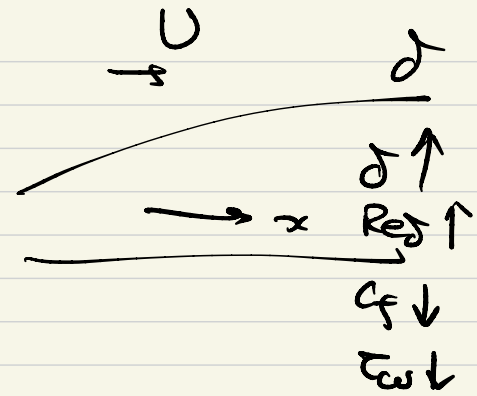
$$u^* = \sqrt{\frac{\tau_w}{\rho}} \rightarrow u^{*2} = \frac{\tau_w}{\rho} = \frac{\frac{1}{2} \rho U^2 C_f}{\rho} = \frac{1}{2} U^2 C_f \rightarrow \frac{u^*}{U} = \sqrt{\frac{C_f}{2}}$$

$$\sqrt{\frac{1}{C_f}} = \frac{1}{\kappa} \ln \frac{\delta U \sqrt{\frac{C_f}{2}}}{\nu} + B = \frac{1}{\kappa} \ln \left(\text{Re}_\delta \sqrt{\frac{C_f}{2}} \right) + B$$

$$\rightarrow \boxed{\sqrt{\frac{1}{C_f}} = \frac{1}{\kappa} \ln \left(\text{Re}_\delta \sqrt{\frac{C_f}{2}} \right) + B} : \text{skin-friction law}$$

Ref	10^4	10^5	10^6	10^7
C_f	0.00493	0.00315	0.00217	0.00188

→ $C_f \approx 0.02 Re_\delta^{-1/6}$ Prandtl

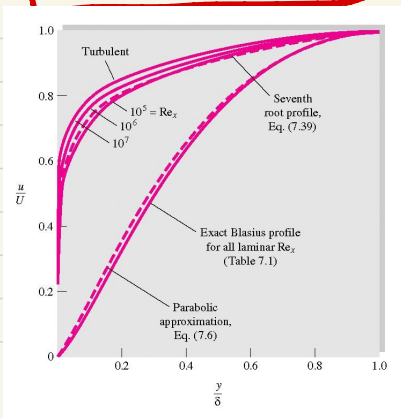


$\Theta = \int_0^\delta \frac{\bar{u}}{U} (1 - \frac{\bar{u}}{U}) dy$ ← log law? complicated!

$\frac{\bar{u}}{U} = \left(\frac{y}{\delta}\right)^{1/7}$

seventh law Prandtl

↑ very good at low Re_x ($Re_x = 10^5 \sim 10^6$)
 errors @ high " " ($Re_x > 10^6$)



$\Theta = \int_0^\delta \frac{\bar{u}}{U} (1 - \frac{\bar{u}}{U}) dy = \frac{7}{72} \delta$

$\delta^* = \int_0^\delta (1 - \frac{\bar{u}}{U}) dy = \frac{1}{8} \delta$

$H = \delta^* / \Theta = 1.3$

$$C_f = \frac{d\theta}{dx} = \frac{17}{72} \frac{d\delta}{dx} = \frac{17}{72} \frac{d\left(\frac{\delta U}{\nu}\right)}{d\left(\frac{xU}{\nu}\right)} = \frac{17}{72} \frac{dRe_\delta}{dRe_x}$$

$$\frac{1}{2} \cdot 0.02 Re_\delta^{-1/6}$$

$$Re_\delta = 0.16 Re_x^{6/5}$$

$$\frac{\delta}{x} = \frac{0.16}{Re_x^{1/5}}$$

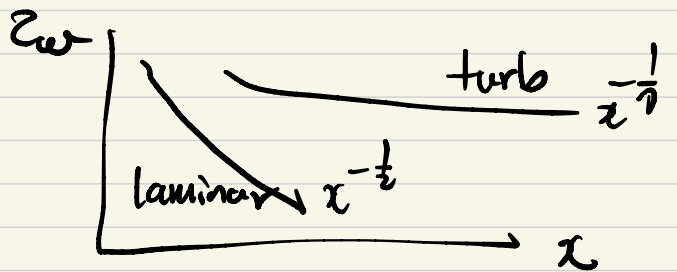
$$\frac{\theta}{x} = \frac{\theta}{\delta} \cdot \frac{\delta}{x} = \frac{1}{7.5} \cdot \frac{0.16}{Re_x^{1/5}} = \frac{0.0155}{Re_x^{1/5}}$$

$\delta \sim x^{5/4}$
lam. $\delta \sim x^{1/2}$

$$C_f = 0.02 Re_\delta^{-1/6} = \frac{0.027}{Re_x^{1/5}} = 0.027 \Delta^{-1/5} x^{-1/5} \Delta^{1/5}$$

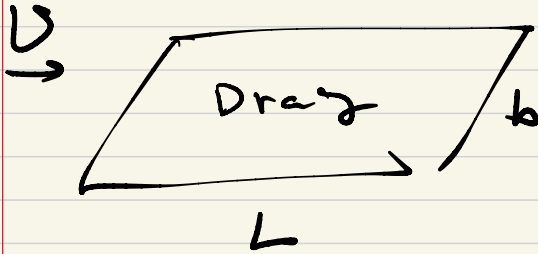
$$\tau_w = \frac{1}{2} \rho U^2 C_f = 0.0135 \mu^{1/5} \rho^{4/5} \Delta^{13/5} x^{-1/5}$$

lam. $\tau_w = 0.332 \rho^{1/2} \mu^{1/2} \Delta^{3/2} x^{-1/2}$



$$\tau_w = \mu \frac{\partial u}{\partial y} \Big|_w \Leftrightarrow \frac{u}{\nu} = \left(\frac{y}{x}\right)^{1/4}$$

$\tau_w \rightarrow \infty$ wrong!



Drag D

$$C_D \equiv \frac{D}{\frac{1}{2} \rho U^2 L b} = \frac{\rho b U^2 \theta(L)}{\frac{1}{2} \rho U^2 L b} = \frac{2\theta(x=L)}{L}$$
$$= \frac{0.031}{Re_L^{1/4}} = \frac{17}{6} C_f(L) \quad Re_L = \frac{UL}{\nu}$$

lam. $C_D = 2 C_f(L)$