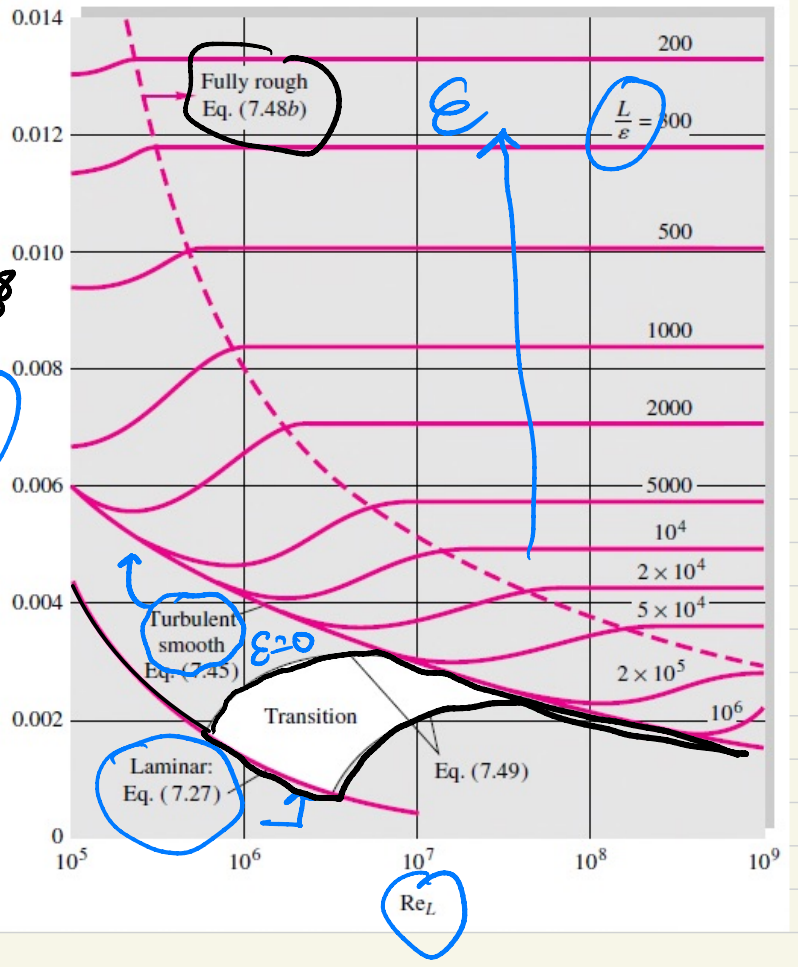


ϵ : roughness

비행기 $L = 50\text{m}$
 $U = 300\text{m/s}$ } $Re_L = \frac{UL}{\nu} \approx 10^9$
 $Re_\delta = 0.16 Re_L^{1/2} = 1.6 \times 10^8$

자동차 $L = 5\text{m}$
 $U = 30\text{m/s}$ } $Re_L = 10^7$
 $Re_\delta = 1.6 \times 10^6$ C_D

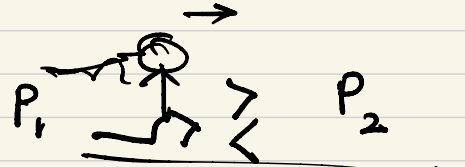
Fig. 7.6 Drag coefficient of laminar and turbulent boundary layers on smooth and rough flat plates. This chart is the flat-plate analog of the Moody diagram of Fig. 6.13.



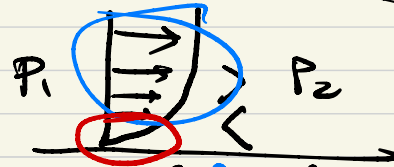
7.5 Boundary layers w/ pressure gradients

flat plate: $U = \text{const} \rightarrow \frac{dU}{dx} = 0 \rightarrow \frac{dp}{dx} = 0$

$\frac{dp}{dx} > 0$: adverse press. grad.
or $\frac{dU}{dx} < 0$ \rightarrow $\frac{dU}{dx} < 0$ \rightarrow $\frac{dU}{dx} < 0$



$\frac{dp}{dx} < 0$: favorable press. grad.
 $\frac{dU}{dx} > 0$ \rightarrow $\frac{dU}{dx} > 0$ \rightarrow $\frac{dU}{dx} > 0$



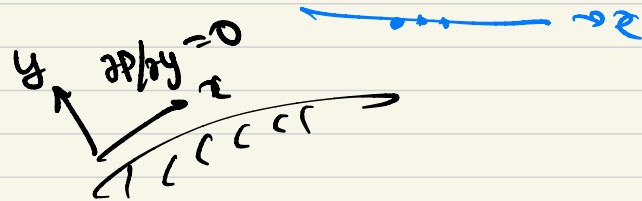
N-S eq:
$$\rho \left(\frac{\partial u}{\partial t} + u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} \right) = -\frac{\partial p}{\partial x} + \mu \left(\frac{\partial^2 u}{\partial x^2} + \frac{\partial^2 u}{\partial y^2} \right)$$

@ $y=0$ (wall), $u = v = 0$ (no slip)

$$\Rightarrow 0 = -\frac{\partial p}{\partial x} + \mu \frac{\partial^2 u}{\partial y^2} \Big|_w$$

curvature

$$\Rightarrow \frac{\partial^2 u}{\partial y^2} \Big|_w = \frac{1}{\mu} \frac{\partial p}{\partial x}$$

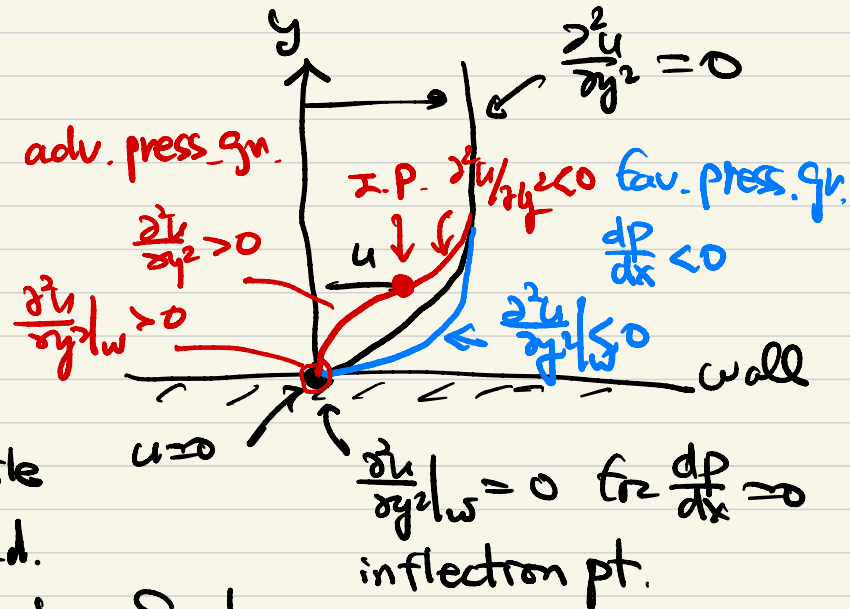


$$\frac{\partial^2 u}{\partial y^2} \Big|_w = \frac{1}{\mu} \frac{dp}{dx}$$

if $\frac{dp}{dx} = 0$, $\frac{\partial^2 u}{\partial y^2} \Big|_w = 0$

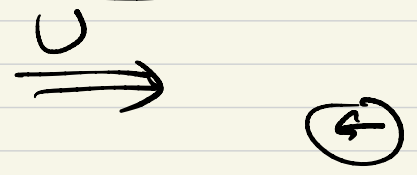
$\frac{dp}{dx} < 0$, $\frac{\partial^2 u}{\partial y^2} \Big|_w < 0$

$\frac{dp}{dx} > 0$, $\frac{\partial^2 u}{\partial y^2} \Big|_w > 0$

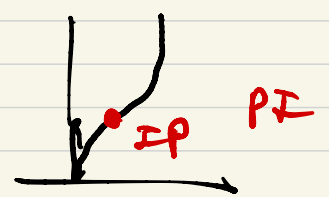


→ Any boundary layer profile in an adverse press. grad. exhibits a characteristic S shape.

Flow Separation $\frac{dp}{dx} > 0$ zero press. grad. $\frac{dp}{dx} = 0$ $\frac{du}{dx} = 0$ no sep.



weak adv. press grad. $\frac{dp}{dx} > 0 \rightarrow \frac{du}{dx} < 0$ no sep.



critical adv. press. gr. $\frac{dp}{dx} > 0$ $\frac{du}{dx} < 0$

separation starts

boundary layer thickness \uparrow



excessive adv. press gr.

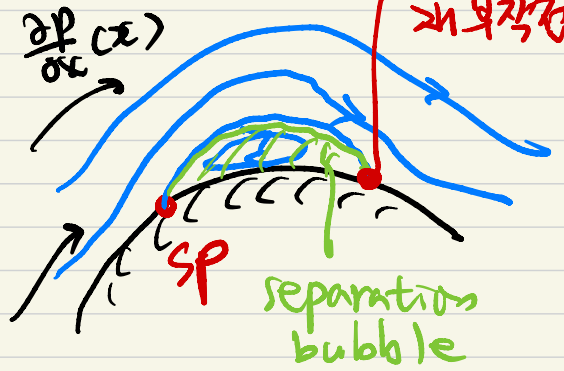
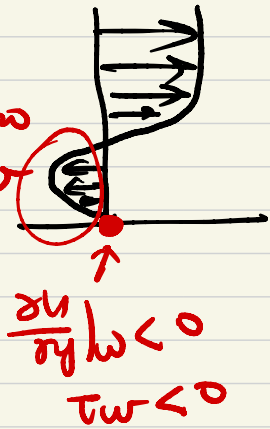


separation pt. $\Rightarrow \frac{\partial u}{\partial y}|_w = 0$
 $\tau_w = 0$

bdry layer approx \times

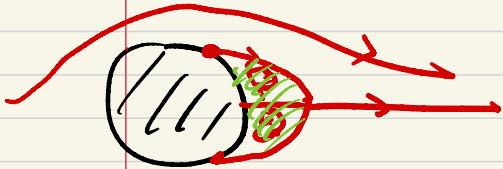
reattach-ment point \Rightarrow $\frac{\partial u}{\partial y}|_w > 0$

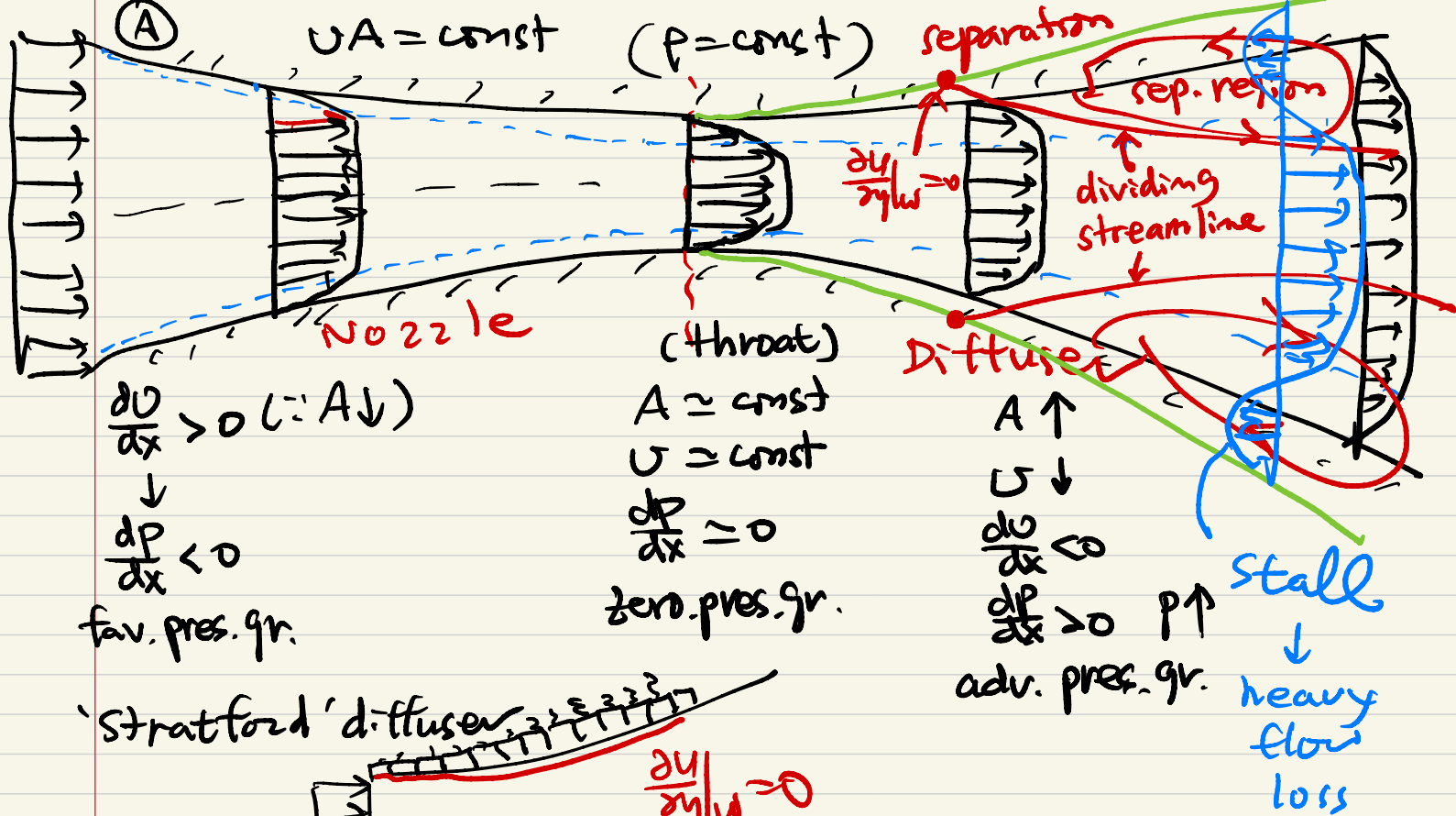
backward flow
reverse flow



separation bubble

Separation region





$UA = \text{const}$ ($P = \text{const}$)

Nozzle

(throat)

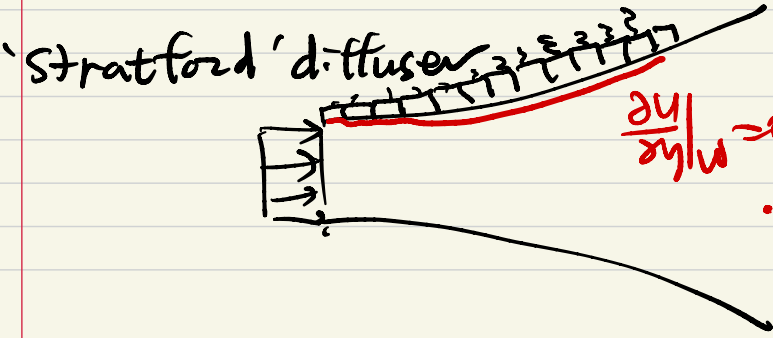
Diffuser

$\frac{dU}{dx} > 0$ ($A \downarrow$)
 \downarrow
 $\frac{dP}{dx} < 0$
 fav. pres. gr.

$A \approx \text{const}$
 $U \approx \text{const}$
 $\frac{dP}{dx} \approx 0$
 zero pres. gr.

$A \uparrow$
 $U \downarrow$
 $\frac{dU}{dx} < 0$
 $\frac{dP}{dx} > 0$ $P \uparrow$
 adv. pres. gr.

Stall
 \downarrow
 heavy flow loss



$\frac{\partial u}{\partial y} \Big|_{y=0} = 0$

$\cdot P_{max}$

Boundary layer theory ($u \gg v$, $\frac{\partial}{\partial y} \gg \frac{\partial}{\partial x}$, $\frac{\partial^2}{\partial y^2} \gg \frac{\partial^2}{\partial x^2}$)
is valid only up to the separation pt.

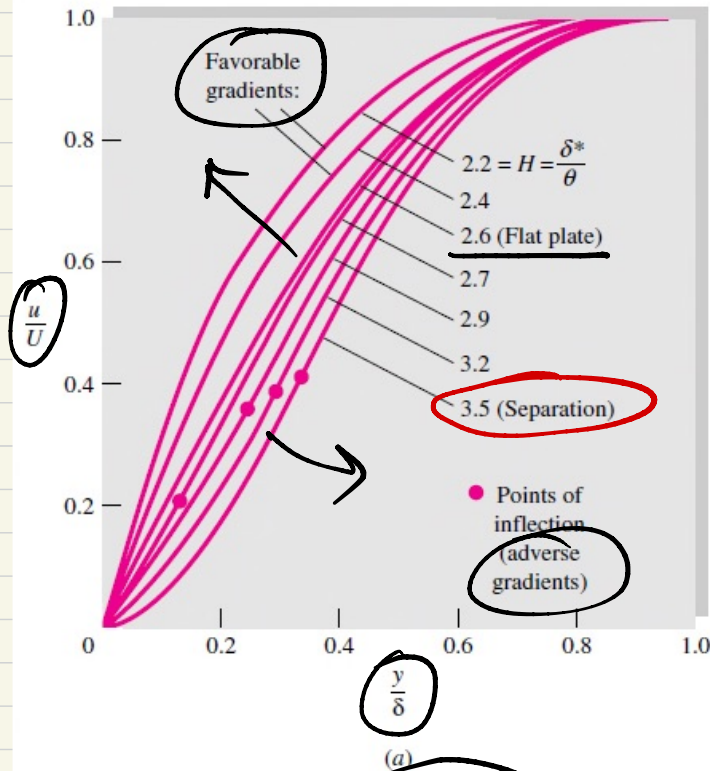
• Laminar bdry layer integral theory (Karman)

$$\frac{\tau_w}{\rho U^2} = \frac{C_f}{2} = \frac{d\theta}{dx} + (2+H) \frac{\theta}{U} \frac{dU}{dx} \quad \left(\frac{dU}{dx} = -\frac{1}{\rho U} \frac{dp}{dx} \right)$$

C_f , θ , H open form

separation occurs @ $H = 3.5$ laminar flow
($C_f = 0$) $= 2.4$ turbulent "

laminar



turbulent

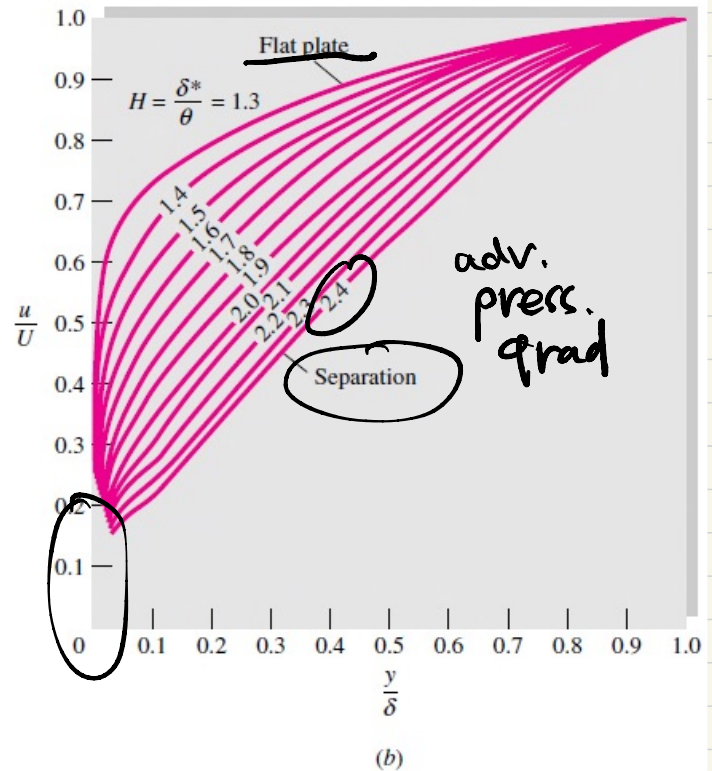


Fig. 7.9 Velocity profiles with pressure gradient: (a) laminar flow; (b) turbulent flow with adverse gradients.

7.6 Experimental external flows