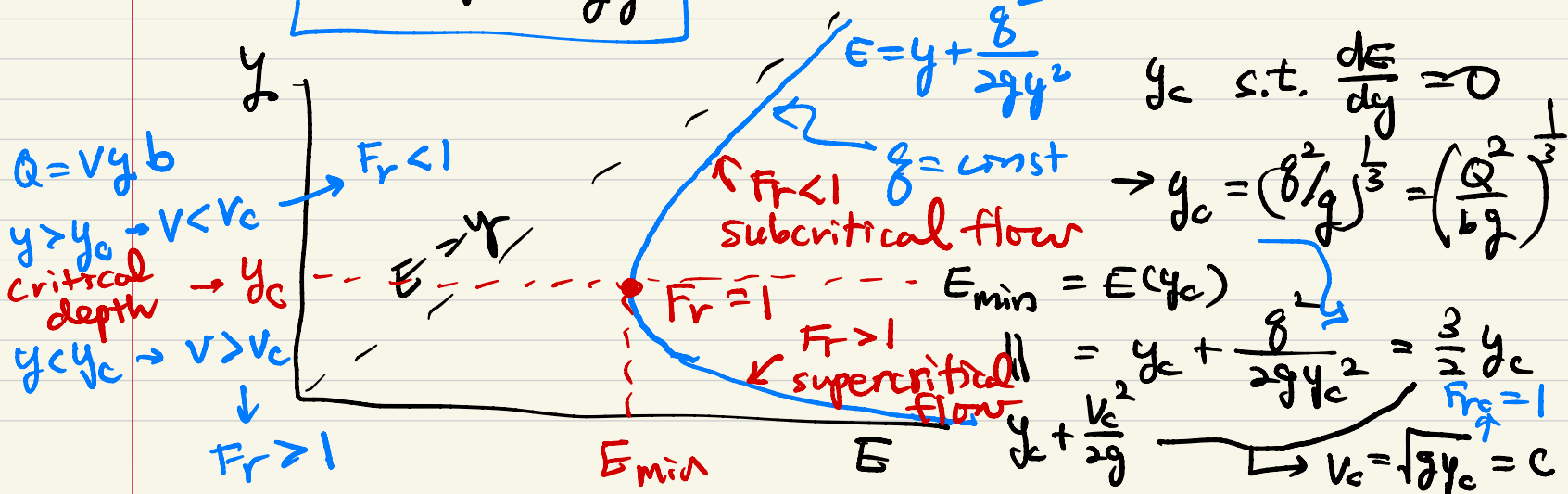


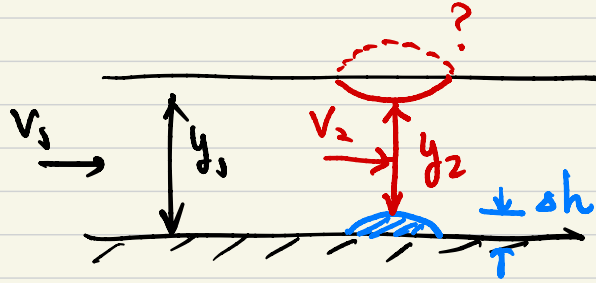
Specific energy:  $E \equiv y + \frac{v^2}{2g}$   $Q = \text{const}$

$Q = Vy b = qb$ ,  $q = \frac{Q}{b}$ : discharge per width

$E = y + \frac{q^2}{2gy^2}$  "const



• Frictionless flow over a bump



Cont:  $v_1 y_1 = v_2 y_2$   
 Bernoulli eq:  $\frac{v_1^2}{2g} + y_1 = \frac{v_2^2}{2g} + (y_2 + \Delta h)$   
 $E_1 = E_2 + \Delta h$

$y_2^3 - E_2 y_2^2 + \frac{1}{2g} v_1^2 y_1^2 = 0$   
 $E_2 = E_1 - \Delta h$

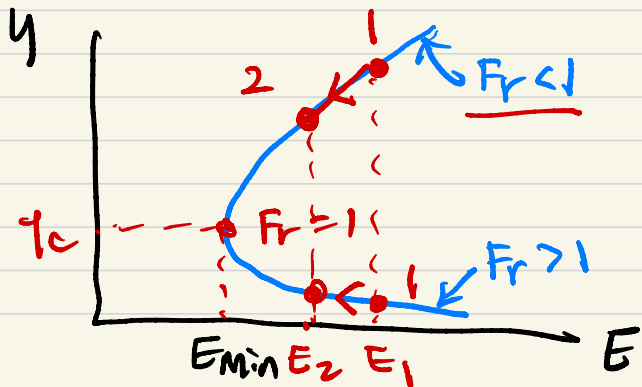
If  $\Delta h$  is not too large,

$Fr_1 = \frac{v_1}{\sqrt{g y_1}} < 1$ :

$(y_2 + \Delta h) - y_1 = \frac{1}{2g} (v_1^2 - v_2^2)$   
 $= \frac{1}{2g} (v_1 + v_2)(v_1 - v_2) < 0$

$E_2 = E_1 - \Delta h < E_1 \Rightarrow y_2 < y_1$   
 $\rightarrow v_2 > v_1$

$\Rightarrow y_2 + \Delta h < y_1 \therefore$  water level down!



$$Fr_1 > 1 : E_2 < E_1 \rightarrow y_2 > y_1 \rightarrow v_2 < v_1$$

$$(y_2 + \delta h) - y_1 = \frac{1}{2g} (v_1^2 + v_2^2) (v_1 - v_2) > 0$$

$\rightarrow y_2 + \delta h > y_1 \Rightarrow$  water level up!

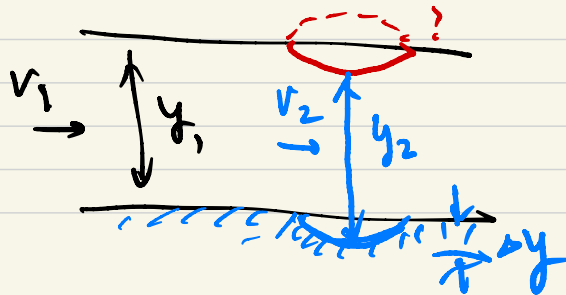
If  $\delta h = \delta h_{max} = E_1 - E_{min}$ , flow at the crest is critical ( $Fr_2 = 1$ ).

If  $\delta h > \delta h_{max}$ , no physical sol.

$\rightarrow$  a bump too large will choke the channel and causes frictional effects, typically

a hydraulic jump.

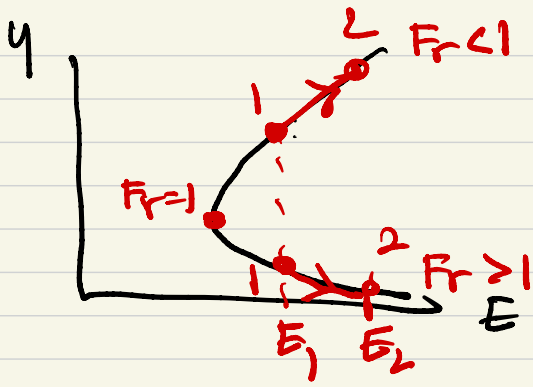
• Frictionless flow over a hollow



$$\text{cont: } v_1 y_1 = v_2 y_2$$

$$\text{Bernoulli eq: } \frac{v_1^2}{2g} + y_1 = \frac{v_2^2}{2g} + (y_2 - \delta h)$$

$$E_1 = E_2 - \delta h$$



$$E_1 = E_2 - \Delta h$$

$$y_2 - \Delta h - y_1 = \frac{1}{2g} (V_1 + V_2) (V_1 - V_2)$$

$$\textcircled{a} Fr_1 < 1, E_2 = E_1 + \Delta h$$

$$\rightarrow y_2 > y_1 \rightarrow V_2 < V_1$$

$$y_2 - \Delta h - y_1 > 0 \Rightarrow y_2 - \Delta h > y_1$$

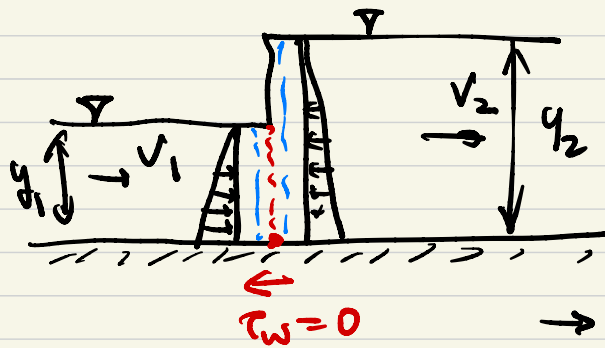
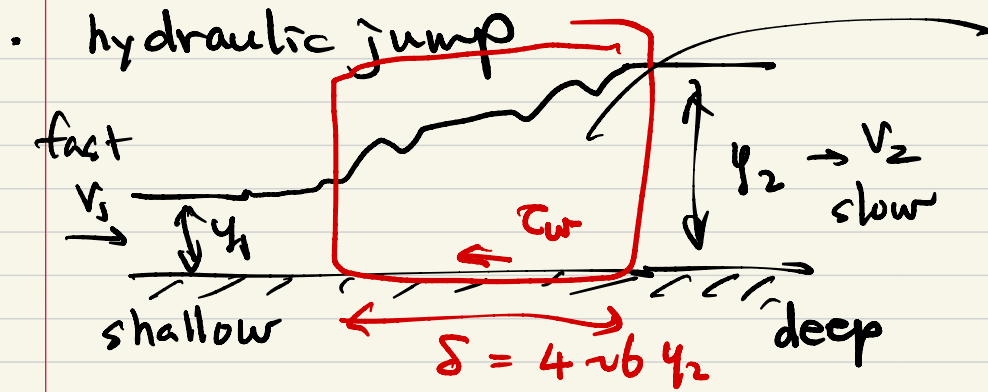
water level up.

$$\textcircled{b} Fr_1 > 1, y_2 < y_1 \rightarrow V_2 > V_1$$

$$y_2 - \Delta h - y_1 < 0 \Rightarrow y_2 - \Delta h < y_1$$

water level down.

critical flow cannot occur.



cont:  $\rho v_1 y_1 b = \rho v_2 y_2 b$

mom:  $-\frac{1}{2} \rho g b (y_2^2 - y_1^2)$   
 $= \rho v_1 y_1 b (v_2 - v_1)$

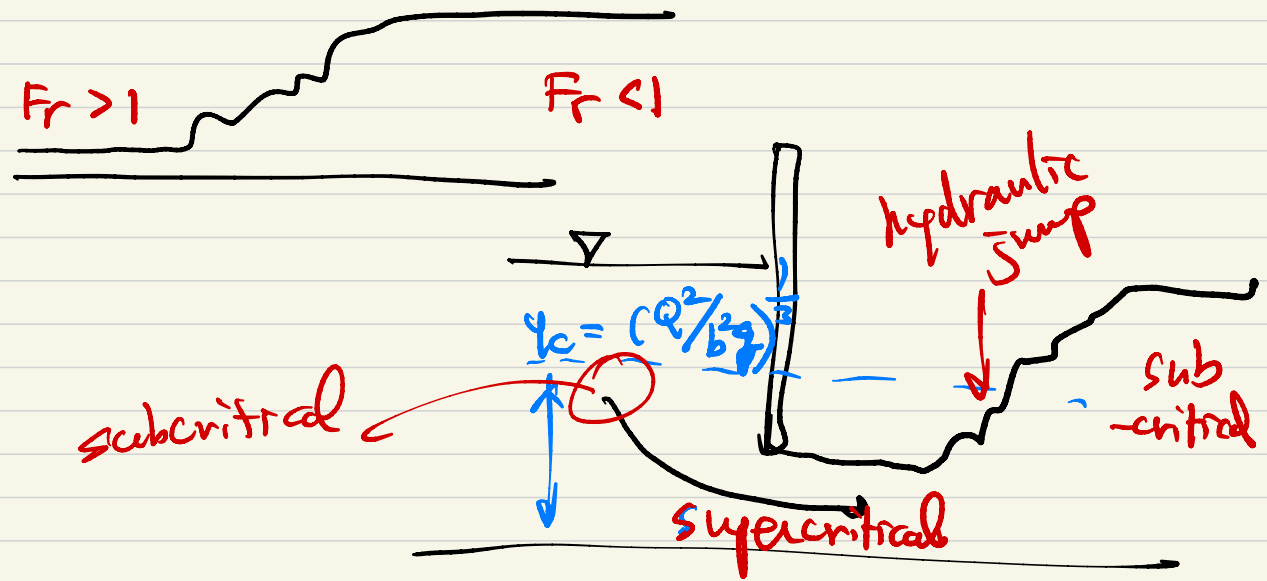
$\rightarrow v_1^2 = g y_1 \eta \cdot \frac{1}{2} (1 + \eta), \quad \eta = \frac{y_2}{y_1}$   
 $v_2 = v_1 \frac{y_1}{y_2} = v_1 / \eta, \quad Fr_1 = \frac{v_1}{\sqrt{g y_1}}$

$\rightarrow \eta = \frac{y_2}{y_1} = \frac{1}{2} (-1 + \sqrt{1 + 8 Fr_1^2}) \rightarrow \frac{v_2}{v_1} = \frac{y_1}{y_2} = \frac{1}{\eta} \rightarrow Fr_2 \sim f(Fr_1)$   
 $Fr_2 = \sqrt{\frac{1}{2}(1 + \eta)} / \eta < 1 \text{ for } \eta > 1$

$$h_f = \left( y_1 + \frac{v_1^2}{2g} \right) - \left( y_2 + \frac{v_2^2}{2g} \right) = \dots = \frac{(y_2 - y_1)^3}{4y_1 y_2} > 0$$

$\rightarrow y_2 > y_1 \rightarrow z = \frac{y_2}{y_1} > 1 \rightarrow \boxed{Fr_1 > 1} \therefore \text{supercritical flow}$

$Fr_2 < 1 \leftarrow v_2 < v_1$   
 subcritical flow



# Ch. 11. Turbomachinery (터보기계)

## Fluid machinery (유체기계)

① pumps: those which add energy to fluid

② turbines: " " extract " from "

→ usually connected to a rotating shaft

↓  
"turbo" machinery  
spin, whirl

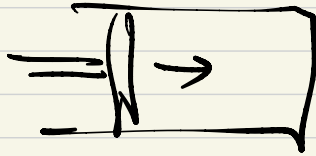
### Pump

• working fluid is liquid → pump

gas → fan:  $\Delta p(\uparrow)$  is small  
blower:  $\Delta p$  is up to 1 atm.  
compressor:  $\Delta p$  is above 1 atm.

# classification of pumps

## ① positive-displacement pump



forces the fluid along one direction  
by volume change  $\Rightarrow$  sp $\uparrow$   
effective in handling high  $\nu$  fluid

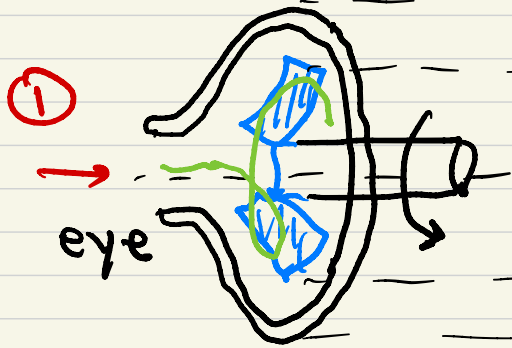
## ② dynamic pump: adds momentum to fluid by means of fast moving blades or vanes or certain special designs



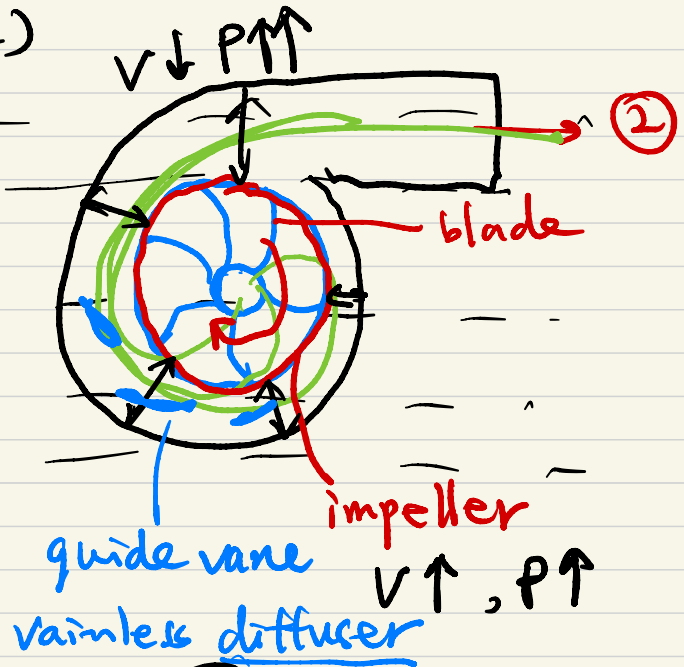
no closed volume  
higher flow rate  
steady discharge



• Centrifugal pump (离心泵)



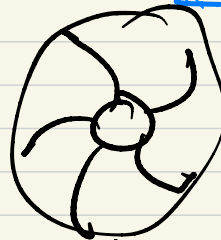
centrifugal compressor  
离心压缩机



forward vane



radial vane



backward vane

• Efficiency

$$\text{Net head : } H = \left( \frac{P}{\rho g} + \frac{v^2}{2g} + z \right)_2 - \left( \frac{P}{\rho g} + \frac{v^2}{2g} + z \right)_1$$
$$= h_s - h_f$$

shaft                  loss

usually  $v_2 \approx v_1$ ,  $z_2 - z_1 < 1 \text{ m}$  neglect

$$\rightarrow H \approx \frac{P_2 - P_1}{\rho g} = \frac{\Delta P}{\rho g}$$

Power delivered to fluid  $P_w = \rho g H Q$        $Q$ : discharge  
(water horse power)

Power required to drive the pump

$$\text{bhp} = \omega T$$

(brake horse power)       $\omega$ : shaft angular vel.

$T$ : torque

Efficiency  $\eta = \frac{P_w}{bhp} = \frac{\rho g H Q}{\omega_T} < 1 \quad (\sim 0.9)$

loss