

Applications of the First Law

(Lecture 4)

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Advanced Thermodynamics (M2794.007900)

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(* Some materials in this lecture note are borrowed from the textbook of Ashley H. Carter.

Heat Capacity

- Definition: the limiting ratio of the heat absorbed divided by the temperature increase

$$C = \lim_{\Delta T \rightarrow 0} \left(\frac{Q}{\Delta T} \right) = \frac{\delta Q}{dT} \rightarrow \text{not truly derivative}$$

- *Specific heat capacity (or specific heat)*

$$c = \frac{1}{m} \left(\frac{\delta Q}{dT} \right) = \frac{\delta q}{dT} \quad (\text{J/kg} \cdot \text{K})$$

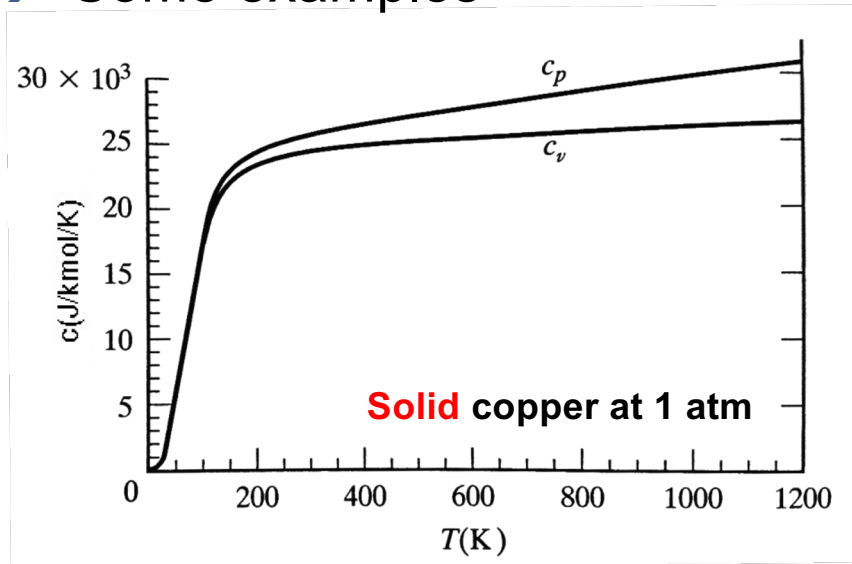
$$\bar{c} = \frac{1}{n} \left(\frac{\delta Q}{dT} \right) = \frac{\delta \bar{q}}{dT} \quad (\text{J/kmol} \cdot \text{K})$$

- *Specific heat at constant volume and at constant pressure*

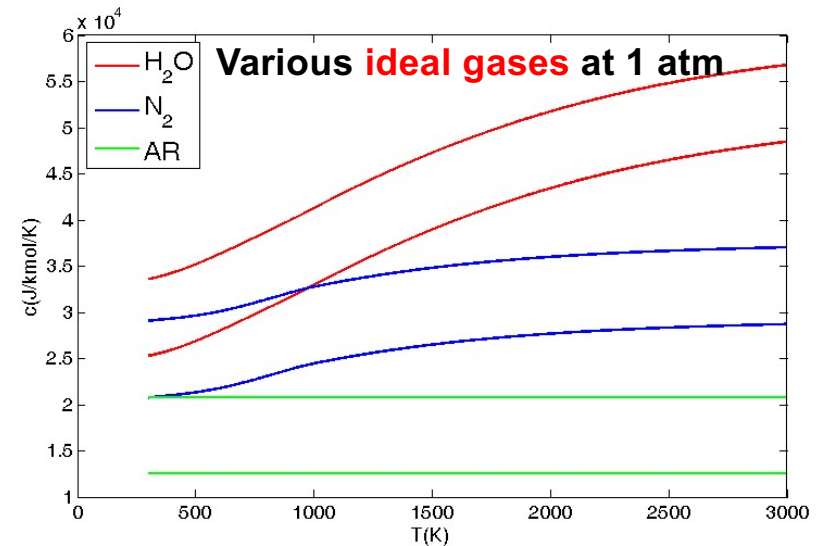
$$c_v = \left(\frac{\delta q}{dT} \right)_v \quad \text{and} \quad c_p = \left(\frac{\delta q}{dT} \right)_p \quad (\text{J/kg} \cdot \text{K})$$

Heat Capacity

→ Some examples



1. At high temperatures, c_v is almost constant.
(Law of Dulong and Petit $\sim 3\bar{R}$ from 6 d.o.f.)
2. At low temperatures, c_p is almost same with c_v .
At high temperatures, they deviate due to thermal expansion.
3. Specific heats tend toward zero as $T \rightarrow 0K$.
(\rightarrow Einstein's or Debye's theory)



1. Various ideal gases show different limit behaviors.
2. Argon has constant specific heats.
3. There is almost constant difference between c_p and c_v .
(\rightarrow Mayer's equation)

Mayer's Equation

→ Let's find the relationship between c_v and c_p for **an ideal gas**.

For a simple compressible substance, the first law is

$$du = \delta q - \delta w = \delta q - Pdv$$

In general, $u = u(v, T) \rightarrow du = \left(\frac{\partial u}{\partial v}\right)_T dv + \left(\frac{\partial u}{\partial T}\right)_v dT$

Then, $\delta q = du + Pdv = \left(\frac{\partial u}{\partial T}\right)_v dT + \left\{\left(\frac{\partial u}{\partial v}\right)_T + P\right\} dv$

$$\rightarrow \delta q = c_v dT + \left\{\left(\frac{\partial u}{\partial v}\right)_T + P\right\} dv \quad \left(\because c_v = \left(\frac{\delta q}{dT}\right)_v = \left(\frac{\partial u}{\partial T}\right)_v\right)$$

But for an ideal gas, $u = u(T)$ only $\rightarrow \left(\frac{\partial u}{\partial v}\right)_T = 0$ (Gay-Lussac-Joule exp.)

Then, $c_v = \left(\frac{\partial u}{\partial T}\right)_v = \frac{du}{dT}$ or $du = c_v dT$ or $u - u_0 = \int_{T_0}^T c_v dT$

Mayer's Equation

→ Continue on.

Using ideal gas EOS, $Pv = RT \rightarrow Pdv + vdP = RdT$

Substituting this equation,

$$\delta q = c_v dT + Pdv \rightarrow \delta q = (c_v + R)dT - vdP$$

Then,

$$c_P \equiv \left(\frac{\delta q}{\partial T} \right)_P = c_v + R$$

Mayer's equation

“Over the range of variables for which the ideal gas law holds, the two specific heat capacities differ by the constant R .”

→ *The ratio of specific heat capacities (or specific heat ratio)*

$$\gamma \equiv \frac{c_P}{c_v}$$

Enthalpy and Heats of Transformation

→ The heat of transformation

- Heat transfer accompanying a phase change
- Phase change is an isothermal and isobaric process with changing volume.
- Applying the first law for a phase change, from phase 1 to phase 2,

$$du = \delta q - Pdv$$

$$u_2 - u_1 = l - P(v_2 - v_1) \rightarrow l = (u_2 + Pv_2) - (u_1 + Pv_1)$$

where l : latent heat of phase change

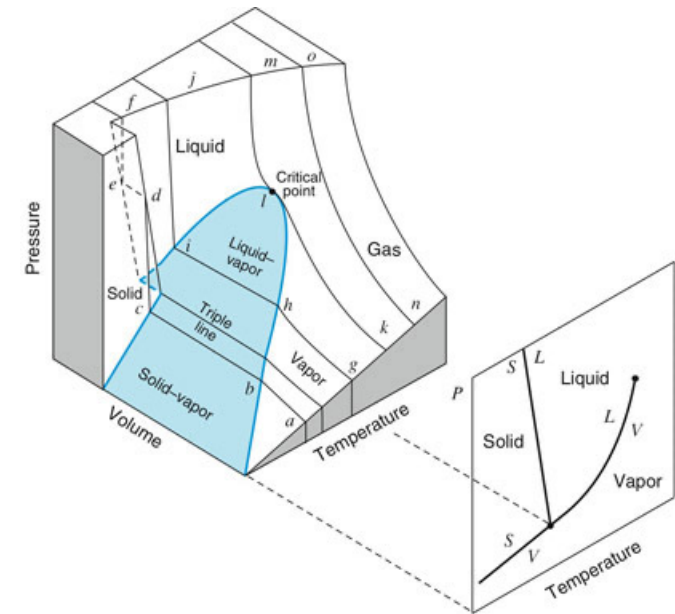
(i.e. vaporization, fusion, sublimation)

Here, we define **enthalpy(h)**, a state variable.

$$h \equiv u + Pv$$

Then,

$$l = h_2 - h_1$$



P-v-T Surface for Water

Latent Heat of Vaporization at Steam Point, 1 atm		Latent Heat of Fusion at Melting Point, 1 atm	
Water	538 kcal/kg	Water	80 kcal/kg
Mercury	63	Mercury	3
Alcohol	207	Lead	5
Gasoline	95	Aluminum	77

Latent Heat of Phase Change

Relationships involving Enthalpy

→ Let's find some useful relationship using enthalpy for **an ideal gas**.

For S.C.S., the first law is $du = \delta q - Pdv \rightarrow du + Pdv = \delta q$

From the definition of enthalpy,

$$dh = d(u + Pv) = du + Pdv + vdP \rightarrow du + Pdv = dh - vdP$$

Then,

$$\delta q = dh - vdP$$

In general, $h = h(P, T) \rightarrow dh = \left(\frac{\partial h}{\partial P}\right)_T dP + \left(\frac{\partial h}{\partial T}\right)_P dT$

$$c_P = \left(\frac{\delta q}{\partial T}\right)_P = \left(\frac{\partial h}{\partial T}\right)_P$$

$$\delta q = \left(\frac{\partial h}{\partial T}\right)_P dT + \left\{\left(\frac{\partial h}{\partial P}\right)_T - v\right\} dP \rightarrow \delta q = c_P dT + \left\{\left(\frac{\partial h}{\partial P}\right)_T - v\right\} dP$$

But for an ideal gas, $h = h(T)$ only $\rightarrow \left(\frac{\partial h}{\partial P}\right)_T = 0$ (Joule-Thomson exp.)

Then, $c_P = \left(\frac{\partial h}{\partial T}\right)_P = \frac{dh}{dT}$ or $dh = c_P dT$ or $h - h_0 = \int_{T_0}^T c_P dT$

Work done in an Adiabatic Process

→ Let's calculate work done in an adiabatic process for **an ideal gas**.

For a simple compressible substance of an ideal gas, the first law is

$$\begin{aligned} \delta q &= c_v dT + P dv \rightarrow P dv = -c_v dT \\ \delta q &= c_p dT - v dP \rightarrow v dP = c_p dT \end{aligned} \rightarrow \frac{v dP}{P dv} = -\frac{c_p}{c_v} = -\gamma$$

Then,

$$\frac{dP}{P} = -\gamma \frac{dv}{v} \quad \text{or} \quad Pv^\gamma = \text{const} = K \quad (\text{when } \gamma \text{ constant})$$

Work is given by the following expression for **a constant specific heats**,

$$w = \int P dv = K \int_{v_1}^{v_2} v^{-\gamma} dv = \frac{1}{1-\gamma} \left(K v^{1-\gamma} \right) \Big|_{v_1}^{v_2} = \frac{1}{1-\gamma} \left[K v_2^{1-\gamma} - K v_1^{1-\gamma} \right] = \frac{1}{1-\gamma} \left[P_2 v_2 - P_1 v_1 \right]$$

$$K = P_1 v_1^\gamma = P_2 v_2^\gamma$$