Advanced Thermodynamics (M2794.007900)

Chapter 7

Applications of the Second Law

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7.1 Entropy Changes in Reversible Processes

For reversible process, $\delta q_r = du + P \, dv$

1. Adiabatic process : $\delta q_r = 0, ds = 0, s = constant$

2. Isothermal process :
$$s_2 - s_1 = \int_1^2 \frac{\delta q_r}{T} = \frac{q_r}{T}$$



7.1 Entropy Changes in Reversible Processes

3. Isothermal (and isobaric) change of phase : $s_2 - s_1 = \frac{l}{T}$

4. Isochoric process :
$$s_2 - s_1 = \int_1^2 c_v \frac{dT}{T} = c_v \ln \frac{T_2}{T_1}$$

5. Isobaric process :
$$\frac{\delta q_r}{T} = \frac{dh}{T} - \frac{v}{T}dP = ds$$

$$s_2 - s_1 = \int_1^2 c_p \frac{dT}{T} = c_p \ln \frac{T_2}{T_1}$$



7.2 Temperature-Entropy Diagrams

The total quantity of heat transferred in a reversible process from state 1 to state 2 is given by

$$q_r = \int_1^2 T \, ds$$

The T-s diagram is simple rectangle for a Carnot cycle.

The area under the curve is

$$\oint Tds = \sum q_r = w$$

since
$$\oint du = 0$$

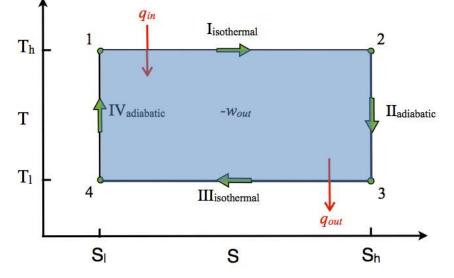


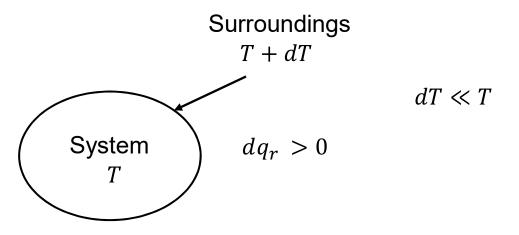
Figure 7.1 T-s diagram for a Carnot cycle [1]



The heat flow out of the surroundings at every point is equal in magnitude and opposite in sign to the heat flow into the system.

$$dq_{in} = dq_{out} = dq_r$$

For a reversible process, temperature of system and its surroundings are equal.





7.3 Entropy Change of the Surroundings (Reversible)

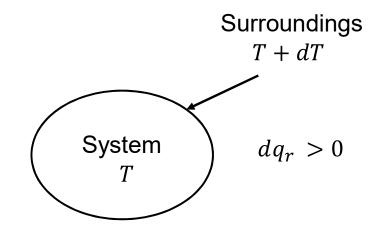
So,

$$\left(\frac{\delta q_r}{T+dT}\right)_{surroundings} \approx \left(\frac{\delta q_r}{T}\right)_{surroundings} = (\delta s)_{surroundings}$$

and from

 $ds_{system} + ds_{surroundings} = ds_{universe}$

$$|ds|_{surroundings} = -|ds|_{system} \quad \& \quad |ds|_{universe} = 0$$



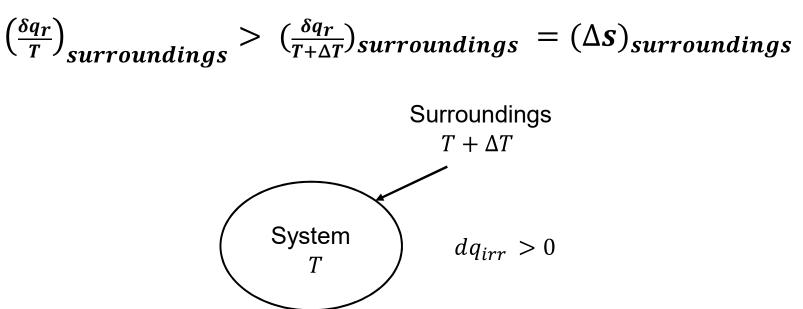


7.3 Entropy Change of the Surroundings (Irreversible)

However for an irreversible case,

 $\Delta T > 0$

and



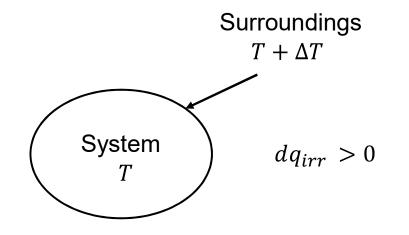


7.3 Entropy Change of the Surroundings (Irreversible)

So,

$$\Delta s_{system} + \Delta s_{surroundings} = \Delta s_{universe} > 0$$

(Entropy generation!)





7.4 Entropy Change for an Ideal Gas

With $du = c_v dT$, we have

$$\frac{q_r}{T} = \frac{c_v dT}{T} + \frac{P}{T} dv = ds$$

For a reversible process, For an ideal gas, P/T = R/v, so

$$ds = c_v \frac{dT}{T} + R \frac{dv}{v}$$

Integrating, we have

$$s_2 - s_1 = c_v \ln \left(\frac{T_2}{T_1}\right) + R \ln \left(\frac{v_2}{v_1}\right)$$



From the combined first and second laws, Tds = du + P dv

$$Tds = c_p dT - T \left(\frac{\partial v}{\partial T}\right)_p dP$$
 $(s = s(T, P))$

(*** Assignments**) Entropy can be expressed as a function of specific volume and pressure or temperature and specific volume. Prove the below two equations using Maxwell relations.

$$Tds = c_{p}\left(\frac{\partial T}{\partial v}\right)_{p} dv + c_{v}\left(\frac{\partial T}{\partial P}\right)_{v} dP \quad (s = s(v, P))$$
$$Tds = c_{v} dT + T\left(\frac{\partial P}{\partial T}\right)_{v} dv \qquad (s = s(T, v))$$



Let T and P be the independent variables .

The enthalpy is $h \equiv u + P v$ thus,

Tds = dh - vdP

$$= \left[\left(\frac{\partial h}{\partial T}\right)_P dT + \left(\frac{\partial h}{\partial P}\right)_T dP \right] - v dP$$
$$ds = \frac{1}{T} \left(\frac{\partial h}{\partial T}\right)_P dT + \frac{1}{T} \left[\left(\frac{\partial h}{\partial P}\right)_T - v \right] dP$$



With s = s(T, P), we have

$$ds = \left(\frac{\partial s}{\partial T}\right)_P dT + \left(\frac{\partial s}{\partial P}\right)_T dP$$
$$ds = \frac{1}{T} \left(\frac{\partial h}{\partial T}\right)_P dT + \frac{1}{T} \left[\left(\frac{\partial h}{\partial P}\right)_T - \nu\right] dP$$

Since *T* and *P* are independent, it follows that

$$(\frac{\partial s}{\partial T})_P = \frac{1}{T} (\frac{\partial h}{\partial T})_P$$
 and $(\frac{\partial s}{\partial P})_T = \frac{1}{T} [(\frac{\partial h}{\partial P})_T - v]$



The differential ds is exact. Therefore,

$$\begin{bmatrix}\frac{\partial}{\partial P}(\frac{\partial s}{\partial T})_P\end{bmatrix}_T = \frac{\partial^2 s}{\partial P \partial T} = \frac{\partial^2 s}{\partial T \partial P} = \begin{bmatrix}\frac{\partial}{\partial T}(\frac{\partial s}{\partial P})_T\end{bmatrix}_P$$

Substituting last two Equations from previous slide, we get

$$\frac{1}{T}\frac{\partial^2 h}{\partial P \partial T} = \frac{1}{T} \left[\frac{\partial^2 h}{\partial T \partial P} - \left(\frac{\partial v}{\partial T} \right)_P \right] - \frac{1}{T^2} \left[\left(\frac{\partial h}{\partial P} \right)_T - v \right]$$

$$\leftrightarrow \ (\frac{\partial h}{\partial P})_T = -T \ (\frac{\partial v}{\partial T})_P + v$$



For a reversible process
$$c_P = \left(\frac{\partial h}{\partial T}\right)_P$$

$$Tds = c_P dT - T \left(\frac{\partial v}{\partial T}\right)_P dP$$

Finally, since the coefficient of volume expansion $\beta = \frac{1}{v} \left(\frac{\partial v}{\partial T} \right)_{P}$, we have

 $Tds = c_P dT - T \, \nu \beta dP$

