

# 458.308 Process Control & Design

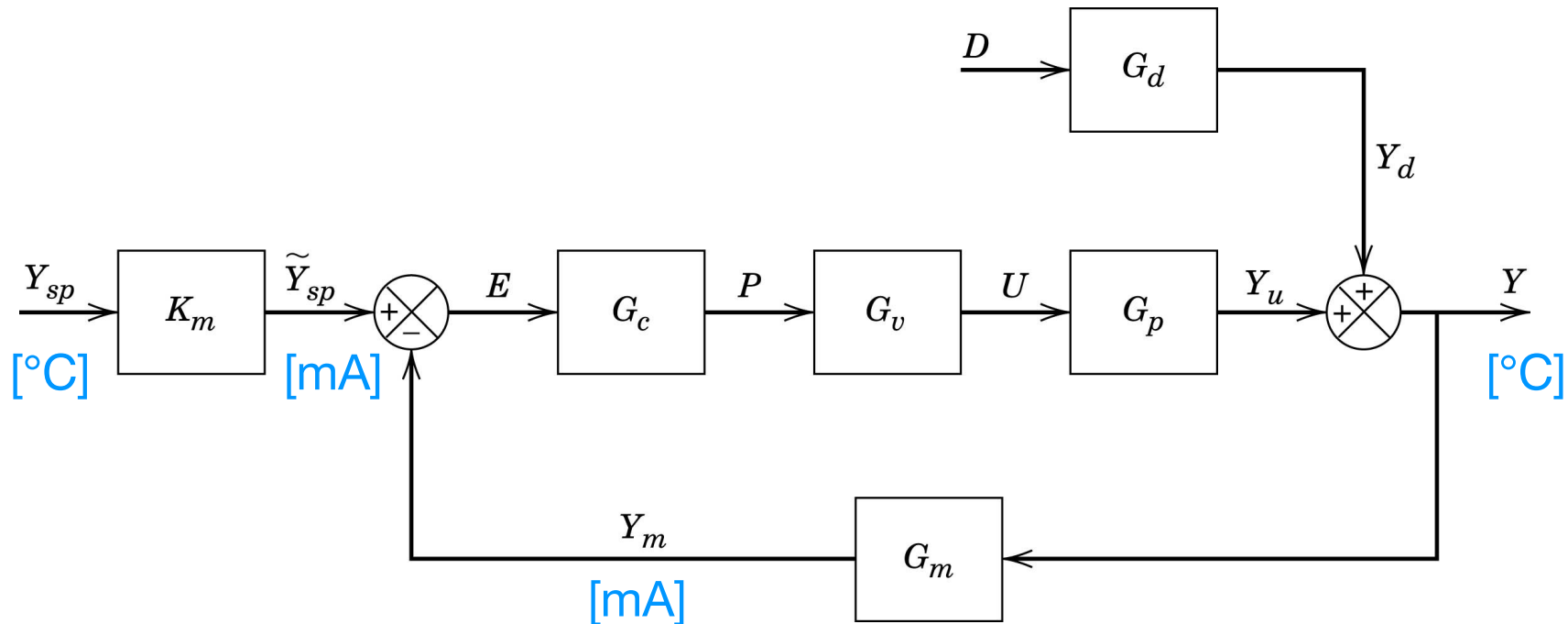
## Lecture 6: Dynamic Behavior and Stability of Closed-Loop Control Systems (Part 2)

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# General Expression of Feedback Control System

Ex) Heated Tank System



$K_m$ : Steady-state gain of \_\_\_\_\_

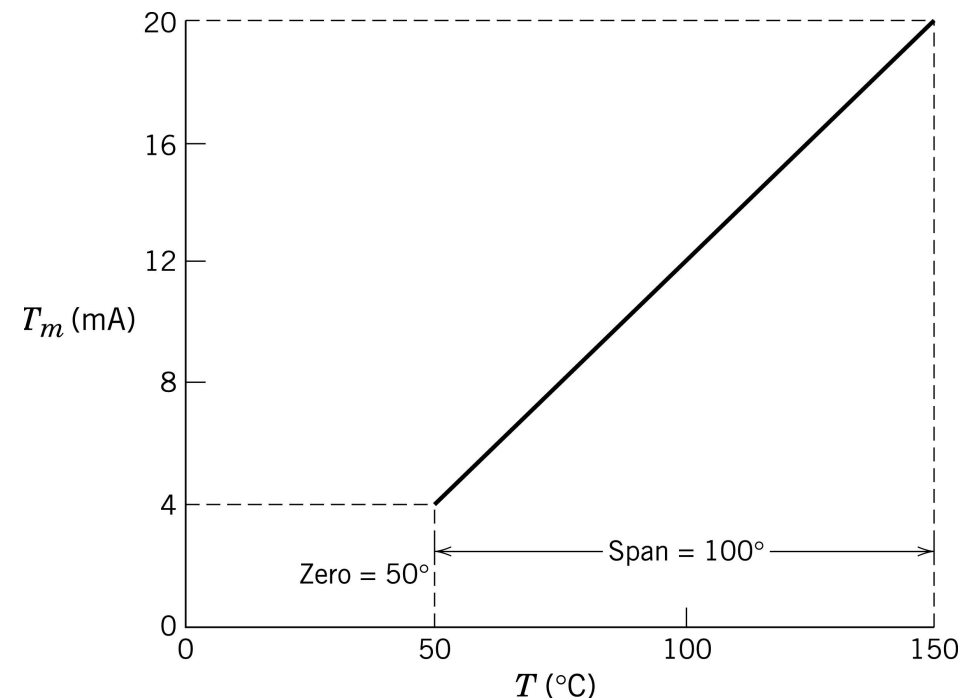
$Y_u$ : Change in  $Y$  due to \_\_\_\_\_

$Y_d$ : Change in  $Y$  due to \_\_\_\_\_

To simplify the notation, the primes and  $s$  dependence have been omitted; thus,  $Y$  is used rather than  $Y'(s)$

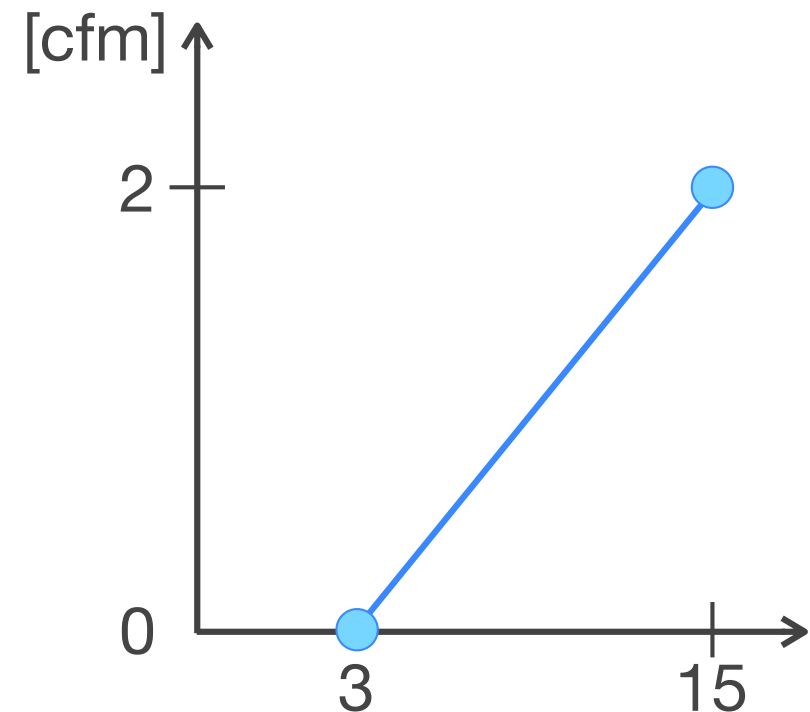
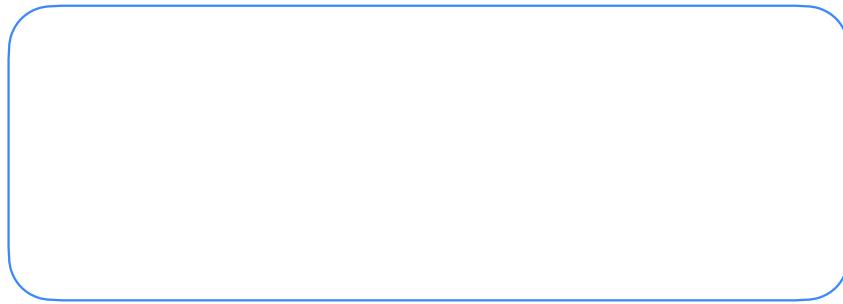
If the input range of a platinum resistance element (temp. sensor) is 50°C - 150°C is used with a standard transmitter, what is  $K_m$ ?

The standard transmitter output is 4 - 20mA

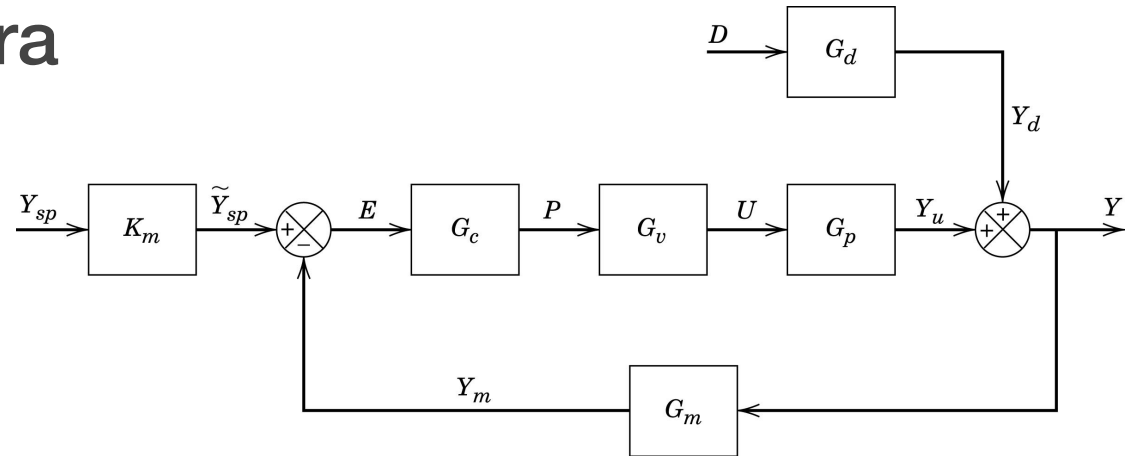


The flow rate through the valve ranges from 0 to 2 [cfm]. If the installed A-O valve exhibits linear characteristic with negligible dynamics what is  $G_v$ ?

The input to the control valve ranges from 3 to 15 psi.



# Transfer Function Algebra



$$Y = Y_u + Y_d = G_p U + G_d D$$

$$= G_p G_v G_c E + G_d D = G_p G_v G_c \left\{ \tilde{Y}_{sp} - Y_m \right\} + G_d D$$

$$= G_p G_v G_c \{ K_m Y_{sp} - G_m Y \} + G_d D$$

$$Y = \frac{K_m G_c G_v G_p}{1 + G_c G_v G_p G_m} Y_{sp} + \frac{G_d}{1 + G_c G_v G_p G_m} D$$

$$G_{OL} \triangleq G_c G_v G_p G_m : \text{_____ transfer function (relates } \tilde{Y}_{sp} \text{ to } Y_m \text{ )}$$

$$\text{Denominator} = 1 + G_{OL}$$

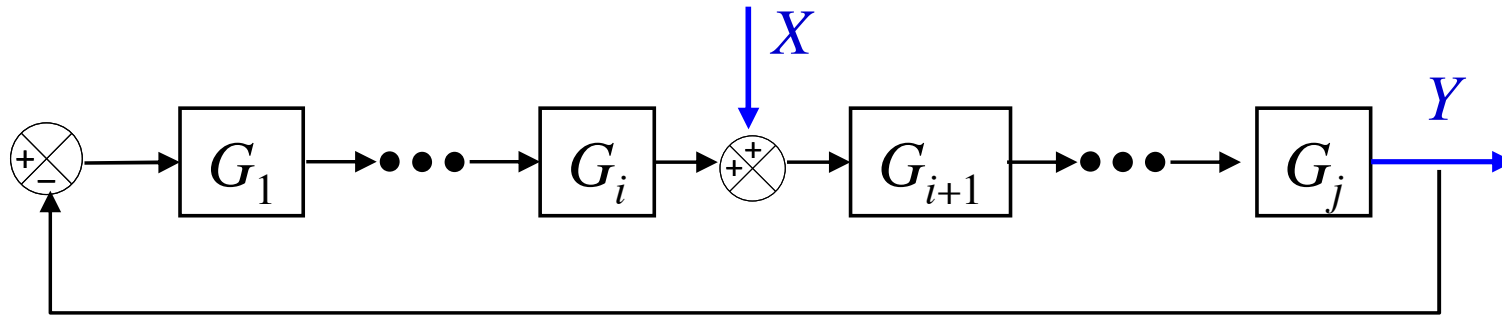
# Analysis and Design Problem

- **Analysis:** Given particular  $G$ 's and  $G_c$ 
  - Are the closed-loop dynamics stable?
  - Speed of response?
  - Damping?
  - Gains for  $Y/Y_{sp}$  and  $Y/D$
- **Design:** Given particular  $G$ 's, choose (“design”)  $G_c$  so that
  - the closed-loop dynamics are stable
  - $Y/Y_{sp}$  has a gain of  $\sim ( \quad )$  and  $Y/D$  has a gain of  $\sim ( \quad )$
  - the dynamics are sufficiently fast (but not too fast) and smooth (without excessive oscillation).

# Model Used for Analysis and Design

- Case 1 (Less Frequent)
  - From a fundamental model, perform linearization and Laplace transform of the linearized ODEs to find  $G_p(s)$  and  $G_d(s)$
  - Find actuator and measurement dynamics  $G_v$  and  $G_m$
- Case 2 (More Frequent)
  - The composite model  $G(= G_m G_p G_v)$  is fitted to data of  $y_m$  obtained by perturbing  $p$  (e.g., by making a step change)

# Calculation of Closed-Loop Functions: Generalization



$$\frac{Y(s)}{X(s)} = \frac{G_{i+1}G_{i+2} \cdots G_j}{1 + G_1G_2 \cdots G_j} = \frac{\Pi_f}{1 + \Pi_e}$$

Assume **negative** feedback

$\Pi_f$ : Product of the transfer functions in the forward path from  $X$  to  $Y$

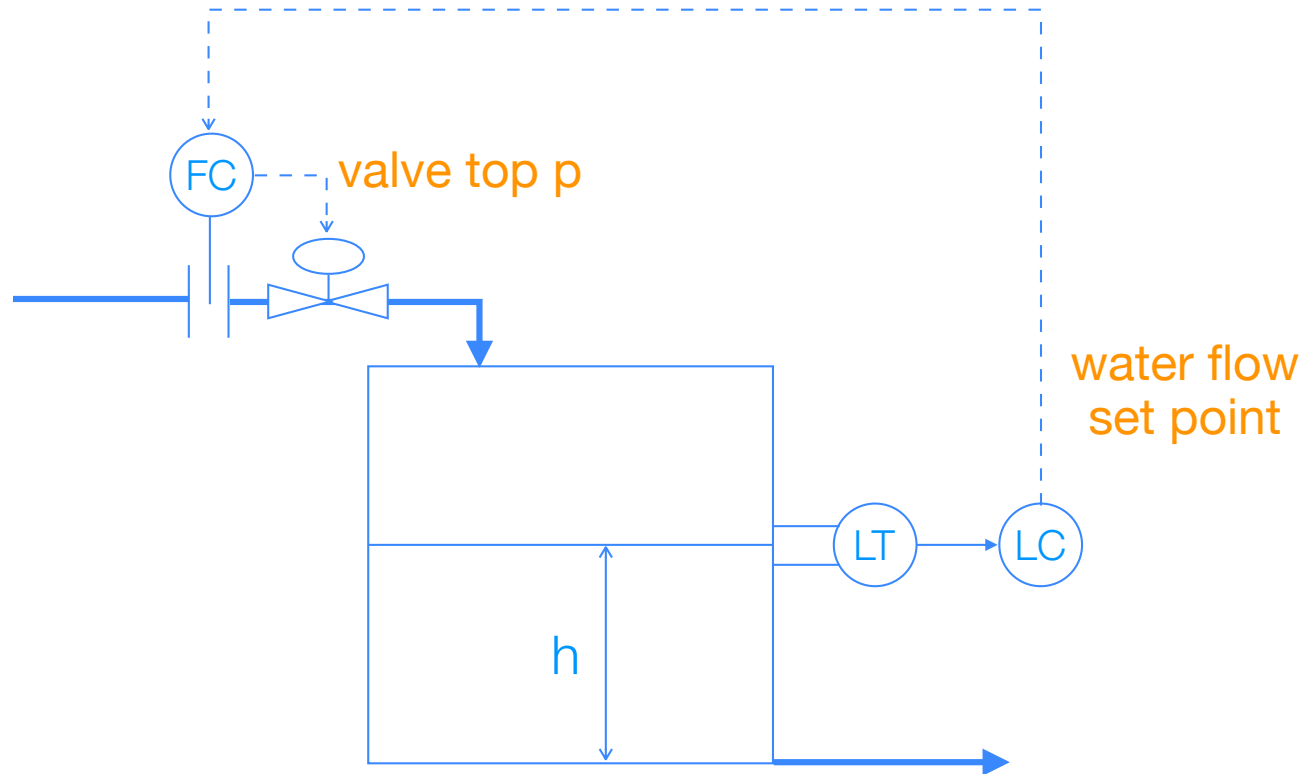
$\Pi_e$ : Product of every transfer function in the feedback loop

Check with slide p. 5



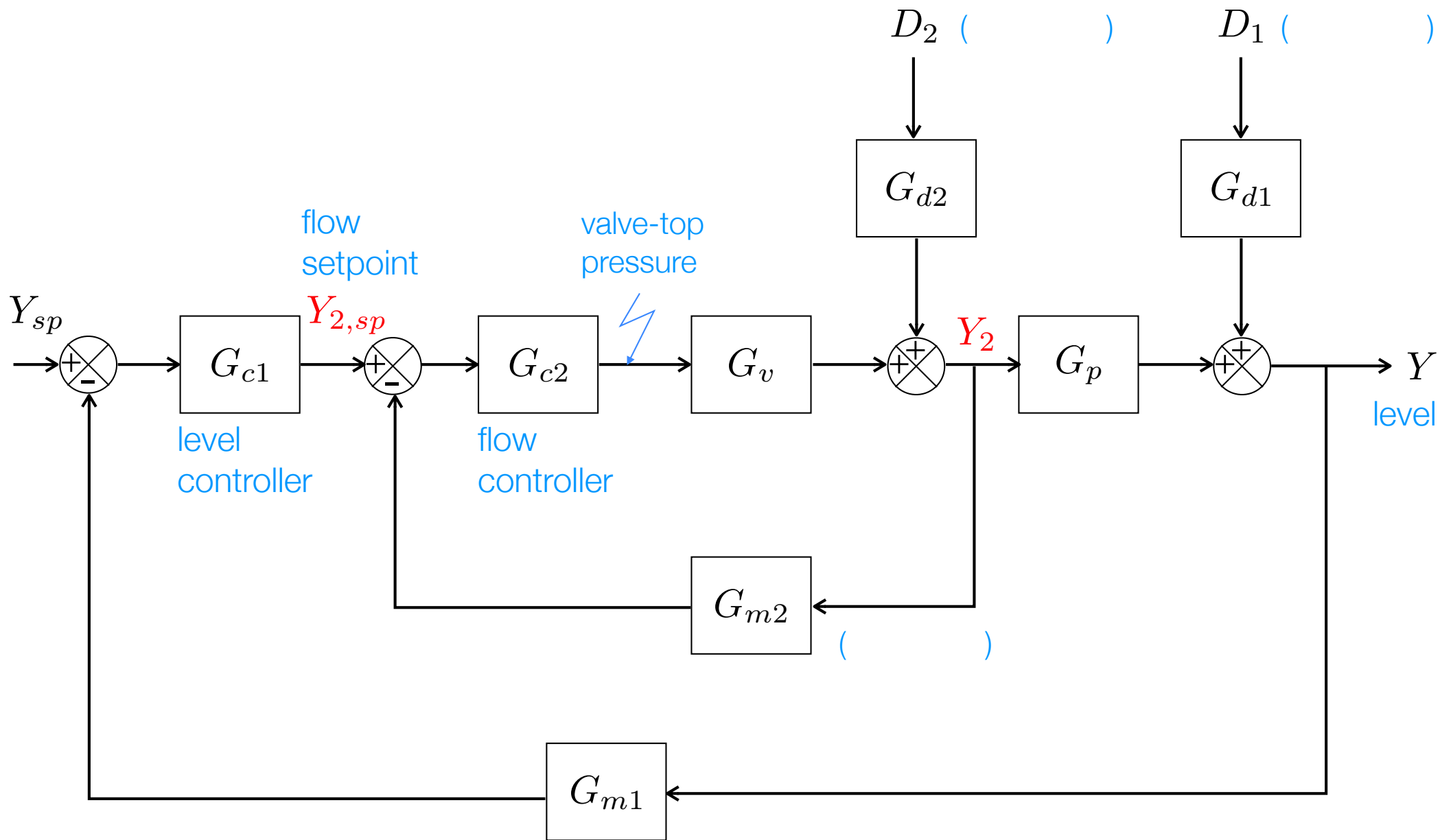
# Cascaded Loop

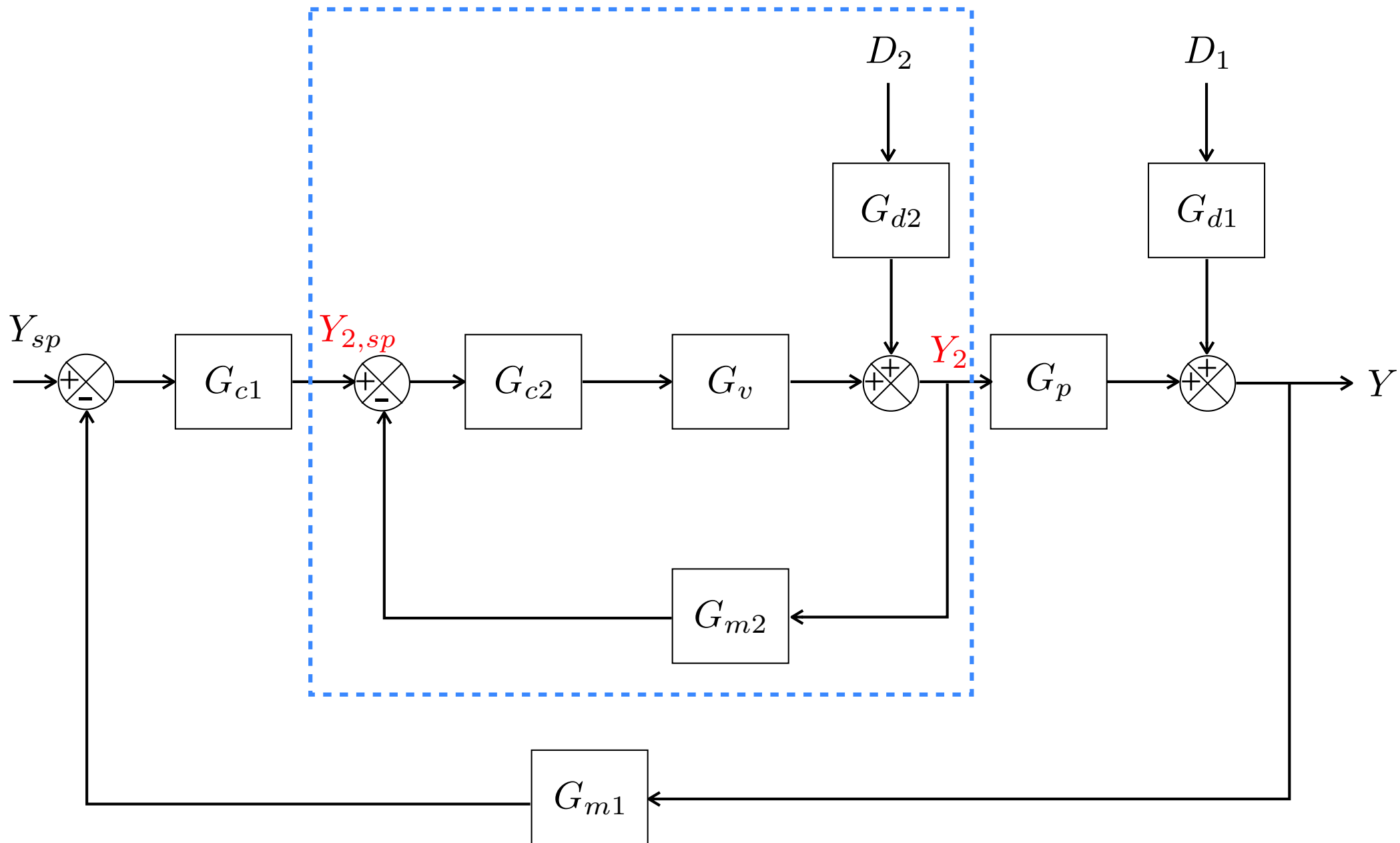
Multiple output measurements & a single manipulated input

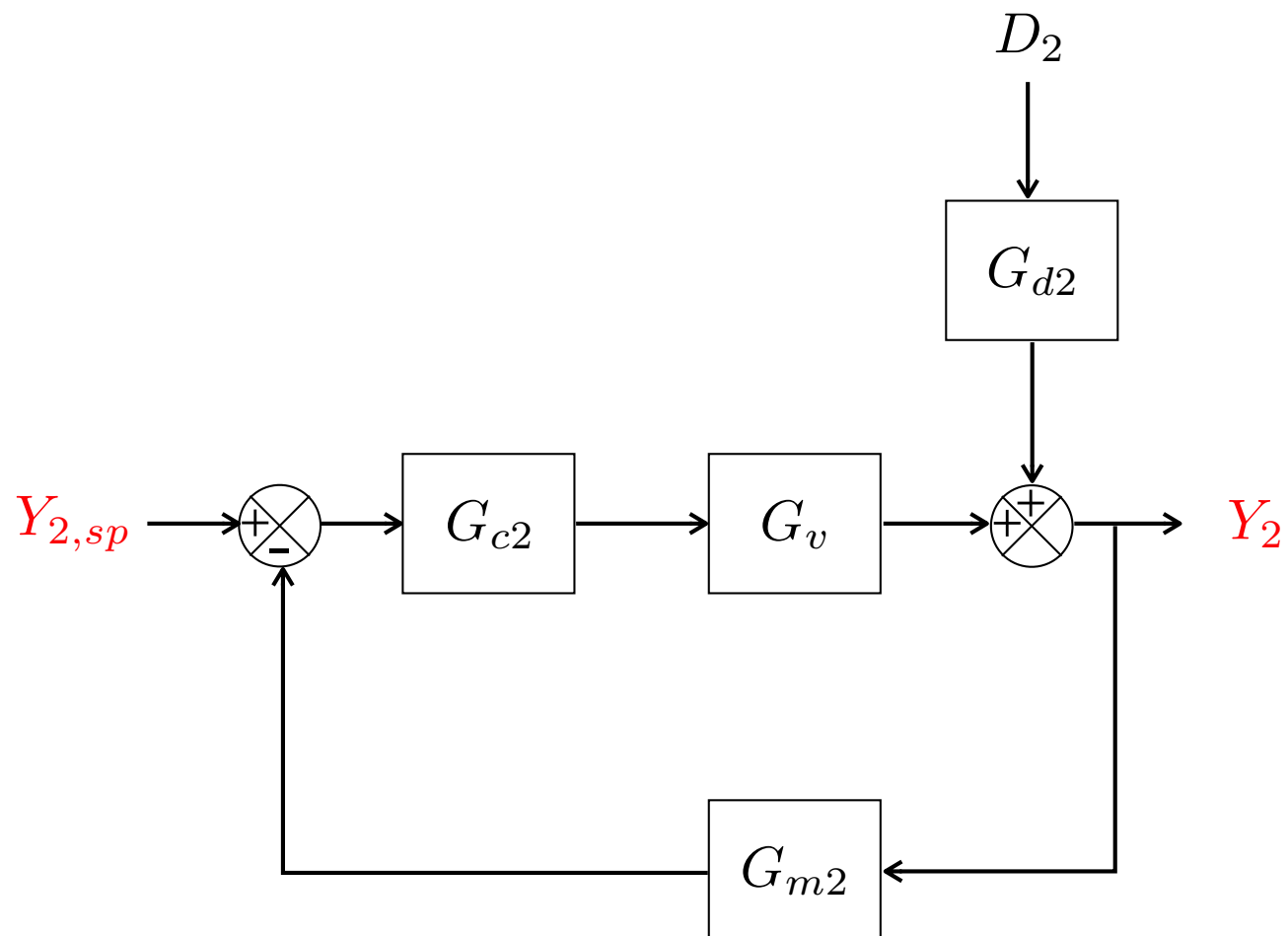


cascades the  
level controller to  
a water flow  
controller

- popularly used for flow control
- compensates for disturbances directly affecting a manipulated flow rate
- disturbance: water header pressure



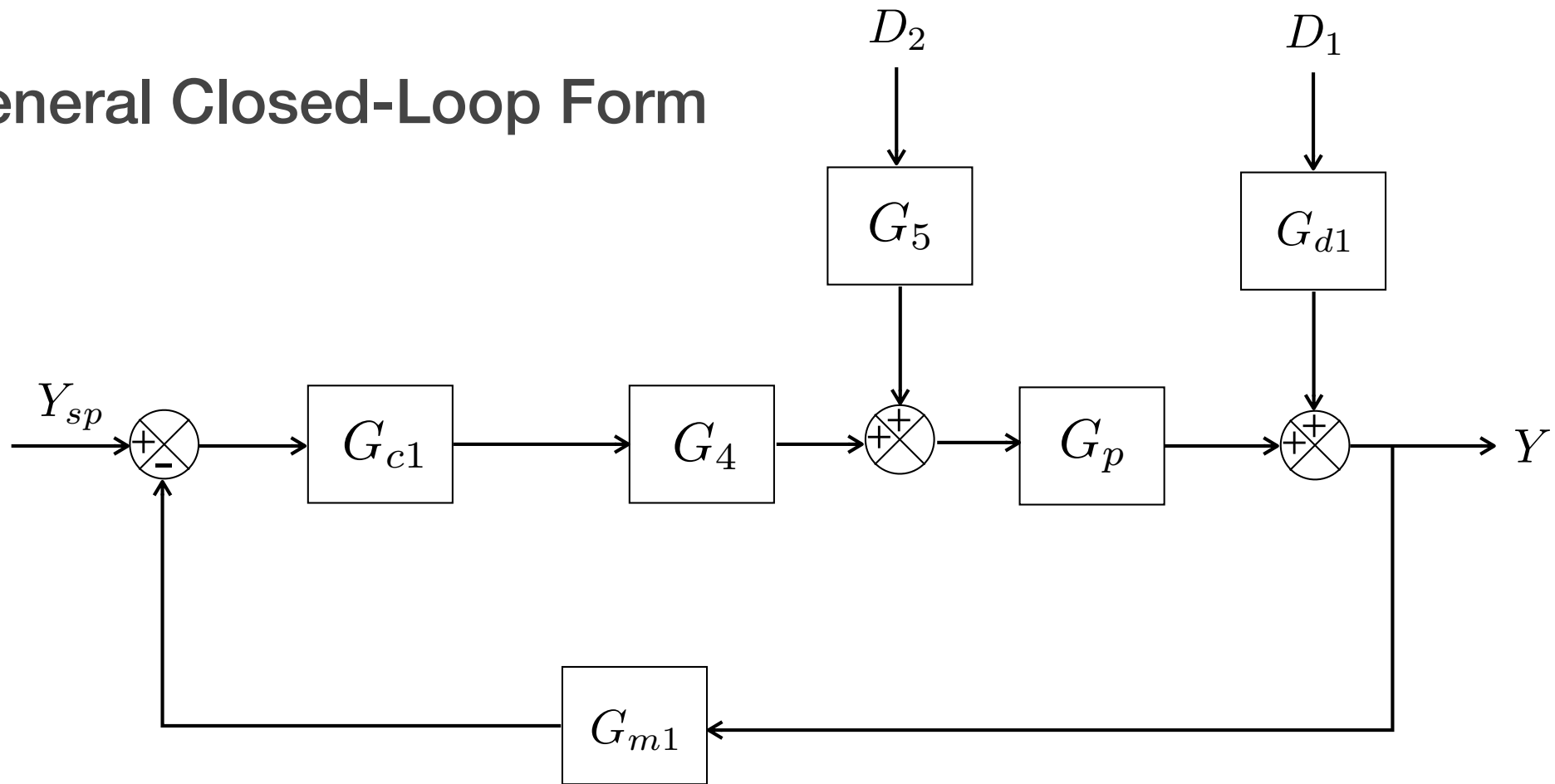




$$Y_2 = \boxed{\phantom{G_4}} Y_{2,sp} + \boxed{\phantom{G_5}} D_2$$

$G_4$   $G_5$

# General Closed-Loop Form



$$\begin{aligned} \frac{Y}{Y_{sp}} &= \frac{G_{c1}G_4G_p}{1 + G_{c1}G_4G_pG_{m1}} = \frac{G_{c1} \frac{G_{c2}G_v}{1+G_{c2}G_vG_{m2}} G_p}{1 + G_{c1} \frac{G_{c2}G_v}{1+G_{c2}G_vG_{m2}} G_p G_{m1}} \\ &= \frac{G_{c1}G_{c2}G_vG_p}{1 + G_{c2}G_vG_{m2} + G_{c1}G_{c2}G_vG_pG_{m1}} \end{aligned}$$

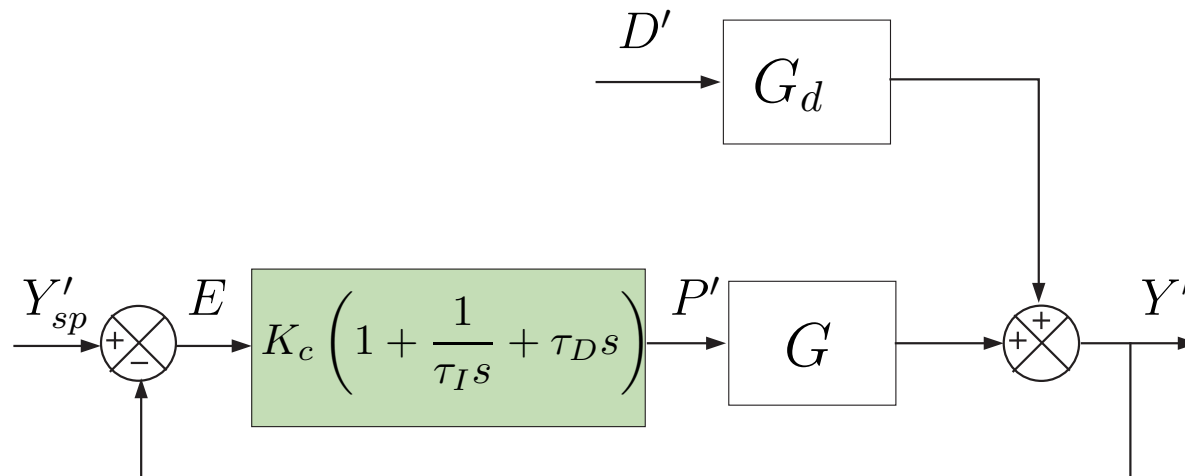
$$\frac{Y}{D_2}, \frac{Y}{D_1}?$$

# TF of PID Controller

$$p(t) = \bar{p} + K_c \left( e(t) + \frac{1}{\tau_I} \int_0^t e(t^*) dt^* + \tau_D \frac{de}{dt} \right)$$

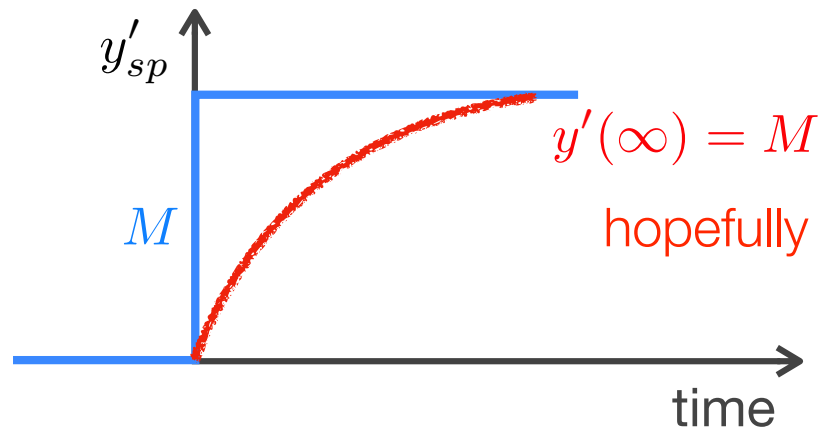
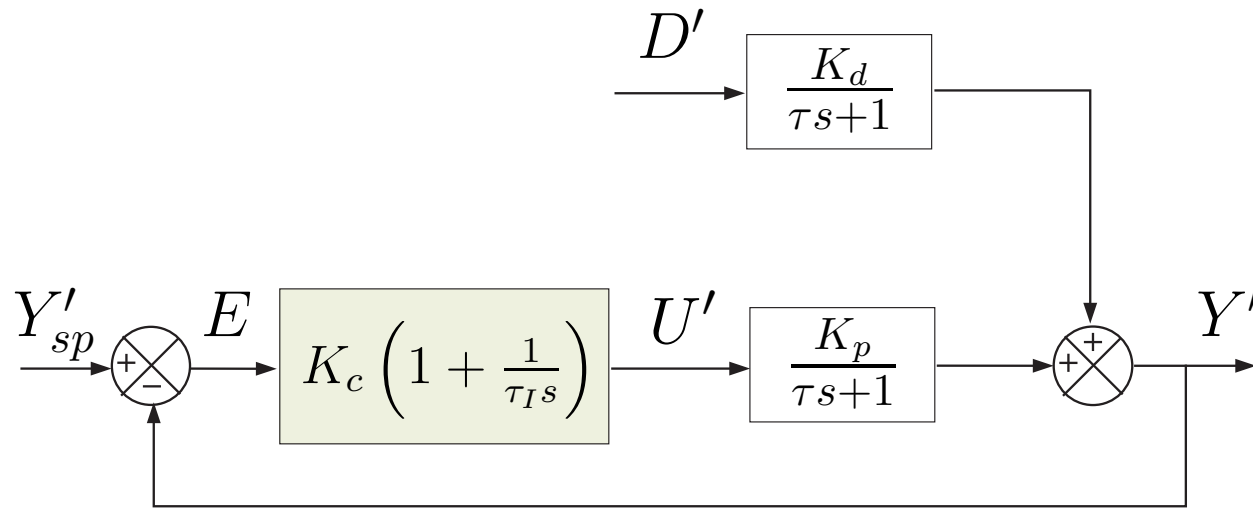
⇒ 
$$P'(s) = K_c \left( E(s) + \frac{1}{\tau_I s} E(s) + \tau_D s E(s) \right)$$

⇒ 
$$\frac{P'(s)}{E(s)} = K_c \left( 1 + \frac{1}{\tau_I s} + \tau_D s \right)$$



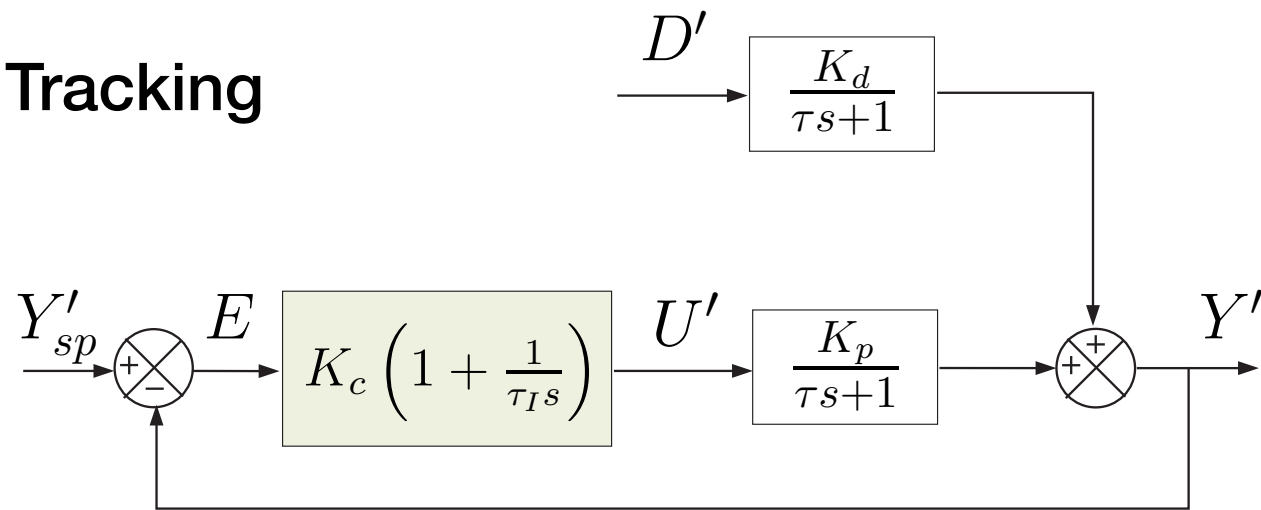
# Closed-Loop Responses of PI Control

Integral mode removes the offset



$$Y'_{sp}(s) = \frac{M}{s}$$

# Set point Tracking



$$\frac{Y'(s)}{Y'_{sp}(s)} = \frac{\frac{K_c K_p (\tau_I s + 1)}{\tau_I s (\tau s + 1)}}{1 + \frac{K_c K_p (\tau_I s + 1)}{\tau_I s (\tau s + 1)}} = \frac{K_c K_p (\tau_I s + 1)}{\tau_I s (\tau s + 1) + K_c K_p (\tau_I s + 1)}$$

$$Y'(s) = \frac{K_c K_p (\tau_I s + 1)}{\tau_I s (\tau s + 1) + K_c K_p (\tau_I s + 1)} \cdot \frac{M}{s}$$

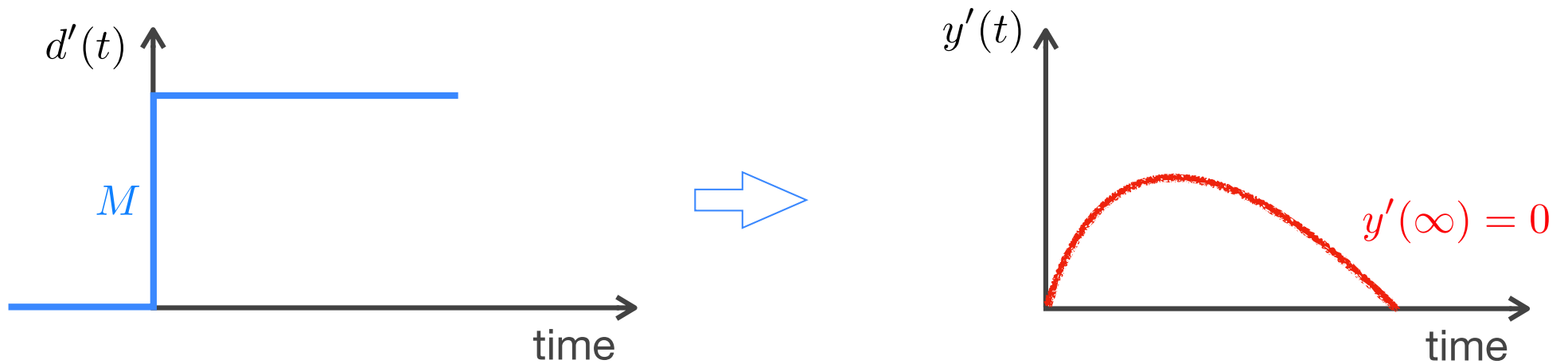
If the closed-loop system is stable,

$$y'(\infty) = \lim_{s \rightarrow 0} \{s \cdot Y'(s)\} = \frac{K_c K_p}{K_c K_p} \cdot M = M \quad (\text{Gain} = 1)$$

$$\text{offset} = y'_{sp}(\infty) - y'(\infty) = M - M = 0$$



# Disturbance Rejection



$$\frac{Y'(s)}{D'(s)} = \frac{K_d/(\tau s + 1)}{1 + K_c \left(1 + \frac{1}{\tau_I s}\right) \left(\frac{K_p}{\tau s + 1}\right)}$$

$$Y'(s) = \frac{K_d \tau_I s}{\tau_I \tau s^2 + (\tau_I + K_p K_c \tau_I) s + K_c K_p} \cdot \frac{M}{s} \quad (\text{Gain} = 0)$$

If the closed-loop system is stable,

$$y'(\infty) = \lim_{s \rightarrow 0} \{s Y'(s)\} = 0 \quad \text{No offset}$$

# Closed-Loop Stability

## Characteristic Equation

$$1 + G_{OL} = 0$$

Roots of the above equation are the **poles of the closed-loop functions** (important information for analyzing closed-loop dynamics)

For stability, make sure all the roots are in the Left-Half-Plane (negative real parts)

- can be checked by **Routh's test**
- or by **direct substitution**

Note: Poles of the systems higher than 2<sup>nd</sup>-order are difficult to find

# Routh's Test

Determining whether any of the roots are positive (unstable) without calculating the roots

## Setting up the Routh Array

$$a_n s^n + a_{n-1} s^{n-1} + \cdots + a_1 s + a_0 = 0 \quad (\Leftrightarrow 1 + G_{OL} = 0)$$

i) Make  $a_n > 0$

ii) A necessary condition for stability

: All of the coefficients ( $a_n, \dots, a_0$ ) must be positive. If any coef. is negative or zero, at least one root lies to the right of, or on, the imaginary axis

If all the  $a_i$ 's are positive, construct Routh Array

### iii) Construct Routh Array

Row				
1	$a_n$	$a_{n-2}$	$a_{n-4}$	$\dots$
2	$a_{n-1}$	$a_{n-3}$	$a_{n-5}$	$\dots$
3	$b_1$	$b_2$	$b_3$	
4	$c_1$	$c_2$	$c_3$	
$\vdots$				
$n+1$				

$$b_1 = \frac{a_{n-1}a_{n-2} - a_n a_{n-3}}{a_{n-1}}$$

$$c_1 = \frac{b_1 a_{n-3} - b_2 a_{n-1}}{b_1}$$

•  
•  
•

$$b_2 = \frac{a_{n-1}a_{n-4} - a_n a_{n-5}}{a_{n-1}}$$

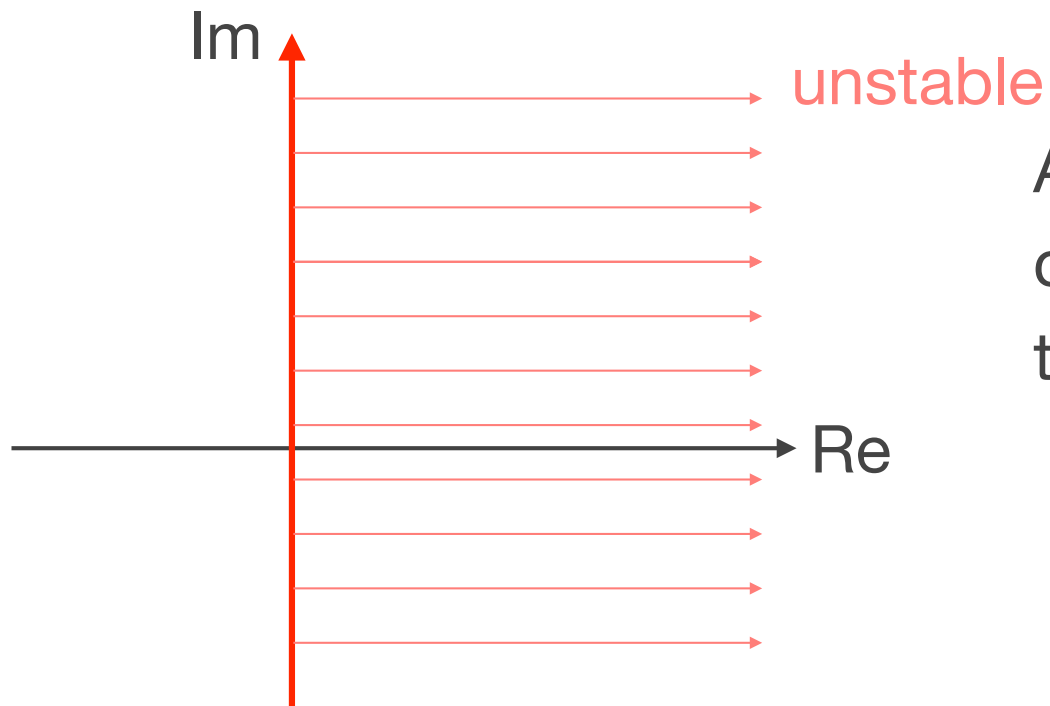
$$c_2 = \frac{b_1 a_{n-5} - b_3 a_{n-1}}{b_1}$$

All the coefficients in the first column are positive  $\longrightarrow$  all the poles are negative.

Find the upper bound on  $K_c$  (P-controller) for closed-loop stability of

$$G_p(s) = \frac{1}{(3s + 1)(2s + 1)(s + 1)} = \frac{1}{6s^3 + 11s^2 + 6s + 1}$$

# Direct Substitution



At the limits of instability, the closed-loop poles will be on the imaginary axis

$$1 + G_{OL} = 0 \quad (s = j\omega)$$



This method works with a system with time delay.  
Routh's method does not

$$6s^3 + 11s^2 + 6s + 1 + K_c = 0$$

$$6(j\omega)^3 + 11(j\omega)^2 + 6(j\omega) + 1 + K_c = 0$$

$$(1 + K_c - 11\omega^2) + 6(-\omega^3 + \omega)j = 0$$