

- $\tau = 0$ (frictionless)
- no heat, work.
- very small CV.

streamtube, CV, fixed.

$dz = ds \cdot \sin\theta$

$dW = \rho g dV$

Vol. of CV. ($\equiv A \cdot ds$)

• mass conservation.

$\frac{d}{dt} \int_{CV} \rho dV + \dot{m}_{out} - \dot{m}_{in} = 0$

$\dot{m}_{out} = \dot{m}_{in} + d\dot{m}$
 $d\dot{m} = d(\rho AV)$

$$\rightarrow \frac{\partial p}{\partial t} \cdot dV + d\dot{m} = 0.$$

$$d\dot{m} = d(\rho AV) = -\frac{\partial \rho}{\partial t} \cdot dV \approx -\frac{\partial \rho}{\partial t} \cdot A \cdot ds.$$

· m-tm conservation (in s-direction)

$$\Sigma F_s = \frac{\partial}{\partial t} \int_{CV} \rho V_s dV + \int_{CS} \rho V_s (\underline{v} \cdot \underline{n}) dA.$$

① gravity: $dF_{s, \text{grav}} = - \underline{dW} \cdot \sin \theta$

$$= - \rho g A \cdot ds \cdot \sin \theta.$$

② pressure: $dF_{s, \text{press}} = p \cdot A - (p + dp)(A + dA) + (p + \frac{1}{2} dp) dA.$

$$\approx -A \cdot dp.$$

③ ~~viscous stress.~~

$$\frac{\partial}{\partial t} \int_{CV} \rho \cdot V_s \, dV \approx \frac{\partial}{\partial t} (\rho V_s) \cdot \underbrace{dV}_{A \, ds} \approx \frac{\partial}{\partial t} (\rho V_s) \cdot A \, ds$$

$$\int_{CS} \rho V_s (\underline{V} \cdot \underline{n}) \, dA = (\dot{m} + d\dot{m})(V_s + dV_s) - \dot{m} V_s$$

$$= \dot{m} dV_s + V_s \cdot d\dot{m}$$

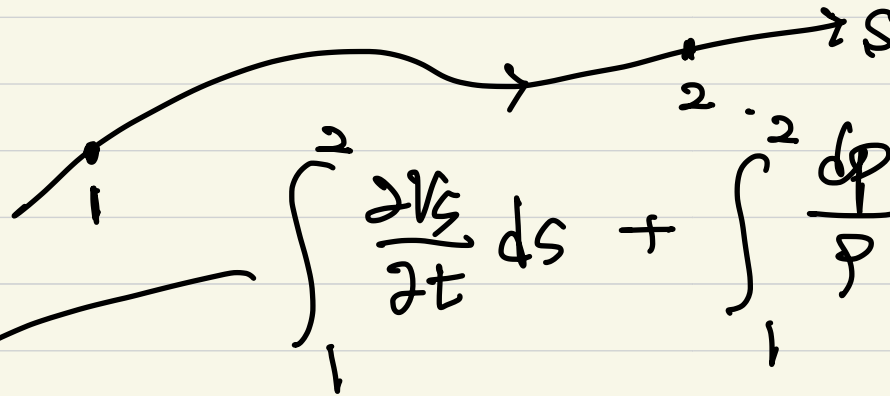
$$\Rightarrow \underbrace{-\rho g A \, ds \cdot \sin \theta - A \, dp}_{= dz} = \frac{\partial}{\partial t} (\rho V_s) A \, ds + \dot{m} dV_s + \underbrace{V_s \cdot d\dot{m}}_{= -\frac{\partial \rho}{\partial t} A \, ds \cdot V_s}$$

$$= \frac{\partial \rho}{\partial t} V_s A \, ds + \frac{\partial V_s}{\partial t} \cdot \rho \cdot A \cdot ds$$

$$\left(-A \, dp - \rho g A \, dz = \frac{\partial V_s}{\partial t} \rho A \, ds + \rho V_s \cdot A \cdot dV_s \right) / \rho A$$

$$\Rightarrow \frac{\partial V_s}{\partial t} \, ds + \frac{dp}{\rho} + V_s \cdot dV_s + g \, dz = 0$$

Bernoulli eq. for unsteady frictionless flow
along a streamline.



The diagram shows a curved streamline with an arrow indicating the direction of flow. Two points, labeled 1 and 2, are marked on the streamline. A coordinate s is shown at the end of the streamline, pointing in the direction of flow.

$$\int_1^2 \frac{\partial V_s}{\partial t} ds + \int_1^2 \frac{dp}{\rho} + \frac{1}{2} (V_2^2 - V_1^2) + g(z_2 - z_1) = 0$$

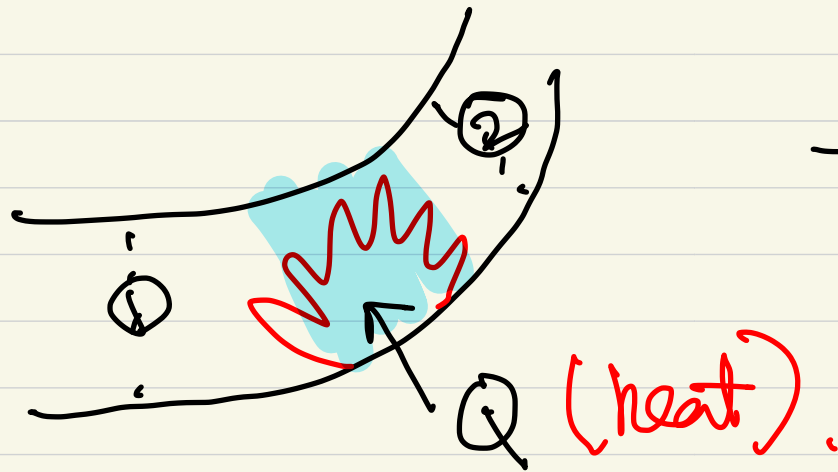
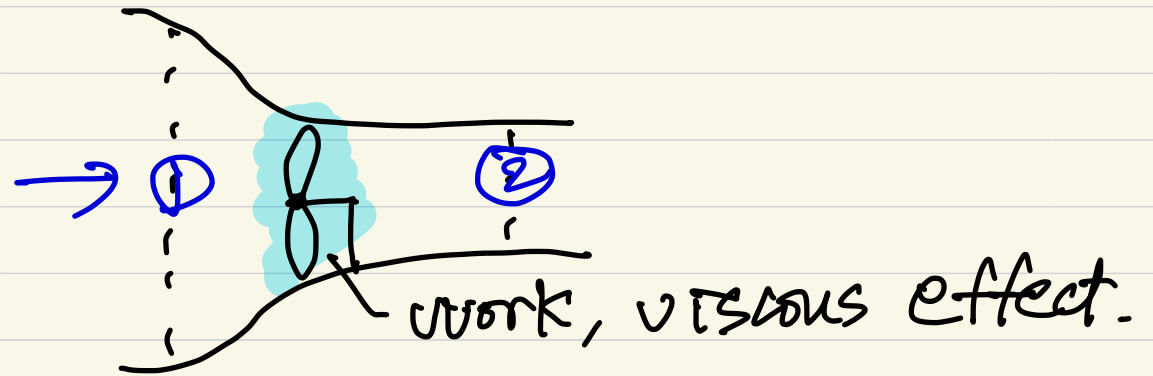
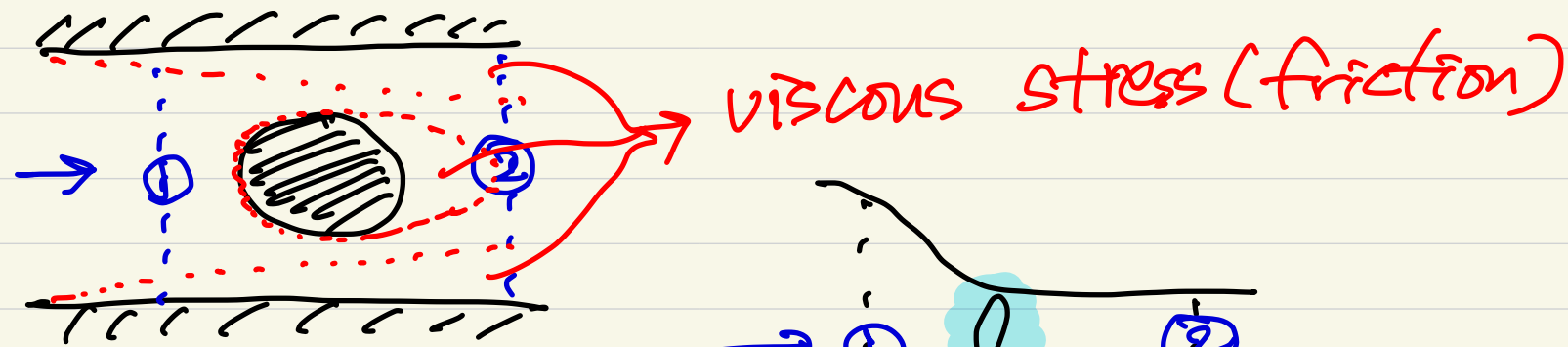
- for steady, incompressible flow

$$\frac{1}{\rho} (P_2 - P_1) + \frac{1}{2} (V_2^2 - V_1^2) + g(z_2 - z_1) = 0.$$

$$\frac{P_1}{\rho} + \frac{1}{2} V_1^2 + g z_1 = \frac{P_2}{\rho} + \frac{1}{2} V_2^2 + g z_2.$$

(Bernoulli eq. for steady, frictionless, incompressible flow along a streamline).

• We assumed no heat, no work, no friction.



$$\Rightarrow \frac{P_1}{\rho} + \frac{1}{2} V_1^2 + \rho z_1 = \frac{P_2}{\rho} + \frac{1}{2} V_2^2 + \rho z_2 + \underbrace{W_s + W_f}_{\text{friction loss}} - \underbrace{W_q}_{\text{heat}}$$

shaft work

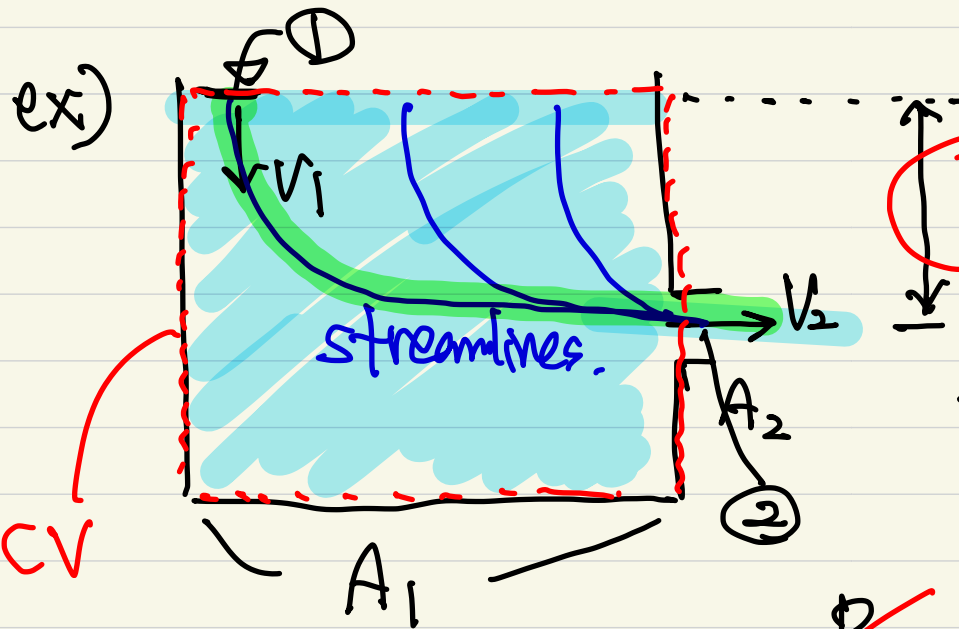
$$\frac{P_1}{\rho g} + \frac{V_1^2}{2g} + z_1 = \frac{P_2}{\rho g} + \frac{V_2^2}{2g} + z_2 + h_s + h_f - h_q$$

work head / heat head

friction head
dimension of length.

for ideal conditions.

$$\frac{P}{\rho g} + \frac{V^2}{2g} + z = \text{constant} = h_0 \text{ (total head)}$$



steady, frictionless.

$$A_1 \gg A_2, V_2 = ?$$

from Bernoulli eq.
(along the streamline).

~~$$\frac{P_1}{\rho} + \frac{1}{2} V_1^2 + g z_1 = \frac{P_2}{\rho} + \frac{1}{2} V_2^2 + g z_2.$$~~

$$z_1 - z_2 = h.$$

$$\Rightarrow \frac{1}{2} V_1^2 + g h = \frac{1}{2} V_2^2$$

• from continuity, (mass conservation)

$$\cancel{\rho} A_1 V_1 = \cancel{\rho} A_2 V_2 \rightarrow V_1 = \frac{A_2}{A_1} V_2$$

$$\therefore V_2^2 = \frac{2gh}{1 - (A_2/A_1)^2} \approx 2gh, \quad V_2 \approx \sqrt{2gh}$$

• How about the unsteady condition?

$$h = h(t), \quad V_2 = V_2(t)$$

$$\frac{\partial \psi}{\partial t} ds + \frac{dp}{\rho} + V_s dV_s + g dz = 0$$

$$\rightarrow \int_1^2 \frac{\partial \psi}{\partial t} ds + \frac{1}{\rho} (\underline{p_2} - \underline{p_1}) + \frac{1}{2} (V_2^2 - V_1^2) + g (\underline{z_2 - z_1}) = 0$$

$$\approx \int_1^2 \frac{\partial V_1}{\partial t} ds \stackrel{=}{=} \frac{\partial V_1}{\partial t} \cdot h + \text{mass conservation } (A_1 V_1 = A_2 V_2)$$

$$\rightarrow 2h \frac{A_2}{A_1} \cdot \frac{dV_2}{dt} + V_2^2 \left(1 - \frac{A_2^2}{A_1^2} \right) = 2gh$$

Coupled. $\leftarrow \frac{dh}{dt} = -V_1 = -\frac{A_2}{A_1} V_2.$

3.6. Angular momentum Theorem.

in RTT, $\underline{B} = \underline{H}_0 = \int_{\text{sys}} (\underline{r} \times \underline{v}) dm.$

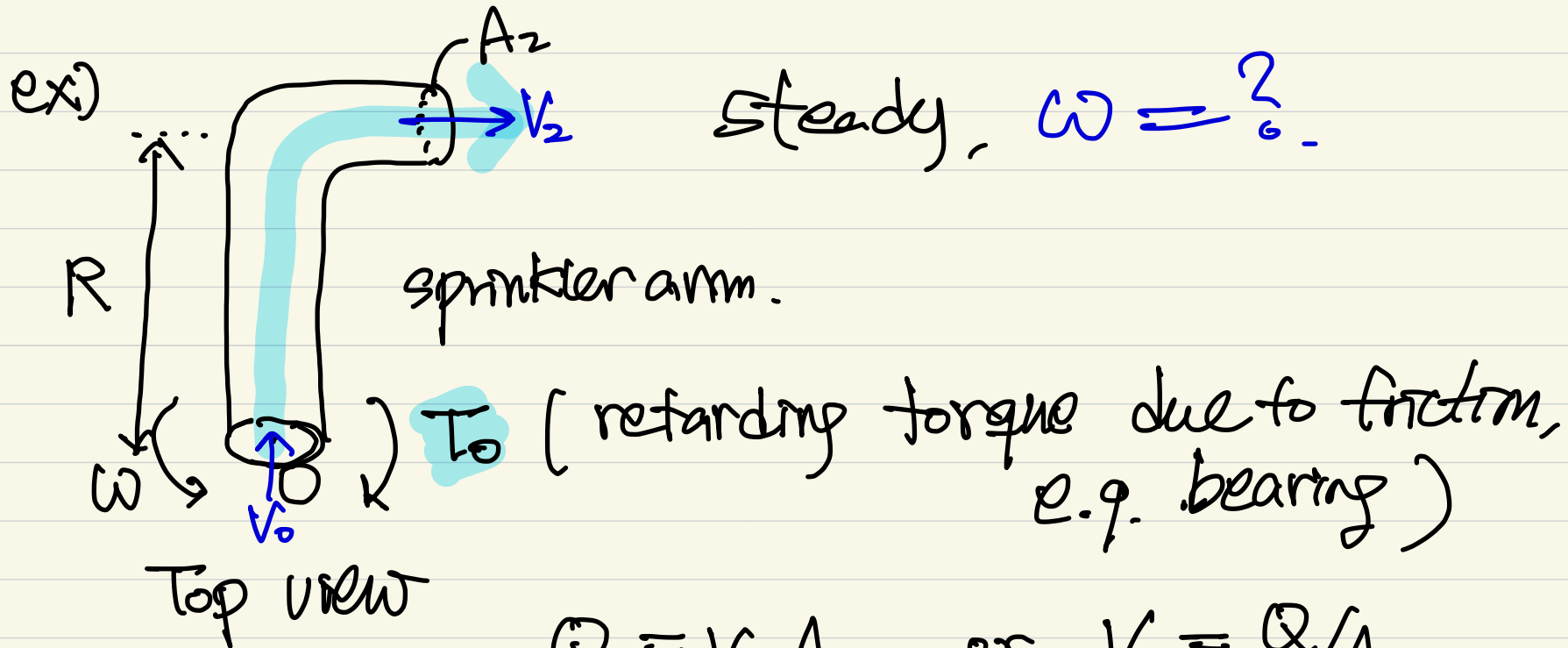
angular momentum vector.

$$\underline{\beta} = \frac{d\underline{B}}{dm} = \underline{r} \times \underline{v}.$$

$$\underbrace{\frac{dH_0}{dt}}_{\text{sys}} = \underbrace{\frac{d}{dt} \int_{CV} \rho (\underline{r} \times \underline{v}) dV}_{CV} + \int_{CS} (\underline{r} \times \underline{v}) \rho (\underline{v}_r \cdot \underline{n}) dA.$$

$$\sum \underline{M}_o = \sum (\underline{r} \times \underline{F})_o.$$

moment



$$\left. \begin{aligned} Q &= V_0 A_2 \quad \text{or} \quad V_0 = Q/A_2. \\ V_2 &= V_0 - R\omega. \end{aligned} \right\}$$

$$\begin{aligned} \odot \sum \underline{M}_o &= T_0 = \underline{\dot{m}} (\underline{r} \times \underline{V})_{out} - \cancel{\underline{\dot{m}} (\underline{r} \times \underline{V})_{in}}. \\ &= \rho Q R V_2 = \rho Q R (V_0 - R\omega). \end{aligned}$$

$$\therefore \omega = \frac{V_0}{R} - \frac{T_0}{\rho Q R^2}$$

3.7 Energy equation.

$$\beta = E, \quad \beta = \frac{d\beta}{dm} = e = e_{\text{internal}} + e_{\text{kinetic}} + e_{\text{potential}} + \dots$$

RTT

$$\Rightarrow \frac{dQ}{dt} - \frac{dW}{dt} = \frac{dE}{dt} = \frac{d}{dt} \int_{CV} \rho e dt + \int_{CS} \rho e (\underline{V} \cdot \underline{n}) dA$$

(heat transfer, applied FM, ...)

Ch. 4 Differential relations for fluid flow.

↳ infinitesimally small CV.

→ differential eq. (+ boundary / initial conditions)

↓
Solutions ← velocity, pressure, Temperature.

4.1. Acceleration field of a fluid.

$$\underline{V} = u \hat{i} + v \hat{j} + w \hat{k}$$

$$u = u(x, y, z, t)$$

$$v = v(x, y, z, t)$$

$$w = w(x, y, z, t)$$

$$\underline{a} = \frac{D\underline{V}}{Dt} = \frac{\partial \underline{V}}{\partial t} + \frac{\partial \underline{V}}{\partial x} \frac{\partial x}{\partial t} + \frac{\partial \underline{V}}{\partial y} \frac{\partial y}{\partial t} + \frac{\partial \underline{V}}{\partial z} \frac{\partial z}{\partial t}$$

↳ material (total) derivative.

$$= \frac{\partial \underline{V}}{\partial t} + \left[u \frac{\partial \underline{V}}{\partial x} + v \frac{\partial \underline{V}}{\partial y} + w \frac{\partial \underline{V}}{\partial z} \right]$$

$$\underline{V} = (u, v, w)$$

$$\nabla = \left(\frac{\partial}{\partial x}, \frac{\partial}{\partial y}, \frac{\partial}{\partial z} \right)$$

$$\underline{V} \cdot \nabla = \left(u \frac{\partial}{\partial x}, v \frac{\partial}{\partial y}, w \frac{\partial}{\partial z} \right)$$

$$\rightarrow = \frac{\partial \underline{V}}{\partial t} + (\underline{V} \cdot \nabla) \underline{V}$$

local acceleration.
(@ steady, zero)

convective acceleration.

4.2 Differential eq. of mass conservation.

in cartesian coordinate.

$$0 = \frac{dm}{dt} = \frac{\partial}{\partial t} \int_{CV} \rho dV + \sum_i (\rho_i A_i V_i)_{out} - \sum_i (\rho_i A_i V_i)_{in}$$

$$\approx \frac{\partial \rho}{\partial t} \cdot dx dy dz$$

Taylor series expansion.

$$\begin{aligned}
 & \rho w \left(\rho w dz dx + \rho w dx dy + \frac{\partial}{\partial z} (\rho w dx dy) dz \right) \\
 & \rho u dy dz + \frac{\partial}{\partial x} (\rho u dy dz) dx + \cancel{\rho w dx dy} \\
 & \rho v dz dx + \frac{\partial}{\partial y} (\rho v dz dx) dy
 \end{aligned}$$

$$\begin{aligned}
 (*) : 0 &= \frac{\partial \rho}{\partial t} dx dy dz \\
 &+ \cancel{\rho u dy dz} + \frac{\partial}{\partial x} (\rho u dy dz) dx \\
 &+ \cancel{\rho v dz dx} + \frac{\partial}{\partial y} (\rho v dz dx) dy \\
 &+ \cancel{\rho w dx dy} + \frac{\partial}{\partial z} (\rho w dx dy) dz \\
 &- \cancel{\rho u dy dz} - \cancel{\rho v dz dx} - \cancel{\rho w dx dy}
 \end{aligned}$$

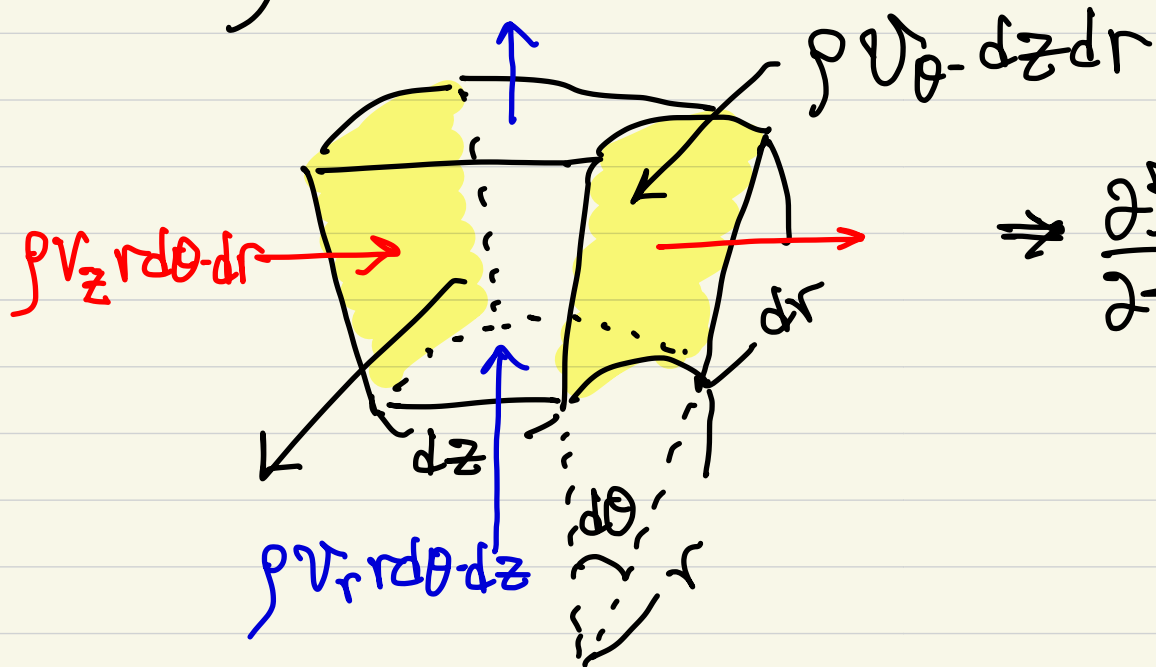
$$\therefore \frac{\partial \rho}{\partial t} + \frac{\partial}{\partial x} (\rho u) + \frac{\partial}{\partial y} (\rho v) + \frac{\partial}{\partial z} (\rho w) = 0$$



: continuity eq. (보존 방정식)

$$\frac{\partial \rho}{\partial t} + \nabla \cdot (\rho \underline{V}) = 0 \quad \leftarrow$$

in cylindrical coordinate (r, θ, z) .



$$\Rightarrow \frac{\partial \rho}{\partial t} + \frac{1}{r} \frac{\partial}{\partial r} (r \rho V_r) + \frac{1}{r} \frac{\partial}{\partial \theta} (\rho V_\theta) + \frac{\partial}{\partial z} (\rho V_z) = 0.$$

• Steady flow $(\frac{\partial}{\partial t} (\cdot) = 0)$: $\nabla \cdot (\rho \underline{V}) = 0$.

• incompressible flow ($\rho = \text{constant}$) : $\nabla \cdot \underline{V} = 0$.

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} + \frac{\partial w}{\partial z} = 0.$$

$$\left(\frac{1}{r} \frac{\partial}{\partial r} (r v_r) + \frac{1}{r} \frac{\partial v_\theta}{\partial \theta} + \frac{\partial v_z}{\partial z} = 0 \right)$$

Condition for incompressibility?

$$\frac{\partial}{\partial x} (\rho u) = \rho \frac{\partial u}{\partial x} + u \frac{\partial \rho}{\partial x} \Rightarrow \left| \rho \frac{\partial u}{\partial x} \right| \gg \left| u \frac{\partial \rho}{\partial x} \right|$$

상대변화량

$$\left| \rho \frac{du}{dx} \right| \gg \left| u \frac{d\rho}{dx} \right| \Rightarrow \left| \frac{du}{u} \right| \gg \left| \frac{d\rho}{\rho} \right| \quad (1)$$

speed of sound, (a).

$$a^2 \equiv \frac{\partial p}{\partial \rho} \quad (\text{ch. 9}) \rightarrow \delta p \approx a^2 \cdot \delta \rho$$

Bernoulli eq.: $\frac{dp}{\rho} + v dv = 0$.

$$a^2 \delta \rho \approx -\rho v dv \quad (2)$$

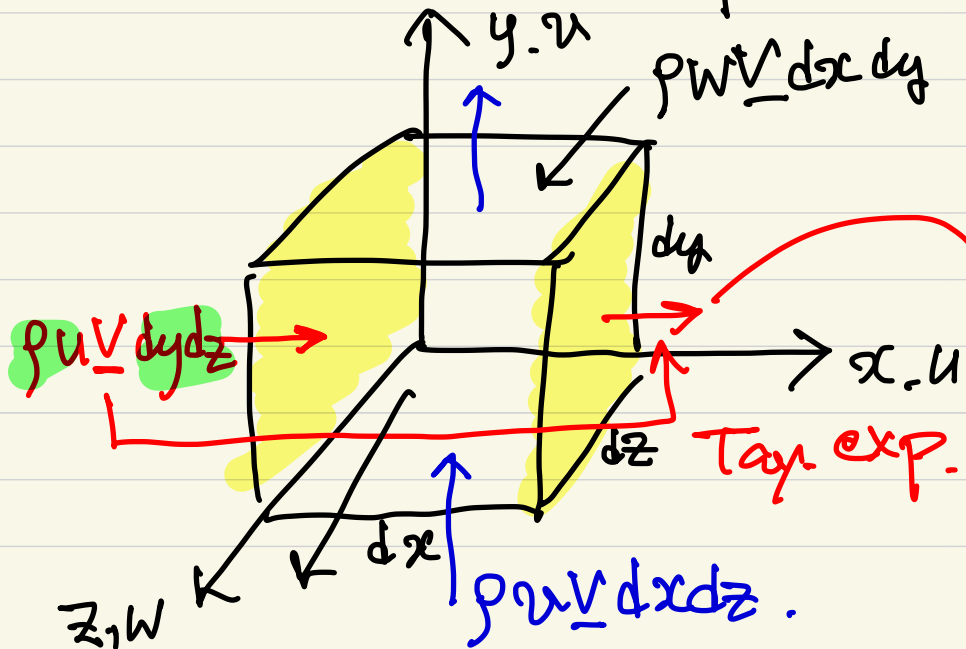
$$\textcircled{1} + \textcircled{2} : \left| \frac{dp}{\rho} \right| = \left| \frac{V}{a^2} \delta V \right| \ll \left| \frac{\delta V}{V} \right|$$

$$\therefore \frac{V^2}{a^2} \ll 1. \quad \frac{V}{a} (\equiv Ma) \ll 1.$$

if $Ma < 0.3$, incompressible in practical.

(for air, $V \leq 100 \text{ m/s}$,
liquid, mostly)

4.3 Differential eq. of linear momentum.



$$\sum \underline{F} = \frac{\partial}{\partial t} \int_{CV} \rho \underline{V} dV + \int_{CS} \rho \underline{V} (\underline{V}_n \cdot \underline{n}) dA$$

$$\approx \frac{\partial}{\partial t} (\rho \underline{V}) dx dy dz$$

$$\rho u \underline{V} dy dz + \frac{\partial}{\partial x} (\rho u \underline{V} dy dz) \cdot dx$$

$$\therefore \Sigma \underline{F} = dx dy dz \left[\frac{\partial}{\partial t} (\rho \underline{v}) + \frac{\partial}{\partial x} (\rho u \underline{v}) + \frac{\partial}{\partial y} (\rho v \underline{v}) + \frac{\partial}{\partial z} (\rho w \underline{v}) \right]$$

$$= \underline{v} \left(\frac{\partial \rho}{\partial t} + \frac{\partial}{\partial x} (\rho u) + \frac{\partial}{\partial y} (\rho v) + \frac{\partial}{\partial z} (\rho w) \right) + \left(\rho \frac{\partial \underline{v}}{\partial t} + \rho u \frac{\partial \underline{v}}{\partial x} + \rho v \frac{\partial \underline{v}}{\partial y} + \rho w \frac{\partial \underline{v}}{\partial z} \right)$$

$$\Sigma \underline{F} = \rho \left(\frac{\partial \underline{v}}{\partial t} + (\underline{v} \cdot \nabla) \underline{v} \right) dx dy dz.$$

$$= \rho \frac{D \underline{v}}{D t} dx dy dz.$$

$\frac{D}{D t}$ material derivative.

$\Sigma \underline{F} = ?$ body force, surface force.

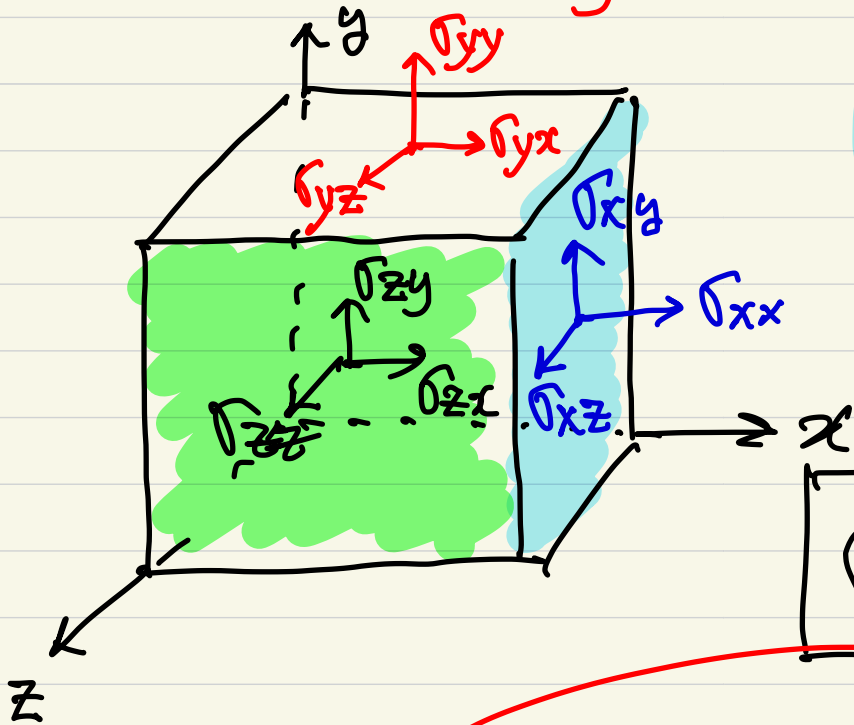
gravity: $dF_{\text{grav}} = \rho \underline{g} dx dy dz$, $\underline{g} = -g \hat{k}$

$$= -\rho g \hat{k} dx dy dz.$$

· magnetic force, electric potential,

stresses on the sides of CV. : σ_{ij}

stress in j -direction on a face normal to i -axis



$$p \equiv -\frac{1}{3}(\sigma_{xx} + \sigma_{yy} + \sigma_{zz}).$$

hydrostatic pressure
@ non-zero velocity cond.

$$\sigma_{ij} = -p \delta_{ij} + \tau_{ij}$$

($i, j = x, y, z$)

hydrostatic pressure

viscous stress.

(Kronecker delta) $\delta_{ij} = \begin{cases} 1 & (i=j) \\ 0 & (i \neq j) \end{cases}$

$$\sigma_{ij} = \begin{bmatrix} -P + \tau_{xx} & \tau_{yx} & \tau_{zx} \\ \tau_{xy} & -P + \tau_{yy} & \tau_{zy} \\ \tau_{xz} & \tau_{yz} & -P + \tau_{zz} \end{bmatrix}$$